

```
INTEGER JN(40.5), NN(40), JB(20), IFLOW(40), LP(8,20), JC(50)
REAL D(50), L(50), A(50.51), QJ(20), E(50), KP(50), V(2), Q(50),
      EXPP(50), AR(50), ARL(50)
```

Data type
Read in data

```
30 READ(5,110,END=99) NP, NJ, NL, MAX, NUNIT, ERR, VIS, DELQ1
110 FORMAT(515.3F10.5)
```

NN - number of nodes
JN - number of pipes at node
JB - unknown
INFLOW - consumption flow rate
LP - unknown
JC - to do with solution of linear equations

D - pipe diameter
L - pipe length
A - flow
QJ - unknown
E - initial absolute roughness
 converted to relative roughness

V - velocity
Q - flow in pipe

KP - Kp value for pipe

EXPP - n exponent in equation $h_f = K_p * Q^n$

AR - pipe x-sectional area

ARL - coefficient in equation $K_p = a * (L / (2 * g * D * A^2))$

Used in equations
2-15 to 2-18 Ref 1

```
# NP - NO. OF PIPES.
# NJ - NO. OF JUNCTIONS,
# NL - NO. OF LOOPS,
# MAX - NO. OF ITERATIONS ALLOWED,
# ERR - allowed error in calculated flows before accepting results
# VIS - kinematic viscosity
# DELQ1 - deviation used to calculate Q1 and Q2 from average Flow
# IF NUNIT=0 D AND E IN INCHES AND L IN FEET,
# IF NUNIT=1 D AND E IN FEET AND L IN FEET,
# IF NUNIT=2 D AND E IN METERS AND L IN METERS,
# IF NUNIT=3 D AND E IN CM AND L IN METERS.
```

```
100 FORMAT(1615)
    NPP = NP + 1
    NJI = NJ - 1
    READ(5,101) (D(I), I=1, NP)
    READ(5,101) (L(I), I=1, NP)
    READ(5,101) (E(I), I=1, NP)
101 FORMAT(8F10.5)
    DO 48 I=1, NP
48 E(I) = E(I) / D(I)
    IF(NUNIT-1) 40, 41, 42
40 WRITE(6,102) D(I), I=1, NP)
102 FORMAT('PIPE DIAMETERS (INCHES)'./(1H, 16F8.1))
    DO 43 I=1, NP
43 D(I) = D(I)/12
    GO TO 44
41 WRITE(6,112) (D(I), I=1, NP)
112 FORMAT('PIPE DIAMETERS (FEET)'./(1H, 16F8.3))
44 WRITE (6,103) L(I), I=1, NP)
103 FORMAT('LENGTH OF PIPE (FEET)'./(1H, 16F8.0))
```

The 100 series line numbers reference formatting only and are not addresses here.

Convert absolute roughness to relative roughness

Based on units selected, convert dia and length to feet or meter

```

      G2 = 64.4
      GO TO 50
42  IF (NUNIT .EQ. 2) GO TO 45
      DO 46 I=1, NP
46  D(I) = .01 * D(I)
45  WRITE(6.113) (D(I), I=1, NP)
113  FORMAT('PIPE DIAMETERS (METERS)',/, (1H.16.F8.4))
      WRITE(6.114) (L(I), I=1, NP)
114  FORMAT('LENGTH OF PIPE (METERS)',/, (1H, 16F8.0)
      G2=19.62
      WRITE(6.115) (E(I), I=1, NP)
115  FORMAT('RELATIVE ROUGHNESS OF PIPES',/, (1H, 16F8.6)

```

NOTE
Undefined

Length and dia
conversion cont'd

```

# INFLOW - IF 0 NO INFLOW,
      IF 1 THEN NEXT CARD GIVES MAGNITUDE IN GPM
      IF 2 NEXT CARD GIVES MAGNITUDE IN CFS
      IF 3 NEXT CARD GIVES MAGNITUDE IN CMS.
# NNJ - NO. OF PIPES AT JUNCTIONS POSITIVE FOR INFLOW
      NEGATIVE FOR OUTFLOW.
# JN - THE NUMBER OF PIPES AT JUNCTION,
      IF FLOW ENTERS MINUS
      IF FLOW LEAVES THE PIPE NUMBER IS POSITIVE.

```

Variables for nodes

```

      DO 70 I=1, NP
      AR(I) = .78539392 * D(I)**2
70  ARL(I) = L(I) / (G2*D(I) * AR(I)**2)
      II = I
      DO 1 I=1, NJ
      READ(5,100) IFLOW(I), NNJ, (JN(I,J), J=1, NNJ)
      NN(I)=NNJ
      IF(IFLOW(I)-1) 1,2,3
2  READ(5,101) QJ(II)
      QJ(II) = QJ(II)/449.
      JB(II)=1
      GO TO 4
3  READ(5, 101) QJ(II)
      BJ(II) = 1
4  II = II + 1
1  CONTINUE

```

Pipe x-sect area

Coefficient for Kp - equation 2-28 Ref 1

Determine the coefficient for the
variables in the node equation
same as:

Calc_Network.py.node_matrix

```

# NUMBER OF PIPES IN EACH LOOP (SIGN INCLUDED)
      DO 35 I=1, NL
      READ(5,100) NNJ, (LP(J,I), J=1 ,NNJ)
35  LP(8,I)=NNJ
      DO 5 I=1, NP
      IF(NUNIT .GT. 1) GO TO 66
      KP(I)=.0009517 * L(I) / D(I)**4.87
      GO TO 5
66  KP(I) = .00212 * L(I) / D(I)**4.87
5  CONTINUE
      ELOG = 9.35 * ALOG10(2.71828183)
      SUM=100
      NCT=0

```

Calculate initial Kp based on
Chw = 100 - equation 2-22
Ref 1

Set constants to be used further
on in iteration loop.

```

20  II = 1
      DO 6 I=1, NJI
      DO 7 J=1, NP
7  A(I,J) = 0
      NNJ = NN(I)

```

MAIN LOOP

Calculation of the energy
equations for closed loops and
pseudo loops same as
Calc_Network.py loop_matrix and
pseudo_matrix

Calculation of the energy equations cont'd

```

DO 8 J=1, NNJ
IJ = JN(I,J)
IF(IJ .GT. 0) GO TO 9
IIJ = ABS(IJ)
A(I,IIJ) = -1.
GO TO 8
9 A(I,IJ) = 1
CONTINUE
IF(IFLOW(I).EQ.0)GO TO 10
A(I,NPP) = QJ(II)
II = II + 1
GO TO 6
10 A(I,NPP) = 0.
CONTINUE
DO 11 I=NP, NP
DO 22 J=I, NP
22 A(I,J)=0.
II = I-NJI
NNJ = LP(8,II)
DO 12 J=I, NNJ
IJ = LP(J,II)
IIJ = ABS(IJ)
IF(IJ .LT. 0) GO TO 13
A(I,IIJ) = KP(IIJ)
GO TO 12
13 A(I,IIJ) = -KP(IIJ)
CONTINUE
11 A(I,NPP) = 0.
V(I) = 4.

```

MAIN LOOP uses the new Kp and n exponent calculated in the lower iteration loop with the code above to rebuild the energy equations. This will continue until the allowed error is reached or the number of allowed iterations is exceeded.

SYSTEM SUBROUTINE FROM UNIVAC MATH PACK TO SOLVE LINEAR SYSTEM OF EQ.
CALL GJR(A, 51, 50, NP, NPP, \$98, JC, V)

Replaced with numpy solver

```

IF (NCT .GT. 0) SUM=0.
DO 51 I=1, NP
BB = A(I,NPP)
IF(NCT) 60,60,61
60 QM = BB
GO TO 62
61 QM = .5 * (Q(I) + BB)
SUM = SUM + ABS(Q(I)-BB)
62 Q(I) = QM
DELQ = QM * DELQ1
QM = ABS(QM)
VI = (QM - DELQ) / AR(I)
IF(VI .LT. .001) V1=.002
V2 = (QM + DELQ) / AR(I)
VE = QM / AR(I)
RE1 = V1 * D(I) / VIS
RE2 = V2 * D(I) / VIS
IF(RE2 .GT. 2.1E3) GO TO 53
F1 = 64./RE1
F2 = 64./RE2
EXPP(I) = 1.
KP(I) = F2 * (Lgth+Le) / Dia
KP(I) = 64.4 * VIS * ARL(I) / D(I)
GO TO 51
53 MM = 0
F = 1 / (1.14 - 2 * ALOG10(E(I)))**2

```

Resetting setting of SUM

1st iteration QM = initially calculated Q, all others use last 2 calculated Qs for QM. BB is previous Q

Iteration loop to calculate the Kp and n exponent for the energy equations based on previous values of Q. For first iteration use Q1 and DELQ. Afterwards use the previous Q and newly calculated Q. Reassign the new Kp and n exponents in the energy equations.

Laminar Flow

NOTE; the original laminar KP equation was replaced with the equation 3-15 from Crane C-410 paper.

```

PAR = VE * SQRT(.125 * F) * D(I) * E(I) / VIS
IF(PAR.GT. 120) GO TO 54
RE = RE1
MCT = 0
FS = SQRT(F)
FZ = .5 / (F*FS)
ARG = E(I) + 9.35 / (RE * FS)
FF = 1./FS - 1.14 + 2.*ALOG10(ARG)
DF = FZ + ELOG *FZ / (ARG * RE)
DIF = FF / DF
F = F + DIF
MCT = MCT + 1
IF(ABS(DIF) .GT. .00001 .AND. MCT .LT. 15) GO TO 52
IF(MM .EQ. I) GO TO 55
MM = I
RE = RE2
F1 = F
GO TO 57
F2 = F
BE = (ALOG(F1) - ALOG(F2)) / (ALOG(QM + DELQ) - ALOG(QM - DELQ))
AE = F1 * (QM - DELQ)**BE
EP = 1 - BI:
EXPP(I) = EP + 1
KP(I) = AE * ARL(I) * QM**EP
GO TO 51
KP(I) = F * ARL(I) * QM**2
EXPP(I) = 2
CONTINUE
NCT = NCT + 1
IF(SUM .GT. ERR AND NCT .LT. MAX) GO TO 20

```

*PAR is proportional to velocity high
par allows for higher pipe velocity.
Recommend PAR <= 120*

*Loop is equivalent to
Calc_Network Iterate_Flow*

Equation 2-25 to 2-28 in Ref 1

MAIN LOOP

```

IF(NCT . EQ. MAX) WRITE(6,108) NCT,SUM
108  FORMAT('DID NOT CONVERGE IN 15 ITERATIONS SUM OF DIFFERENCES')

```

```

IF(NUNIT ,LT. 2) GO TO 63
WRITE(6,127) (Q(I), I=1, NP)
127  FORMAT('FLOWRATE IN PIPES IN CMS',/,(1H, 131.10.4))
DO 64 I=1, NP
64  KP(I) = KP(I) * ABS(Q(I))
WRITE(6, 139) (KP(I), I=1, NP)
GO TO 30
63  WRITE(6,107) (Q(I), I=1, NP)
107  FORMAT('O FLOW RATES IN PIPES IN CFS'./,(1H.13F10,3))
DO 21 I=1, NP
21  KP(I) = KP(I) * ABS(Q(I))
Q(I) = 449. * Q(I)
WRITE(6,138) (KP(I), I=1, NP)
138  FORMAT(' HEAD LOSSES IN PIPES',/,(1H ,13F10.3))
WRITE(6,105) (Q(I), I=1, NP)
105  FORMAT('FLOW RATES (GPM)',/,(1H ,13F10.1))
GO TO 30

```

Beginning of program

Beginning of program

```

98  WRITE(6,106) JC(1),V
106  FORMAT('OVERFLOW OCCURRED -- CHECK SPECIFICATIONS FOR REDUNDANT EQ.  
RESULTING IN SINGULAR MATRIX',15,2F8.2)
GO TO 30
99  STOP
END

```

Beginning of program

Output Kp and Q

REFERENCE 1 'Steady Flow Analysis of Pipe Networks An Instructional Manual.pdf'