

# Performance Enhancements for Zero-Flow Simulation of Vapor Compression Cycles

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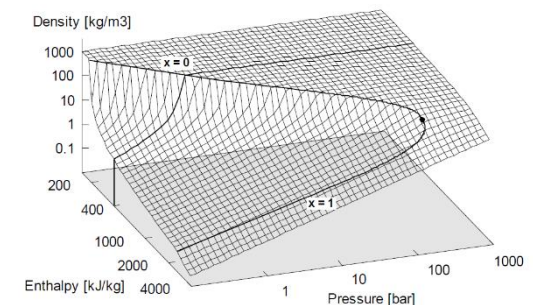
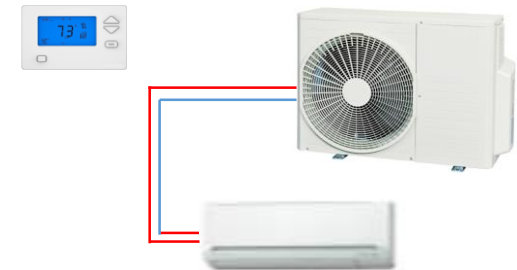
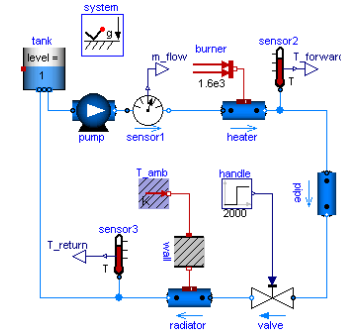
# Motivation & Objective

## Motivation:

- Numerical simulations are widely employed in the HVAC&R industries
- Low and zero-flow phenomena are often encountered in the operation of vapor compression systems with large transients
- Simulation of system dynamics under low and zero-flow conditions presents numerical challenges
- Reported approaches cannot produce satisfactory results sometimes

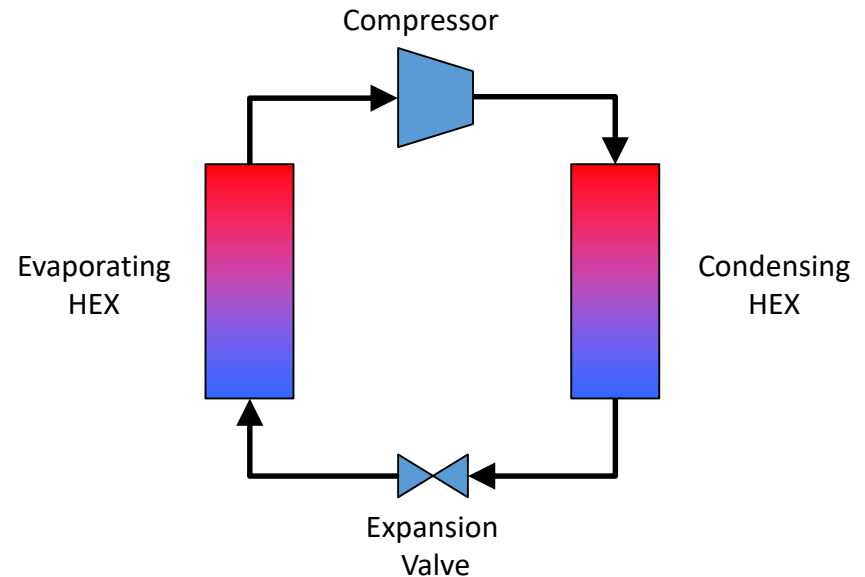
## Objective:

- Explore effective techniques to improve the performance of zero-flow simulations, especially focusing on robustness and improvements in the simulation speed, with a goal of achieving faster than real-time dynamic simulation



# Vapor Compression Cycle Model

- System dynamics are dominated by heat exchangers
- Refrigerant properties defined via Equation of State
  - Pressure and specific enthalpy
- Compressor and valve performance curves defined by the user



## Dynamic HEX model

$$\frac{\partial(\rho A)}{\partial t} + \frac{\partial(\rho A v)}{\partial x} = 0$$

$$\frac{\partial(\rho v A)}{\partial t} + \frac{\partial(\rho v^2 A)}{\partial x} = -A \frac{\partial p}{\partial x} - F_f$$

$$\frac{\partial(\rho u A)}{\partial t} + \frac{\partial(\rho v h A)}{\partial x} = v A \frac{\partial p}{\partial x} + v F_f + \frac{\partial Q}{\partial x}$$

## Static compressor model

$$\eta_v(f, P_r, \dots) = \frac{\dot{m}_{comp}}{\rho_{suc} V f}$$

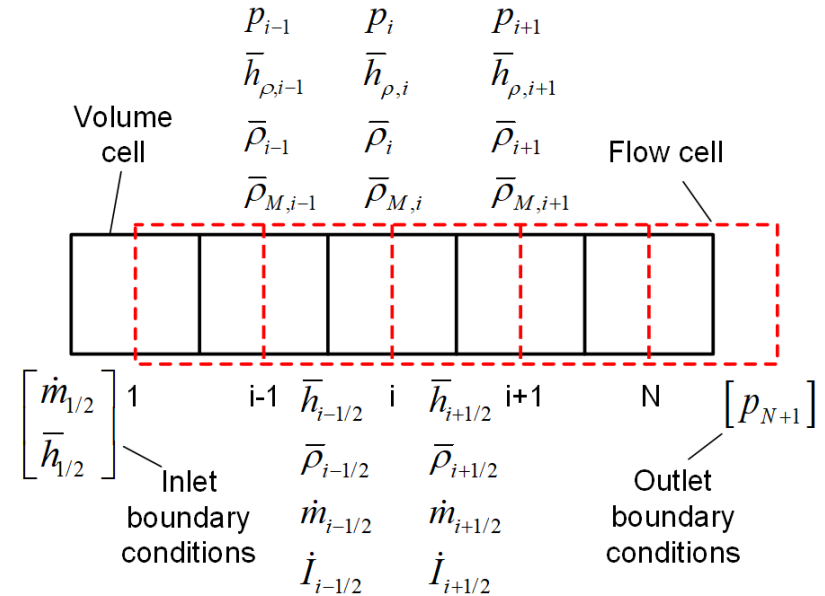
$$\eta_{is}(f, \dots) = \frac{h_{dis,isen} - h_{suc}}{h_{dis} - h_{suc}}$$

## Static valve model

$$\dot{m} = C_v a_v \sqrt{\rho_{in} \Delta P}$$

# Staggered Grid Scheme

- Use 1D separated flow model w/o interfacial exchange
- Shift the momentum balance half a cell compared to the mass- and energy balances to obtain a staggered grid
- The staggering tends to decouple the fast pressure from the slow thermal part of the equation system and thereby creates a more robust discretization scheme
- Use the upwind scheme to approximate interface variables



Mass balance

$$\frac{dM_i}{dt} = \dot{m}_{i-1/2} - \dot{m}_{i+1/2}$$

Energy balance

$$\frac{dU_i}{dt} = \dot{m}_{i-1/2} \bar{h}_{i-1/2} - \dot{m}_{i+1/2} \bar{h}_{i+1/2} + P \Delta z q_i''$$

*Ignored in our models*

Momentum balance

$$\Delta z \frac{d\dot{m}_{i+1/2}}{dt} = \left( \dot{I}_i - \dot{I}_{i+1} \right) - A \left( p_{i+1} - p_i \right) - \bar{\tau}_{w,i+1/2} P \Delta z - \bar{\rho}_{i+1/2} g A \Delta z \sin \theta$$

# Momentum Balance Approximations

Uniform  $dp/dt$ :

$2N+1$  dynamic states

$$\frac{dp_1}{dt} = \dots = \frac{dp_i}{dt} = \dots = \frac{dp_{N+1}}{dt}$$

Linear  $\Delta p$ :

$N+3$  dynamic states

$$\frac{dp_i}{dt} = \left(1 - \frac{i-1}{N}\right) \frac{dp_1}{dt} + \frac{i-1}{N} \frac{dp_{N+1}}{dt}$$

$$N\Delta z \frac{d\bar{m}}{dt} = (\dot{I}_1 - \dot{I}_{N+1}) - A(p_{N+1} - p_1) - P\Delta z \sum_{i=1}^N \bar{\tau}_{w,i+1/2}$$

Friction only:

$2N$  dynamic states

$$p_{i+1} = p_i - \frac{P}{A} \bar{\tau}_{w,i+1/2} \Delta z$$



Pressure drop calculation

$$\frac{\Delta p}{\Delta p_0} = K \left( \frac{\dot{m}}{\dot{m}_0} \right)^\lambda$$

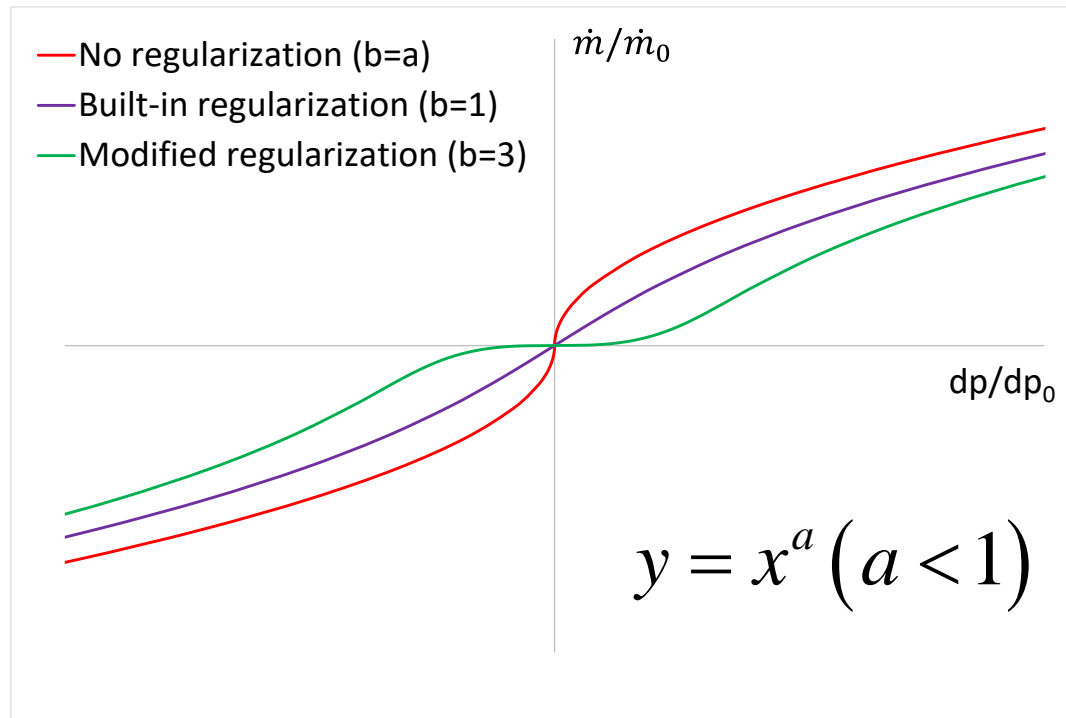
$$\Rightarrow \dot{m} = \dot{m}_0 \left( \frac{\Delta p}{K \Delta p_0} \right)^{1/\lambda}$$

$$\lambda > 1$$

$$\frac{d\dot{m}}{d(\Delta p)} = \frac{\dot{m}_0^\lambda}{\lambda K \Delta p_0} \frac{1}{\dot{m}^{\lambda-1}} \quad \xrightarrow{\dot{m} \rightarrow 0} \text{Infinity}$$

**We need to regularize the relation with locally non-singular substitute**

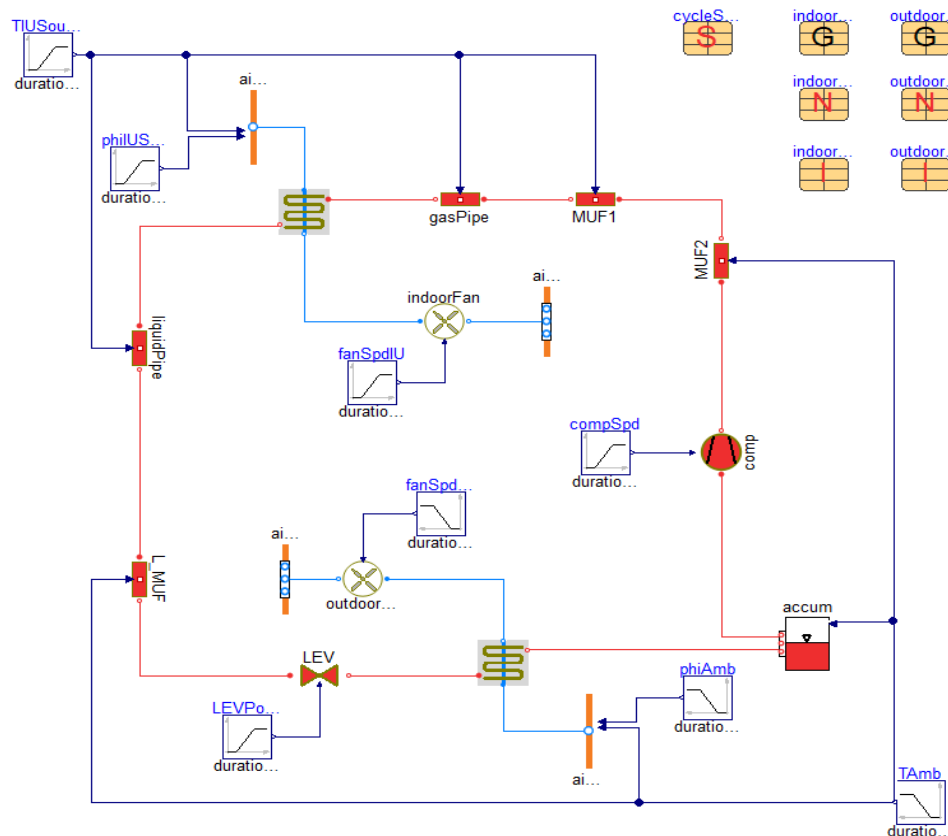
# Pressure Drop Regularization



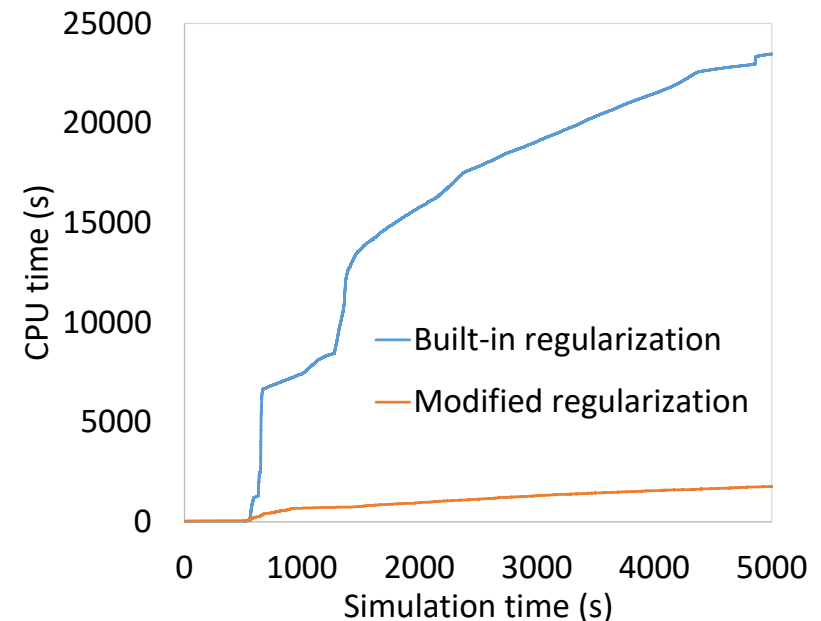
```
function regPowGen
  extends Modelica.Icons.Function;
  input Real x;
  input Real a;
  input Real delta=0.01;
  input Real b=1;
  output Real y;
algorithm
  y := x^b*(x*x+delta*delta)^((a-b)/2);
end regPowGen;
```

- Original relation without regularization is not Lipschitz continuous
- Smaller Lipschitz constants around origin are very helpful

# Case Study



The DAE has 14626 scalar unknowns and 14626 scalar equations.



- System was shut down at 500 sec and off-cycle lasted for 4500 sec
- CPU time: **23000** sec with built-in regularization vs. **1700** sec with modified regularization

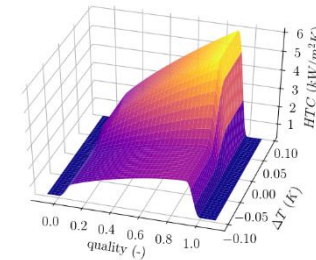
# Heat Transfer Model: Static or Filtered?

- Multiple regimes are blended together to form a universal function
- Simplified closure relations can approximate full correlations

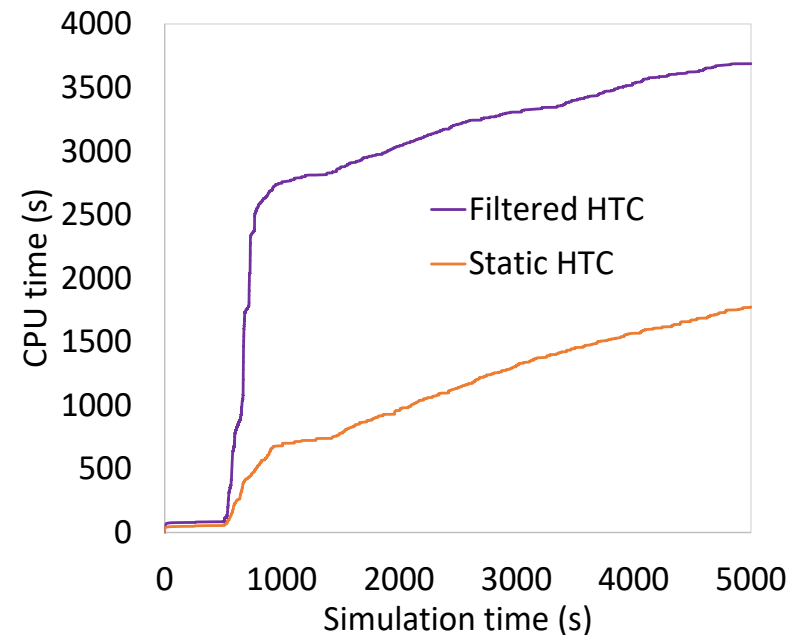
Static HTC 
$$\alpha = K \alpha_0 \left( \frac{\dot{m}}{\dot{m}_0} \right)^c$$

Filtered HTC 
$$\frac{d\alpha}{dt} = \frac{1}{\tau} (\hat{\alpha} - \alpha)$$

- Filtered HTC model decouples the closure variable with other state variables, but increases the number of states
- Turning on 'log norm' showed filtered HTCs limited integration time steps
- CPU time: **3700** sec with filtered HTCs vs. **1700** sec with static HTCs



```
6 197 1137 indoorCoil.circuits[1].heatTransfer.alphas[21] (#118)
17 357 1373 indoorCoil.circuits[1].heatTransfer.alphas[22] (#119)
28 315 1666 indoorCoil.circuits[1].heatTransfer.alphas[23] (#120)
32 501 2022 indoorCoil.circuits[1].heatTransfer.alphas[24] (#121)
51 544 2138 indoorCoil.circuits[1].heatTransfer.alphas[25] (#122)
32 333 1674 indoorCoil.circuits[1].heatTransfer.alphas[26] (#123)
19 193 1146 indoorCoil.circuits[1].heatTransfer.alphas[27] (#124)
0 0 2 indoorCoil.header[1].mediums[1].p (#152)
0 0 4 indoorCoil.header[1].mediums[2].p (#154)
13 21 120 indoorCoil.header[2].mediums[1].p (#156)
```





# Discretization Methods

Continuity

$$\frac{\partial(\rho A)}{\partial t} + \frac{\partial(\rho A v)}{\partial z} = 0$$

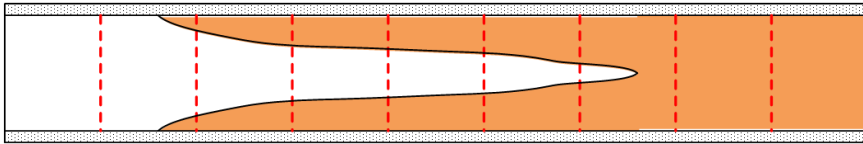
Momentum

$$\frac{\partial(\rho v A)}{\partial t} + \frac{\partial(\rho v^2 A)}{\partial z} = -A \frac{\partial p}{\partial z} - F_f$$

Energy

$$\frac{\partial(\rho u A)}{\partial t} + \frac{\partial(\rho v h A)}{\partial z} = v A \frac{\partial p}{\partial z} + v F_f + \frac{\partial Q}{\partial z}$$

*Finite Volume Method*



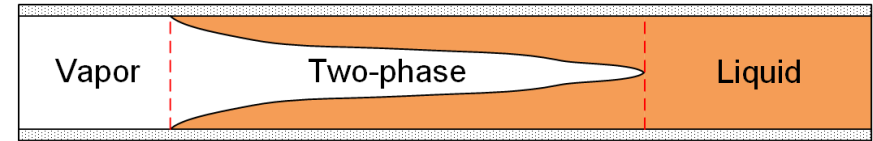
*Staggered grid scheme with upwind difference*

$$A \Delta z \frac{d \rho_i}{dt} = \dot{m}_{i-1/2} - \dot{m}_{i+1/2}$$

$$\Delta z \frac{d \dot{m}_{i+1/2}}{dt} = -\Delta \dot{I}_i - A \Delta p_i - \bar{\tau}_{w,i+1/2} P \Delta z$$

$$A \Delta z \frac{d(\rho_i u_i)}{dt} = \dot{m}_{i-1/2} h_{i-1/2} - \dot{m}_{i+1/2} h_{i+1/2} + P \Delta z q_i''$$

*Moving Boundary Method*

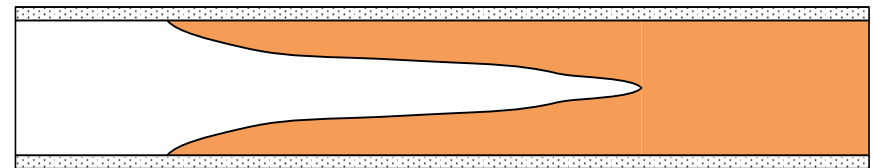


*Reynolds transport theorem*

$$\frac{d}{dt} \int_0^L \frac{\partial(\rho A)}{\partial t} dz + \frac{d}{dt} \int_0^L \frac{\partial \dot{m}}{\partial z} dz = 0$$

$$\frac{d}{dt} \int_0^L \frac{\partial [A(\rho h - p)]}{\partial t} dz + \frac{d}{dt} \int_0^L \frac{\partial(\dot{m} h)}{\partial z} dz = q'$$

*Lumped Parameter Method*



*Single control volume with mean properties*

$$A L \frac{d \bar{\rho}}{dt} = \dot{m}_{in} - \dot{m}_{out}$$

$$A L \frac{d(\bar{\rho} h - p)}{dt} = \dot{m}_{in} h_{in} - \dot{m}_{out} h_{out} + P L q''$$

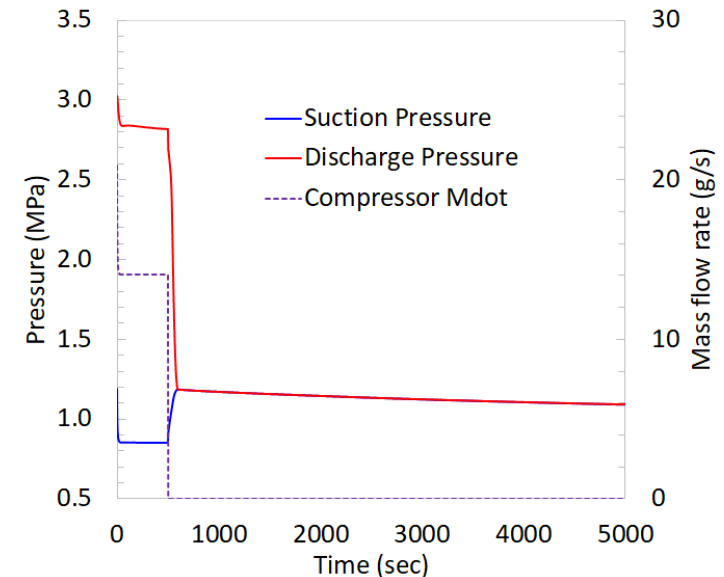
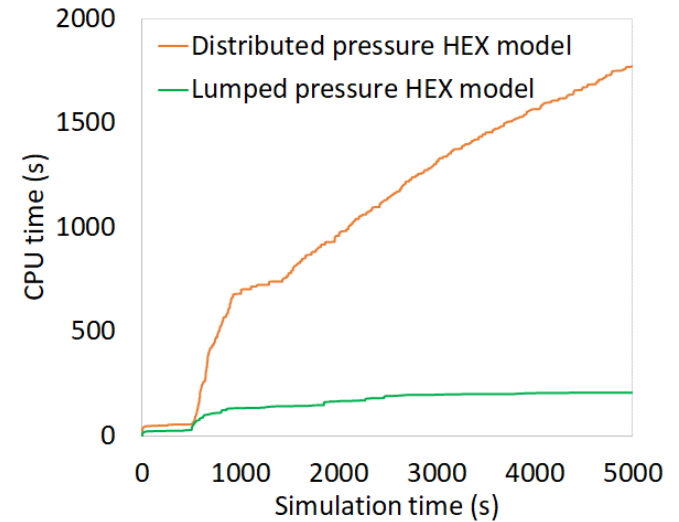
# Single-Pressure HEX Model

$$A\Delta z \left( \frac{\partial \bar{\rho}_i}{\partial p} \frac{dp}{dt} + \frac{\partial \bar{\rho}_i}{\partial \bar{h}_{\rho,i}} \frac{d\bar{h}_{\rho,i}}{dt} \right) = \dot{m}_{i-1/2} - \dot{m}_{i+1/2}$$

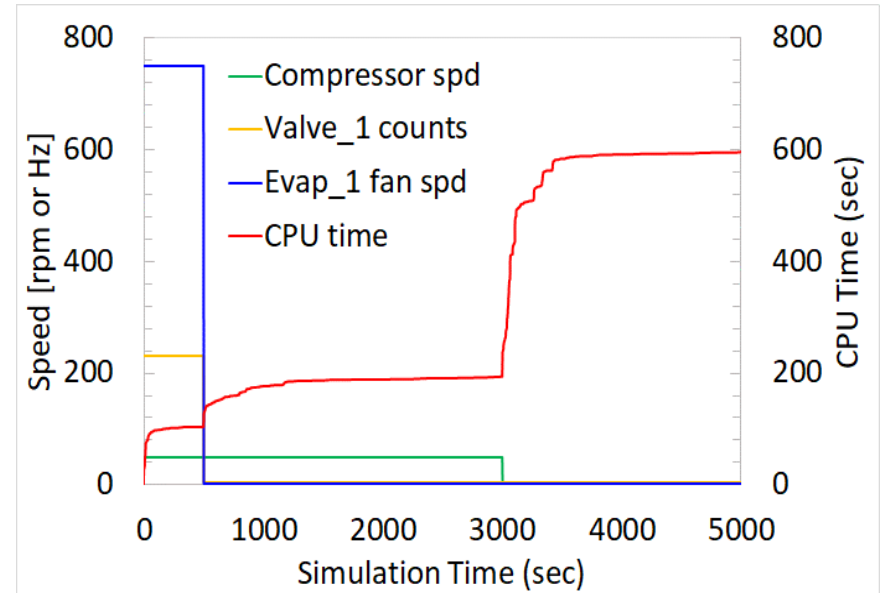
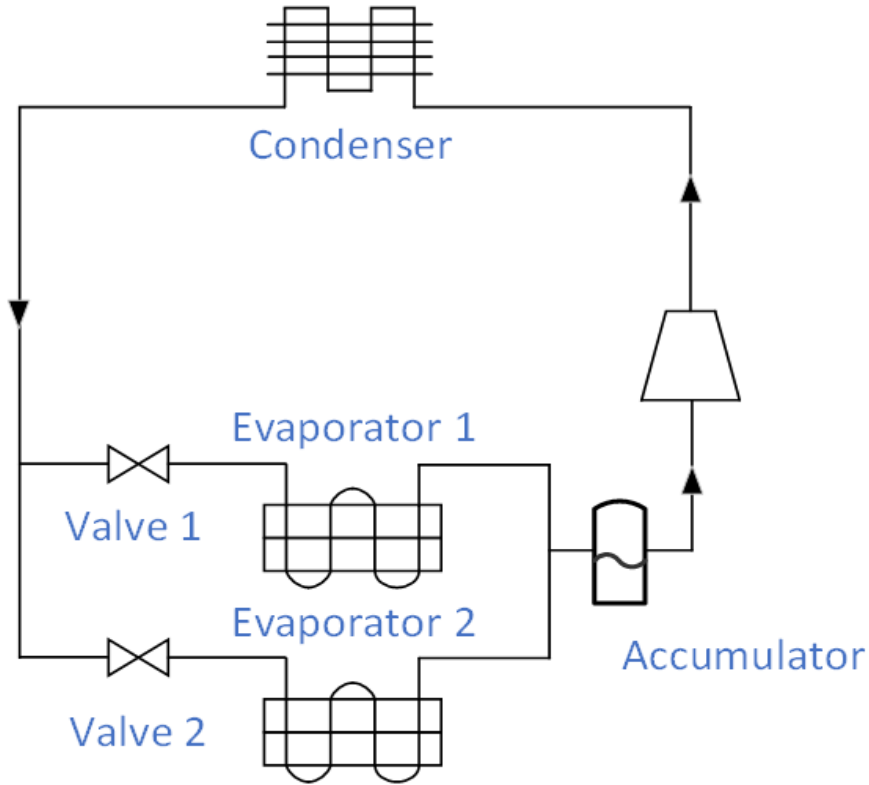
$$A\Delta z \left( \bar{\rho}_i \frac{d\bar{h}_{\rho,i}}{dt} - \frac{dp}{dt} \right) =$$

$$\dot{m}_{i-1/2} \left( \bar{h}_{i-1/2} - \bar{h}_{\rho,i} \right) \bar{h}_{i-1/2} - \dot{m}_{i+1/2} \left( \bar{h}_{i+1/2} - \bar{h}_{\rho,i} \right) + P\Delta z q_i''$$

- Dependence of mass flow rates upon pressure difference can be removed
- N+1 states and pressure drop is lumped together and calculated at the inlet or outlet depending on model structure
- CPU time: **1700** sec with distributed HEX model vs. **200** sec with lumped pressure drop model
- 100x speedup with all the enhancements



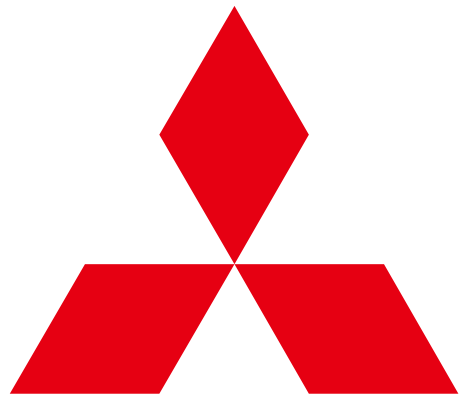
# Another Case Study



- System operated for the first 500 sec with two active evaporator branches
- The first branch was off (the associated fan and valve were closed) since 500 sec
- Entire system was turned off at 3000 sec
- 600 sec CPU time with all the enhancements

## Conclusions & Future Work

- Reducing the sensitivity of mass flow to pressure differences is a key to accelerating zero-flow simulation
- Static heat transfer model seems more efficient, if no spurious oscillations appear in the simulation
- Lumping pressure drops at the inlet or outlet of HEXs or pipes is helpful for further speeding up simulation
- We would like to evaluate these enhancements with models that can generate Analytical Jacobians



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