

# Chap 9.

Application of divergence theorem to obtain differential forms of conservation of mass and conservation of momentum

$$\iint \vec{F} \cdot \vec{n} dA = \iiint \nabla \cdot \vec{F} dV$$

piece-wise smooth surface,  $\vec{F}$  different

(I) Conservation of mass

$$\underbrace{\iint_{CS} \rho(\vec{v} \cdot \vec{n}) dA}_{\text{}} + \frac{\partial}{\partial t} \iiint_{CV} \rho dV = 0$$

$$\iiint_{CV} \nabla \cdot (\rho \vec{v}) dV$$

$$\Rightarrow \iiint_{CV} \nabla \cdot (\rho \vec{v}) dV + \iiint_{CV} \frac{\partial \rho}{\partial t} dV = 0$$

$$\Rightarrow \iiint_{CV} \left[ \nabla \cdot (\rho \vec{v}) + \frac{\partial \rho}{\partial t} \right] dV = 0$$

$$\Rightarrow \nabla \cdot (\rho \vec{v}) + \frac{\partial \rho}{\partial t} = 0 \quad (9-2)$$

Net rate of mass efflux per unit volume  $\quad \quad \quad$  rate of accumulation of mass per unit volume

$$\Rightarrow \left[ \vec{v} \cdot \nabla \rho + \rho(\nabla \cdot \vec{v}) \right] + \frac{\partial \rho}{\partial t} = 0$$

$$\Rightarrow \frac{D\rho}{Dt} + \rho(\nabla \cdot \vec{v}) = 0 \quad (9-5)$$

$\rho \vec{v}$  = mass flux  
( $\frac{M}{L^2 t}$ )

$\frac{D\rho}{Dt} = \frac{\partial \rho}{\partial t} + \vec{v} \cdot \nabla \rho$   
substantial derivative of  $\rho$

## # Substantial derivative

2

$$\frac{D}{Dt} = \frac{\partial}{\partial t} + u_x \frac{\partial}{\partial x} + v_y \frac{\partial}{\partial y} + w_z \frac{\partial}{\partial z}$$

For example

$$\frac{DP}{Dt} = \frac{\partial P}{\partial t} + \underline{u_x \frac{\partial P}{\partial x} + v_y \frac{\partial P}{\partial y} + w_z \frac{\partial P}{\partial z}}$$

$$= \frac{\partial P}{\partial t} + \underline{\vec{v} \cdot \nabla P}$$

local  
rate of  
change of  
pressure

rate of change of  
pressure due to motion (convective)  
fluid

Total derivative

$$\frac{dP}{dt} = \frac{\partial P}{\partial t} + \underline{\frac{dx}{dt} \frac{\partial P}{\partial x} + \frac{dy}{dt} \frac{\partial P}{\partial y} + \frac{dz}{dt} \frac{\partial P}{\partial z}}$$

rate of change of pressure  
due to motion

To measure the rate change of pressure

(i) At a weather station  $\frac{\partial P}{\partial t}$

(ii) On an aircraft  $\frac{dP}{dt}$

(iii) On a balloon  $\frac{DP}{Dt}$

$$\nabla \cdot (\rho \vec{v}) + \frac{\partial \rho}{\partial t} = 0 \quad \text{or} \quad \frac{D\rho}{Dt} + \rho(\nabla \cdot \vec{v}) = 0$$

is called continuity eq.

(II) Conservation of momentum

$$\underline{\Sigma \vec{F}} = \underbrace{\iint_{CS} \rho \vec{v} (\vec{v} \cdot \vec{n}) dA} + \underbrace{\frac{\partial}{\partial t} \iiint_{C.V.} \rho \vec{v} dV}$$

$$\underbrace{\iint_{C.S.} \vec{\tau} \cdot \vec{n} dA + \iiint_{C.V.} \rho \vec{g} dV}_{\text{sum of the external forces acting on the C.V.}} = \underbrace{\iint_{C.S.} \rho \vec{v} (\vec{v} \cdot \vec{n}) dA}_{\text{net rate of linear momentum efflux from C.V.}} + \underbrace{\iiint_{C.V.} \frac{\partial(\rho \vec{v})}{\partial t} dV}_{\text{time rate of change of linear momentum within the C.V.}}$$

sum of the external forces acting on the C.V.

net rate of linear momentum efflux from C.V.

time rate of change of linear momentum within the C.V.

$\vec{\tau}$  : stresses (normal and shear)  
momentum flux by viscous transfer.  
 $\iiint_{C.V.} \nabla \cdot \vec{\tau} dV$        $\iint_{C.S.} \vec{\tau} \cdot \vec{n} dA$

Apply divergence theorem

$$\iiint_{C.V.} [\nabla \cdot \vec{\tau} + \rho \vec{g}] dV = \iiint_{C.V.} \nabla \cdot (\rho \vec{v} \vec{v}) dV + \iiint_{C.V.} \frac{\partial(\rho \vec{v})}{\partial t} dV$$

$$\Rightarrow \nabla \cdot \vec{\tau} + \rho \vec{g} = \underbrace{\nabla \cdot (\rho \vec{v} \vec{v})}_{(\rho \vec{v}) \cdot \nabla \vec{v} + (\nabla \cdot \rho \vec{v}) \vec{v}} + \frac{\partial(\rho \vec{v})}{\partial t}$$



$$\Rightarrow \nabla \cdot \vec{L} + \rho \vec{g} = (\rho \vec{v}) \cdot \nabla \vec{v} + (\nabla \cdot \rho \vec{v}) \vec{v} + \frac{\partial(\rho \vec{v})}{\partial t}$$

$$\Rightarrow \nabla \cdot \vec{L} + \rho \vec{g} = \underbrace{(\rho \vec{v}) \cdot \nabla \vec{v}} + \underbrace{(\nabla \cdot \rho \vec{v}) \vec{v}} + \underbrace{\frac{\partial \rho}{\partial t} \vec{v} + \rho \frac{\partial \vec{v}}{\partial t}}$$

$$\Rightarrow \nabla \cdot \vec{L} + \rho \vec{g} = \underbrace{\rho \left( \frac{\partial \vec{v}}{\partial t} + \vec{v} \cdot \nabla \vec{v} \right)} + \underbrace{(\nabla \cdot \rho \vec{v} + \frac{\partial \rho}{\partial t}) \vec{v}}_{=0}$$

$$\Rightarrow \nabla \cdot \vec{L} + \rho \vec{g} = \rho \frac{D\vec{v}}{Dt} \quad (9-16)$$

$$\underbrace{\sum \vec{F}}_{\text{local change of } \vec{v}, \text{ that is, local acceleration}} = \underbrace{\frac{M}{V} \cdot \vec{a}}_{\text{rate of change in } \vec{v} \text{ due to fluid motion (convection), that is, convective acceleration}} \quad \text{Newton's 2nd law of motion}$$

where  $\frac{D\vec{v}}{Dt} = \frac{\partial \vec{v}}{\partial t} + \vec{v} \cdot \nabla \vec{v}$

Strictly speaking, the only assumption for (9-16) is the continuity of fluid.

If the fluid applies Stokes's viscosity relation then gives eq. (9-17)

$$\rho \frac{Dv_x}{Dt} = \rho g_x + \frac{\partial \sigma_{xx}}{\partial x} + \frac{\partial \tau_{yx}}{\partial y} + \frac{\partial \tau_{zx}}{\partial z} \quad (9-16a)$$

$$\rho \frac{Dv_y}{Dt} = \rho g_y + \frac{\partial \tau_{xy}}{\partial x} + \frac{\partial \sigma_{yy}}{\partial y} + \frac{\partial \tau_{zy}}{\partial z} \quad (9-16b)$$

$$\rho \frac{Dv_z}{Dt} = \rho g_z + \frac{\partial \tau_{xz}}{\partial x} + \frac{\partial \tau_{yz}}{\partial y} + \frac{\partial \sigma_{zz}}{\partial z} \quad (9-16c)$$

For 9-16a, applying Stokes's viscosity relation

$$\rho \frac{Dv_x}{Dt} = \rho g_x + \frac{\partial}{\partial x} \left[ \mu \left( \frac{\partial v_x}{\partial x} - \frac{2}{3} (\nabla \cdot \vec{v}) \right) \right] - \frac{\partial p}{\partial x} \\ + \frac{\partial}{\partial y} \left[ \mu \left( \frac{\partial v_x}{\partial y} + \frac{\partial v_y}{\partial x} \right) \right] + \frac{\partial}{\partial z} \left[ \mu \left( \frac{\partial v_x}{\partial z} + \frac{\partial v_z}{\partial x} \right) \right]$$

$$\rho \frac{Dv_x}{Dt} = \rho g_x - \frac{\partial p}{\partial x} - \frac{\partial}{\partial x} \left( \frac{2}{3} \mu (\nabla \cdot \vec{v}) \right) \\ + \frac{\partial}{\partial x} \left( \mu \frac{\partial v_x}{\partial x} \right) + \frac{\partial}{\partial y} \left( \mu \frac{\partial v_x}{\partial y} \right) + \frac{\partial}{\partial z} \left( \mu \frac{\partial v_x}{\partial z} \right) + \nabla \cdot (\mu \nabla v_x) \quad (9-17a)$$

Same for (9-16b) and (9-16c)

Navier-Stokes eq.

6

(9-17)

If the fluid is incompressible ( $\rho = \text{const}$ )  
then the continuity eq. becomes  $\nabla \cdot \vec{v} = 0$  and const viscosity ( $\mu = \text{const}$ )

$$\nabla \cdot \vec{v} = 0$$

and Navier-Stokes eq. becomes

$$\rho \frac{D\vec{v}}{Dt} = \rho \vec{g} - \nabla p + \mu \nabla^2 \vec{v} \quad (9-18) \quad \text{or } (9-19)$$

Reynolds number

From  $\rho \frac{\partial \vec{v}}{\partial t} + \rho \vec{v} \cdot \nabla \vec{v} = \rho \vec{g} - \nabla p + \mu \nabla^2 \vec{v}$

$\rho \frac{v^2}{a}$  characteristic  
inertial force length  
per unit volume

$\mu \frac{v}{a^2}$   
viscous force  
per unit volume

$$\begin{aligned} Re = \frac{\text{inertial force}}{\text{viscous force}} &= \frac{\rho \frac{v^2}{a} \cdot a^3}{\mu \frac{v}{a^2} \cdot a^3} \\ &= \frac{\rho v a}{\mu} \end{aligned}$$



$$\nabla \cdot \vec{\tau} + \rho \vec{g} = \nabla \cdot (\rho \vec{v} \vec{v}) + \frac{\partial (\rho \vec{v})}{\partial t}$$

rate of momentum  
gain by viscous  
transfer per unit  
volume

rate of momentum  
gain by convection  
per unit volume

rate of increase  
of momentum  
per unit volume

+  
pressure force  
on element per  
unit volume

normal and shear  
forces acting on  
the C.V. per unit  
volume

+  
pressure force  
on element per  
unit volume

+  
pressure force  
on element per  
unit volume

$$\nabla \cdot (\rho \vec{v} \vec{v})$$

$$\nabla \cdot \vec{\tau} + \rho \vec{g} = \rho \frac{D\vec{v}}{Dt} \quad (9-16)$$

$$\frac{\sum \vec{F}}{V} = \frac{M}{V} \cdot \vec{a}$$

Newton's 2nd law of motion

$$(\rho \vec{v}^2 \vec{v} - \nabla p) + \rho \vec{g} = \rho \frac{D\vec{v}}{Dt} \quad (9-18)$$

$$(9-19)$$

# 9.4 A rotating solid sphere (p100-101)

Creeping flow

Assumption

1. The fluid : Newtonian and behaves as continuum
2. The flow : laminar, incompressible, steady-state, fully developed
3. No-slip condition applies.
4. Neglect gravity and pressure.

$$\vec{v} = (\overset{0}{u_r}, \overset{0}{u_\theta}, v_\phi)$$

laminar flow

$$\underline{\underline{\tau}} = \begin{bmatrix} \tau_{rr} & \tau_{r\theta} & \tau_{r\phi} \\ \tau_{\theta r} & \tau_{\theta\theta} & \tau_{\theta\phi} \\ \tau_{\phi r} & \tau_{\phi\theta} & \tau_{\phi\phi} \end{bmatrix}$$

$$v_\phi(r, \theta, \phi)$$

symmetric  
~~symmetric~~

$$\tau_{\theta\theta} = \tau_{\phi\phi} = \mu \left[ \frac{\sin\theta}{r} \frac{\partial}{\partial\theta} \left( \frac{v_\phi}{\sin\theta} \right) \right]$$

$\phi$  - direction  $0 = \underline{\underline{\mu \nabla^2 \vec{v}}}$

$$\tau_{\phi r} = \tau_{r\phi} = \mu \left[ r \sin\theta \frac{\partial}{\partial r} \left( \frac{v_\phi}{r} \right) \right]$$

$$0 = \mu \left[ \frac{1}{r^2} \frac{\partial}{\partial r} \left( r^2 \frac{\partial v_\phi}{\partial r} \right) + \frac{1}{r^2 \sin\theta} \frac{\partial}{\partial\theta} \left( \sin\theta \frac{\partial v_\phi}{\partial\theta} \right) - \frac{v_\phi}{r^2 \sin^3\theta} \right]$$

Trial solution

$$v_\phi = f(r) \sin\theta$$

$$0 = \frac{1}{r} \frac{\partial}{\partial r} (r^2 f' \sin\theta) + \frac{1}{r^2 \sin\theta} \frac{\partial}{\partial\theta} (\sin\theta \cdot f \cos\theta) - \frac{f}{r^2 \sin\theta}$$



$$0 = \frac{1}{r^2} [2r f' \sin \theta + r^2 f'' \sin \theta] + \frac{f}{r^2 \sin \theta} [\cos^2 \theta - \sin^2 \theta] - \frac{f}{r^2 \sin \theta}$$

$$0 = \frac{1}{r^2} \frac{d}{dr} (r^2 f' \sin \theta) - \frac{2 f' \sin \theta}{r^2} \quad (f' = \frac{df}{dr})$$

$$0 = \frac{d}{dr} (r^2 \frac{df}{dr}) - 2f$$

This is a Cauchy-type eq.

the solution  $f(r) = r^n$

~~$$\frac{d}{dr} (r^{n+2}) - 2r^n$$~~

$$\frac{d}{dr} (r^2 \cdot n r^{(n-1)}) - 2r^n = 0$$

$$n(n+1) \cdot r^n - 2r^n = 0$$

$$n^2 + n - 2 = 0$$

$$(n-1)(n+2) = 0$$

$$n = 1, -2$$

General solution  $f(r) = C_1 r + \frac{C_2}{r^2}$

From B.C.s  $v_\phi|_{r=R} = R \cdot \Omega \sin \theta$ ,  $v_\phi|_{r \rightarrow \infty} = 0$

$$\Rightarrow v_\phi = \frac{R^3 \Omega}{r^2} \sin \theta$$

shear stress

$$\tau_{r\phi} = \tau_{\phi r} = \mu \left( r \frac{\partial}{\partial r} \left( \frac{v_\phi}{r} \right) \right) = \mu (1-3) \frac{R^3 \Omega}{r^3} \sin \theta$$