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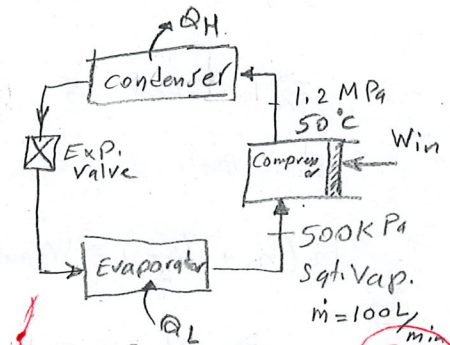
- 1- An air-conditioner with refrigerant-134a as the working fluid is used to keep a room at 26°C by rejecting the waste heat to the outdoor air at 34°C. The room gains heat through the walls and the windows at a rate of 250 kJ/min while the heat generated by the computer, TV, and lights amounts to 900 W. The refrigerant enters the compressor at 500 kPa as a saturated vapor at a rate of 100 L/min and leaves at 1200 kPa and 50°C. Determine:
- the actual COP,
 - the maximum COP, and
 - the minimum volume flow rate of the refrigerant at the compressor inlet for the same compressor inlet and exit conditions. (Score 50) (7-113)

Given: R134-a, $T = 26^\circ\text{C} = 299\text{K}$,

$$\dot{Q} = 250 \frac{\text{kJ}}{\text{min}}, \dot{Q}_{\text{equipment}} = 0.9 \text{ kW}, \dot{m}_{\text{in}} = 100 \text{ L/min}$$

(a) Table A-12 \Rightarrow for $P_1 = 500 \text{ kPa} \Rightarrow \begin{cases} h_g = 259.30 \text{ kJ/kg} \\ v_g = 0.041118 \text{ m}^3/\text{kg} \end{cases}$
 $x_1 = 1$

Table A-13 for $\begin{cases} P_2 = 1.2 \text{ MPa} \\ T_2 = 50^\circ\text{C} \end{cases} \Rightarrow h_2 = 278.27 \text{ kJ/kg}$



mass flow rate for refrigerant $\Rightarrow \dot{m}_R = \frac{\dot{V}_1}{v_1} = \frac{(100 \text{ L/min}) \left(\frac{1 \text{ m}^3}{1000 \text{ L}} \right) \left(\frac{1 \text{ min}}{60 \text{ s}} \right)}{0.041118 \frac{\text{m}^3}{\text{kg}}} = 0.04053 \frac{\text{kg}}{\text{s}}$

Power consumption of the compressor: $\dot{W}_{\text{in}} = \dot{m}_R (h_2 - h_1) = (0.04053) (278.27 - 259.30) = 0.76885 \text{ kW}$

The heat gains to the room must be rejected by the air-conditioner.

So $\Rightarrow \dot{Q}_L = \dot{Q}_{\text{heat}} + \dot{Q}_{\text{equipment}} = (250 \frac{\text{kJ}}{\text{min}}) \left(\frac{1 \text{ min}}{60 \text{ sec}} \right) + 0.9 \text{ kW} = 5.0667 \text{ kW}$

The actual COP $\Rightarrow \text{COP} = \frac{\dot{Q}_L}{\dot{W}_{\text{in}}} = \frac{5.0667}{0.76885 \text{ kW}} = 6.5899 \approx 6.59$

(b) COP of a reversible Refr. operating between the same temp:

$\text{COP}_{\text{max}} = \frac{1}{\frac{T_H}{T_L} - 1} = \frac{1}{\left(\frac{34+273}{26+273} \right) - 1} = 37.375$

(c) The minimum power input to the comp. for the same refrigeration load is:

$\dot{W}_{\text{in, min}} = \frac{\dot{Q}_L}{\text{COP}_{\text{max}}} = \frac{5.0667}{37.375} = 0.13556 \text{ kW}$

Min mass flow rate is: $\dot{m}_{R, \text{min}} = \frac{\dot{W}_{\text{in, min}}}{h_2 - h_1} = \frac{0.13556}{(278.27 - 259.30)} = 0.007146 \frac{\text{kg}}{\text{s}}$

Min flow rate: $\dot{V}_{\text{min}} = \dot{m}_{R, \text{min}} v_g = (0.007146 \text{ kg/s}) (0.041118 \frac{\text{m}^3}{\text{kg}}) = 0.000294 \frac{\text{m}^3}{\text{s}}$

(See back of the page)

$\dot{V}_{\text{min}} = 17.6298 \frac{\text{L}}{\text{min}} \approx 17.63 \frac{\text{L}}{\text{min}}$

- 2- Steam enters an adiabatic turbine at 7 MPa, 600°C, and 80 m/s and leaves at 50 kPa, 150°C, and 140 m/s. If the power output of the turbine is 6 MW, determine:
 (a) the mass flow rate of the steam flowing through the turbine and,
 (b) the isentropic efficiency of the turbine. (Score 50) (8-132)

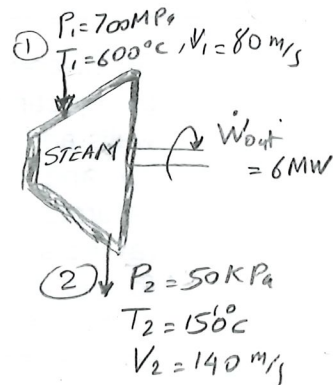
Given: Fig with data indicated

Find: \dot{m} & η_T , Assumption: Steady, No PE,

(a) From table A-6 $\left\{ \begin{array}{l} P_1 = 7 \text{ MPa} \\ T_1 = 600^\circ\text{C} \end{array} \right. \Rightarrow \begin{array}{l} h_1 = 3650.6 \text{ kJ/kg} \\ s_1 = 7.0910 \text{ kJ/kg} \end{array}$

Again table A-6 $\left\{ \begin{array}{l} P_2 = 50 \text{ kPa} = 0.05 \text{ MPa} \\ T_2 = 150^\circ\text{C} \end{array} \right. \Rightarrow h_2 = 2780.2 \text{ kJ/kg}$

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$\Rightarrow 1 \text{ inlet \& 1 outlet} \Rightarrow \dot{m}_1 = \dot{m}_2 = \dot{m}$

En. Bal. $\Rightarrow \dot{E}_{in} - \dot{E}_{out} = \Delta \dot{E}_{sys} = 0$ Since Steady. $\Rightarrow \dot{E}_{in} = \dot{E}_{out}$

$\dot{m} \left(h_1 + \frac{V_1^2}{2} \right) = \dot{W}_{out} + \dot{m} \left(h_2 + \frac{V_2^2}{2} \right)$ $\Delta P_E = 0 = \dot{Q} \rightarrow \text{adiab.}$

$\Rightarrow -\dot{W}_{out} = \dot{m} \left(h_2 + \frac{V_2^2}{2} - h_1 - \frac{V_1^2}{2} \right) = \dot{m} \left(h_2 - h_1 + \frac{V_2^2 - V_1^2}{2} \right)$
 $-6000 \frac{\text{kJ}}{\text{s}} = \dot{m} \left(2780.2 - 3650.6 + \frac{(140 \frac{\text{m}}{\text{s}})^2 - (80 \frac{\text{m}}{\text{s}})^2}{2} \times \frac{1 \text{ kJ/kg}}{1000 \text{ m}^2/\text{s}^2} \right)$

$\Rightarrow \dot{m} = 6.944 \text{ kg/s}$

Ans.

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- b) The isentropic exit enthalpy & the power output of the isentropic turbine are:

$\left. \begin{array}{l} P_{2s} = 50 \text{ kPa} \\ s_{2s} = s_1 \end{array} \right\} \Rightarrow x_{2s} = \frac{s_{2s} - s_f}{s_{fg}} = \frac{7.0910 - 1.0912}{6.5019} \xrightarrow{s_f \text{ @ } P_{2s} = 50 \text{ kPa}} \xrightarrow{s_{fg} \text{ @ } P_{2s} = 50 \text{ kPa}}$
 $\Rightarrow x_{2s} = 0.9228$

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$\Rightarrow h_{2s} = h_f + x_{2s} h_{fg} = 340.54 + (0.9228)(2304.7) = 2467.3 \text{ kJ/kg}$

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$\dot{W}_{sout} = -\dot{m} \left(h_{2s} - h_1 + \frac{V_2^2 - V_1^2}{2} \right) = -(6.95 \frac{\text{kg}}{\text{s}}) \left(2467.3 - 3650.9 + \frac{140^2 - 80^2}{2} \times \frac{1 \text{ kJ}}{1000 \text{ m}^2/\text{s}^2} \right)$

$= 8174 \text{ kW}$

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\Rightarrow Isentropic EFF of Turbine:

$\eta_T = \frac{\dot{W}_{actual}}{\dot{W}_s} = \frac{6000 \text{ kW}}{8174 \text{ kW}} = 0.734 = 73.4 \%$

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