

# Chapter 6

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## Underwater granular flows

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### 6.1 Introduction

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Avalanches, landslides, and debris flows are geophysical hazards, which involve rapid mass movement of granular solids, water, and air as a single phase system. Globally, landslides cause billions of pounds in damages, and thousands of deaths and injuries each year. Hence, it is important to understand the triggering mechanism and the flow evolution. The momentum transfer between the discrete and the continuous phases significantly affects the dynamics of the flow as a whole (Topin et al., 2012). Although certain macroscopic models are able to capture the simple mechanical behaviours (Peker and Helvacı, 2007), the complex physical mechanisms occurring at the grain scale, such as hydrodynamic instabilities, formation of clusters, collapse, and transport, (Topin et al., 2011) have largely been ignored. In particular, when the solid phase reaches a high volume fraction, the strong heterogeneity arising from the contact forces between the grains, and the hydrodynamic forces, are difficult to integrate into the homogenization process involving global averages.

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In order to describe the mechanism of immersed granular flows, it is important to consider both the dynamics of the solid phase and the role of the ambient fluid (Denlinger and Iverson, 2001). The dynamics of the solid phase alone is insufficient to describe the mechanism of granular flow in fluid. It is important to consider the effect of hydrodynamic forces that reduce the weight of the solids inducing a transition from dense-compacted to dense-suspended flows, and the drag interactions which counteract the movement of the solids (Meruane et al., 2010). Transient regimes characterized by change in the solid fraction, dilation at the onset of flow and the development of excess pore pressure, result in altering the balance between the stress carried by the fluid and that carried by the grains, thereby changing the overall behaviour of the flow.

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The presence of a fluid phase in a granular medium has profound effects on its mechanical behaviour. In dry granular media the rheology is governed by grain inertia and static stresses sustained by the contact network depending on the shear-rate and the confining pressure, respectively (Midi, 2004). As the fluid inertia and viscosity come into play, complications arise as a result of contradictory effects. On one hand, the fluid may delay the onset of granular flow or prevent the dispersion of the grains by developing negative pore pressures (Pailha et al., 2008; Topin et al., 2011). On the other hand, the fluid lubricates the contacts between grains, enhancing the rate of granular flow, on the other hand it has a retarding effect at the same time by inducing drag forces on the grains. The objective of the present study is to understand the differences in the mechanism of flow initiation and kinematics between dry and submerged granular flow. In the present study, 2D Lattice-Boltzmann and Discrete Element Method is used to model the fluid-soil interactions in underwater granular flows. The choice of a 2D geometry has the advantage of cheaper computational effort than a 3D case, making it feasible to simulate very large systems.

## 14 6.2 LBM-DEM Permeability

15 In a 3D granular assembly, the pore spaces between the grains are interconnected, whereas in a  
 16 2-D assembly, a non-interconnected pore-fluid space is formed as the grains are in contact with  
 17 each other. Which means that the fluid enclosed between the grains cannot flow to neighbouring  
 18 pore-spaces. This results in a unnatural no flow condition in a 2-D case (see figure 6.1). In order  
 19 to overcome this effect, a reduction in radius is assumed only during the LBM computation (fluid  
 20 and fluid – solid interaction) steps. The reduced radius of the soil grain, i.e., the *hydrodynamic*  
*radius r*, allows for interconnected pore space through which the pore-fluid can flow similar  
 1 to the 3D behaviour. The reduction in the radius is assumed only during LBM computations,  
 2 hence this technique has no effect on the grain – grain interactions computed using DEM.  
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4 Realistically, the hydrodynamic radius can be varied from  $r = 0.7R$  to  $0.95R$ , where  $R$  is  
 5 the grain radius. Different permeabilities can be obtained for any given initial packing by  
 6 varying the hydrodynamic radius of the grains, without having to change the actual granular  
 7 packing. This introduces a new parameter into the system. In a physical sense, a hydrodynamic  
 8 radius represents the three-dimensional permeability of a granular assembly simulated as a  
 9 two-dimensional geometry. The hydrodynamic radius can also be assumed to represent the  
 10 irregularities on the granular surface. The hydrodynamic radius represents simulating asperities  
 11 on the grain surface, which represents a channel for the fluid to flow between the grains.  
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13 In order to understand the relation between the hydrodynamic radius and the permeability of  
 the granular assembly, horizontal permeability tests are performed by varying the hydrodynamic

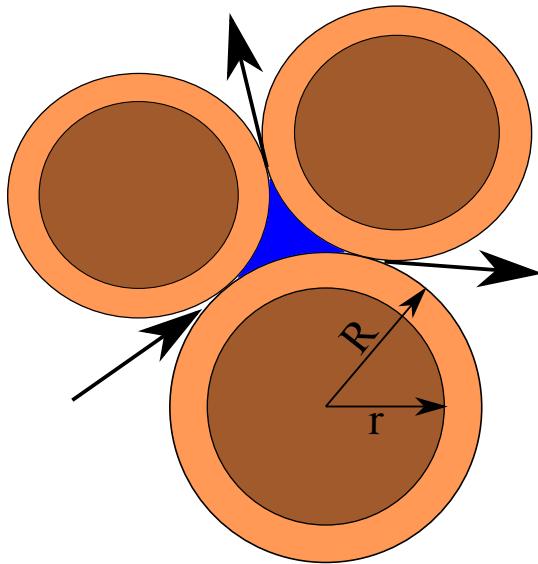


Figure 6.1 Schematic representation of the hydrodynamic radius in LBM-DEM computation

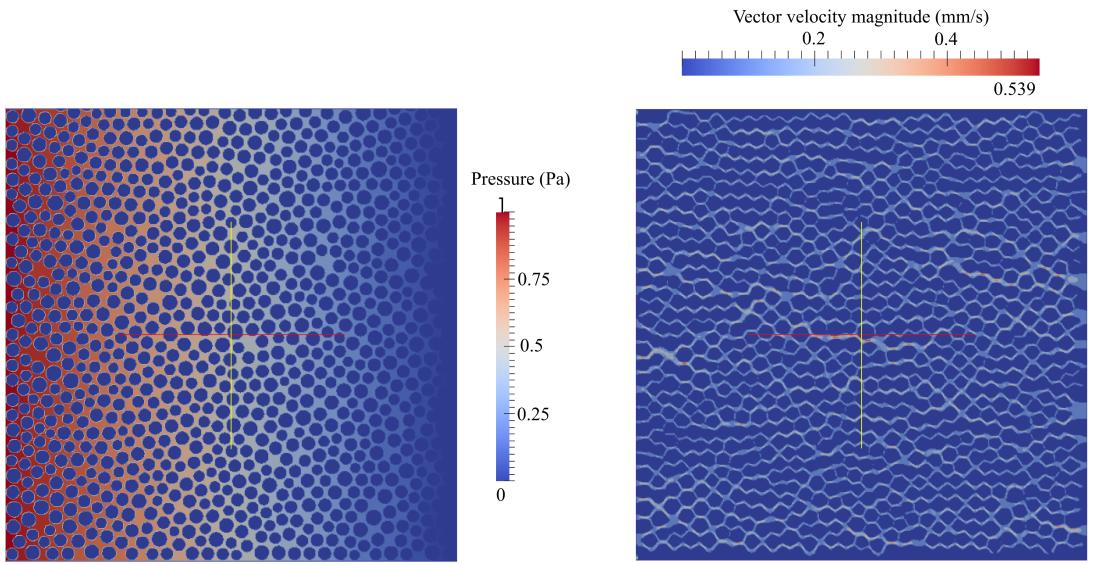
radius as 0.7 R, 0.75 R, 0.8 R, 0.85 R, 0.9 R and 0.95 R. A square sample of 50 mm × 50 mm filled with poly-disperse ( $d_{max}/d_{min} = 1.8$ ) grains having a mean diameter of 1.7 mm is used to determine the relation between the hydrodynamic radius and the permeability. Dirichlet boundary condition (discussed in ??), i.e., density constrain, is applied along the left and the right boundaries of the sample. The fluid density on the left boundary is increased in small steps ( $10^{-4}\Delta P$ ), while a constant density is maintained on the right boundary. This results in a pressure gradient causing the fluid to flow (see figure 6.2) through the pore-space.

For a given hydrodynamic radius, the pressure gradient  $\Delta P$  is varied to obtain different flow

- 1 rates. Probing the fluid space showed a Poiseuille flow behaviour between grains. The flow is
- 2 still within the Darcy's laminar flow regime, which is verified by the linear slope between the
- 3 pressure gradient and mean flow velocity (see figure 6.3). From the mean velocity of the flow
- 4 ( $v$ ), the transverse permeability ( $k$ ) of the sample is computed as:

$$k = v \cdot \mu \cdot \frac{\Delta x}{\Delta P}, \quad (6.1)$$

- 5 where  $\mu$  is the dynamic viscosity of the fluid (Pa s),  $\Delta x$  is the thickness of the bed of porous
- 6 medium m, and  $\Delta P$  is the applied pressure difference Pa. It can be observed that with increase
- 7 in the hydrodynamic radius the permeability decreases, i.e., the slope of the mean flow velocity
- 8 to the pressure gradient decreases. At very low pressure gradient ( $\Delta P \leq 0.1$ ), both 0.9 R and
- 9 0.95 R have no flow. Even at higher pressure gradients, a hydrodynamic radius of  $r = 0.95R$
- 10 shows almost no flow behaviour. A high value of hydrodynamic radius  $r > 0.95R$  results in
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(a) Pressure gradient in the granular assembly      (b) Horizontal flow due to pressure gradient

Figure 6.2 Evaluation of the horizontal permeability for a hydrodynamic radius of 0.7R.

12 unnatural flow/no-flow behaviour. Hence, hydrodynamic radii in the range of 0.7 to 0.95 R are  
 13 adopted in the present study.

14 Increase in the hydrodynamic radius from 0.7 to 0.95 reduces the porosity from 0.60 to  
 15 0.27. The permeability computed from LB – DEM method is verified by comparing it with the  
 1 analytical solution. One of the widely used analytical solution for permeability is the Carman –  
 2 Kozeny equation (CK Model), which is based on the Poiseuille's flow through a pipe and is  
 3 mainly used for 3D, homogeneous, isotropic, granular porous media at moderate porosities.  
 4 In the present study, a modified Carman – Kozeny equation that takes into account the micro-  
 5 structure of the fibres and that is valid in a wide range of porosities is adopted ([Yazdchi et al., 2011](#)).  
 6 The normalized permeability is defined as

$$\frac{k}{d^2} = \frac{\varepsilon}{\psi_{CK}(1-\varepsilon)^2}. \quad (6.2) \quad 7$$

In the CK model, the hydraulic diameter  $D_h$ , is expressed as a function of measurable quantities:  
 8 porosity and specific surface area  
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$$D_h = \frac{4\varepsilon V}{S_v} = \frac{\varepsilon d}{(1-\varepsilon)}, \quad (6.3) \quad 10$$

$$a_v = \frac{\text{grain surface}}{\text{grain volume}} = \frac{S_v}{(1-\varepsilon V)} = \frac{4}{d}, \quad (6.4) \quad 11$$

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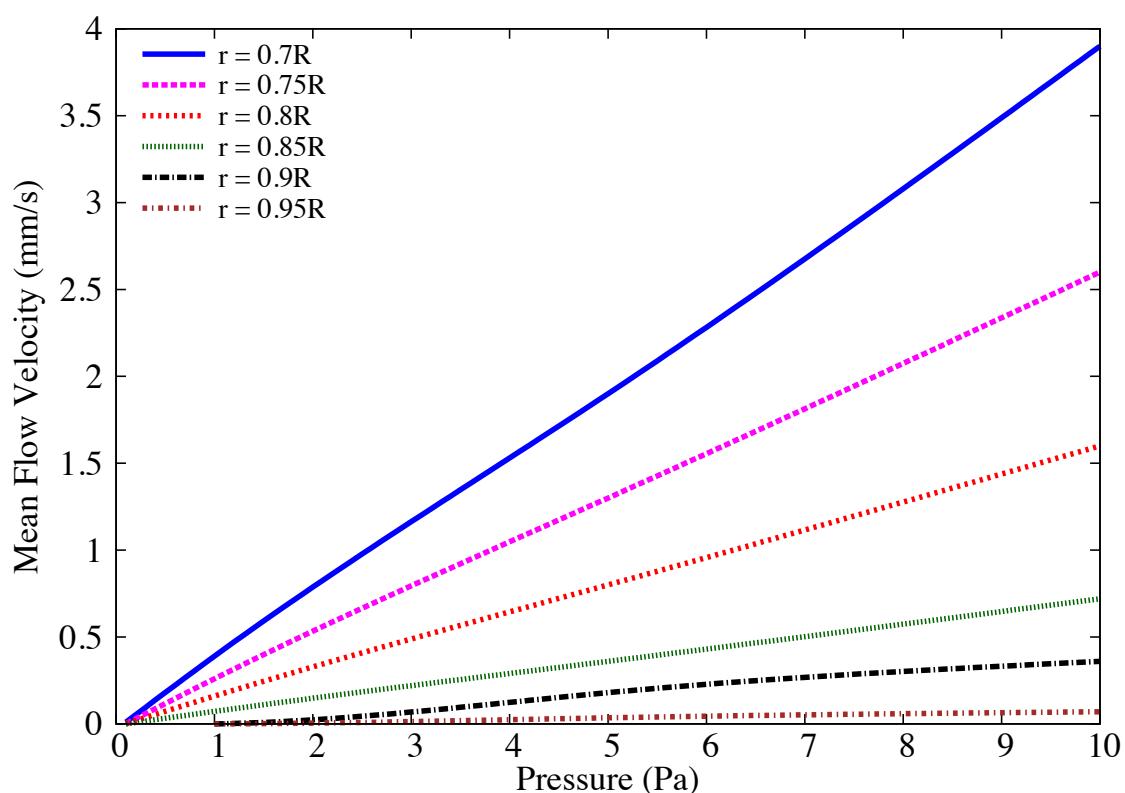


Figure 6.3 Variation of the mean flow velocity with pressure gradient for different hydrodynamic radius.

where  $S_v$  is the total wetted surface, and  $a_v$  is the specific surface area. The above value of  $a_v$  is for circles (cylinders) - for spheres  $a_v = 6/d$ .  $\psi_{CK}$  is the empirically measured CK factor, which represents both the shape factor and the deviation of flow direction from that in a duct. It is simulated for randomly packed beds of spherical grains. The variation of normalized permeability with porosity, obtained by varying the radius from 0.7 to 0.95, is presented in figure 6.4. The permeability values obtained from LBM - DEM simulations are found to match the qualitative trend of the Carman-Kozeny equation. The LB – DEM permeability curve lies between the permeability curves for spherical and cylindrical grain arrangements implying a better simulation of three-dimensional permeability using a 2D granular assembly. Thus using a hydrodynamic radius, realistic 3D fluid - grain interactions can be simulated in a 2D geometry.

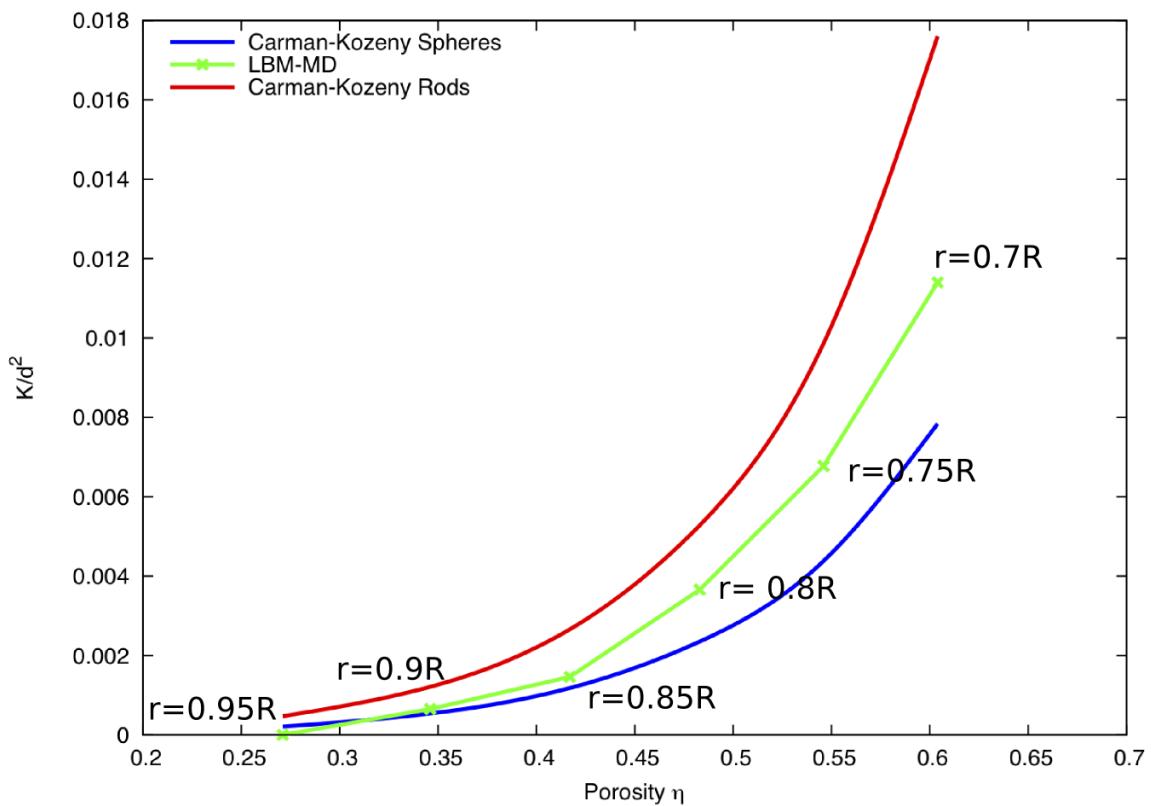


Figure 6.4 Relation between permeability and porosity for different hydrodynamic radius and comparison with the analytical solution.

## 6.3 Granular collapse in fluid

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The collapse of a granular column, which mimics the collapse of a cliff, has been extensively studied in the case of dry granular material, when the interstitial fluid plays no role (see ??). The problem of the granular collapse in a liquid, which is of importance for submarine landslides, has attracted less attention (Rondon et al., 2011). Thompson and Hupper (2007) observed that the presence of liquid dramatically changes the way a granular column collapses compared to the dry case. The destabilization of a granular pile strongly depends on the initial volume fraction. For dense packings the granular flow is localized at the free surface of the pile, whereas for loose packings the destabilization occurs in the bulk of the material and has a parabolic profile (Bonnet et al., 2010; Iverson, 2000; Topin et al., 2011).

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### 6.3.1 LBM-DEM set-up

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In the present study, the collapse of a granular column in fluid is studied using 2D LBM - DEM. The effect of initial aspect ratio on the run-out behaviour is investigated. The flow kinematics are compared with the dry and buoyant granular collapse to understand the influence of hydrodynamic forces and lubrication on the run-out. Unlike dry column, the role of permeability and the initial volume fraction is expected to have a significant influence on the flow dynamics. Hence the effect of these parameters on the run-out behaviour are investigated.

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The granular column collapse set-up in fluid is very similar to the dry granular column collapse. A rectangular channel of length  $L_0$  and height  $H_0$  is filled with poly-dispersed discs,  $d_{max}/d_{min} = 1.8$  (see Figure 6.5). The granular column is then placed in a fluid with a density of  $1000 \text{ kg m}^{-3}$  and a kinematic viscosity of  $1 \times 10^{-6} \text{ m}^2 \text{ s}^{-1}$ . The gate supporting the right-hand side boundary of the granular column is opened allowing the column to collapse and flow in a fluid. The final run-out distance is measured as  $L_f$  and final collapse height as  $H_f$ . The collapse takes place on a horizontal surface. The initial aspect ratio of the column is varied as 0.2, 0.4, 0.6, 0.8, 1, 2, 4 and 6.

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The cumulative  $\beta$  distribution is adopted to generate grains with  $d_{max}$  and  $d_{min}$  as 2.2 mm and 1.25 mm, respectively. The soil column is modelled using  $\sim 2000$  discs of density  $2650 \text{ kg m}^{-3}$  and a contact friction angle of  $26^\circ$ . A linear-elastic contact model is used in the DEM simulations. The granular assembly has a packing fraction of 83%. The critical time step for DEM is computed based on the local contact natural frequency and damping ratio. A sub-cycling time integration is adopted in DEM (see ??). A fluid flow (LBM) time step of  $\Delta t = 2.0E^{-5} \text{ s}$  is determined based on the viscosity and the relaxation parameter  $\tau = 0.506$ . An integer ratio  $n_s$ , between the fluid flow time step  $\Delta t$  and the DEM time step  $\Delta t_D$  is determined as 15, i.e., every LBM iteration involves a sub-cycle of 15 DEM iterations.

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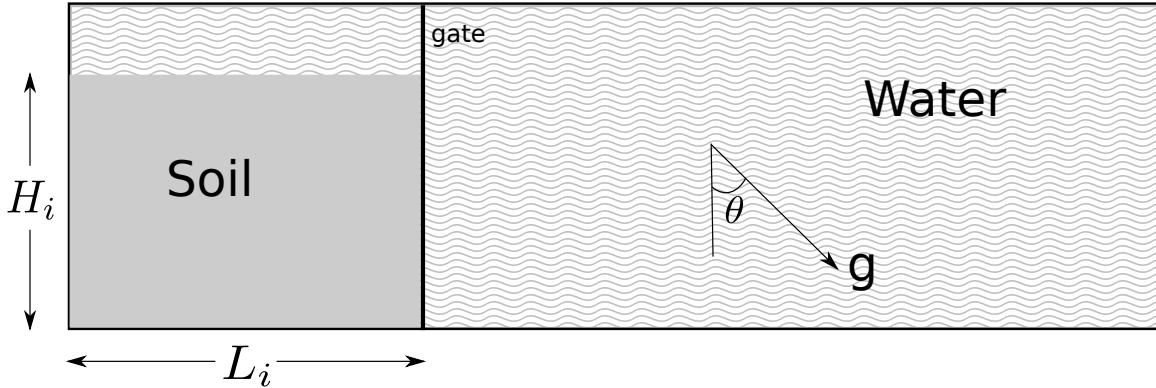


Figure 6.5 Underwater granular collapse set-up.

In order to capture the realistic physical behaviour of the fluid – grain systems, it is essential to model the boundary condition between the fluid and the grain as a non-slip boundary condition, i.e. the fluid near the grain should have similar velocity as the grain boundary. The solid grains inside the fluid are represented by lattice nodes. The discrete nature of lattice, results in a stepwise representation of the surfaces (see figure 6.6), which are otherwise circular, hence sufficiently small lattice spacing  $h$  is required. The smallest DEM grain in the system controls the size of the lattice. In the present study, a very fine discretisation of  $d_{min}/h = 10$  is adopted, i.e., the smallest grain with a diameter  $d_{min}$  in the system is discretised into 100 lattice nodes ( $10h \times 10h$ ). This provides a very accurate representation of the interaction between the solid and the fluid nodes. A hydrodynamic radius of 0.7R is adopted during the LBM computations.

### 6.3.2 Collapse in fluid: Flow evolution

Two-dimensional plane-strain LBM-DEM simulations of granular column collapse are performed by varying the initial aspect ratio of the column from 0.2 to 6. The normalized final run-out distance is measured as  $\Delta L = (L_f - L_0)/L_0$ . Similar to the dry granular collapse, the duration of collapse is normalised with a critical time  $\tau_c = \sqrt{H/g}$ , where  $H$  is the initial height of the granular column and  $g$  is the acceleration due to gravity. Dry and buoyant analyses of granular column collapse are also performed to understand the effect of hydrodynamic forces on the run-out distance.

Snapshots of the flow evolution of a granular column collapse with an initial aspect ratio of 0.4 are shown in figure 6.7. The failure begins at the toe end of the column, and the fracture surface propagates into the column at an angle of about 50°, similar to the dry column collapse. For the short column, the failure is due to collapse of the flank. Once the material is destabilised, the granular mass interacts with the surrounding fluid resulting in formation of

## 6.3 Granular collapse in fluid

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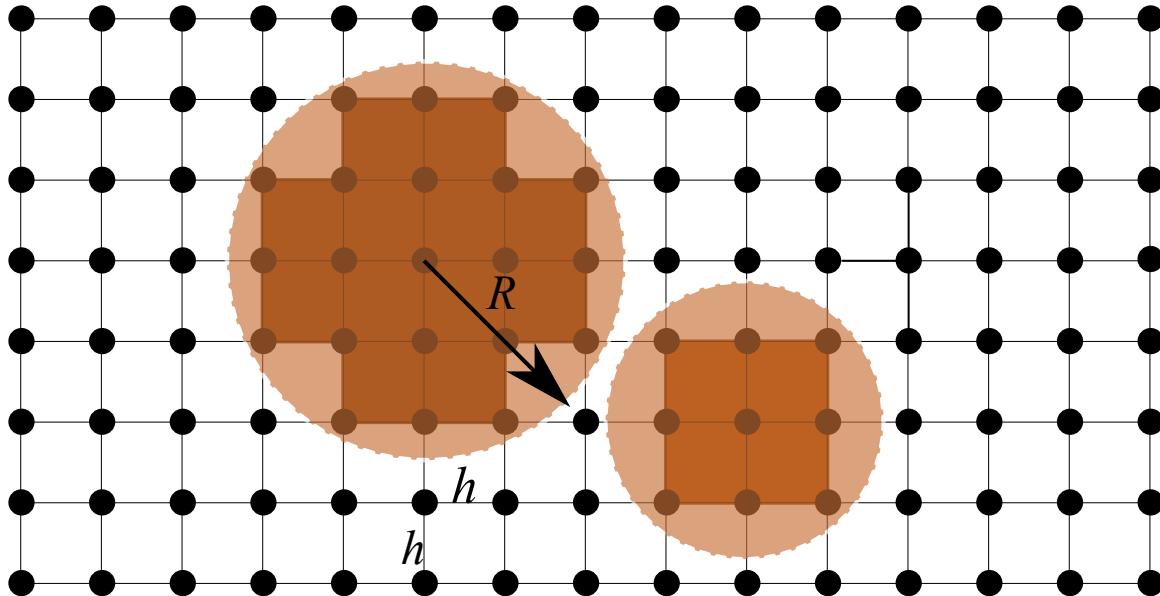


Figure 6.6 Discretisation of solid grains in LBM grid. Shows the step-wise representation of circular disks in the lattice.

turbulent vortices. These vortices interact with the grains at the surface resulting in irregularities on the free surface. Force chains can be observed in the static region of collapse, which indicates the flow can be described using a continuum theory. As the granular material ceases to flow, force chains develop at the flow front, revealing consolidation of the granular mass resulting in an increase in the shear strength.

The evolution of run-out with time for a short column ( $a = 0.4$ ) is presented in figure 6.8a. The dry column exhibits longer run-out distance in comparison to the submerged column. The collapse of a dry column using DEM represents a collapse in vacuum, without any influence of drag forces or viscosity of air. A LBM-DEM simulation of a granular column collapse using the kinematic viscosity of air is performed to compare the dry column with the collapse in air. It can be observed that both the “dry” condition and the collapse in air show almost the same run-out behaviour. However, the collapse in fluid (water) results in a much shorter run-out distance. The granular mass in fluid has the buoyant mass, in contrast to the dry density. A dry granular collapse with the buoyant unit weight also exhibits longer run-out behaviour than the collapse in fluid. However, due to decrease in the initial potential energy, the run-out observed in the buoyant condition is shorter than the dry condition. The column collapse in fluid takes longer to evolve, which might be due to the development of large negative pore water pressure that is generated during the shear failure along the fracture surface. This large negative pore pressure has to be dissipated before the granular mass, above the fracture surface, can collapse and flow. The shorter run-out distance in the fluid case, in comparison with the dry and buoyant

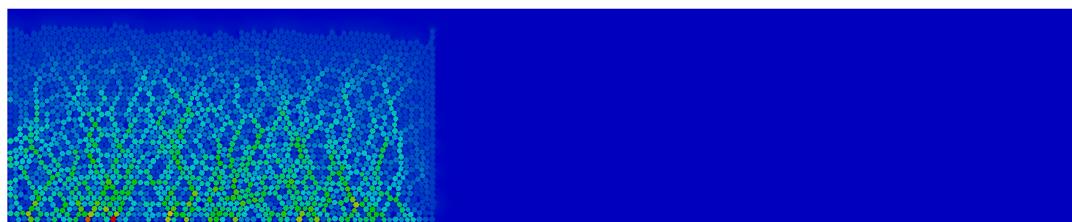
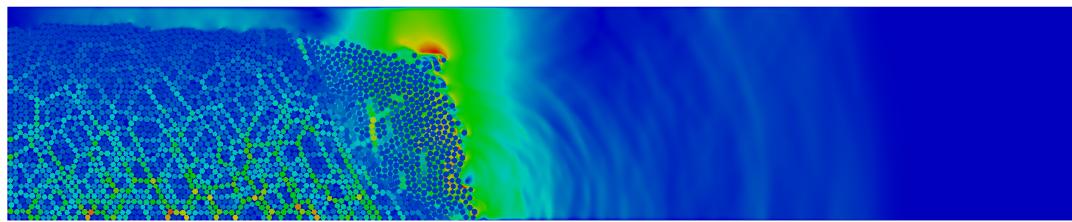
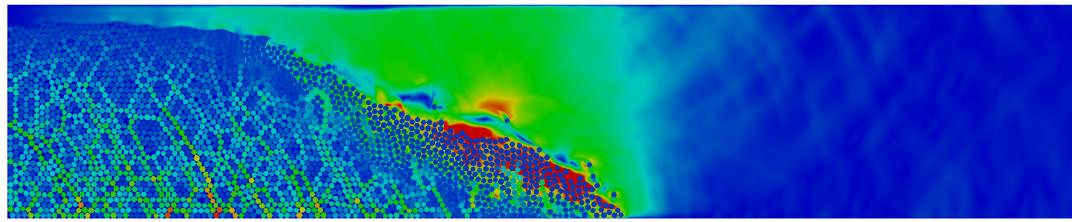
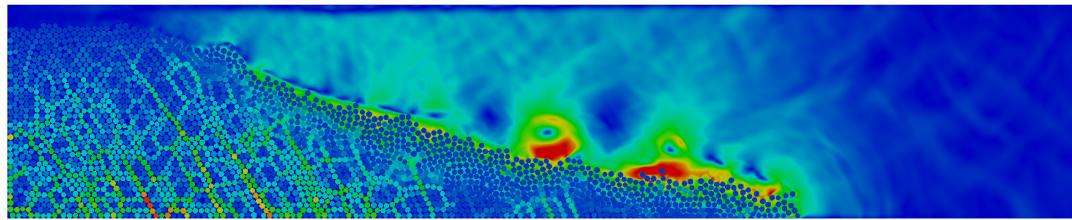
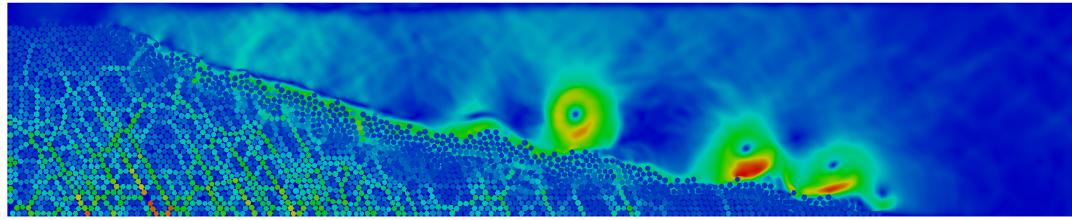
(a)  $t = 0\tau_c$ (b)  $t = 1\tau_c$ (c)  $t = 3\tau_c$ (d)  $t = 6\tau_c$ (e)  $t = 8\tau_c$ 

Figure 6.7 Flow evolution of a granular column collapse in fluid ( $a = 0.4$ ). Shows the velocity profile of fluid due to interaction with the grains (red - higher velocity).

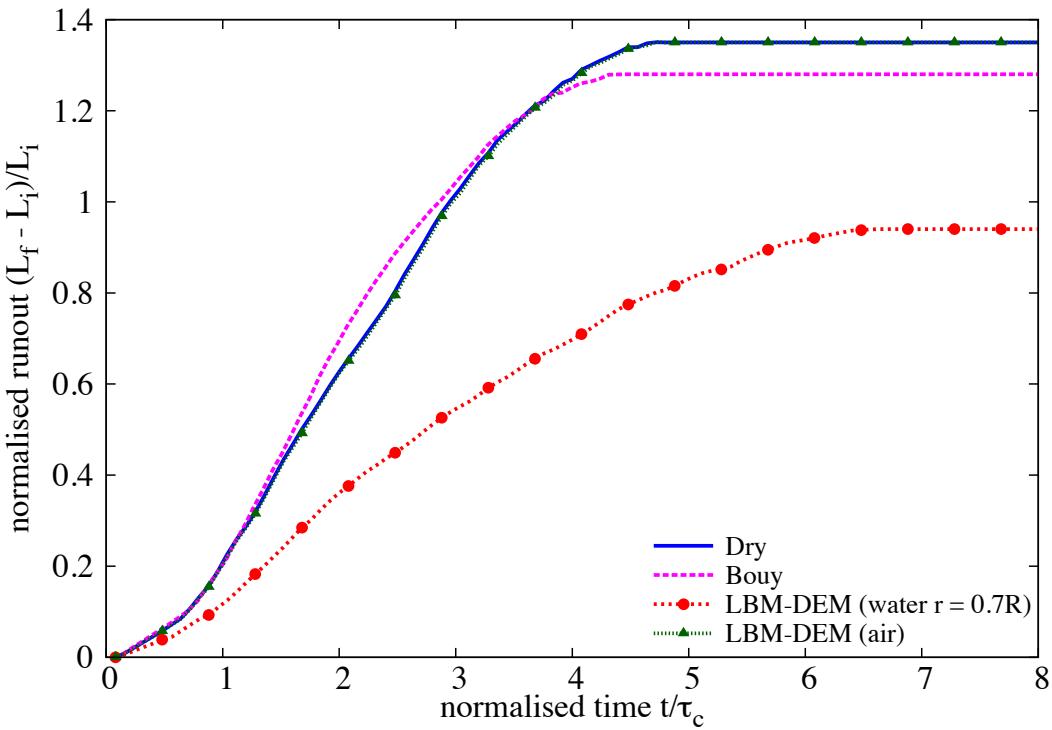
conditions, shows that the collapse in fluid is significantly affected by the hydrodynamic drag forces acting on the soil grains. The evolution of height  $H/L$  is presented in ???. Since the failure of the column is only at the flank, the central static region remains unaffected. Hence, the final height of the column is the same in dry and submerged conditions.

The evolution of the normalised kinetic energy with time for a column with an initial aspect ratio of 0.4 is shown in figure 6.9. It can be observed that the peak kinetic energy is attained later in the submerged condition than the dry collapse. This can be attributed to the time required

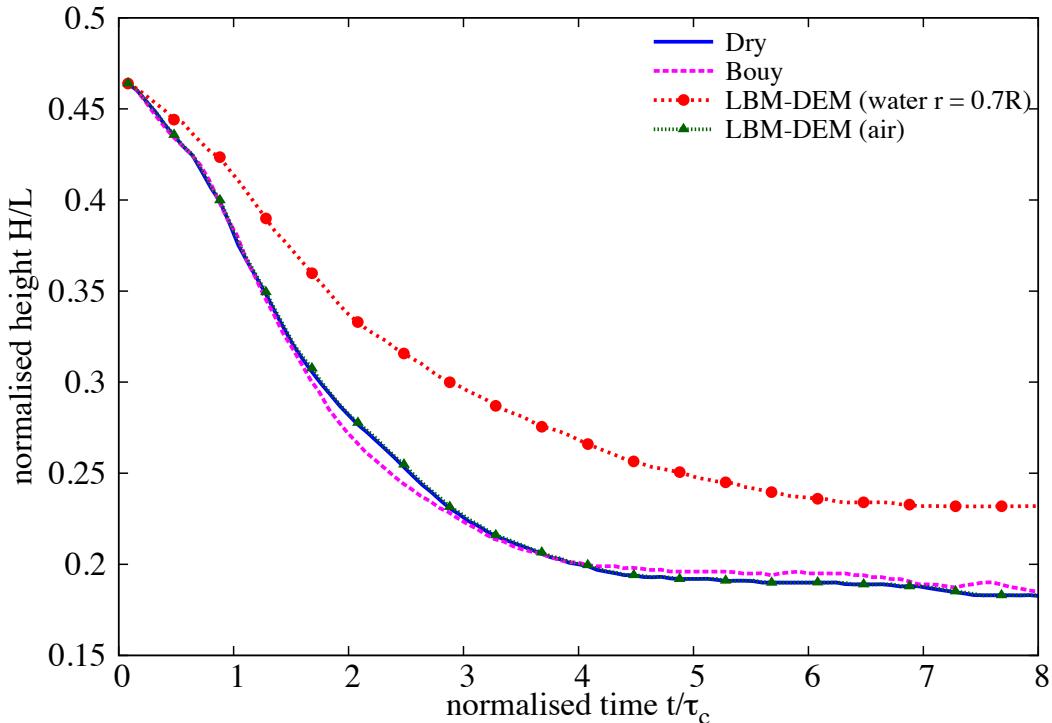
- 1 to overcome the negative pore pressure generated during the shear along the fracture surface.
- 2 For short columns the critical time  $\tau_c$  is controlled by the vertical kinetic energy. The amount
- 3 of kinetic energy in submerged case is significantly lower than the dry condition. Also, the
- 4 potential energy evolution (see figure 6.10) shows a significant influence of the hydrodynamic
- 5 forces on the amount of material destabilised during the collapse. The drag forces on the soil
- 6 grains reduce and slow down the amount of material that undergo collapse resulting in shorter
- 7 run-out distance for short columns.

Snapshots of the flow evolution of a granular column collapse with an initial aspect ratio of 4 is shown in figure 6.11. For a tall column, the collapse mechanism changes. The entire column is involved in the collapse. The height of the static region, which is below the fracture surface, is shorter than the total height of the column. This results in a free-fall of grains above the fracture surface. As the grains experience free-fall they interact with the surrounding fluid. However, no vortices are observed during the initial stage of collapse. In the second phase, when the grains reach the base, the vertical acceleration gained during the free-fall is converted to the horizontal velocity. As the grains are ejected horizontally, the free surface of the granular mass interacts with the fluid resulting in formation of the turbulent vortices. Unlike short columns, these vortices have significant influence on the mass distribution along the run-out. Heaps of granular material can be observed in front of each vortex. The number of vortices formed during a collapse is found to be proportional to the amount of material destabilised, i.e., the length of free-surface interacting with the fluid influences the number of vortices generated during the collapse. The reappearance of force chains at  $t = 6\tau_c$  and  $8\tau_c$  indicates the granular mass is consolidating resulting in an increase in the shear strength.

The time evolution of the run-out and the height of a tall column ( $a = 4$ ) is presented in figure 6.12a and figure 6.12b, respectively. Similar to the short column, the run-out observed in the dry condition is much longer than that observed in the submerged condition. Also, the evolution of run-out is slower in the case of submerged condition, which indicates the influence of drag force on the run-out evolution. The height of the column is significantly affected by the hydrodynamic forces (see figures 6.12b and 6.13), which reduces the amount of material destabilised during the collapse.

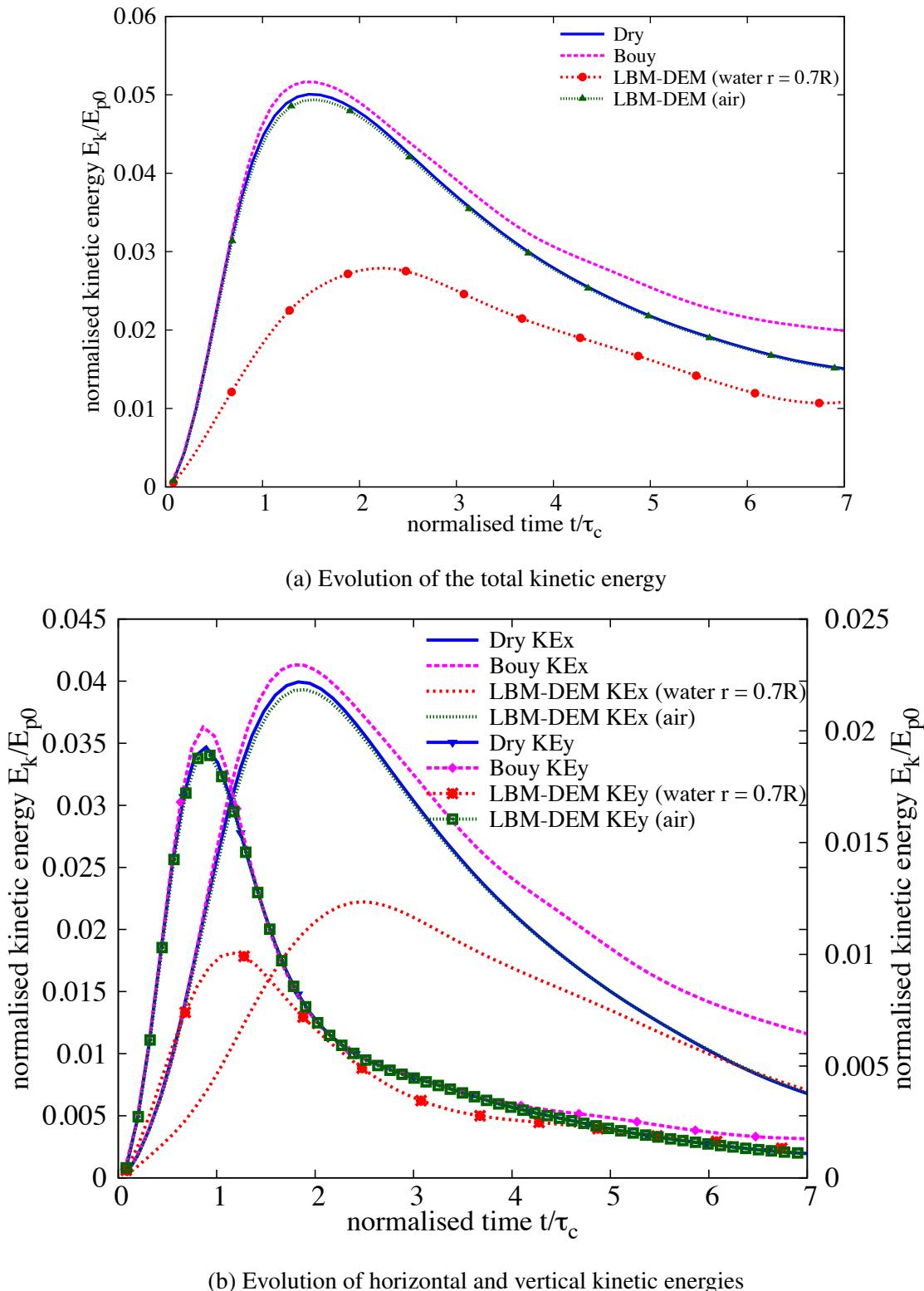


(a) Evolution of run-out with time



(b) Evolution of height with time

Figure 6.8 Evolution of height and run-out with time for a column collapse in fluid ( $a = 0.4$ )

Figure 6.9 Evolution of kinetic energies with time for a granular column collapse in fluid ( $a = 0.4$ )

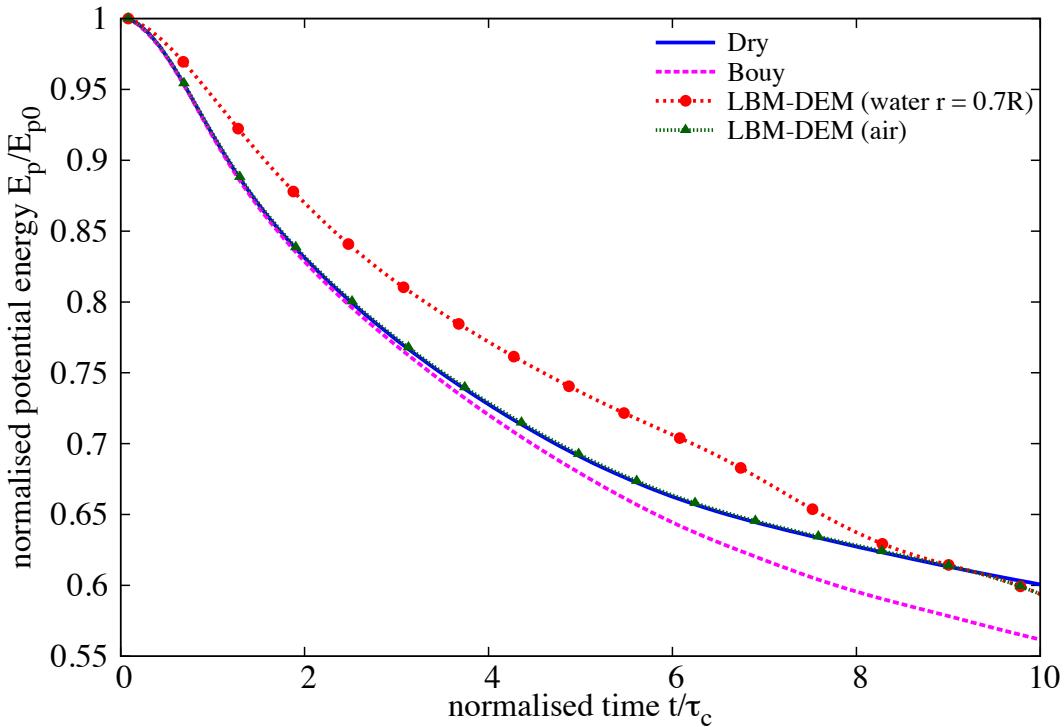


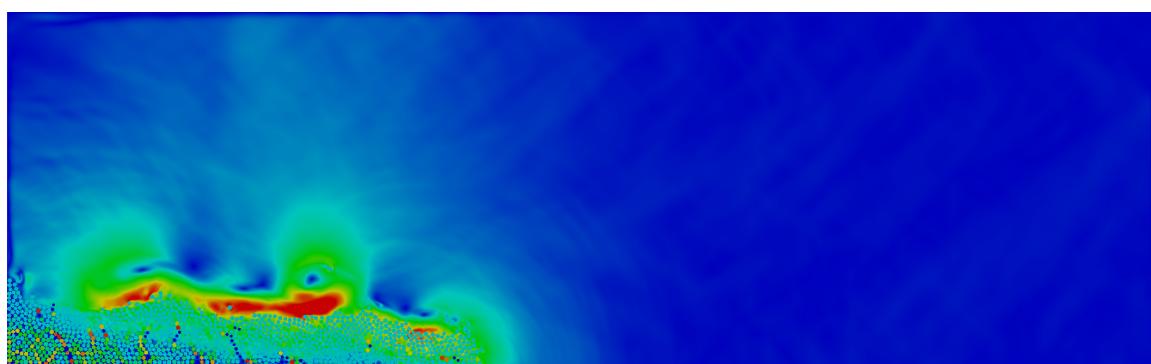
Figure 6.10 Evolution of the potential energy with time for a granular column collapse in fluid ( $a = 0.4$ )

30 The evolution of kinetic energies with time for an initial aspect ratio 4 is presented in figure 6.14. Even during the free-fall stage, the peak vertical energy is delayed in the case of fluid,  
 31 which shows the influence of viscosity on the flow evolution. Almost half of the kinetic energy  
 32 that is available in the case of dry granular collapse is dissipated due to the drag forces experi-  
 33 enced by the grains. This shows that the influence of viscous drag on the run-out evolution is  
 34 significantly higher than the effect of lubrication.  
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1 The final run-out distance as a function of the initial aspect ratio of the column is presented  
 2 in figure 6.15a. For all aspect ratios, the run-out observed in the dry case is significantly higher  
 3 than the submerged condition. For short columns, the run-out distance is found to have a  
 4 linear relationship with the initial aspect ratio of the column. A power law relation is observed  
 5 between the run-out and the initial aspect ratio of the column.

$$\frac{L_f - L_0}{L_0} \propto \begin{cases} a, & a \lesssim 2.7 \\ a^{2/3}, & a \gtrsim 2.7 \end{cases} \quad (6.5)$$

8 The normalised final height as a function of the initial aspect ratio of the column is presented  
 in figure 6.15b. It can be observed that the final collapse height is much higher in the submerged  
 1 condition than the dry condition. The drag force on the granular column reduces the amount of  
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 $t = 0\tau_c$  $t = 1\tau_c$  $t = 3\tau_c$

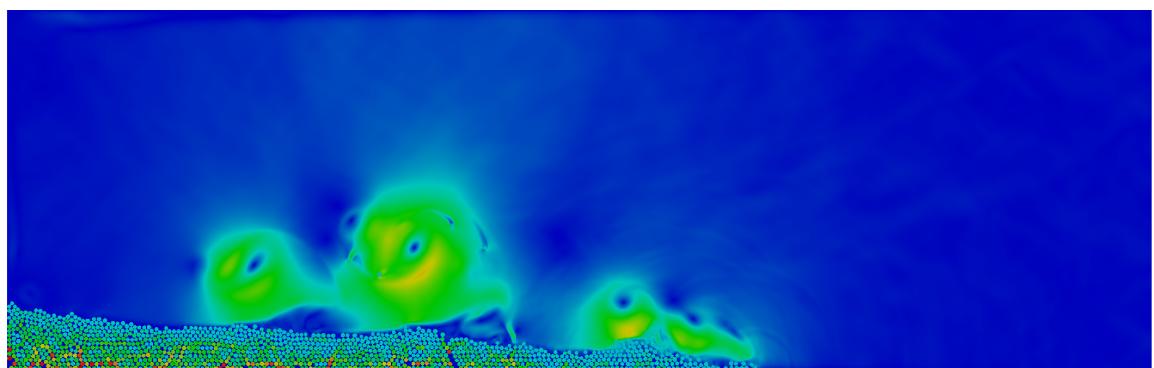
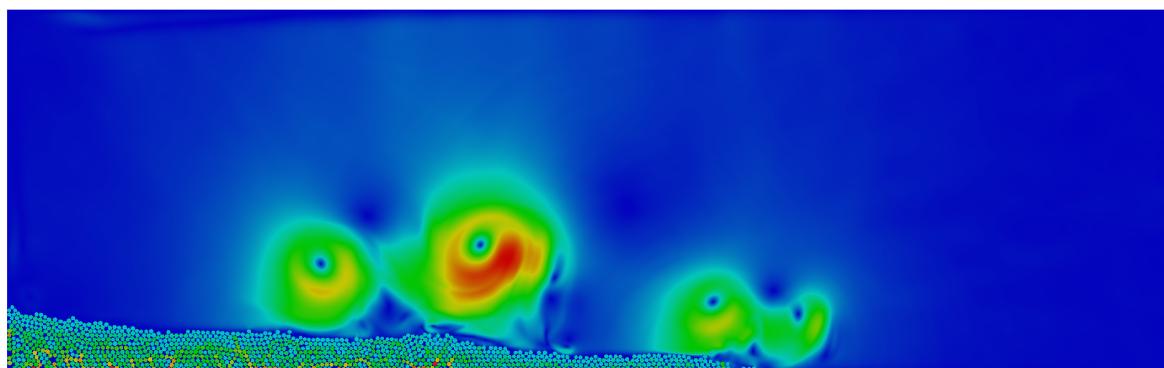
 $t = 6\tau_c$  $t = 8\tau_c$ 

Figure 6.11 Flow evolution of a granular column collapse in fluid ( $a = 4$ ). Shows the velocity profile of fluid due to interaction with the grains (red - higher velocity).

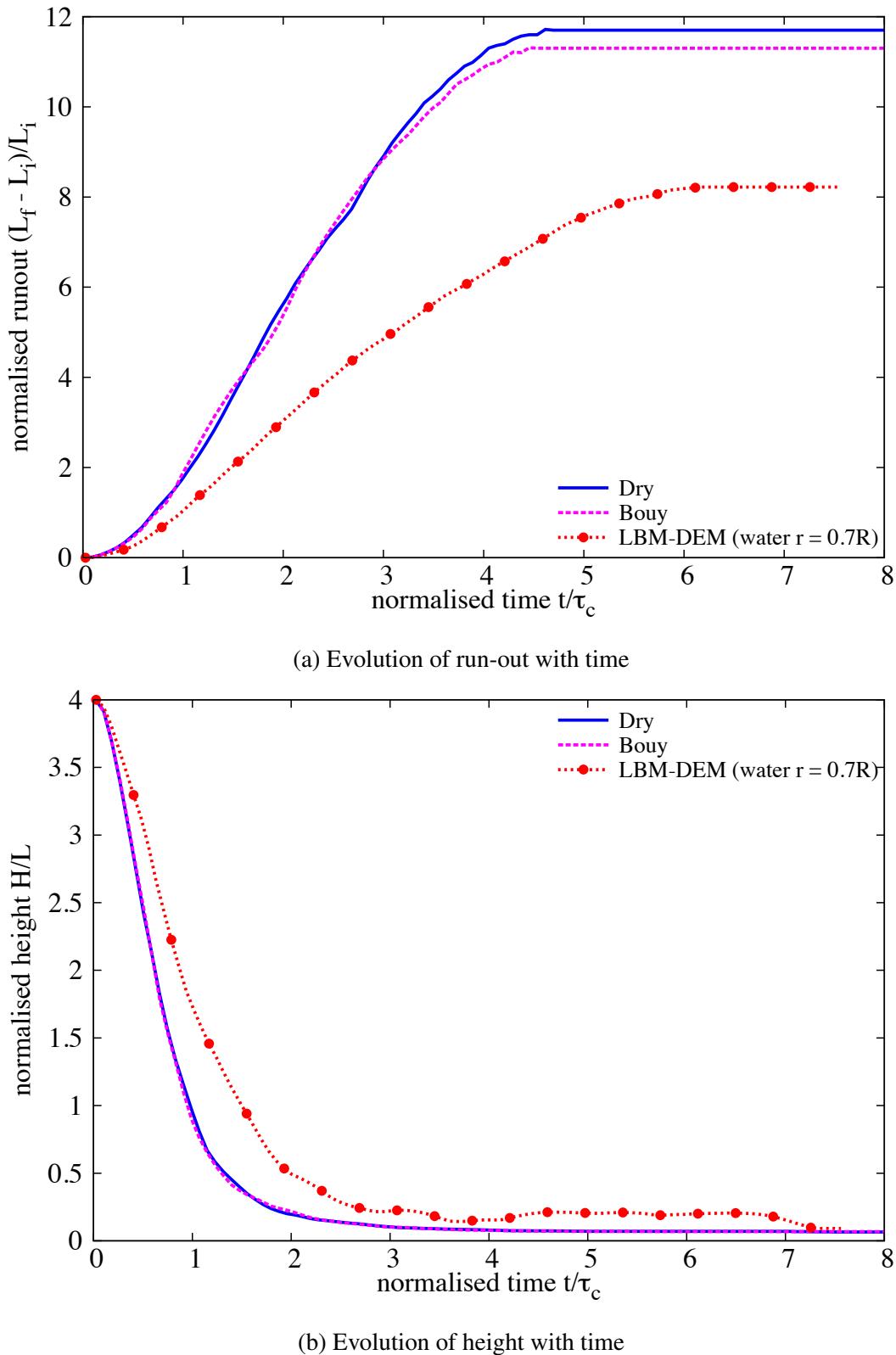


Figure 6.12 Evolution of run-out and height with time for a column collapse in fluid ( $a = 4$ )

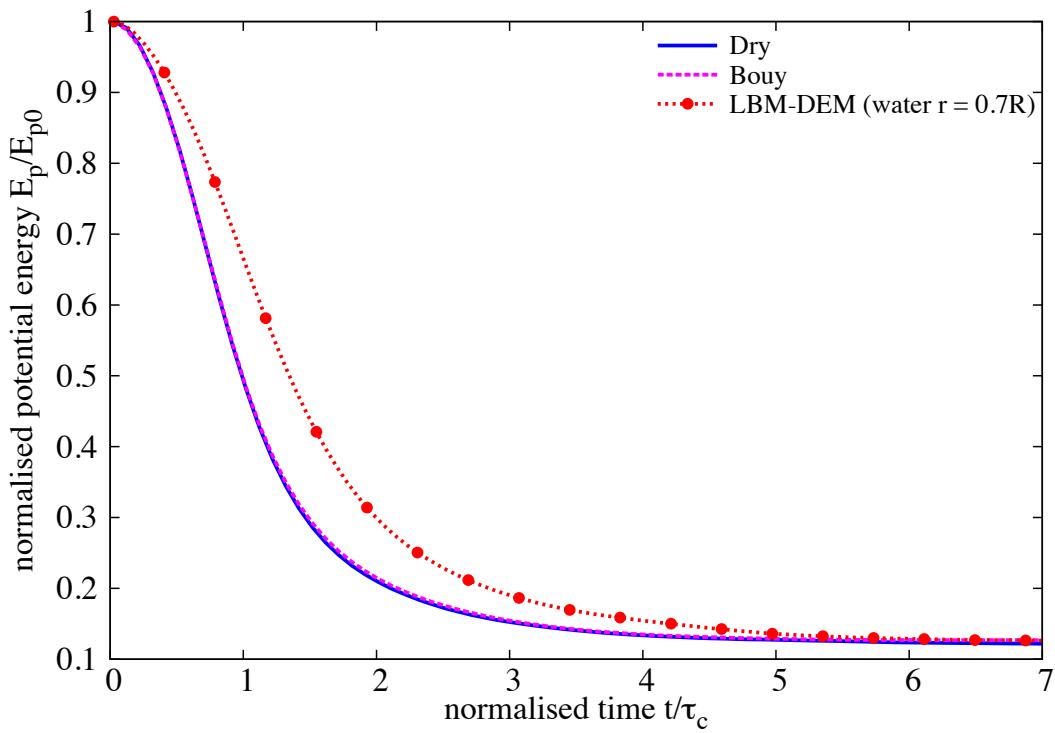


Figure 6.13 Evolution of the potential energy with time for a granular column collapse in fluid ( $a = 4$ )

collapse, resulting in a shorter run-out distance. The drag force seems to have a predominant influence on the run-out behaviour than the lubrication effect in fluid.

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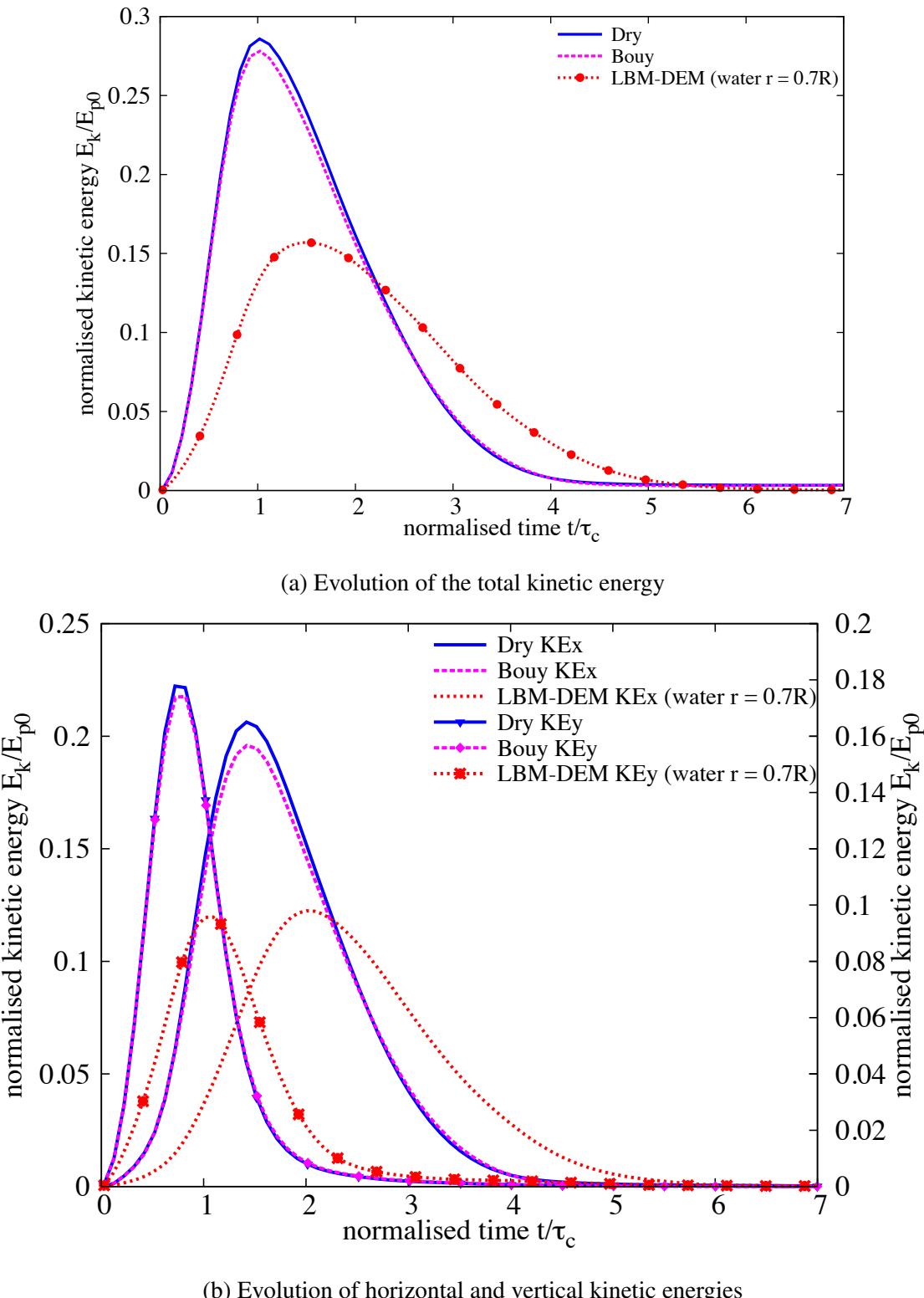
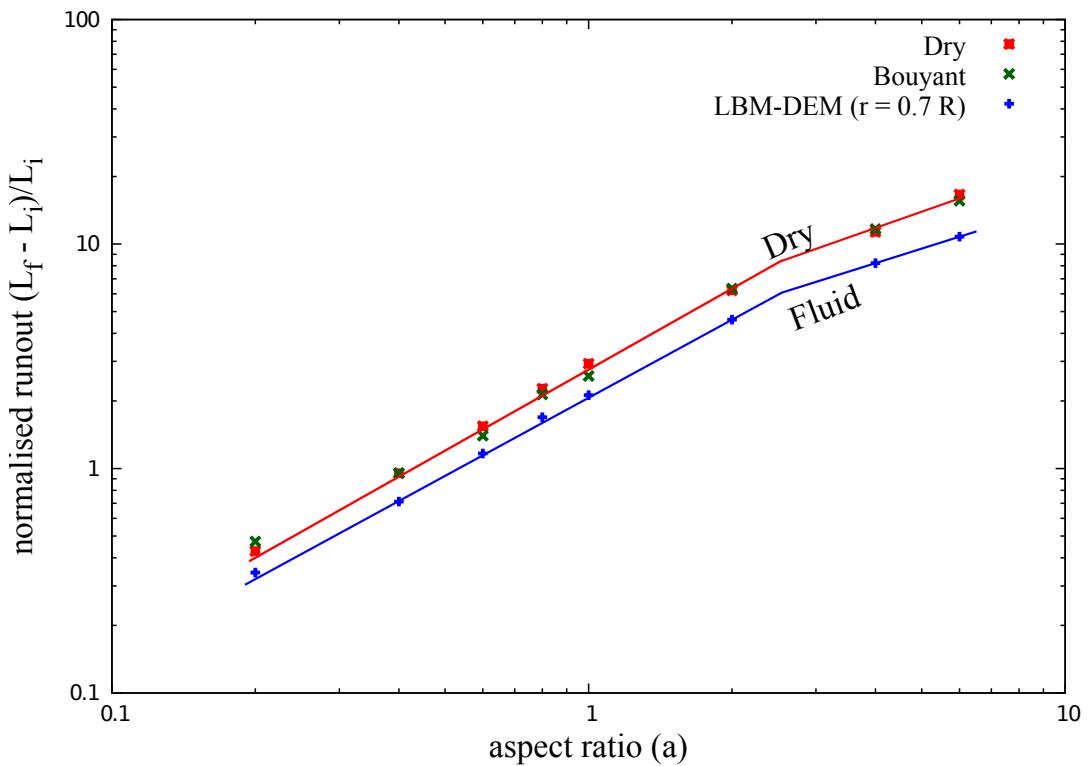
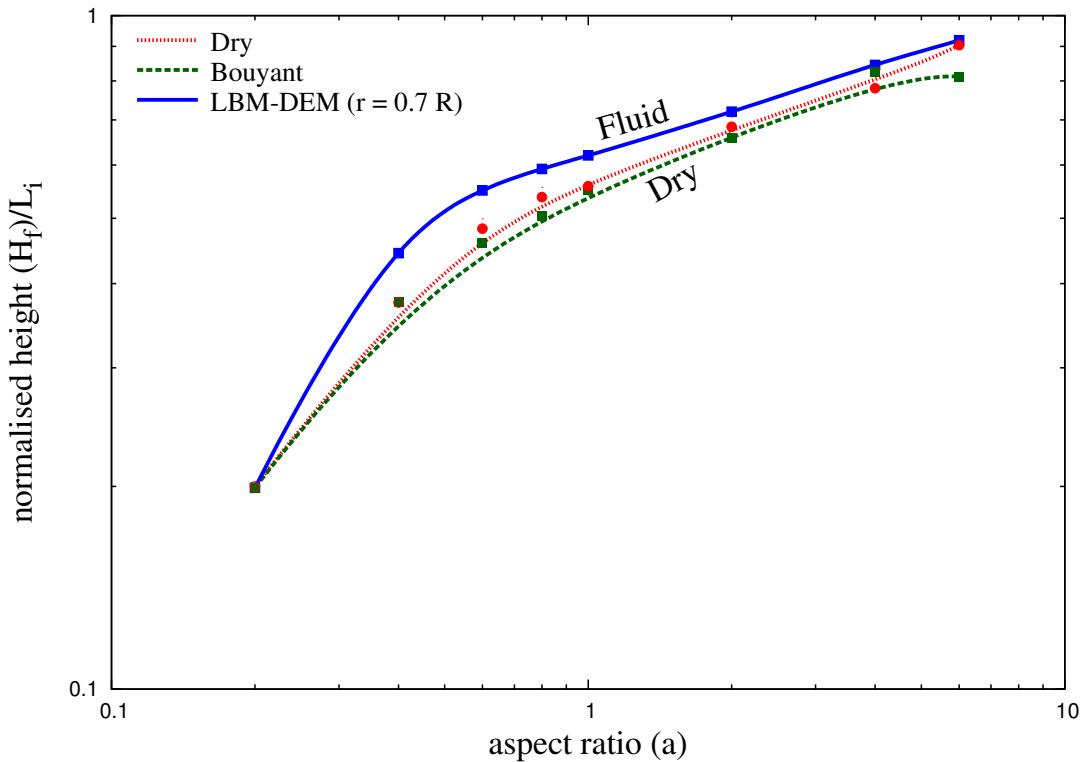


Figure 6.14 Evolution of kinetic energies with time for a granular column collapse in fluid ( $a = 4$ )



(a) Normalised final run-out distance for columns with different initial aspect ratios. Comparison of dry and submerged granular column collapse.



(b) Normalised final collapse height for columns with different initial aspect ratios. Comparison of dry and submerged granular column collapse.

Figure 6.15 Normalised final collapse run-out and height for columns with different initial aspect ratios.

### 6.3.3 Effect of permeability

Topin et al. (2011) observed development of large negative pore pressure during dispersion of grains. The rate of dissipation of the negative pore pressure is directly proportional to the permeability of the granular assembly. In the previous section, the evolution of run-out with the initial aspect ratio is studied using a constant hydrodynamic radius  $r = 0.7 R$ . In order to understand the effect of permeability on the run-out behaviour, the hydrodynamic radius  $r$  is varied from 0.7 R through 0.95 R for all aspect ratios. Increase in the hydrodynamic radius decreases the permeability of the granular assembly resulting in longer duration for the dissipation of negative pore pressure.

The normalised run-out for different hydrodynamic radii for a granular column with an initial aspect ratio of 0.8 is presented in figure 6.16. The run-out increases with decrease in the permeability, which is equivalent to increase in the hydrodynamic radius. An increase in the hydrodynamic radius from 0.7 to 0.95 R increases the normalised run-out by 25%. However,

- <sup>1</sup> even under very low permeability condition ( $r = 0.95 R$ ), the run-out observed in fluid is shorter
- <sup>2</sup> than the dry and the buoyant conditions.

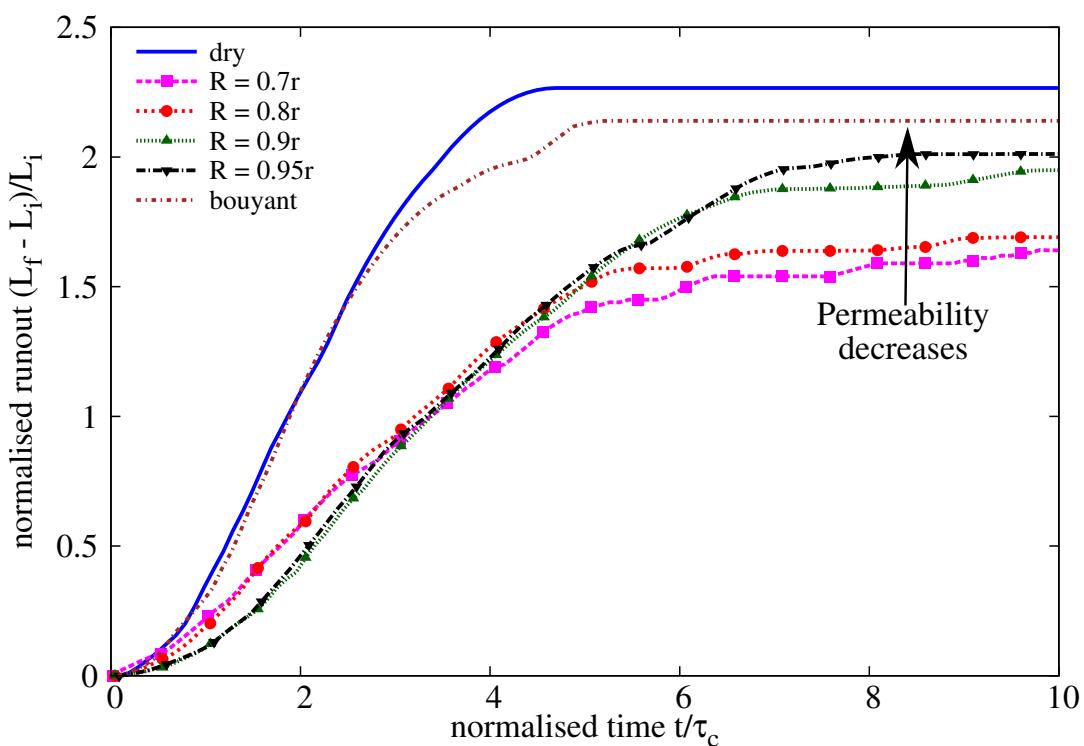


Figure 6.16 Effect of permeability on the evolution of run-out for a column collapse in fluid ( $a = 0.8$ )

- <sup>3</sup> At high permeability ( $r = 0.7 R$ ), the evolution of run-out at the initial stage is quicker,
- <sup>4</sup> which means that the negative pore-pressure that is developed during the shearing along the

fracture surface is dissipated faster. Even though the negative pore-pressure is dissipated, due to the development of negative pore-pressure the evolution of run-out in fluid is slower than its dry counterpart. The rate of dissipation decreases with decrease in the permeability. This can be observed by a flatter slope in the run-out evolution with decrease in permeability. Figure 6.17 shows the distribution of pore-pressure in high and low permeable granular media. At the same time  $t = \tau_c$ , the high permeable ( $r = 0.7 R$ ) granular column shows smaller negative pore-pressure in comparison to large negative pore-pressures observed in the shearing zone for low permeable column ( $r = 0.9 R$ ). This shows that not only does it take longer time for the pore-pressure to dissipate with decrease in permeability, the negative pore-pressure developed in the low permeable condition is almost twice that of the high permeable case (see figure 6.17b).

Although low permeable granular columns take longer duration for the run-out to evolve, the final run-out distance is found to be much longer than high permeable condition. Figure 6.18 shows that the potential energy available for the flow for low permeable column is 20 % smaller than the collapse of high permeable granular column. The kinetic energy evolution (see figure 6.19) shows that the low permeable column has a wider peak kinetic energy distribution in comparison to a sharp peak observed in the high permeable condition. This indicates the influence of lubrication, i.e., hydroplaning of the granular flow in low permeable conditions. The evolution of horizontal kinetic energy reveals that the peak kinetic energy is sustained longer as the permeability of the granular material decreases (see figure 6.19b). Although, the peak kinetic energy is smaller in the low permeability case, the hydroplaning of the flowing granular mass results in longer run-out distance. A high positive pore-pressure is observed at the base of the granular flow in low permeability condition (figure 6.20b) indicating the occurrence of hydroplaning. The evolution of local packing density shows a drop in the packing density at low permeability (see figure 6.21). The drop in the value of packing density between  $t = 2\tau_c$  and  $t = 3\tau_c$  corroborates with the duration of hydroplaning during which large amount of water is entrained at the flow front.

High permeable column shows lower water entrainment, which indicates that for highly permeable flows the drag force acting on the soil grains predominates over the lubrication effect. In both low permeable and high permeable granular flows, the granular material consolidates at the final stage of the flow. This can be observed as the packing density increases at the final stage due to grains settling and expulsion of entrained water. The final deposit profile for both low and high permeability condition are shown in figure 6.22. High permeable collapse show a more parabolic (convex) deposit profile in contrast to the more concave profile observed in low permeability condition. The observation of hydroplaning in low permeable condition may be due to the distribution of the granular mass at the flow front. Instigation of hydroplaning

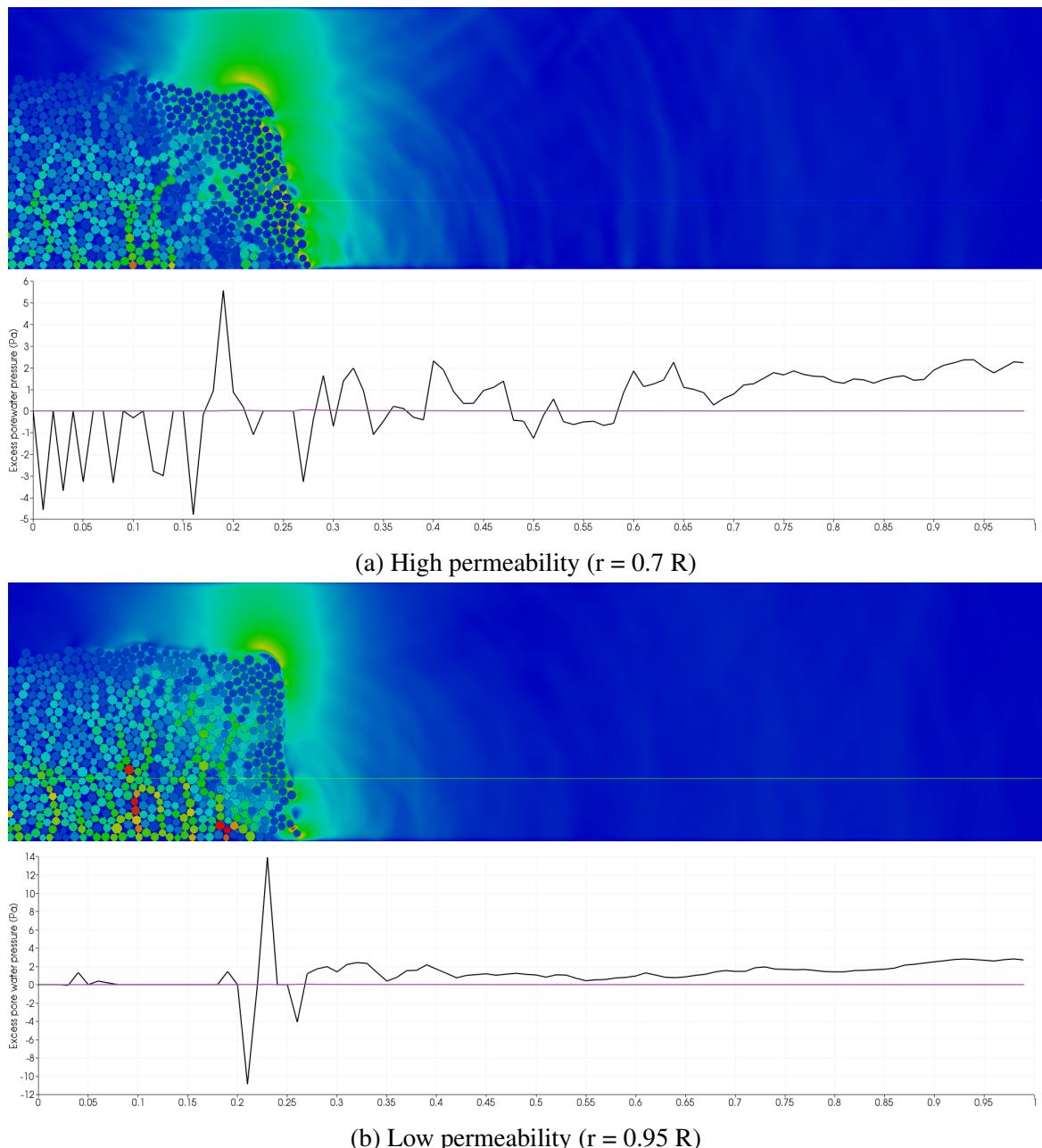


Figure 6.17 Effect of permeability on the excess pore water pressure distribution for a granular column collapse in fluid ( $a = 0.8$  & dense packing) at  $t = \tau_c$

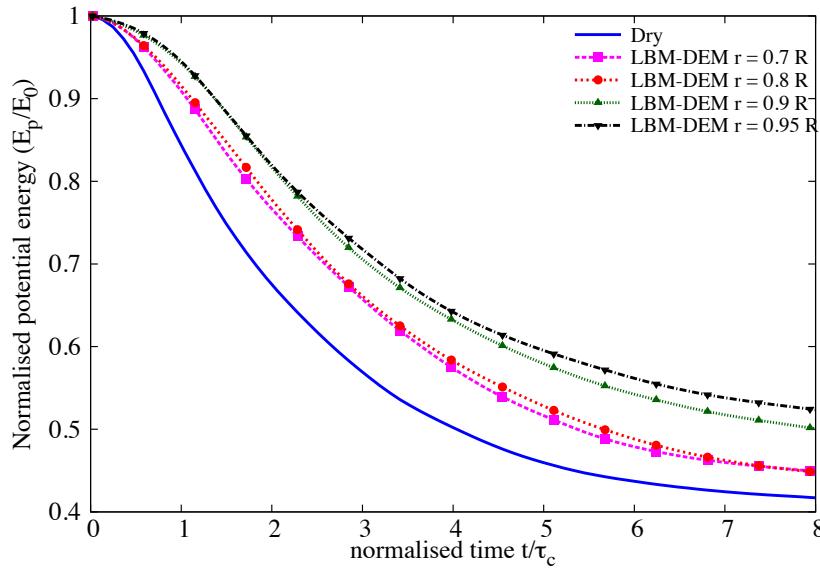


Figure 6.18 Effect of permeability on the evolution of the potential energy with time for a granular column collapse in fluid ( $a = 0.8$ )

5 is controlled by the balance of gravity and inertia forces at the debris front and is suitably  
6 characterized by the densimetric Froude's number:

$$7 \quad Fr_d = \frac{U}{\sqrt{(\frac{\rho_d}{\rho_w} - 1)gH \cos \theta}} \quad (6.6)$$

8 where  $U$  is the average velocity of sliding mass,  $\rho_d$  and  $\rho_w$  are the densities of soil and water,  
9 respectively,  $H$  is the thickness of the sliding mass,  $g$  is acceleration due to gravity and  $\theta$   
10 represents the slope angle. Harbitz (2003) observed hydroplaning above a critical value of  
11 densimetric Froude's number of 0.4. A Froude's  $Fr_d$  value of 0.427 is observed for low  
12 permeable flow ( $r = 0.95 R$ ), which indicates the occurrence of hydroplaning. Whereas a  
13  $Fr_d = 0.273$  is observed for high permeable granular flow indicating absence of hydroplaning,  
14 the low permeable collapse is predominated by the viscous drag force resulting in a parabolic  
15 profile and shorter run-out distance.

16 The normalised final run-out distance as a function of the initial aspect ratio of the column  
17 is presented in figure 6.23. For all aspect ratios, the dry condition yields the longest run-out  
18 distance. For a given aspect ratio, the dry collapse acquires the highest kinetic energy due to the  
1 lack of viscous dissipation during vertical collapse. This extra kinetic energy is high enough  
2 to propel the heap, in-spite of a high frictional dissipation, over a distance that is longer than  
3 the run-out distance in the fluid regime. In submerged condition, for the same aspect ratio, the

## 6.3 Granular collapse in fluid

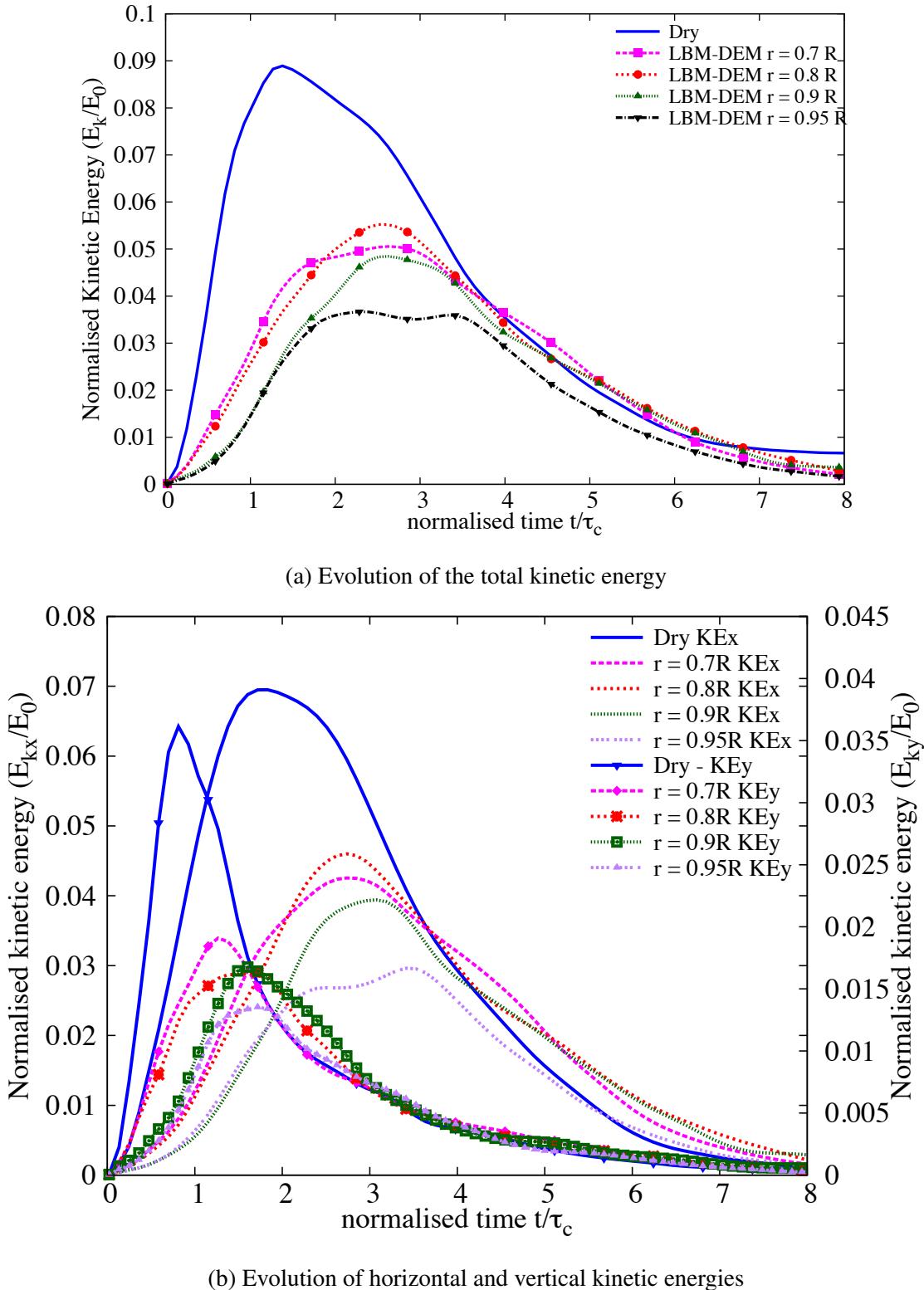


Figure 6.19 Effect of permeability on the evolution of kinetic energies with time for a granular column collapse in fluid ( $a = 0.8$ )

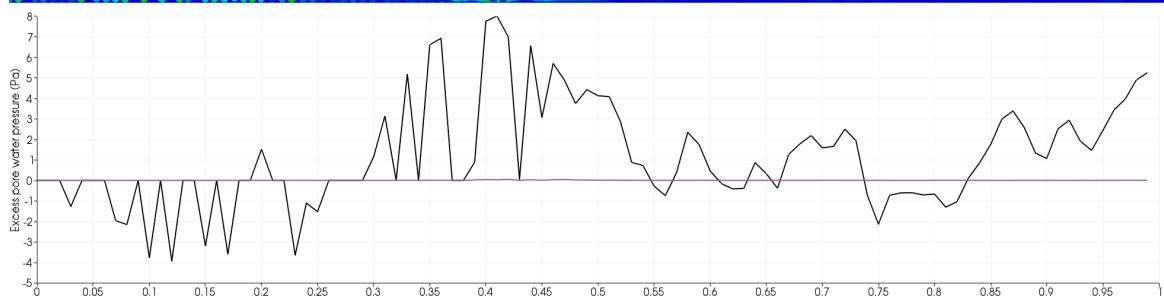
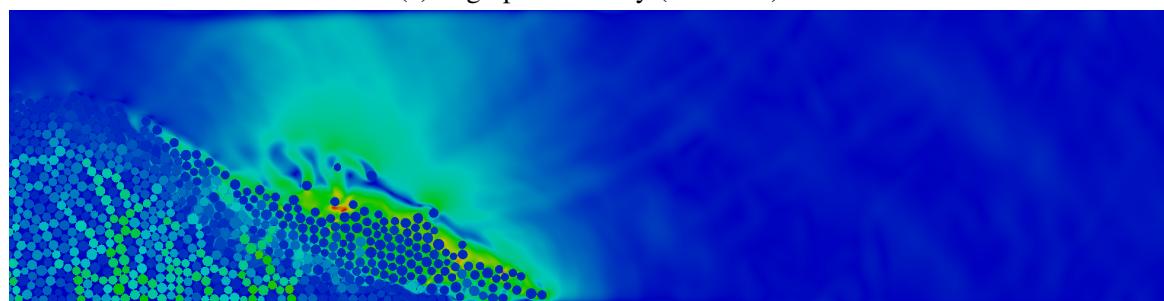
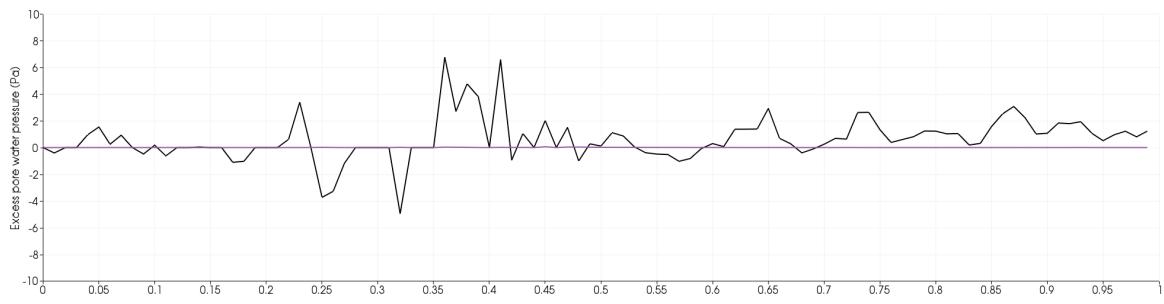
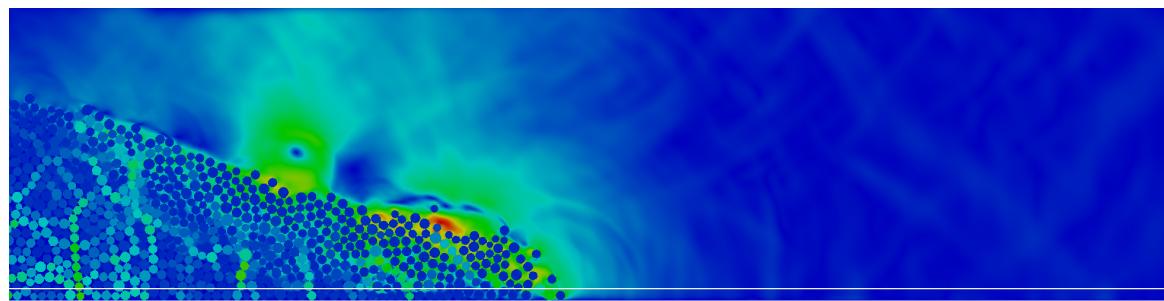


Figure 6.20 Effect of permeability on the excess pore water pressure distribution for a granular column collapse in fluid ( $a = 0.8$  & dense packing) at  $t = 2\tau_c$

## 6.3 Granular collapse in fluid

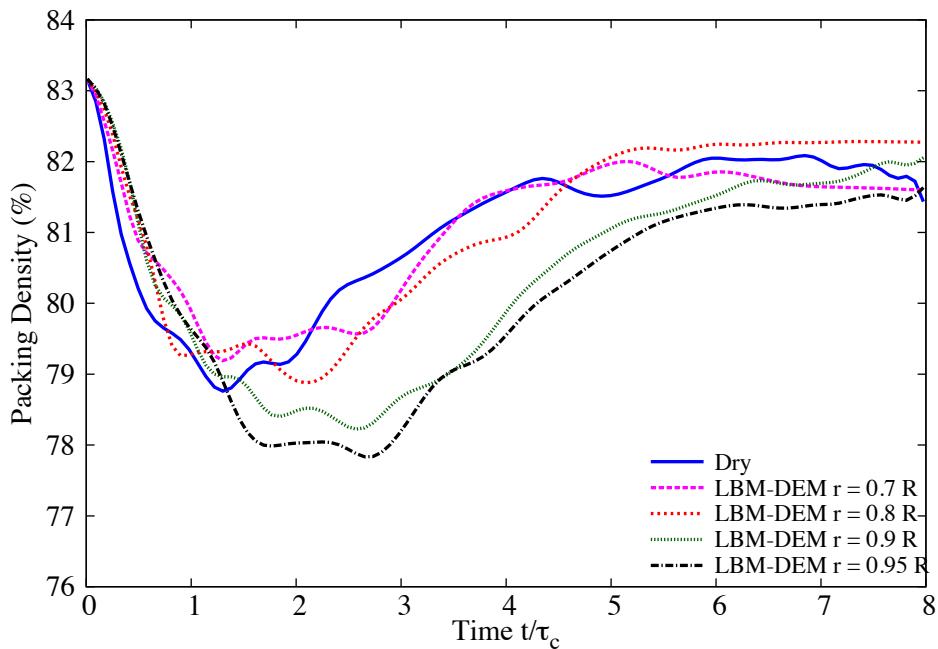
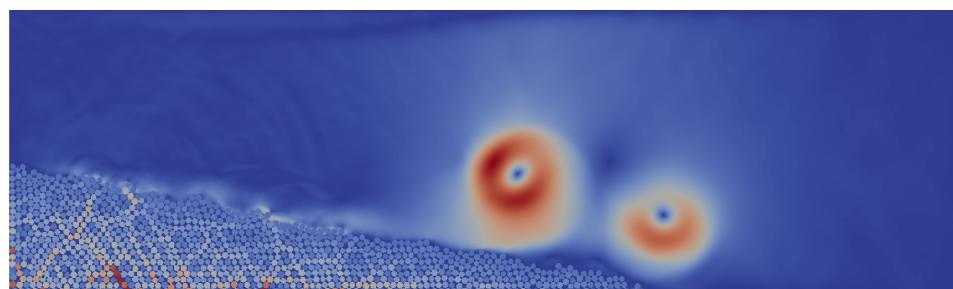
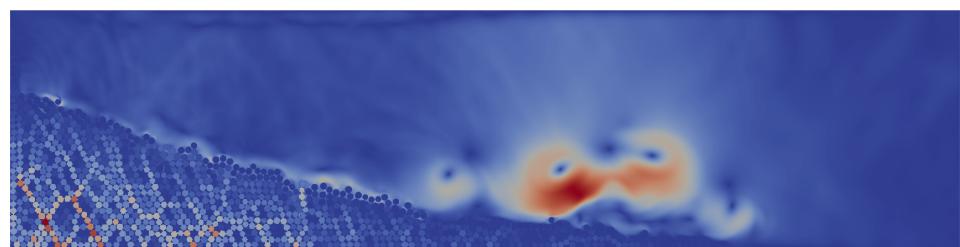


Figure 6.21 Effect of permeability on the evolution of packing density for a granular column collapse in fluid ( $a = 0.8$  & dense initial packing)



(a) High permeability ( $r = 0.7 R$ )



(b) Low permeability ( $r = 0.95 R$ )

Figure 6.22 Effect of permeability on the deposit morphology of a granular column collapse in fluid ( $a = 0.8$ )

<sup>4</sup> kinetic energy available for spreading is lower and the dissipation due to viscous drag is higher,  
<sup>5</sup> thus leading to a much shorter run-out distance.

<sup>6</sup> For short columns, with decrease in permeability the run-out distance increases, however,  
<sup>7</sup> the run-out distance is not higher than the dry condition. At higher aspect ratios, decrease in  
<sup>8</sup> permeability from  $r = 0.8 R$  to  $r = 0.9 R$  does not have a significant influence on the run-out  
<sup>9</sup> behaviour. This can be attributed to the turbulent nature of the granular flows for tall columns.  
<sup>10</sup> The run-out behaviour is a result of transformation of (part of) the initial potential energy to the  
<sup>11</sup> peak kinetic energy, which in turn controls the subsequent run-out along the plane. The run-out  
<sup>12</sup> distance is plotted as a function of the normalised peak kinetic energy in figure 6.24. For the same  
<sup>13</sup> aspect ratio, the peak kinetic energy is higher in the case of dry column. This represents  
<sup>1</sup> grain inertial regime in dry granular collapse, which indicates that a part of the potential energy,  
<sup>2</sup> in the presence of the fluid, is dissipated during the vertical collapse due to viscous friction. In  
<sup>3</sup> all regimes, the run-out distance increases as a power law  $L_f \propto KE_{max}^\gamma$ . For the same value of  
<sup>4</sup> peak kinetic energy, the run-out distance in fluid is longer than the dry column collapse. Also,  
with decrease in permeability the run-out distance increases for the same peak kinetic energy.

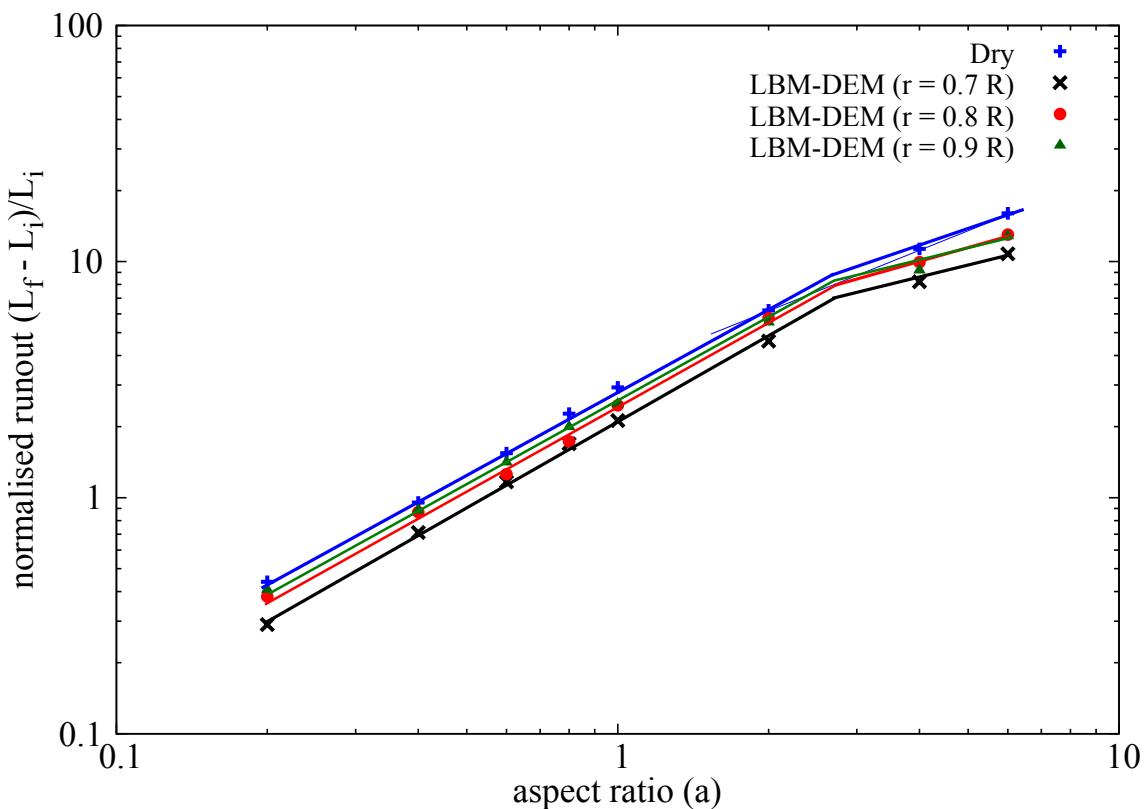


Figure 6.23 Normalised final run-out distance for columns with different initial aspect ratios. Comparison of dry and submerged granular column collapse for different hydrodynamic radius ( $0.7R$ ,  $0.8R$  and  $0.9R$ ).

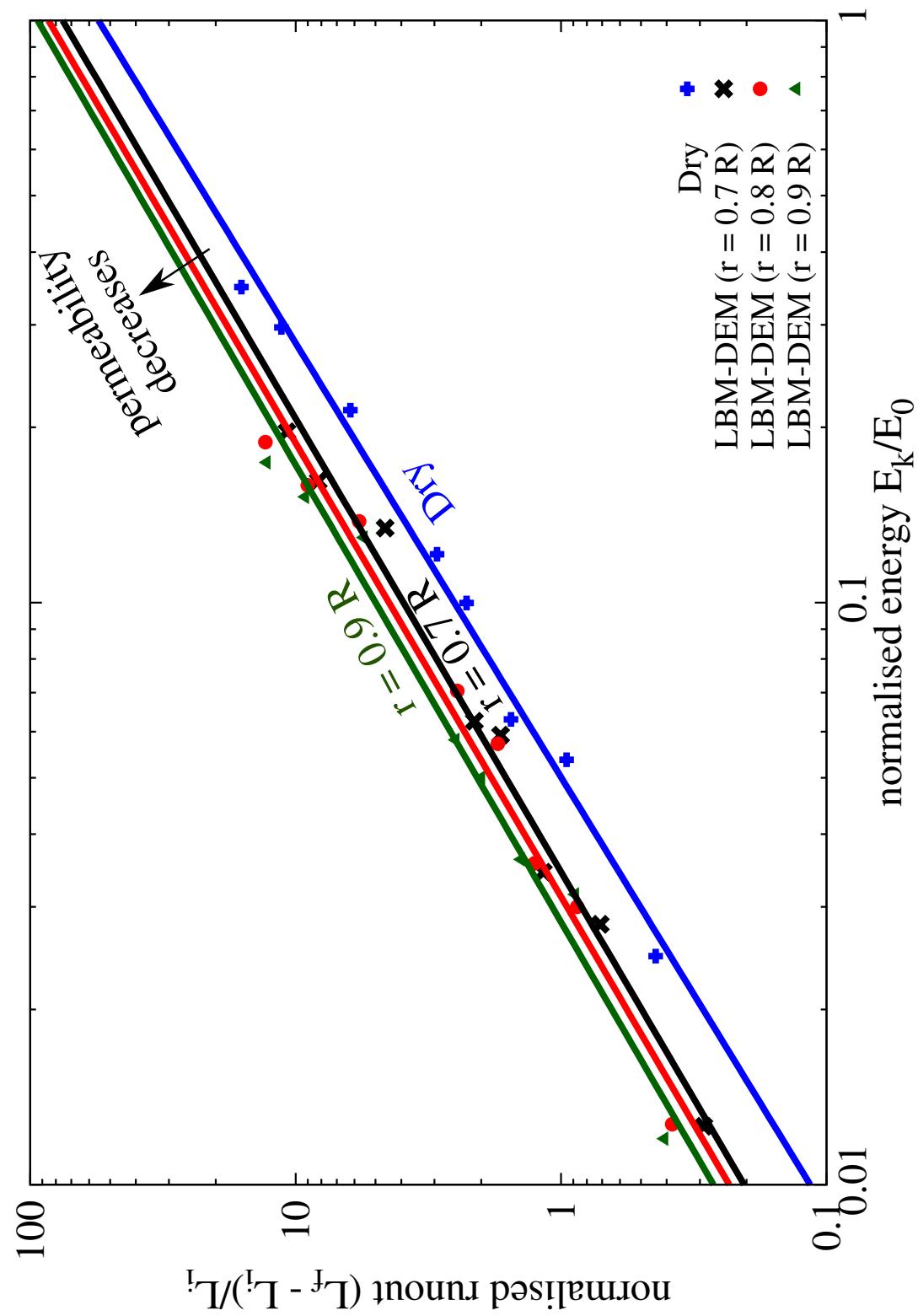


Figure 6.24 Normalised final run-out distance for columns as a function of peak kinetic energy. Comparison of dry and submerged granular column collapse for different hydrodynamic radius (0.7R, 0.8R and 0.9R).

### 6 6.3.4 Effect of initial packing density

7 Rondon et al. (2011) observed that the loose packings flow rapidly on a time scale proportional  
8 to the initial height and results in longer run-out distance in comparison to the dense packing.  
9 Hydroplaning occurs above a critical Froude's number of 0.4. The Froude's number is inversely  
10 related to the thickness of the flow and its density. Hence, for the same thickness of flow, a  
11 loose granular column will experience more hydroplaning than a dense granular flow. This  
12 effect might result in longer run-out behaviour in fluid than the dry condition for the same  
13 initial aspect ratio. The initial packing density and the permeability of a 2D granular column,  
14 with an aspect ratio of 0.8, are varied to understand their influence on the run-out behaviour.  
15 The run-out behaviour of the dense case (83% packing density), discussed in the previous  
16 section, is compared with a loose granular column (79% packing fraction). The permeability is  
17 varied by changing the hydrodynamic radius from 0.7 R to 0.95 R.

18 The normalised run-out evolution with time for a loose initial packing (79% packing frac-  
19 tion) with different hydrodynamic radii 0.7 R, 0.8 R, 0.9 and 0.95 R are presented in figure 6.25.  
20 The run-out evolution of dry and a column with grains in suspension with an initial aspect ratio  
21 of 0.8 is also presented to understand the influence of hydrodynamic forces on the flow kine-  
22 matics. Similar to dense granular column, the run-out distance increases with increase in the  
23 hydrodynamic radius (i.e., decrease in permeability). At low permeability ( $r = 0.9$  and  $0.95R$ ),  
24 the run-out distance is longer than the dry condition. This shows that the lubrication effect in  
25 low permeability condition overcomes the influence of the drag force and the development of  
26 large negative pore pressure resulting in longer run-out distance. Although suspended granular  
27 mass experience high drag force and turbulent effects, the run-out evolves almost at the same  
28 rate in comparison with granular columns with high permeability. This shows the effect of  
29 permeability on the dissipation rate of negative pore pressure developed during the initial stage  
30 of collapse.

31 Figure 6.26 shows the development of negative pore pressure in low permeability ( $r = 0.95$   
32 R) and dissipation of negative pore pressure in high permeability ( $r = 0.7$  R) at the same time  
33  $t = \tau_c$ . This difference in the quantity and the rate of dissipation of negative pore pressure  
34 results in difference in the rate of flow evolution. Low permeable column takes longer duration  
35 for the flow to evolve. As the flow progresses, low permeability of the granular column  
36 causes hydroplaning to occur at the base of the column resulting in longer run-out distance  
(see figure 6.27).

1 The evolution of potential energy with time reveals that at a very low permeability ( $r =$   
2  $0.95$  R), the initial potential energy mobilised is smaller than at  $r = 0.9R$ . Also with decrease in  
3 permeability, the time required to dissipate the negative pore pressure increases. This results in  
4 a shorter run-out distance in the case of  $r = 0.95$  R than  $r = 0.9$  R. As the quantity of material  
5

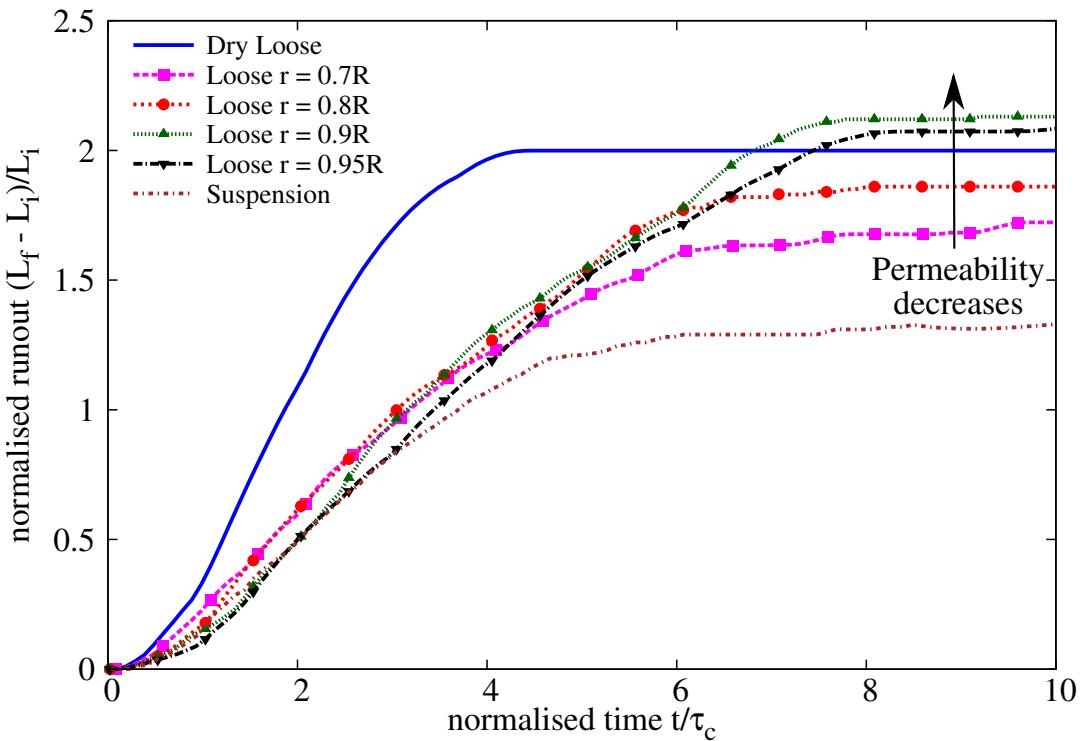


Figure 6.25 Effect of permeability on the evolution of run-out for a column collapse in fluid ( $a = 0.8$  & loose packing)

destabilised is small, which results in a thinner flow having a high Froude's number. However, the peak horizontal kinetic velocity observed in the case of  $r = 0.9 R$  is higher than  $r = 0.95 R$  (see figure 6.30b). A Froude's number of 0.59 for  $r = 0.9 R$  is observed in contrast to 0.46 for  $r = 0.95 R$ . Both values of hydrodynamic radii result in a Froude's number that indicates occurrence of hydroplaning. The difference in the amount of material destabilised for  $r = 0.95 R$  and the decreased effect of hydroplaning results in shorter run-out distance for  $r = 0.95 R$  in comparison to  $r = 0.9 R$ .

As the column collapses, water is entrained at the flow front. This can be observed by decrease in the packing fraction during  $t = 1\tau_c$  and  $t = 3\tau_c$ . As the flow progresses, the entrained water is expelled and the soil grains consolidate to reach a critical packing density at the end of the flow (see figure 6.29). The permeability (hydrodynamic radius) plays a crucial role in the rate of dissipation of the entrained water. As the permeability decreases, the water entrained at the flow front takes longer time to be dissipated resulting in lubrication of the flow at low permeability. This lubrication effect results in increased run-out distance for columns with low permeability.

The evolution of grain trajectories with time are presented in figure 6.31 for low permeability ( $r = 0.95 R$ ) and high permeability condition ( $r = 0.9 R$ ). It can be observed that a high

(a) High permeability ( $r = 0.7 R$ )(b) Low permeability ( $r = 0.95 R$ )

Figure 6.26 Effect of permeability on the excess pore water pressure distribution for a granular column collapse in fluid ( $a = 0.8$  & loose packing) at  $t = \tau_c$

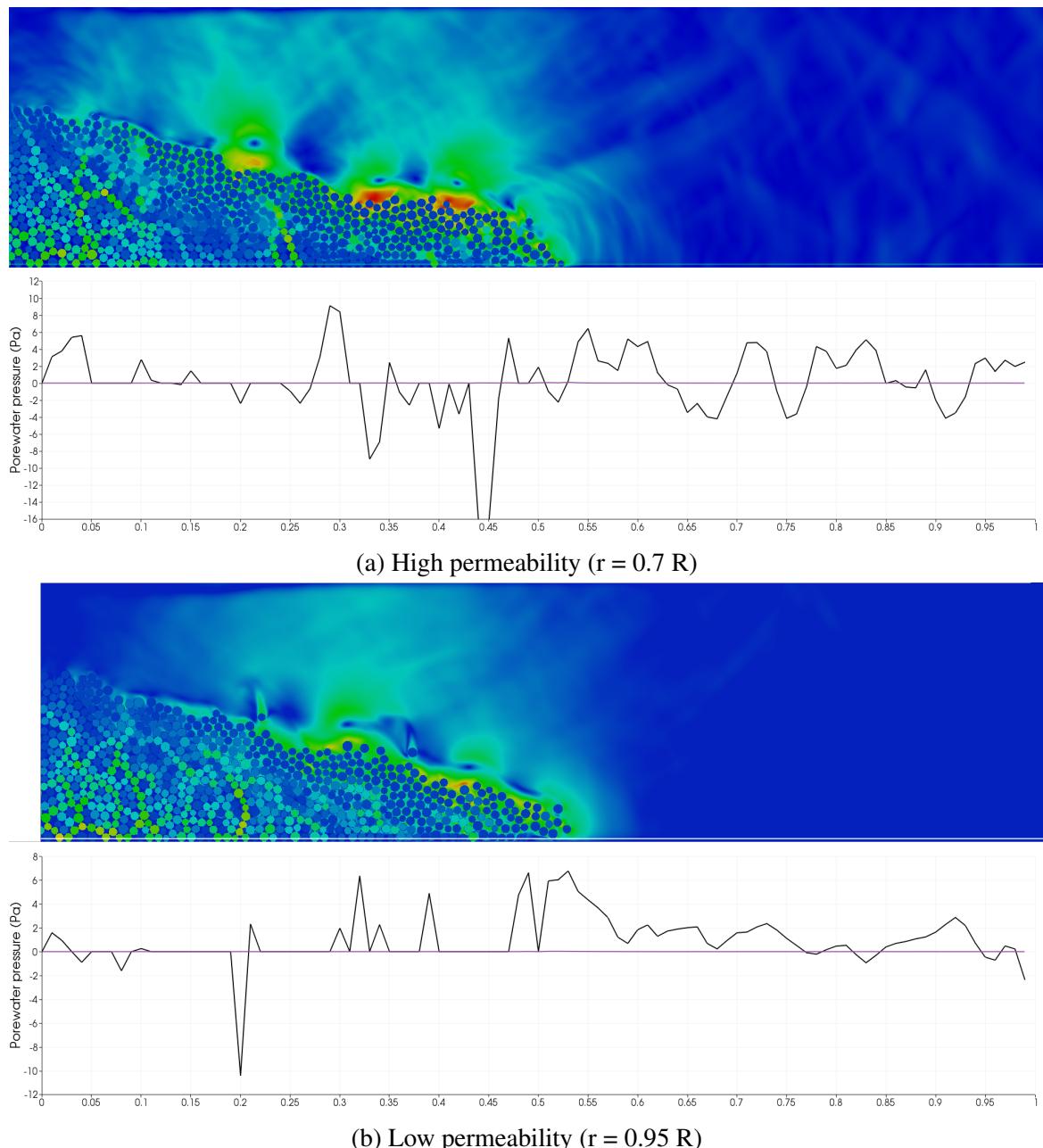


Figure 6.27 Effect of permeability on the excess pore water pressure distribution for a granular column collapse in fluid ( $a = 0.8$  & loose packing) at  $t = 2\tau_c$

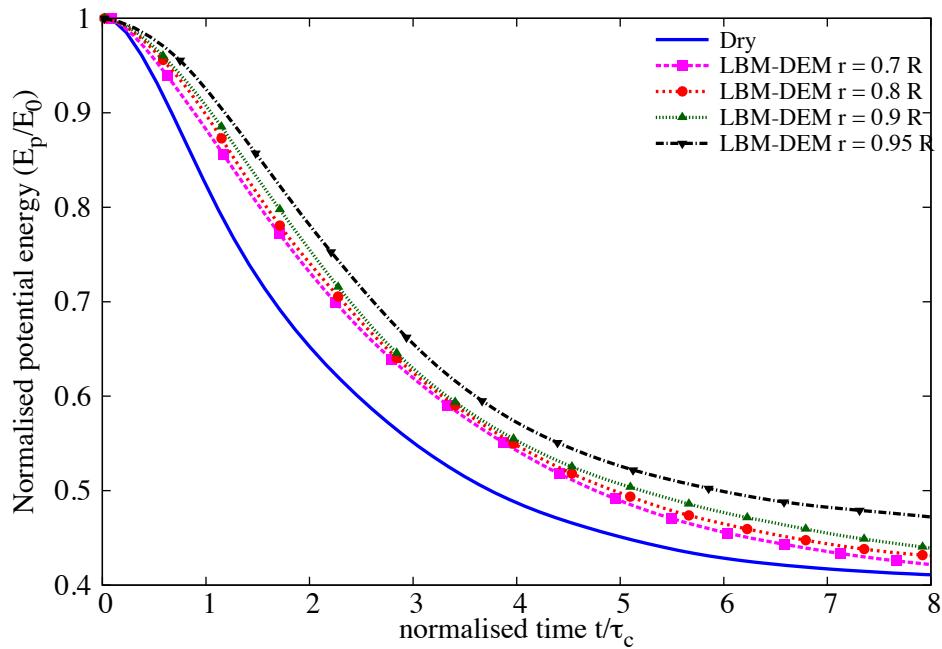


Figure 6.28 Effect of permeability on the evolution of the potential energy with time for a granular column collapse in fluid ( $a = 0.8$  & loose packing)

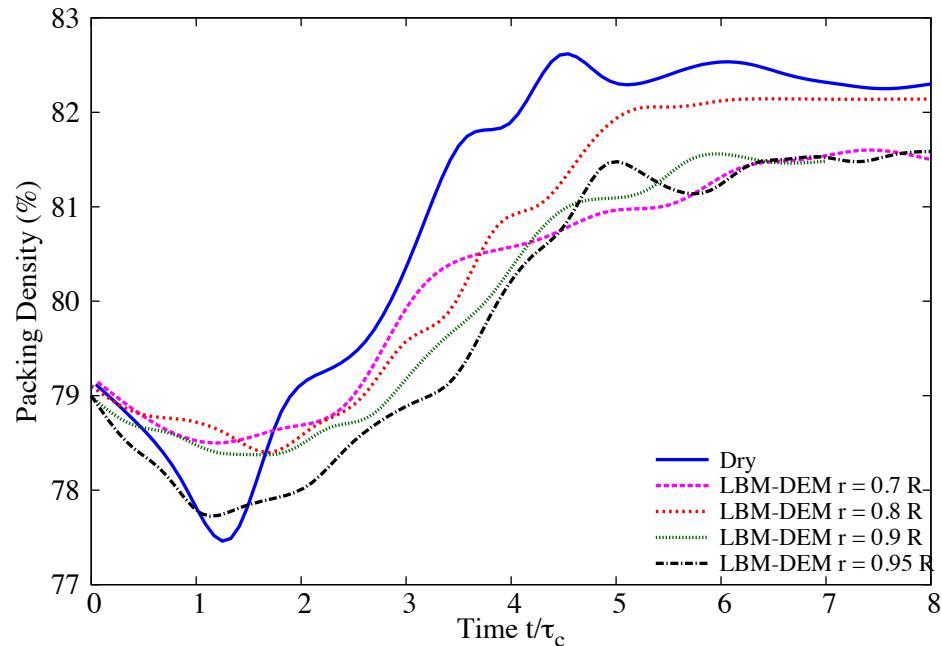
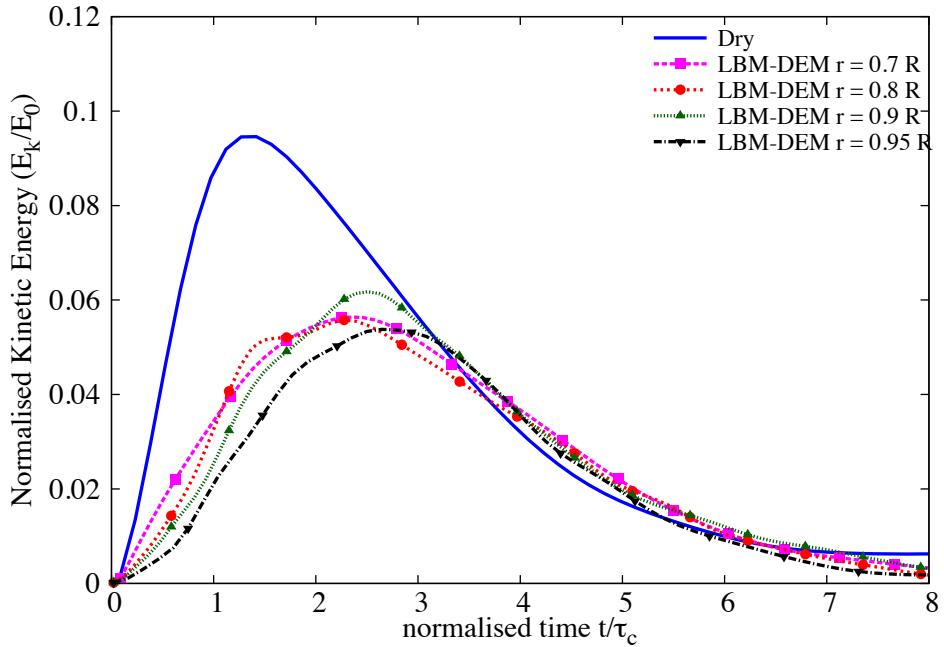
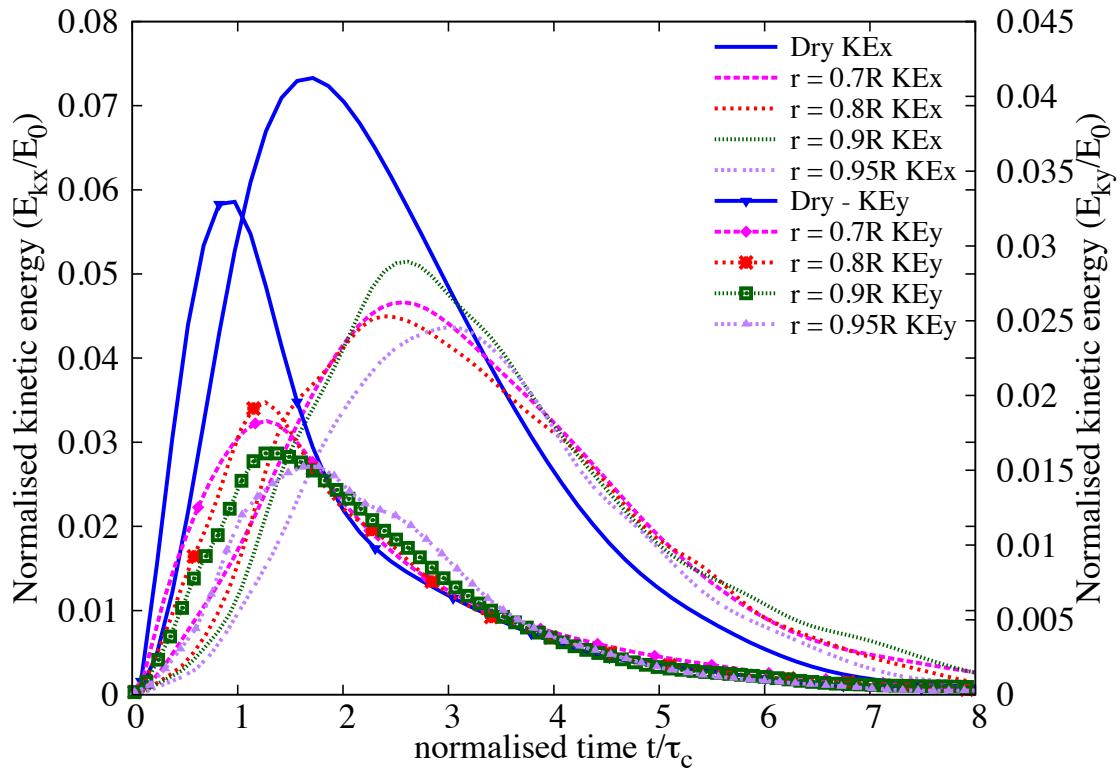


Figure 6.29 Effect of permeability on the evolution of packing density for a granular column collapse in fluid ( $a = 0.8$  & loose initial packing)

## 6.3 Granular collapse in fluid



(a) Evolution of the total kinetic energy



(b) Evolution of horizontal and vertical kinetic energies

Figure 6.30 Effect of permeability on the evolution of kinetic energies with time for a granular column collapse in fluid ( $a = 0.8$  & loose packing)

6 permeability column shows a parabolic (convex) final profile in contrast to the more concave  
7 profile observed in low permeability condition. This difference in the flow thickness results  
8 in higher value of Froude's number and the occurrence of hydroplaning in low permeability  
9 condition. Due to high permeability, the water entrained at the flow front is dissipated quicker  
10 and thus no lubrication effect is observed. A Froude's number of 0.272 (no hydroplaning) is ob-  
11 served for high permeability condition ( $r = 0.7 R$ ). This shows that the drag force predominates  
12 at high permeability, while the low permeability condition is characterised by hydroplaning  
13 and lubrication.

14 Figure 6.32 shows the normalised pressure at the base for the low and high permeability  
15 flows at  $t = 2\tau_c$ . The normalised effective stress plotted is obtained as the average over 5 time  
16 steps at  $2\tau_c$ . The effective stress at the base is normalised to the effective stress of a static  
17 granular column before the collapse. A value of 1 indicates that the effective stress hasn't  
18 changed, which can be observed in the static region of the granular column. It can be observed  
19 that the normalised effective stress is significantly high for low permeability condition at the  
20 flow front in comparison to almost non-existence of effective stress in the low permeability  
21 condition. The observation of trivial effective stress at the flow front corroborates the lubrication  
22 effect observed at low permeability conditions.

23 Figure 6.33 shows the grain trajectories of a dense and a loose initial packing for a hydro-  
24 dynamic radius ( $r = 0.95R$ ). It can be observed that the dense initial packing results in a lot of  
25 turbulent behaviour at the flow surface in contrast to the more plug like flow observed in the  
26 loose condition. The thickness of the deposit in both dense and loose condition is almost the  
27 same, however the density of the flow results in a Froude's number of 0.46 and 0.429 for loose  
28 and dense conditions, respectively. The low initial density results in more hydroplaning in the  
29 loose condition. The effect of water entrainment at the flow front between dense and loose  
30 condition can be seen in figure 6.34. Comparing the packing density (see figures 6.21 and 6.29)  
31 reveals almost the same amount of water entrainment in both dense and loose conditions.  
1 Hence, it is the density of the flowing granular mass that controls the influence of hydroplaning  
2 for a given hydrodynamic radius and initial aspect ratio. A loosely packed granular column  
3 with low permeability entrains more water at the flow front, resulting in a hydroplaning effect  
4 that overcomes the influence of viscous drag forces and thereby yields a higher run-out distance  
5 than the dry condition.

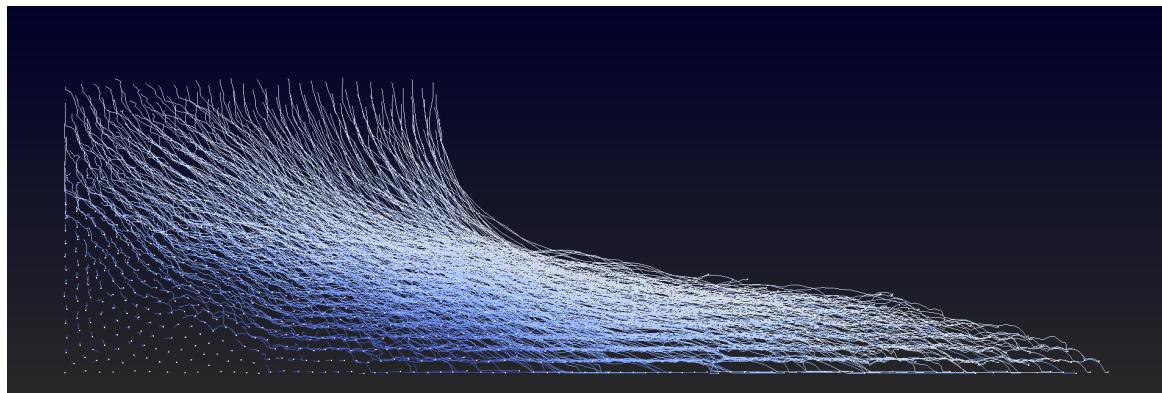
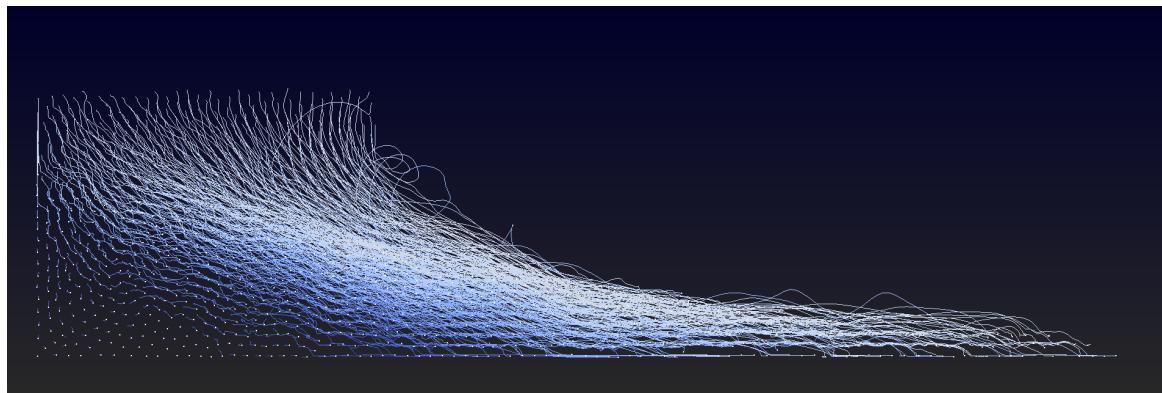
(a) High permeability ( $r = 0.7 R$ )(b) Low permeability ( $r = 0.95 R$ )

Figure 6.31 Particle tracking of the deposit morphology for a granular column collapse in fluid ( $a = 0.8$  & loose packing), influence of permeability

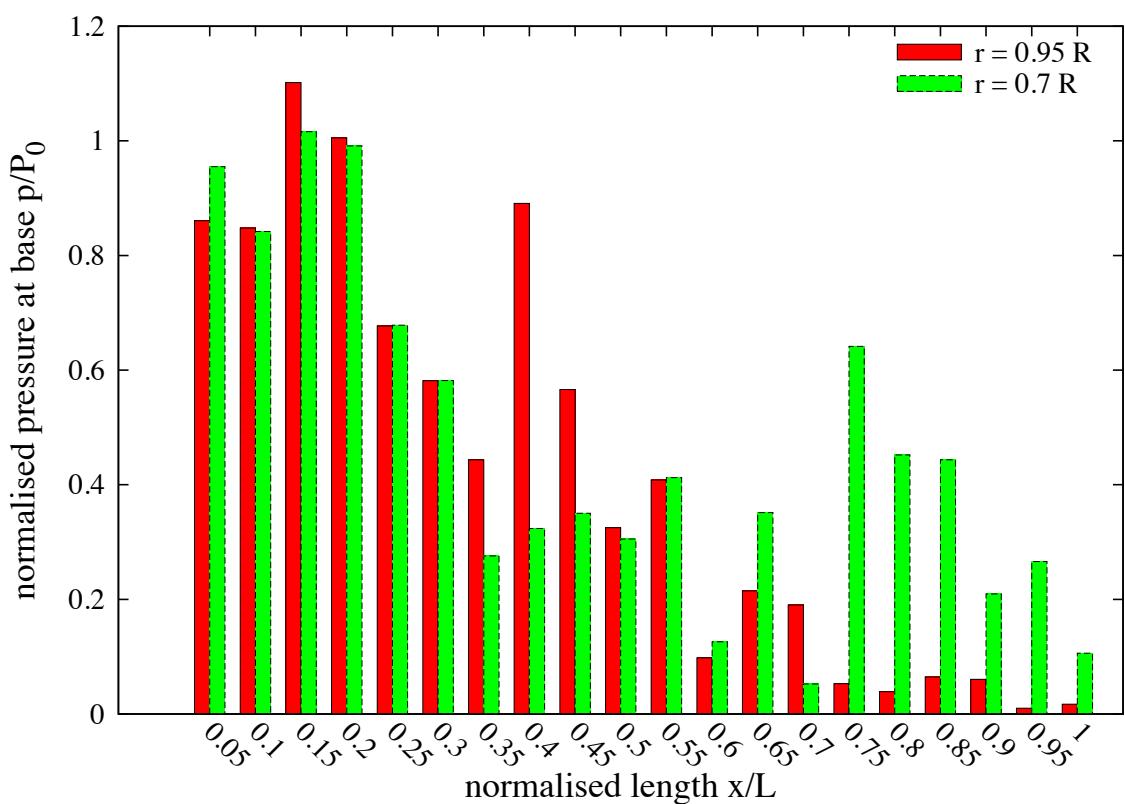
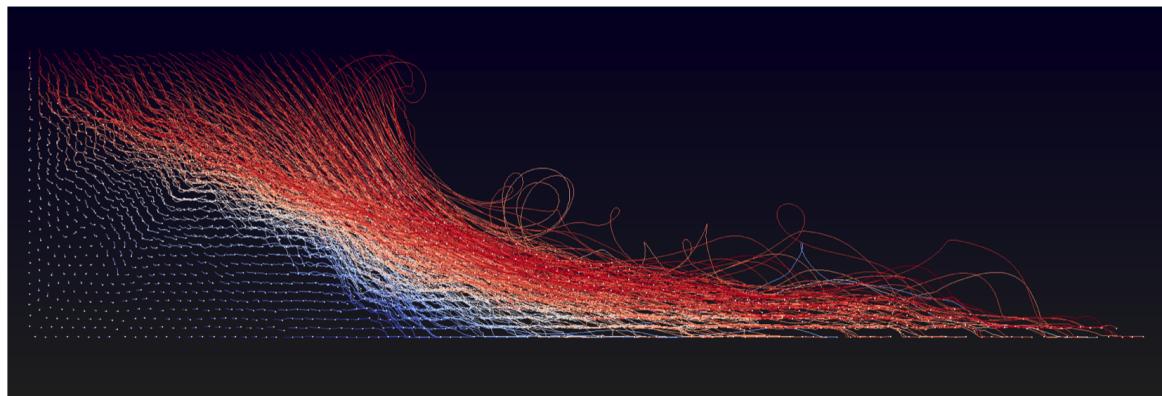
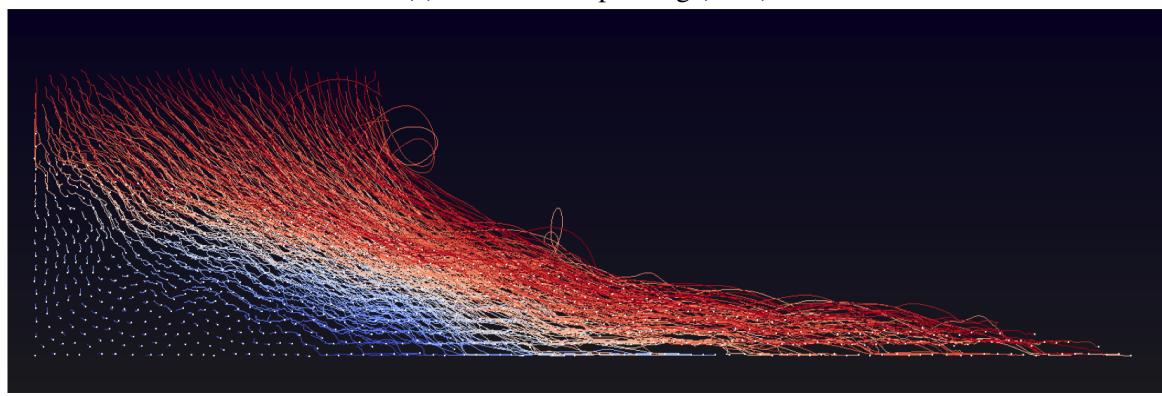


Figure 6.32 Effect of permeability on the normalised effective stress for loose initial packing at  $t = 2\tau_c$



(a) Dense initial packing (83%)

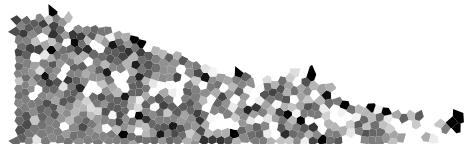


(b) Loose initial packing (79%)

Figure 6.33 Effect of initial density on the deposit morphology for a granular column collapse in fluid ( $\alpha = 0.8$ ). Dense vs loose initial packing fraction ( $r = 0.95R$ ). Darker means dense packing, white indicates loose packing density.



(a) Dense initial packing (83%)



(b) Loose initial packing (79%)

Figure 6.34 Evolution of packing fraction at  $t = \tau_c$  for dense and loose initial packing fraction.

## 6 6.4 Submarine granular flows down incline plane

7 Slope failure is a problem of high practical importance for both civil engineering structures  
8 and natural hazards management. Catastrophic events such as landslides, debris flows, rock  
9 avalanches or reservoir embankment failures exemplify the potential consequences of a soil  
10 gravitational instability. One of the most critical situation concerns a submerged sandy slope  
11 since pore pressure changes, related to groundwater seepage flow or soil dilation/contraction,  
12 can significantly affect the stability of many earth structures or natural soils.

13 The influence of slope angle on the effect of permeability and the initial packing density  
14 on the run-out behaviour are studied. In this study, a 2D poly-disperse system ( $d_{max}/d_{min} = 2$ )  
15 of circular discs forming a granular column in fluid is used to understand the behaviour of  
16 granular flows down inclined planes (see ??). The soil column is modelled using  $\sim 1000$  to  
17  $2000$  discs of density  $2650 \text{ kg m}^{-3}$  and a contact friction angle of  $26^\circ$ . The collapse of the  
18 granular column is simulated inside a fluid with a density of  $1000 \text{ kg m}^{-3}$  and a kinematic  
19 viscosity of  $1 \times 10^{-6} \text{ m}^2 \text{ s}^{-1}$ . A granular column with an initial aspect ratio  $a$  of  $0.8$  is used.  
20 A hydrodynamic radius  $r = 0.9 R$  is adopted during the LBM computations. Dry analyses  
21 are also performed to study the effect of hydrodynamic forces on the run-out distance. The  
22 slope angle is varied as  $0^\circ$ ,  $2.5^\circ$ ,  $5^\circ$ , and  $7.5^\circ$ . The effect of initial packing density is studied  
23 using a dense packing (83% packing fraction) and a loose packing (79% packing fraction) of  
24 granular columns that collapse on to an inclined plane at different slope angles. The influence  
25 of permeability (with hydrodynamic radius varied as  $0.7$ ,  $0.75$ ,  $0.8$ ,  $0.85$  and  $0.9 R$ ) on the  
26 run-out behaviour of collapse of granular columns with initial packing density of 83% and 79  
27 % on to an inclined plane with a slope angle of  $5^\circ$  is also analysed.

### 28 6.4.1 Effect of initial density

29 The morphology of granular deposits in fluid is shown to be mainly controlled by the initial  
30 volume fraction of the granular mass and not by the aspect ratio of the column (Pailha et al.,  
31 2008; Rondon et al., 2011). In order to understand the influence of the initial packing density  
32 on the run-out behaviour, a dense sand column (initial packing density,  $\Phi = 83\%$ ) and a  
33 loose sand column ( $\Phi = 79\%$ ) are considered. The granular columns collapse and flow down  
slopes of varying inclinations ( $2.5^\circ$ ,  $5^\circ$  and  $7.5^\circ$ ). The run-out behaviour is compared with the  
collapse of a granular column in fluid on a horizontal surface. For all slope angles, the flow  
kinematics in the submerged condition is compared with its dry counterpart to understand the  
influence of lubrication and viscous drag. A hydrodynamic radius of  $r = 0.9 R$  is adopted in all  
cases, because low permeability conditions result in longer run-out distance as observed in the  
previous section.

The evolution of run-out for a dense sand column with time in dry and submerged conditions for varying slope inclinations are presented in figure 6.35a. For all slope angles, the run-out distances in the dry condition are longer than those observed in the submerged condition. Similar to the case of collapse on a horizontal plane, the dense granular columns experience significant drag forces than the lubrication effect. The difference in the run-out between the dry and the submerged condition decreases with increase in the slope angle. At a slope angle of 5° the difference in the run-out between the dry and the submerged condition is the smallest. This is due to significant hydroplaning of a thin flowing layer, the occurrence of hydroplaning can be observed by a sustained peak kinetic energy (see figure 6.35b). At higher slope angles (> 5°), the drag force predominates over the lubrication effect and results in shorter run-out distance.

Similar to the case of collapse on a horizontal surface, dense granular columns in fluid require a longer time to collapse and flow, due to the development of large negative pore pressures. Large negative pore pressures are developed as the dense granular material dilates due to shearing along the fracture surface in the initial phase of the flow. The snapshots of the dense granular column collapse down slopes of varying inclinations at the time ( $t = \tau_c = 3\sqrt{H/g}$ ), are shown in figure 6.36.

It can be seen that the viscous drag on the dense column tend to predominate over the influence of hydroplaning on the run-out behaviour. This influence can be observed in the smaller peak kinetic energy for submerged granular in comparison to the dry condition (see Figure 6.35b). With increase in the slope angle, the volume of material that dilates increases. This results in large negative pore pressures and more viscous drag on the granular material. Hence, the difference in the run-out between the dry and the submerged conditions, for a dense granular assembly, increases with increase in the slope angle above an inclination of 5°.

In contrast to the dense granular columns, the loose granular columns (packing fraction of 79%) show longer run-out distance in immersed conditions (see Figure 6.37a). The run-out distance in fluid increases with increase in the slope angle in comparison to the dry cases. The loose granular flow tends to entrain more water at the base of the flow front, creating a lubricating surface, which results in a longer run-out distance (see Figure 6.38). For the same thickness of the flow, the loose granular flow has smaller density and hence higher Froude's number than the dense flow resulting in a higher probability of hydroplaning. The hydroplaning effect causes an increase in the flow velocity for the loose granular material in comparison with the dense condition (see Figure 6.37b).

The snapshots at  $t = 3\tau_c$  of a loose granular column ( $\alpha = 0.8$ ) collapse down slopes inclined at an angle of 2.5°, 5° and 7.5° are presented in figure 6.38. In contrast to dense granular flows, a plug-like flow can be observed. Due to low permeability, the water entrapped in the flow front results in a drop in the density of the flowing mass thus enabling hydroplaning. The

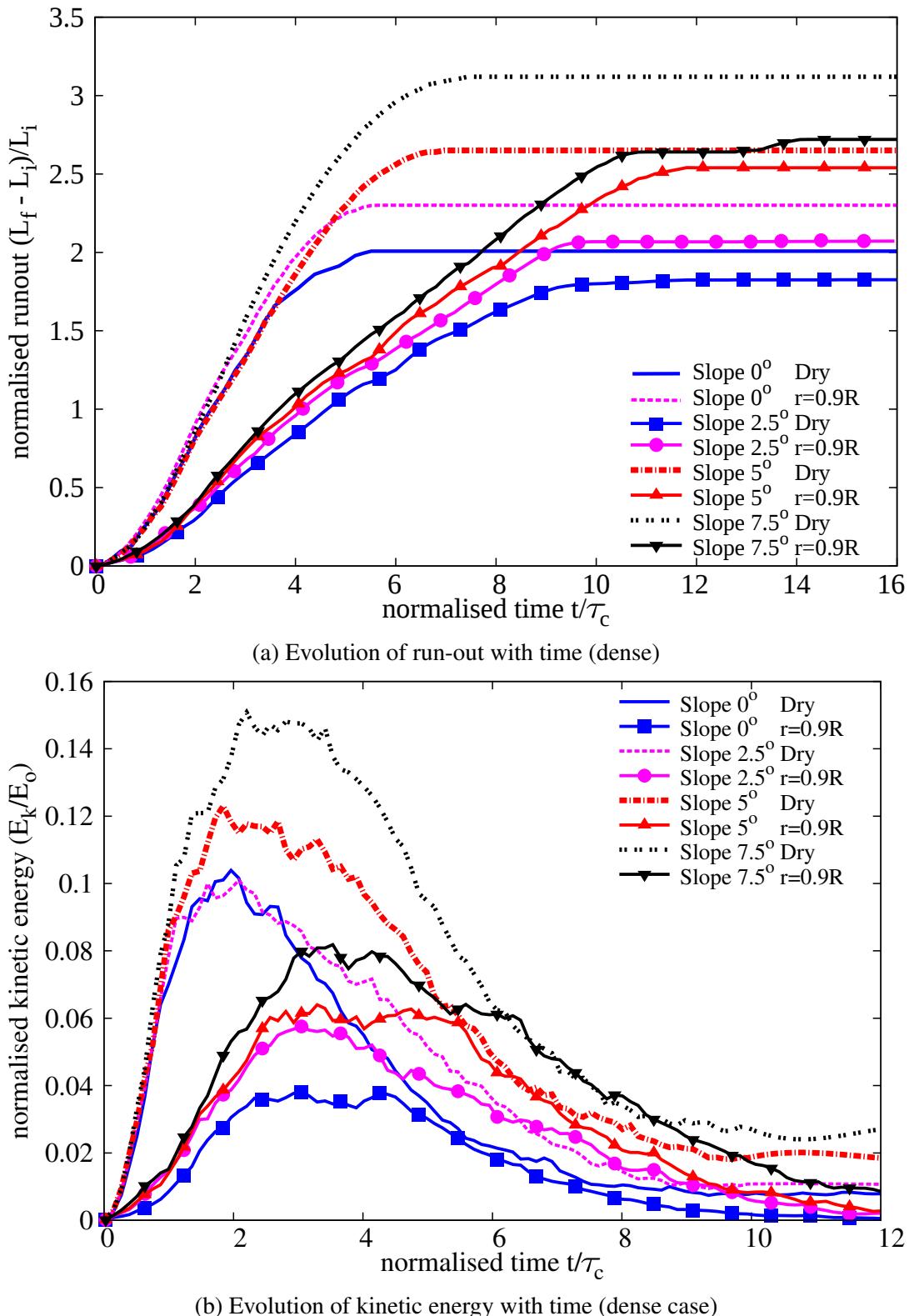
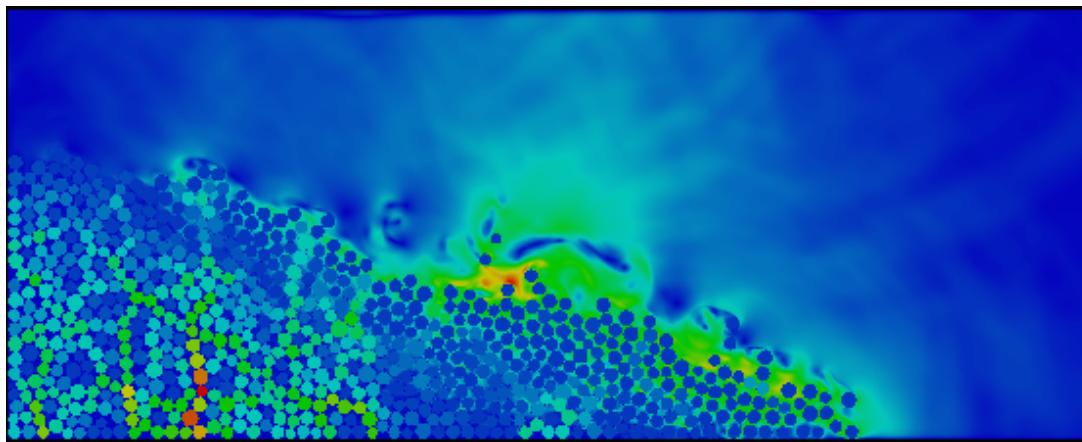
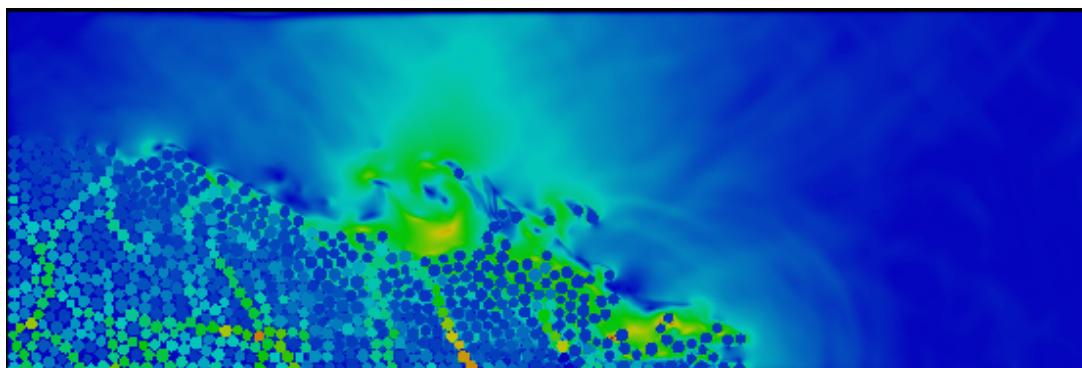


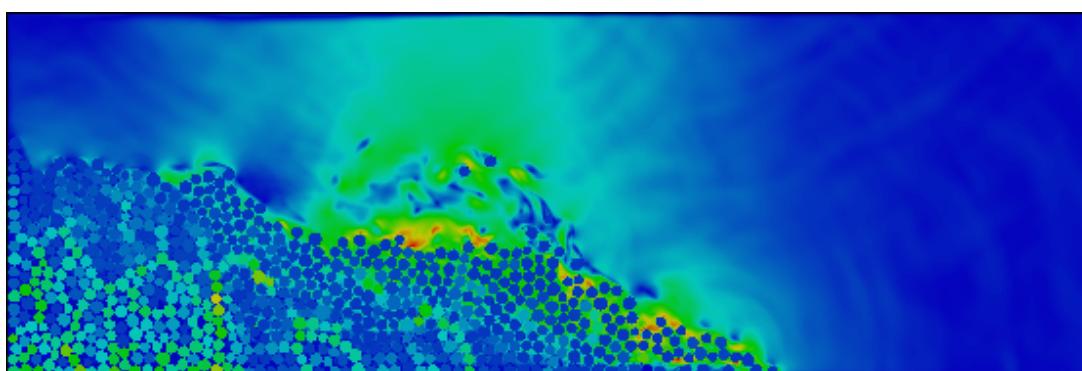
Figure 6.35 Evolution of run-out and kinetic energy with time (dense)



(a) Slope 2.5



(b) Slope 5.0



(c) Slope 7.5

Figure 6.36 Flow morphology at  $t = 3\tau_c$  for different slope angles (dense)

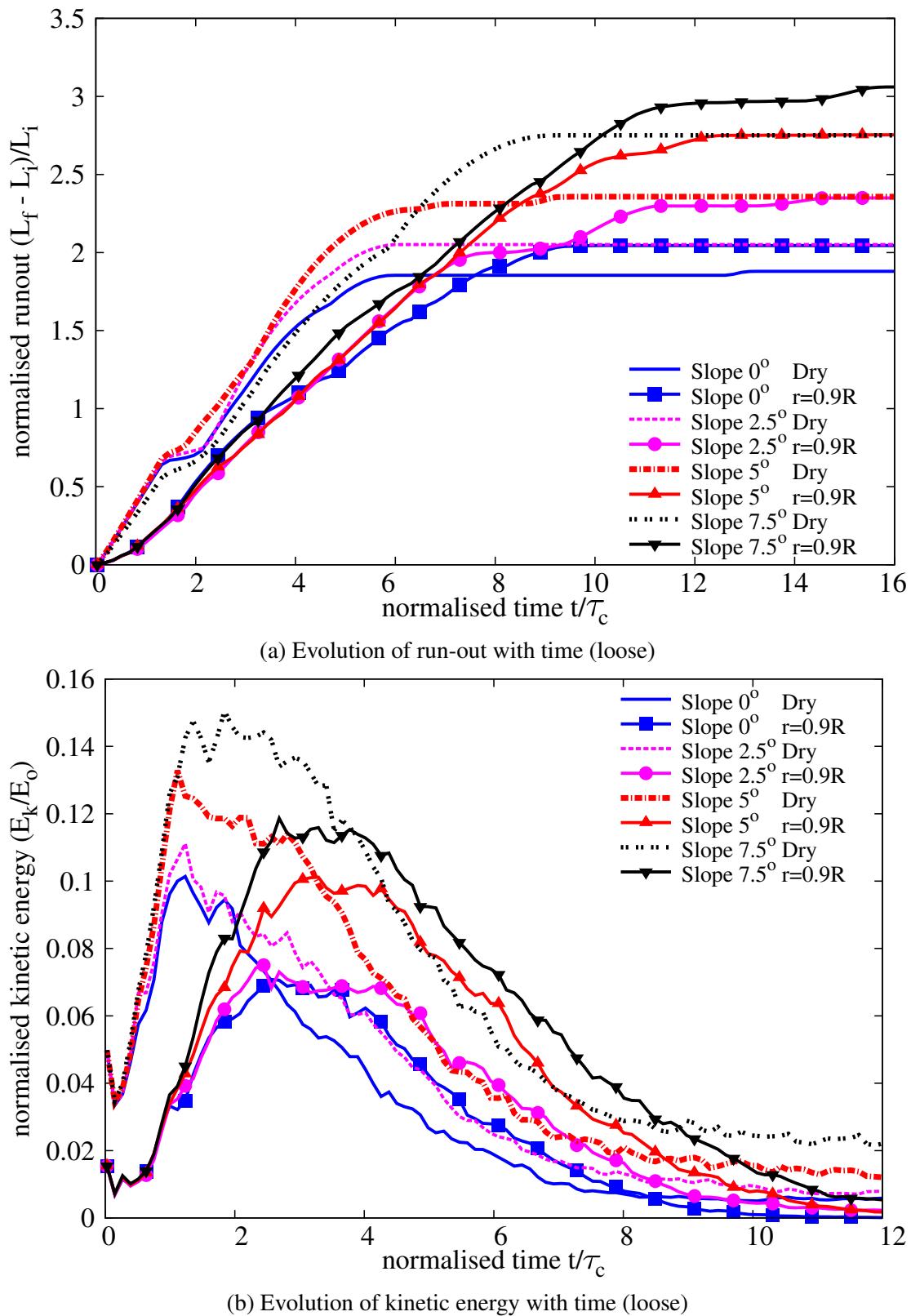


Figure 6.37 Evolution of run-out and kinetic energy with time (loose)

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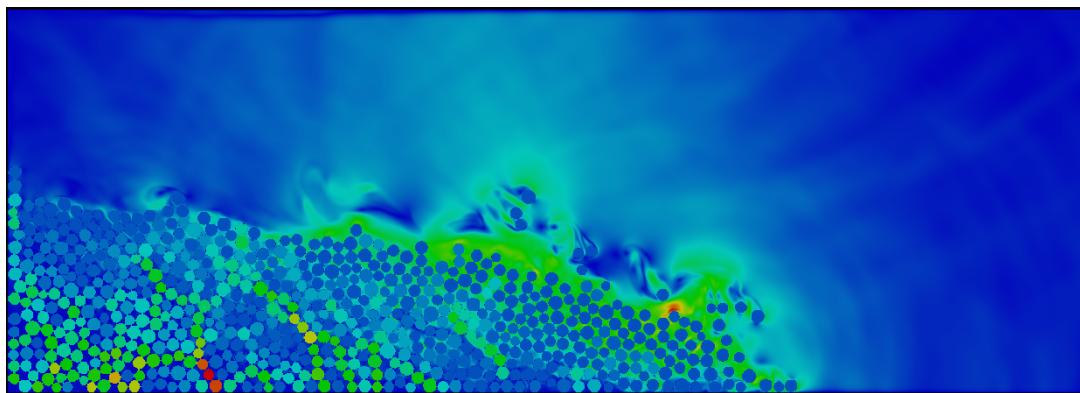
6.4 Submarine granular flows down incline plane

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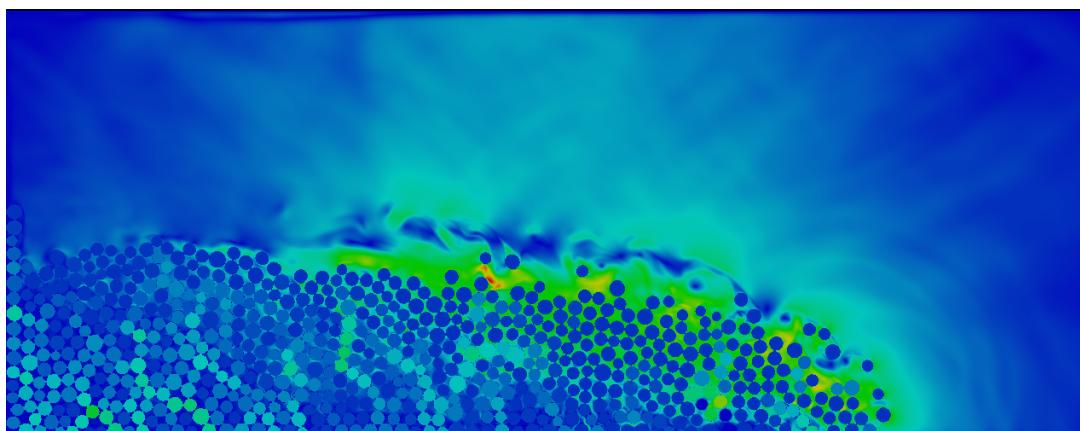
turbulence effect observed on the surface of the dense granular flow is absent in the loose granular collapse. This along with the lubrication effect result in longer run-out distance in the submerged condition for a loose granular column than the dry collapse.

The evolution of packing density (see Figure 6.39) shows that, at the end of the flow, both dense and the loose conditions reach similar packing density. This indicates that the dense granular column dilates more and is susceptible to higher viscous drag forces. Whereas in the loose condition, a positive pore-pressure is observed at the base of the flow, indicating entrainment of water at the base, i.e. lubrication and drop in the effective stress resulting in longer run-out distance. The amount of water entrained in the loose granular column is higher than the dense condition, this can be observed by the low packing fraction observed between  $2\tau_c$  and  $5\tau_c$ .

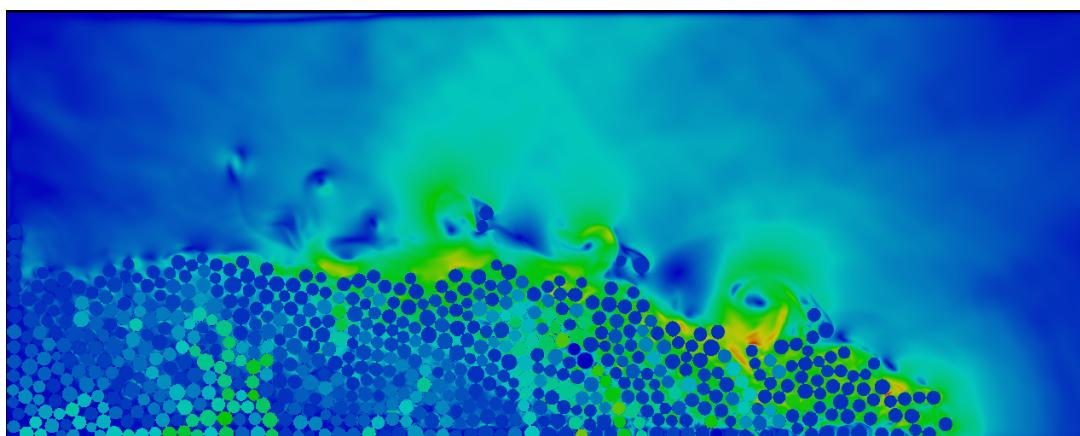
Figure 6.40a shows the evolution of run-out with slope angle for an initially dense granular column. With increase in slope angle, the run-out increases in both dry and submerged conditions. For all slope angles, the run-out in the dry condition is higher than the submerged conditions. With increase in the slope angle, the drag force experienced by the dense granular column predominates the run-out behaviour over the lubrication effect, this results in increase in the difference between the dry and the submerged conditions with increase in the slope angle. Whereas with increase in slope angle, the loose granular column flows longer than the dry conditions. The longer run-out in the loose granular column collapse is due to hydroplaning experienced at the flow front as a result of entrainment of water. Figure 6.41 shows that for a given initial aspect ratio and slope angle, the run-out distance in the loose granular collapse in fluid is higher than the dense condition. This observation in fluid is in contrast to the dry condition, where the dense granular column flows longer due to higher initial potential energy.  
The low permeability observed in the loose granular flow ensures that water entrained at the base of the flow front is retained resulting in sustained lubrication effect. Also, the low permeability ensures that the density of the flowing mass remains in a slurry state resulting in longer duration of hydroplaning. These effects in the loose granular column with low permeability condition result in longer run-out distance.



(a) Slope 2.5



(b) Slope 5.0



(c) Slope 7.5

Figure 6.38 Flow morphology at time  $t = 3\tau_c$  for different slope angles (loose)

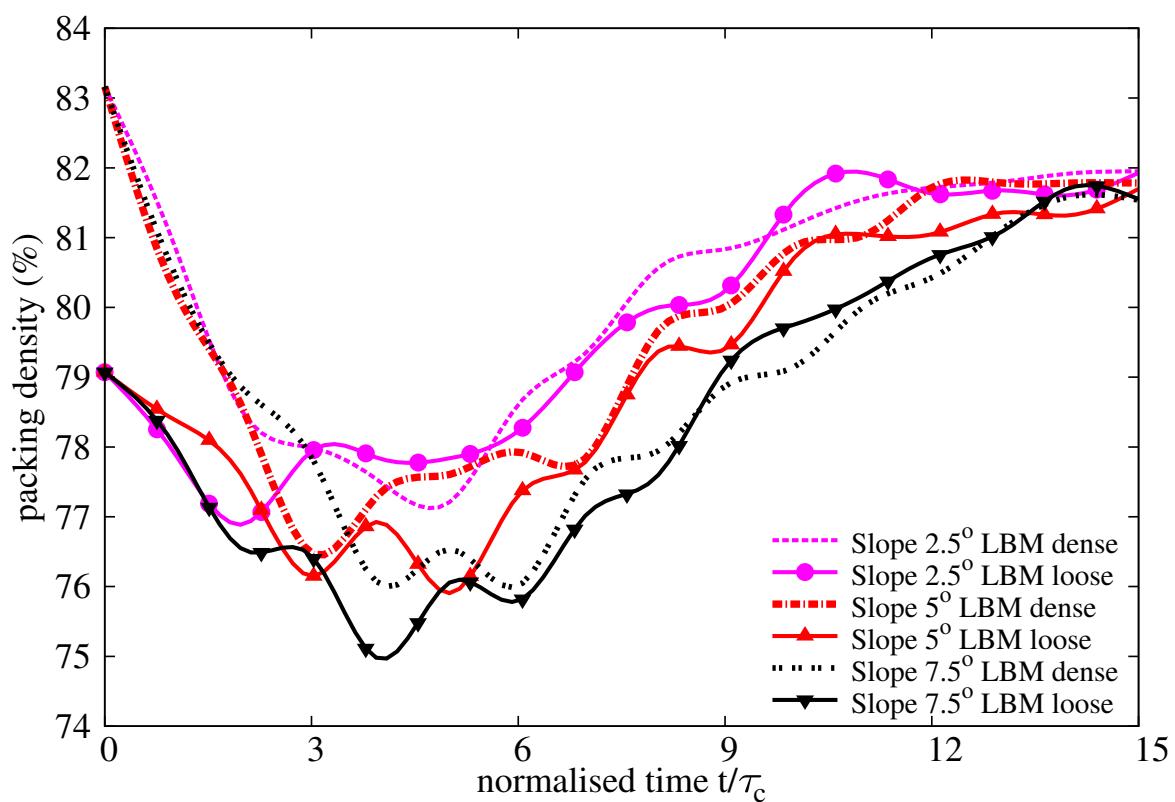
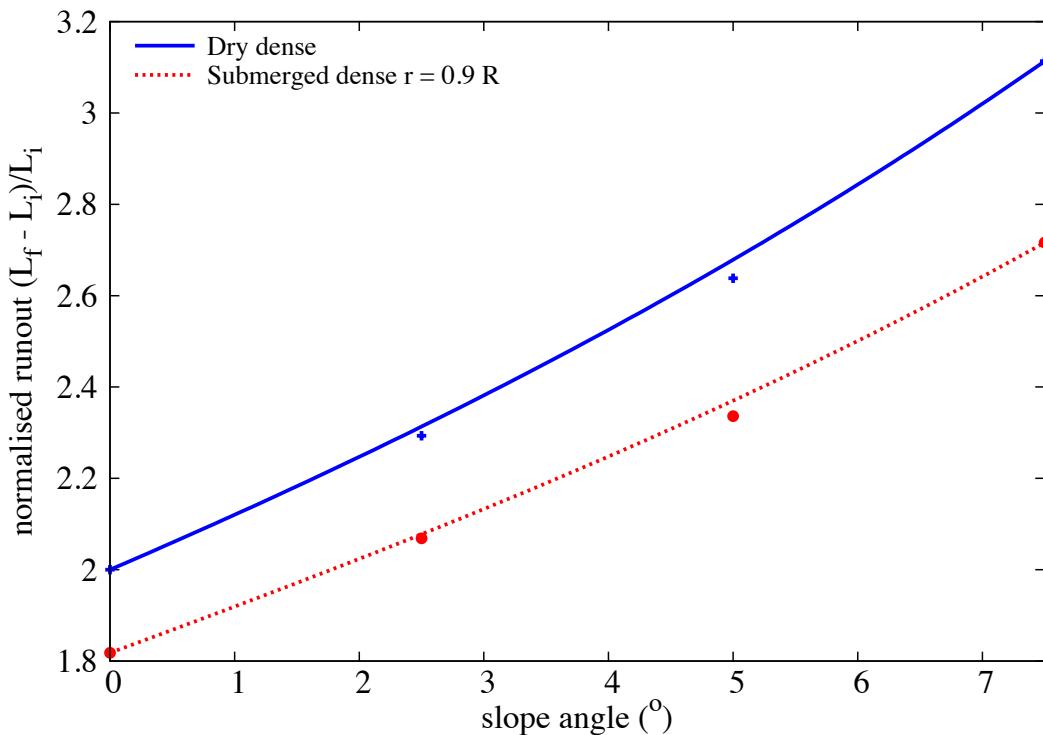
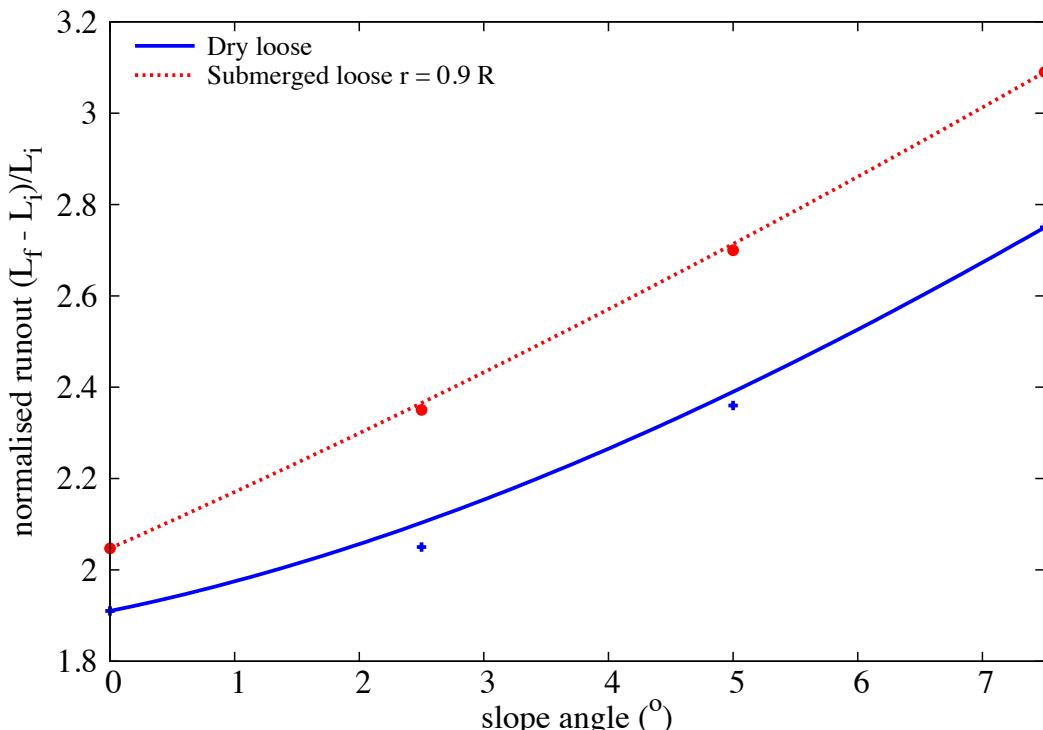


Figure 6.39 Evolution of packing density with time



(a) Dense



(b) Loose

Figure 6.40 Effect of slope angle on the run-out distance (Dense and Loose). Comparison between dry and submerged granular column.

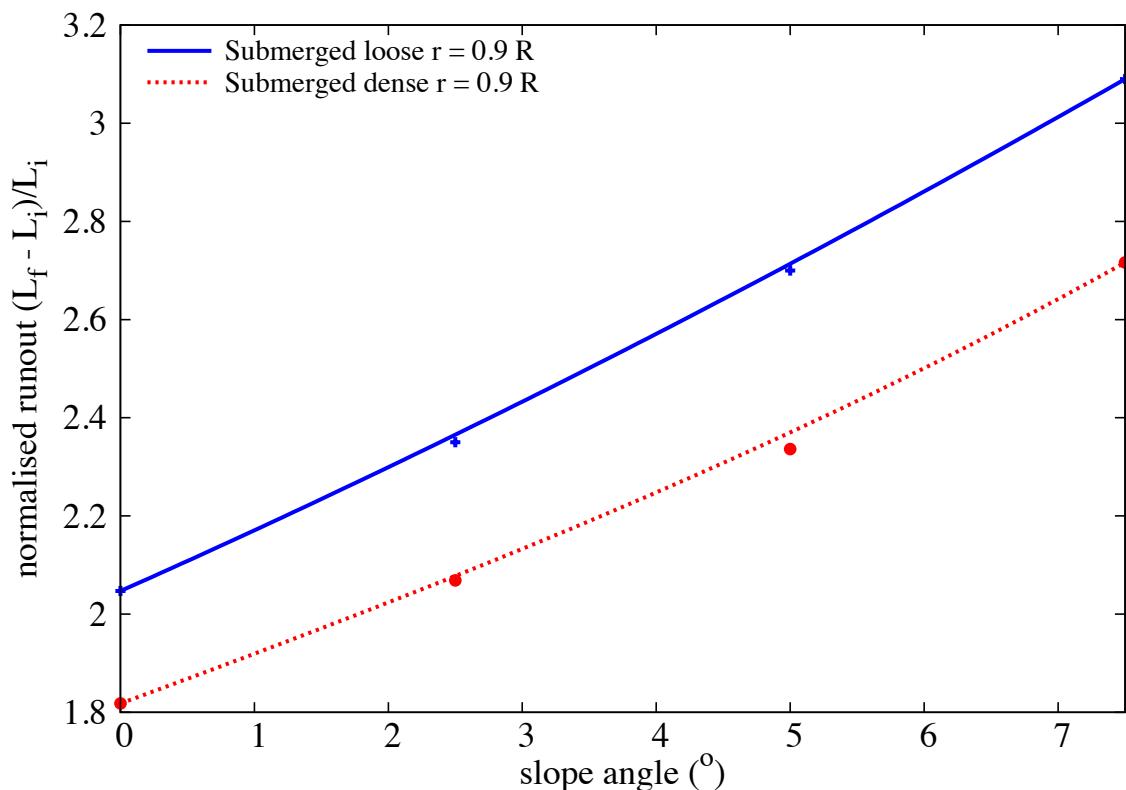


Figure 6.41 Effect of slope angle on the run-out behaviour for different initial packing density.

### 7 6.4.2 Effect of permeability

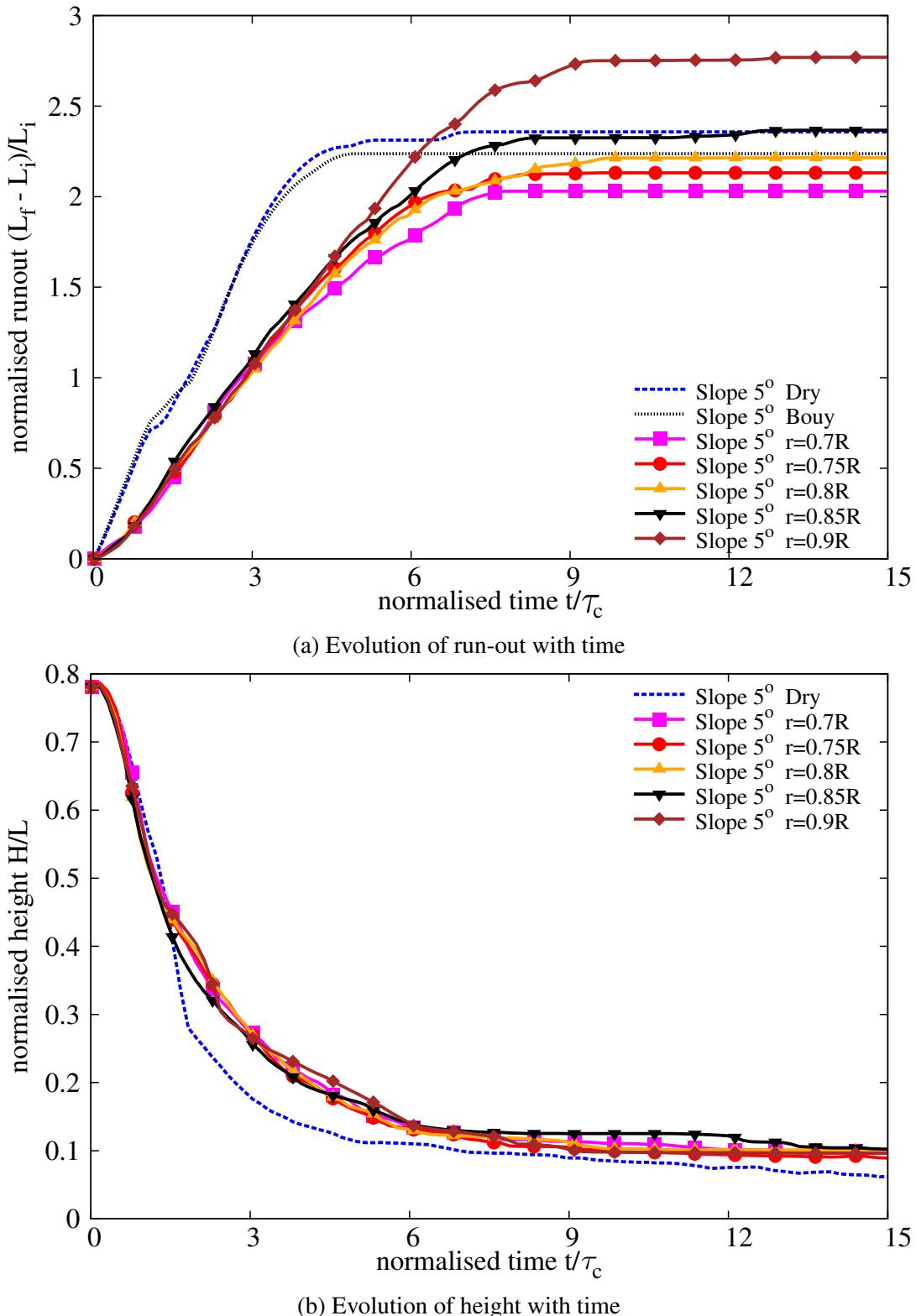
8 In order to understand the effect of permeability at a slope angle of 5°, the collapse of a  
9 granular column with an initial aspect ratio of 0.8 is simulated with different permeabilities.  
10 The hydrodynamic radius of a loosely packed granular column is varied from  $r = 0.7 R$  (high  
11 permeability), 0.75 R, 0.8 R, 0.85 R to 0.9 R (low permeability). The run-out distance is found  
12 to increase with decrease in the permeability of the granular assembly (see Figure 6.42a). The  
13 run-out distance for high permeable conditions ( $r = 0.7 R - 0.8 R$ ) are lower than their dry  
14 counterparts. Although, decrease in permeability resulted in an increase in the run-out distance,  
15 no significant change in the run-out behaviour is observed for a hydrodynamic radius of up to  
16 0.8 R.

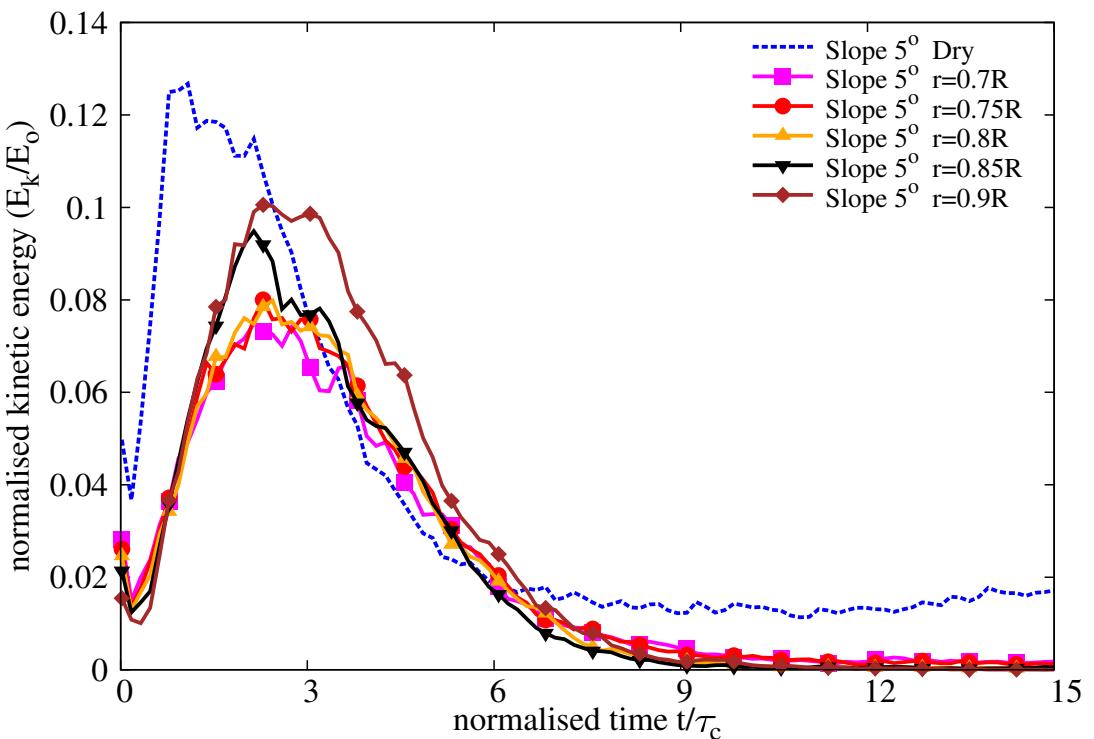
17 With further decrease in permeability ( $r = 0.85 R$  and 0.9 R), the run-out distance in the  
18 fluid is greater than the run-out observed in the dry condition. At a very low permeability ( $r =$   
19 0.9 R), the flowing granular mass entrains more water at the base, which causes a reduction in  
20 the effective stress accompanied by a lubrication effect on the flowing granular media. This  
21 can be seen as a significant increase in the peak kinetic energy and the duration of the peak  
22 energy, in comparison to dry and high permeable conditions (see Figure 6.43a). However, the  
23 permeability of the granular column did not have an influence on the evolution of height during  
24 the flow. But, the dry granular column tends to collapse more than the immersed granular  
25 column due to lack of viscous dissipation (see Figure 6.42b).

26 Positive pore-pressure generation at the base of the flow is observed for low permeable con-  
27 ditions. Inspection of the local packing density showed entrainment of water at the base of the  
28 flow, which can also be observed by the steep decrease in the packing density (see Figure 6.43b)  
29 for the very low permeability condition ( $r = 0.9R$ ). At the end of the flow ( $t \geq 10 \times \tau_c$ ), the  
30 excess pore-pressure dissipates and the granular flows, irrespective of their permeability, reach  
31 almost the same packing density.

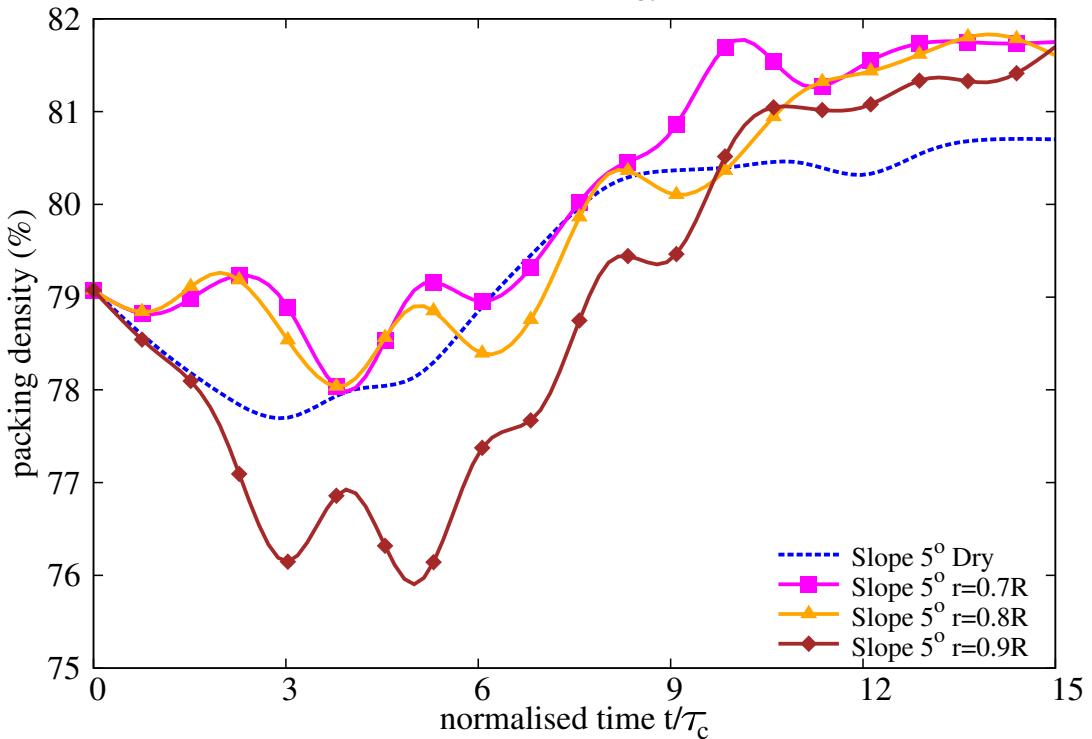
32 Figure 6.45 shows the effect of permeability on the run-out behaviour for a dense and a  
33 loose granular column collapse on a slope of 5° and 0°. In both cases, the run-out distance  
34 increases with increase in the hydrodynamic radius (decrease in permeability). However in  
35 the dense case, the run-out distance observed in the fluid is shorter than the dry condition.  
36 Whereas in the loose condition, the run-out distance increases significantly at low permeability  
1 and results in longer run-out distance in the submerged condition in comparison with the dry  
2 granular collapse. The comparison of loose and dense collapse on a slope of 0° and 5° shows  
3 that density plays a significant role in the case of collapse on a horizontal plane, however at a  
slope of 5°, the run-out distance is unaffected by the initial packing density at high permeability  
conditions. This shows that at high permeability condition, the viscous drag forces predominate  
resulting in almost the same run-out distance for both dense and loose condition. However at  
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## 6.4 Submarine granular flows down incline plane

Figure 6.42 Evolution of run-out and height with time for different permeability (loose slope  $5^\circ$ )



(a) Evolution of kinetic energy with time



(b) Evolution of packing density with time

Figure 6.43 Evolution of kinetic energy and packing density with time for different permeability (loose slope 5°)

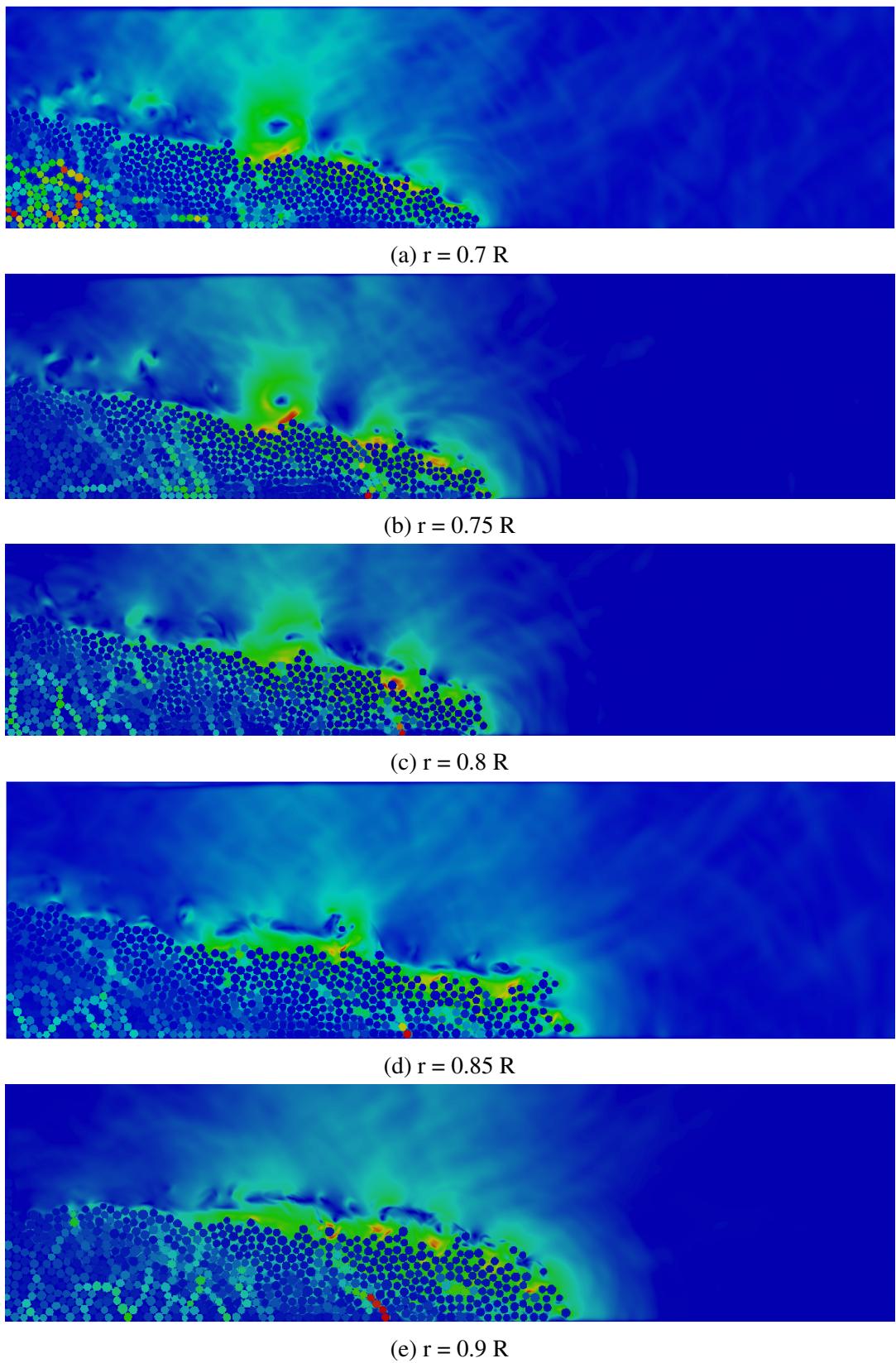


Figure 6.44 Evolution of the flow front at  $t = 3\tau_c$  for different permeabilities (loose slope  $5^\circ$ ).

low permeability ( $r = 0.9 R$ ), hydroplaning is observed in the case of loose granular column resulting in substantially longer run-out distance than the dense granular column in submerged condition.

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## 6.4 Submarine granular flows down incline plane

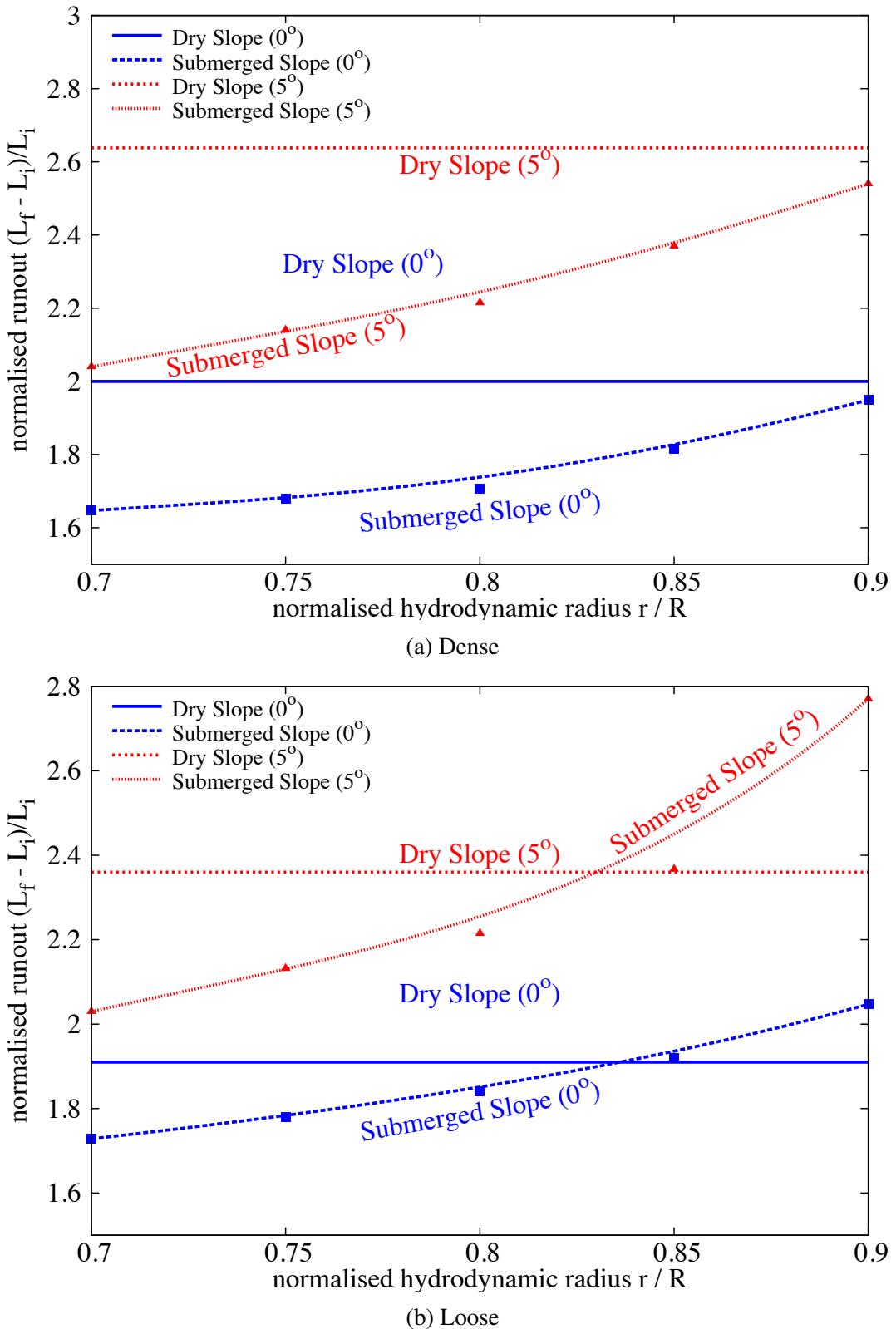


Figure 6.45 Effect of permeability on the run-out distance (Dense and Loose). Comparison between dry and submerged granular column for a slope angle of  $0^\circ$  and  $5^\circ$ .

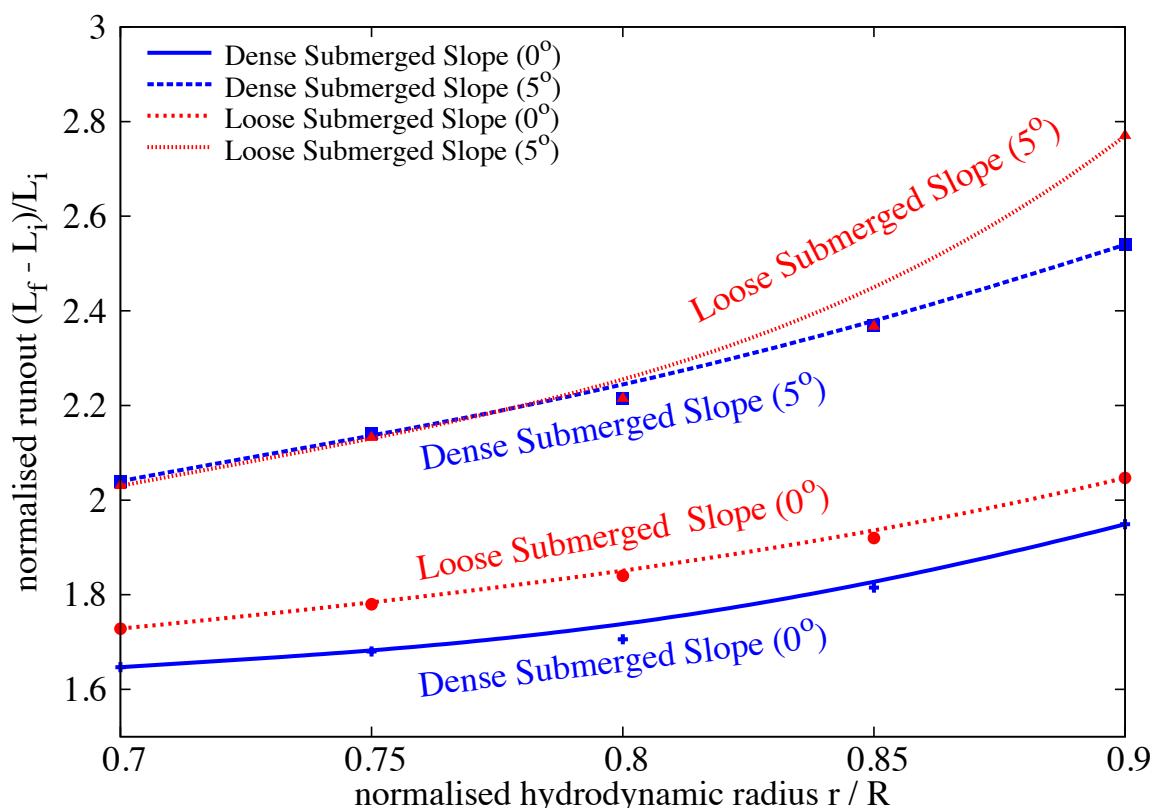


Figure 6.46 Effect of permeability on the run-out behaviour for different slope angle and the initial packing density.

## 6.5 Tall columns

In contrast to the collapse of short columns in fluid, the amount of material destabilised and in turn the surface area of the mobilised mass that interacts with the surround fluid increases. This increased interaction of granular mass with fluid results in formation of turbulent vortices that alters the deposit morphology during the collapse. It was observed (see section 6.3.2) that vortices result in formation of heaps, this significantly affects the distribution of mass in the flow. Staron and Hinch (2007) observed that the distribution of the mass in the granular flow significantly affects the flow kinematics. In order to understand the behaviour of tall columns, the run-out behaviour of a dense granular column with an initial aspect ratio of 6 is studied. The collapse of a tall granular column on slopes of 0°, 2.5°, 5° and 7.5° are studied. A hydrodynamic radius  $r = 0.85 R$  is adopted. Unnatural permeability conditions were observed at higher hydrodynamic radii.

The snapshots of the collapse of an aspect ratio 6 column on a horizontal surface are shown in figure 6.47. The initial stage of collapse is characterised by free-fall of grains above the failure surface. As the grains experience free-fall due to gravity, they interact with the surrounding fluid experiencing drag force. This results in a significant drop in the kinetic energy available for the flow. As the grains reach the static region, they interact with the neighbouring grains and the energy gained during the free fall is converted horizontal acceleration. Only during this stage ( $t = 3\tau_c$ ) the interactions between the soil grains on the flow surface with the fluid result in formation of eddies. The number of eddies formed during the flow is proportional to the surface area interacting with the fluid. Hydroplaning can be observed at the flow front ( $t = 3\tau_c$ ). Two large vortices with almost the same size can be observed at the final stage of collapse. The soil grains on the surface experience suction due to formation of eddies and this results in formation of heaps of granular mass in front of each vortex. The formation of heaps, although is evident, doesn't significantly affect the distribution of mass in the case of collapse on a horizontal plane.

The snapshots of a collapse of a granular column ( $a = 6$ ) on a inclined plane at angle of 5° are shown in figure 6.48. Similar behaviour in the flow evolution is observed for the collapse on a slope of 5°. The vortices are formed only during the horizontal spreading stage  $t = 3\tau_c$ , but the number of vortices formed during the collapse is higher than the collapse on a horizontal plane. However, as the flow progresses a single large vortex engulfs other smaller vortices, thus having a significant influence on the mass distribution. figure 6.49 shows the distribution of mass and the packing density at  $t = 6\tau_c$  and  $t = 8\tau_c$ . A heap can be observed in front of the large vortex almost at the middle of the flow. The height of the heap is higher than the collapse height next to the wall. However, when the flow comes to rest and the vortex moves away from

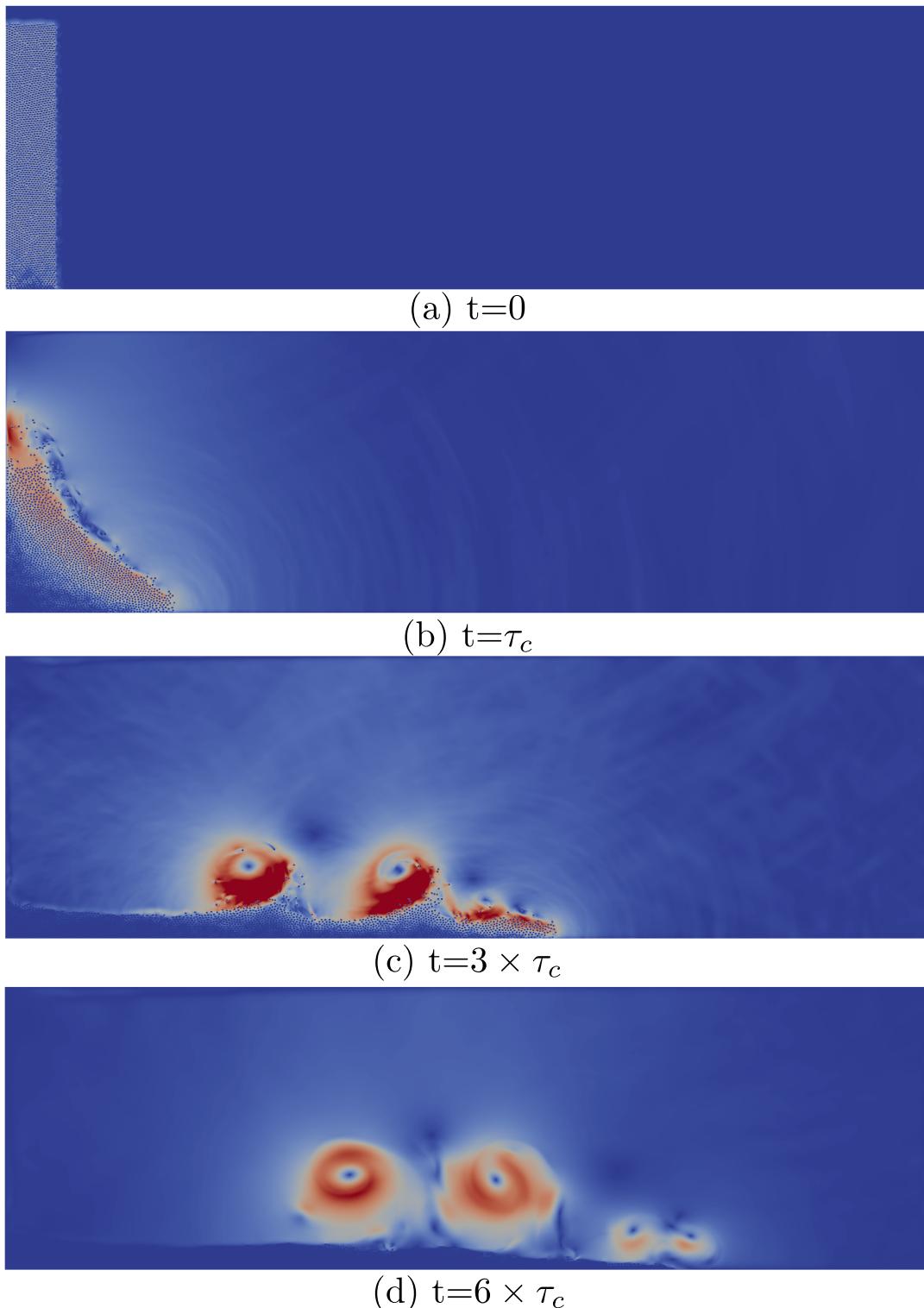


Figure 6.47 Flow evolution of a granular column collapse in fluid ( $a = 6$ ) on a horizontal surface

the flowing surface, the mass present in the heap gets redistributed (as seen in  $t = 8\tau_c$ ). This behaviour is significantly different from that observed in the case of short columns.

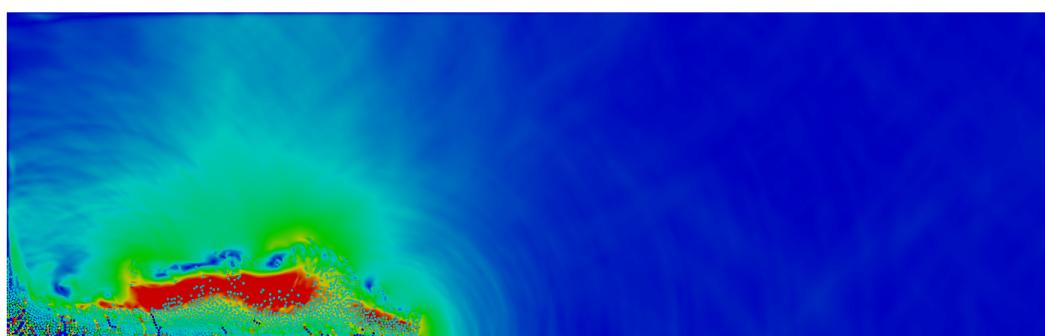
In order to understand the influence of slope angles on the run-out behaviour, the collapse of a granular column with an initial aspect ratio of 6 is performed on slopes of 0, 2.5°, 5° and 7.5°. The run-out evolution with time for different slope angles are presented in figure 6.50a. The run-out distance increases with increase in the slope angle, however the run-out distance in the fluid is significantly shorter than the dry condition. The slow evolution of run-out in the submerged condition is due to the delay in the dissipation of the large negative pore-pressure developed during the initial stage of the collapse. The formation of eddies during the flow indicates that most of the potential energy gained during the free-fall is dissipated through viscous drag and formation of eddies. This effect predominates the hydroplaning observed during the flow resulting in shorter run-out distance in the case of fluid. The evolution of height with time indicates that the amount of material destabilised is much smaller due to the drag force experienced by the grains (see figure 6.50b).

The amount of kinetic energy available for the flow in the submerged condition is almost half that of the dry condition (see figure 6.51a). It can be see from figure 6.52b that the vertical kinetic energy is dissipate over a longer duration, in contrast to the free-fall release observed in the dry condition. The slower dissipation is attributed to the viscous drag force experienced by the grains and through formation of eddies.

The behaviour of tall columns are significantly different from that observed in the case of short columns. The slope angle has a strong influence on the number and size of eddies during the flow. The eddies interact with the surface of the granular flow and forms heaps in front of each vortex. This significantly affects the mass distribution and in turn the run-out evolution. Although, tall cliffs are quite rare in submarine condition in comparison to short cliffs or slopes, further research is required to understand the influence of permeability and packing density on the run-out evolution of tall columns.

## 6.6 Summary

Two-dimensional LB-DEM simulations are performed to understand the behaviour of submarine granular flows. Unlike dry granular collapse, the run-out behaviour in fluid is dictated by the initial volume fraction. Granular columns with loose packing and low permeability tend to flow longer in comparison to dense columns, due to entrainment of water at the base resulting in lubrication. In both dense and loose conditions, the run-out distance increases with decrease in the permeability. With decrease in permeability, the duration required for the flow to initiate takes longer due to development of large negative pore-pressure. However, the low permeability

 $t = 0\tau_c$  $t = 1\tau_c$  $t = 3\tau_c$

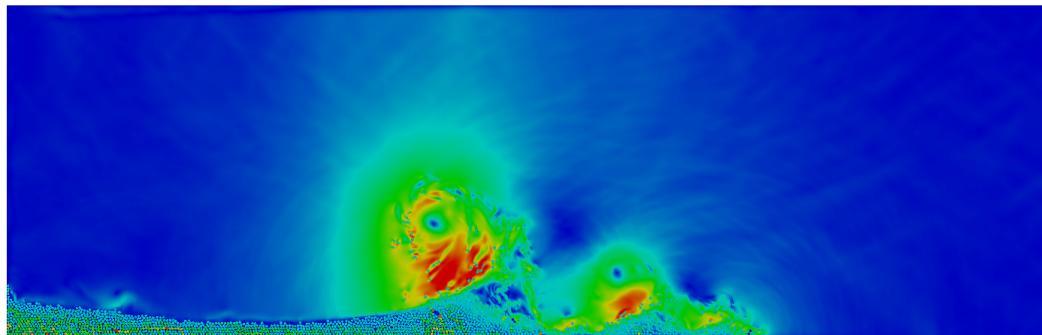
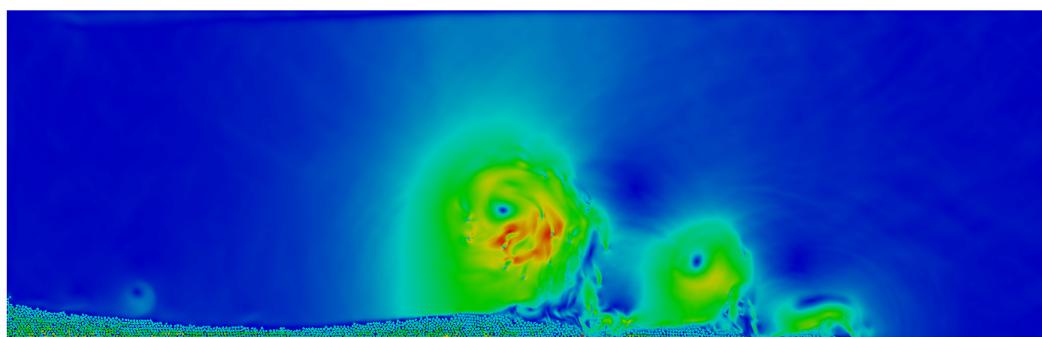
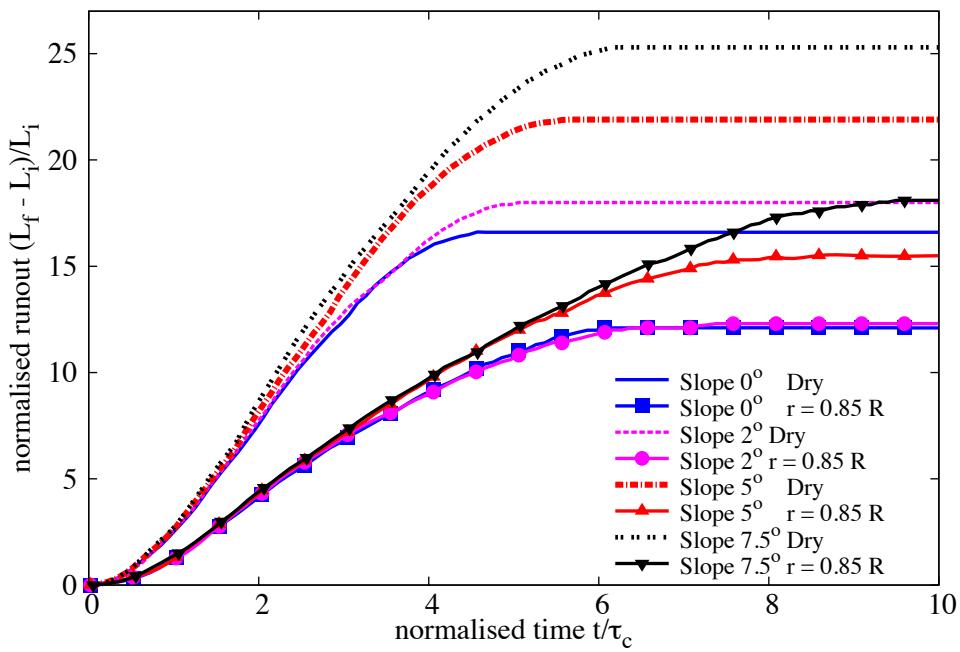
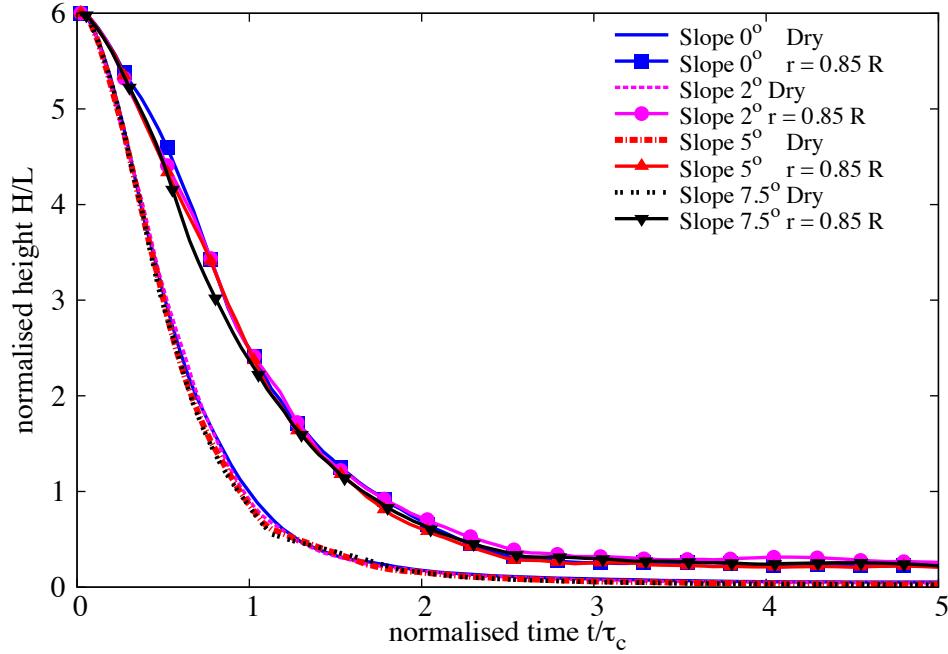
 $t = 6\tau_c$  $t = 8\tau_c$ 

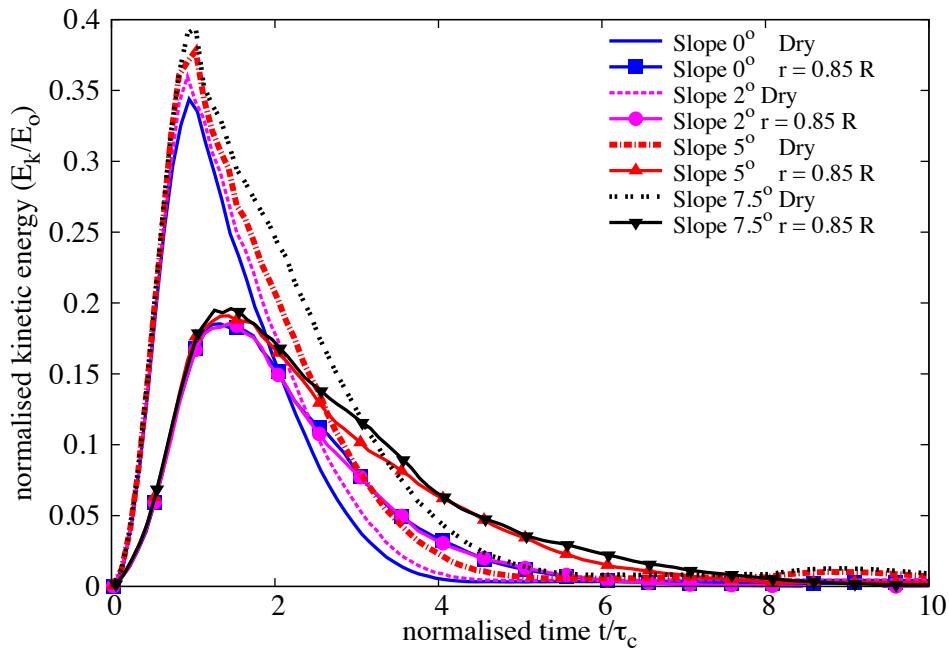
Figure 6.48 Flow evolution of a granular column collapse in fluid ( $a = 6$ ) on a slope of  $5^\circ$ . Shows the velocity profile of fluid due to interaction with the grains (red - higher velocity).

 $t = 6\tau_c$  $t = 8\tau_c$ 

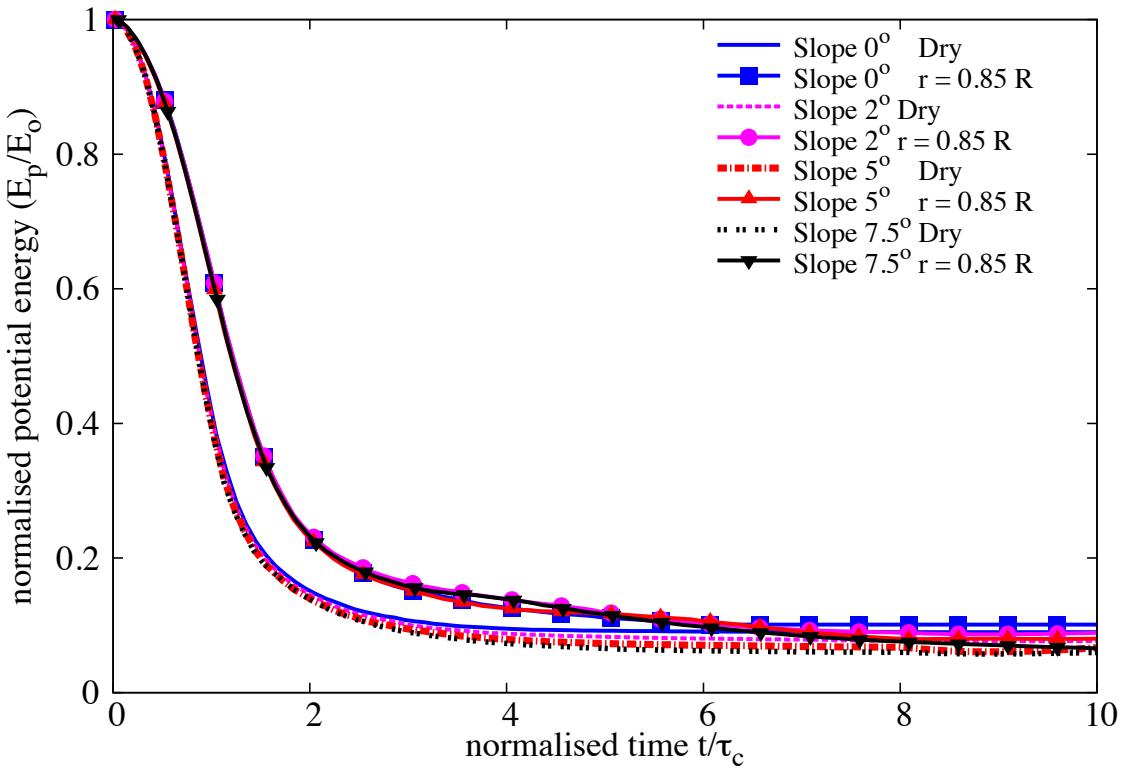
Figure 6.49 Packing density of a granular column collapse in fluid ( $a = 6$ ) on a slope of  $5^\circ$ .

(a) Evolution of run-out for a column collapse in fluid ( $a = 6$ ) on a slope of  $5^\circ$ (b) Evolution of height with time for a column collapse in fluid ( $a = 6$ ) on a slope of  $5^\circ$ Figure 6.50 Evolution of run-out and height for a column collapse in fluid ( $a = 6$ ) on a slope of  $5^\circ$

## 6.6 Summary

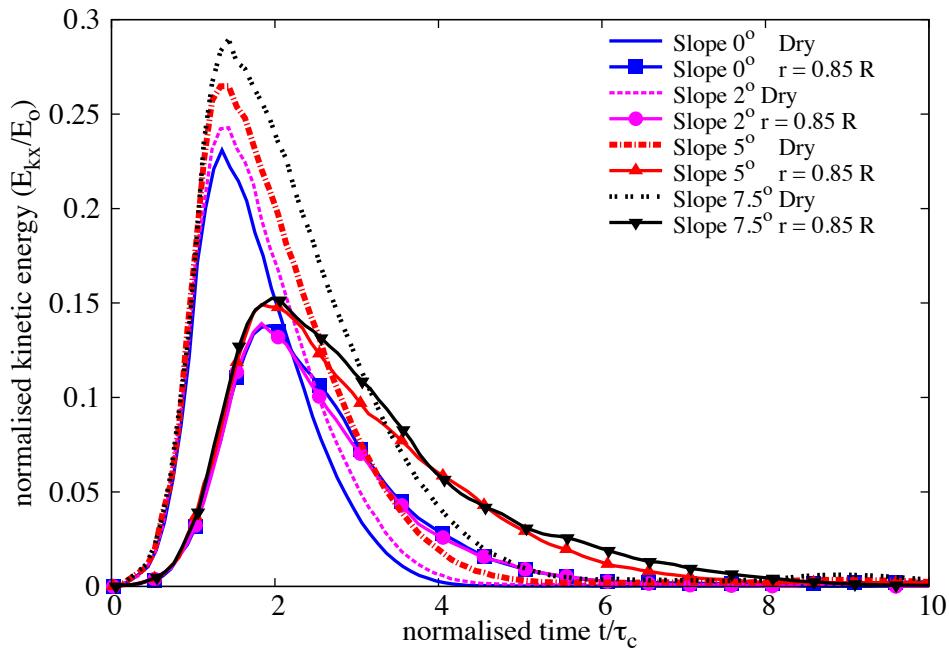


(a) Evolution of the total kinetic energy

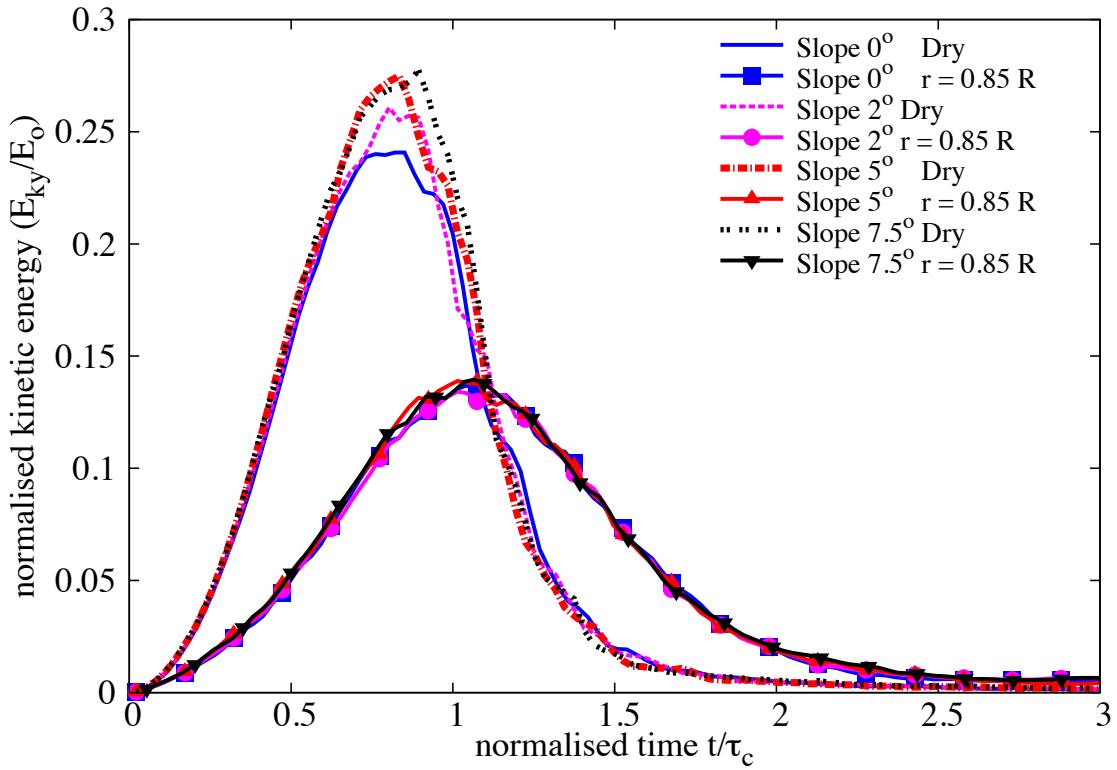


(b) Evolution of the total potential energy

Figure 6.51 Evolution of the kinetic and the potential energy with time for a granular column collapse in fluid (a = 6) on a slope of  $5^\circ$



(a) Evolution of the horizontal kinetic energy



(b) Evolution of the vertical kinetic energy

Figure 6.52 Evolution of the kinetic energies with time for a granular column collapse in fluid ( $a = 6$ ) on a slope of  $5^\circ$

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**6.6 Summary****65**

of the granular mass results in entrainment of water resulting in hydroplaning. For the same thickness and velocity of the flow, the potential of hydroplaning is influenced by the density of the flowing mass. Loose column has more potential of hydroplaning than the dense granular mass. The loose column entrains more water at the flow front, leading to a partial fluidization of the material. Thus resulting in longer run-out distance than the dry condition. However, with increase in the slope angle, the run-out in fluid is influenced by the viscous drag on the granular materials.

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