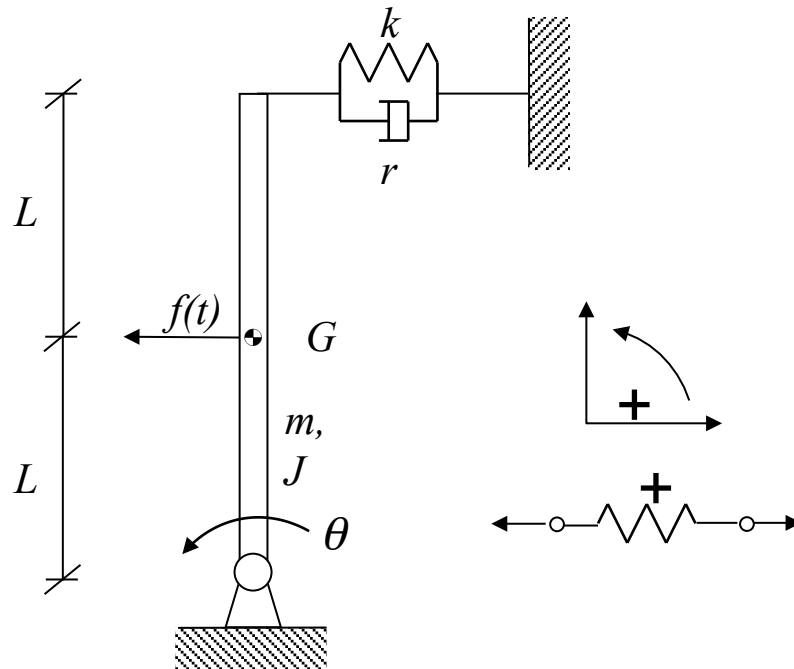




**PROPORTIONAL-DERIVATIVE (PD)  
CONTROLLER**

**PROPORTIONAL-INTEGRAL (PI)  
CONTROLLER**



$$\begin{aligned} L &= 1 \text{ m} \\ m &= 80 \text{ kg} \\ J &= 20 \text{ kgm}^2 \\ k &= 250 \text{ N/m (or 125 N/m)} \\ r &= 25 \text{ Ns/m} \end{aligned}$$

$$(mL^2 + J)\ddot{\vartheta} + 4rL^2\dot{\vartheta} + (4kL^2 - mgL)\vartheta = f(t)L = F(t)$$

$$m^*\ddot{\vartheta} + r^*\dot{\vartheta} + k^*\vartheta = F(t)$$

$$F(t) = k_p(\vartheta_{ref} - \vartheta) + k_d(\dot{\vartheta}_{ref} - \dot{\vartheta})$$

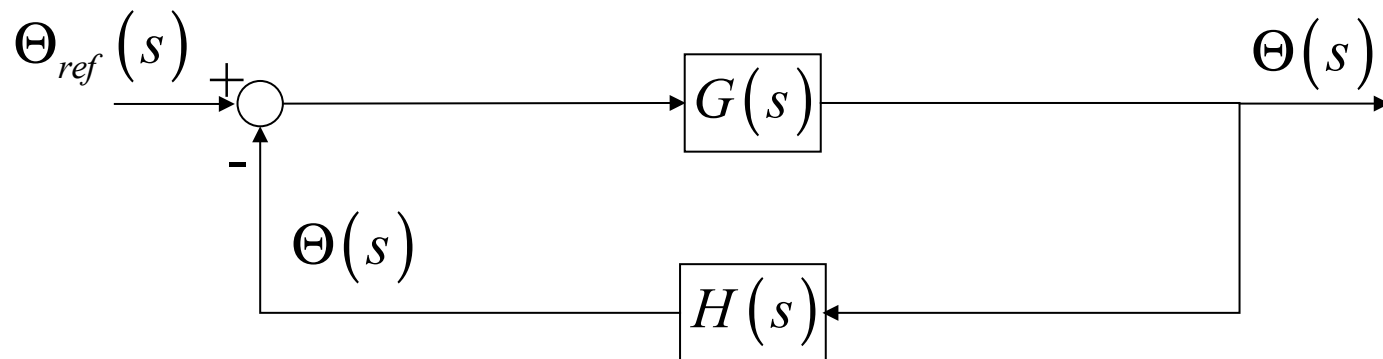
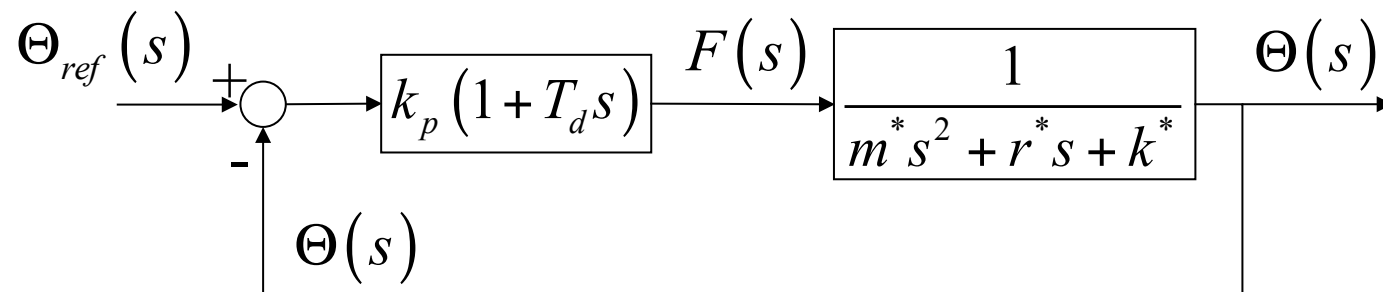
$$m^*\ddot{\vartheta} + r^*\dot{\vartheta} + k^*\vartheta = k_p(\vartheta_{ref} - \vartheta) + k_d(\dot{\vartheta}_{ref} - \dot{\vartheta})$$



$$m^* \ddot{\vartheta} + r^* \dot{\vartheta} + k^* \vartheta = k_p (\vartheta_{ref} - \vartheta) + k_d (\dot{\vartheta}_{ref} - \dot{\vartheta})$$
$$(m^* s^2 + r^* s + k^*) \Theta(s) = k_p (1 + T_d s) (\Theta_{ref}(s) - \Theta(s))$$

Input

Output





$$GH(s) = G(s)H(s) = \frac{k_p (1 + T_d s)}{m^* s^2 + r^* s + k^*}$$

open loop transfer function

$$L(s) = \frac{G(s)}{1 + G(s)H(s)} = \frac{k_p (1 + T_d s)}{m^* s^2 + (r^* + k_p T_d) s + (k^* + k_p)}$$

closed loop transfer function

The stability analysis can be performed:

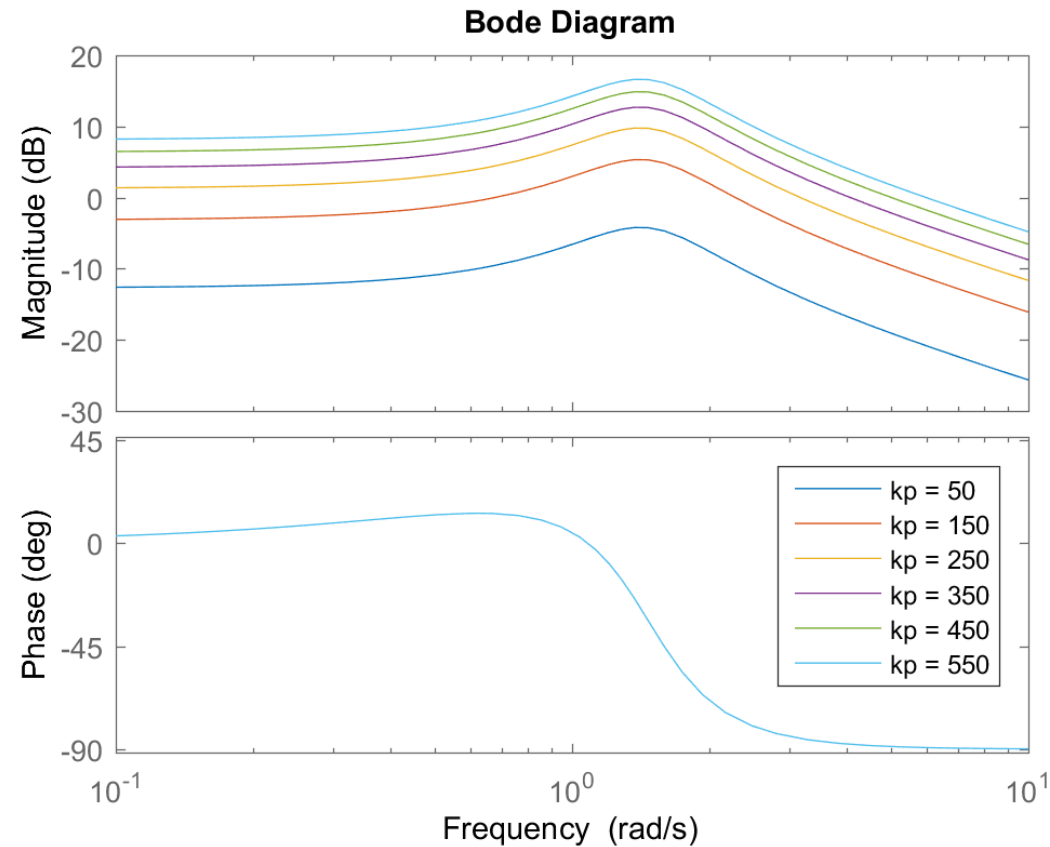
- 1) studying the poles of the closed loop transfer function  $L(s)$ ;
- 2) using Nyquist criterion (we must draw the Nyquist diagram of  $GH(s)$ );
- 3) using Bode criterion, if and only if the uncontrolled system is stable (we must draw the Bode diagram of  $GH(s)$ ).



$k = 250 \text{ N/m}$  (zero before the c.c. poles)

5

Bode diagram of the open loop transfer function  $GH(s)$

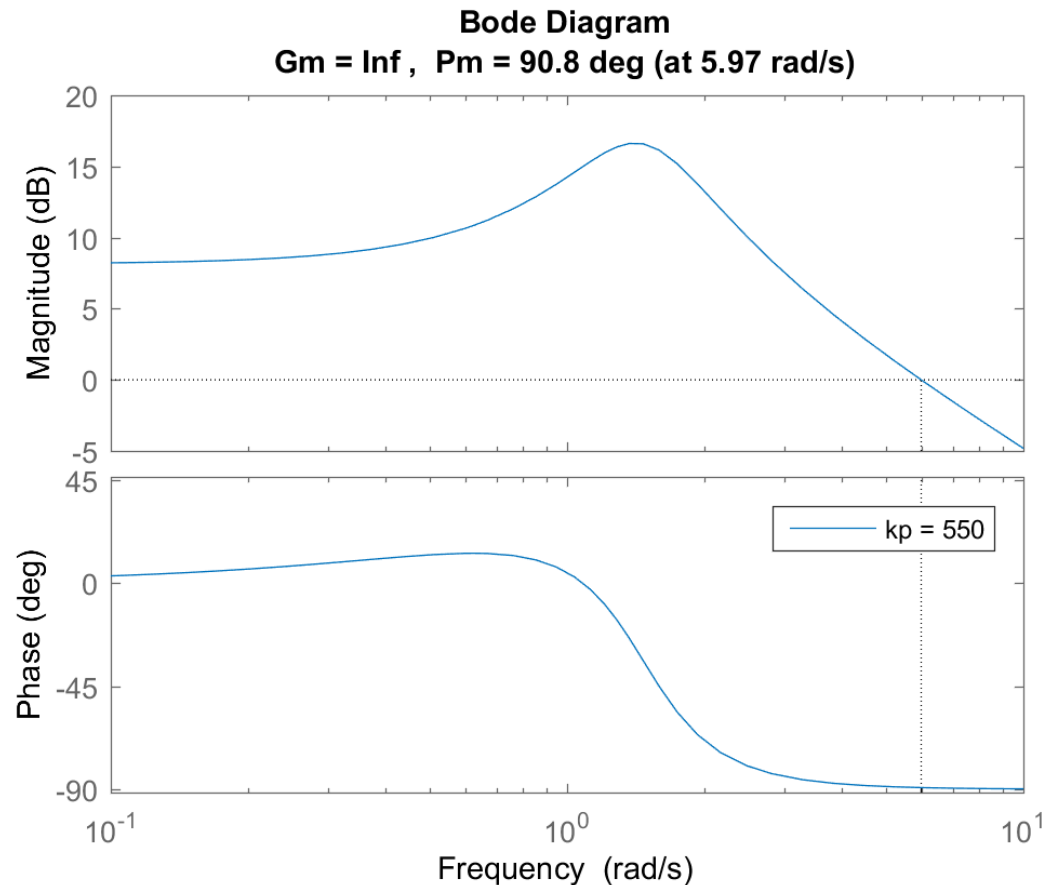




$k = 250 \text{ N/m}$  (zero before the c.c. poles)

6

Bode diagram of the open loop transfer function  $GH(s)$



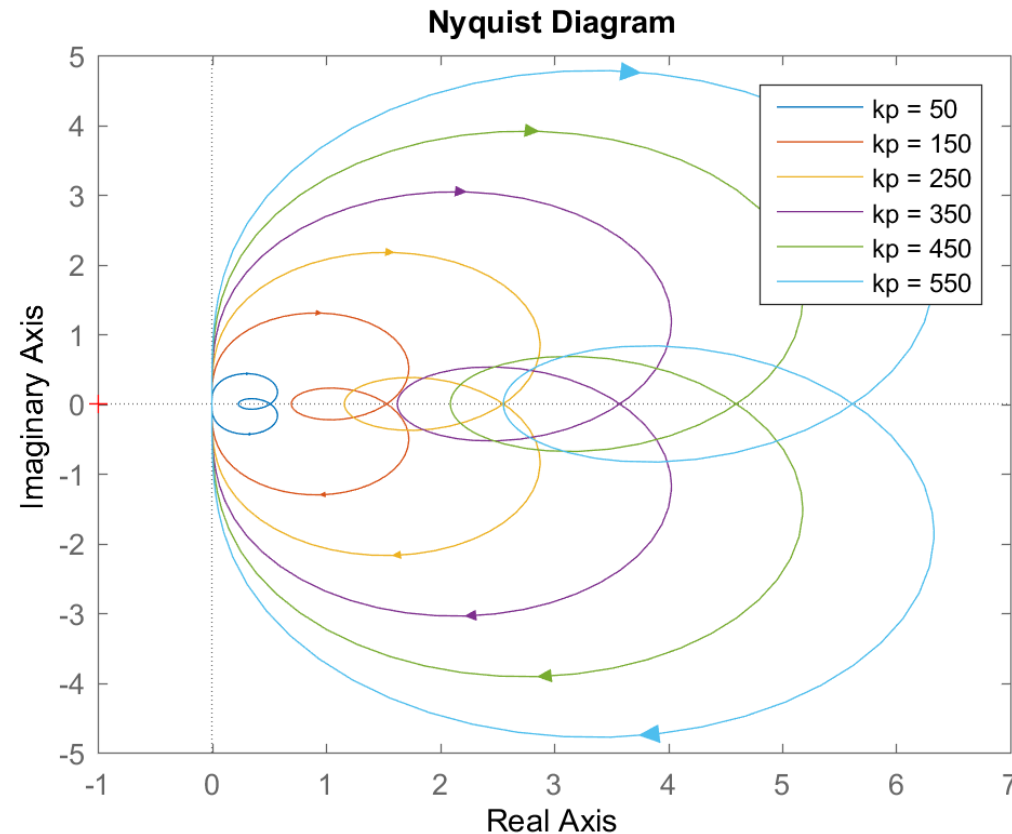
Using Bode criterion, being  $P_m > 0$  and  $G_m > 0$  we can say that the controlled system is stable.



$k = 250 \text{ N/m}$  (zero before the c.c. poles)

7

Nyquist diagram of the open loop transfer function  $GH(s)$



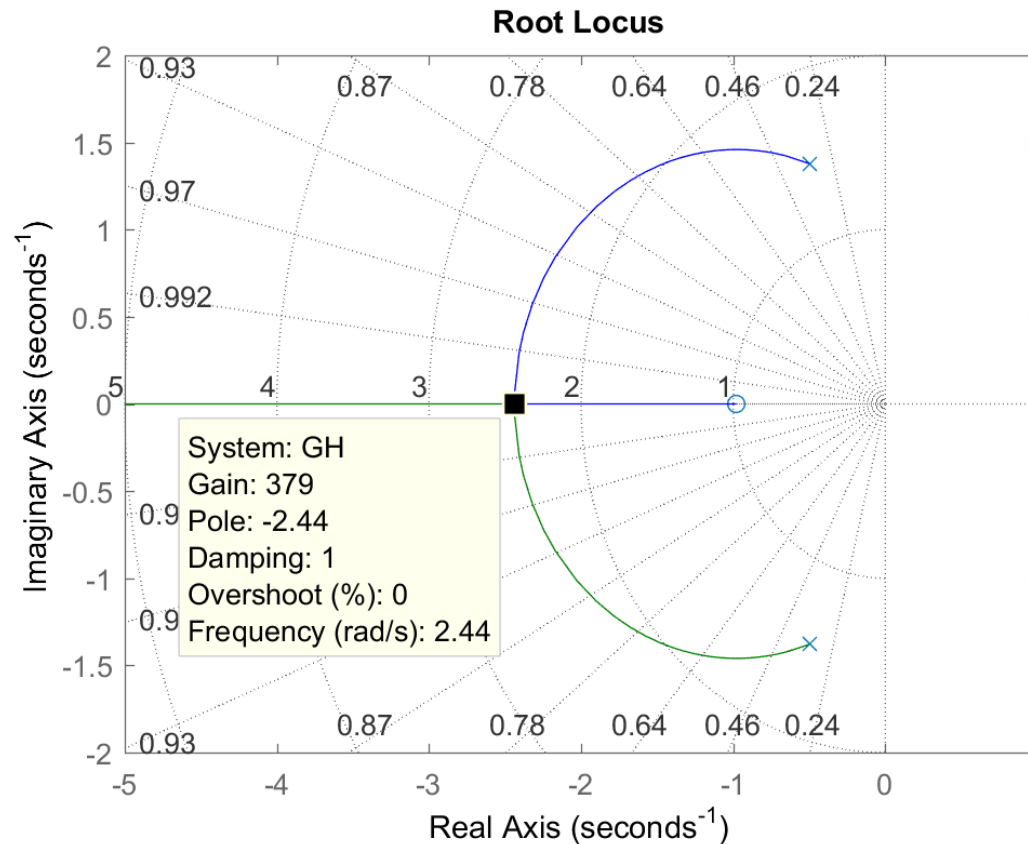
No encirclement of the point  $(-1,0)$  is found. Using Nyquist criterion we can say that the controlled system is stable.



$k = 250 \text{ N/m}$  (zero before the c.c. poles)

## Root locus

8



The poles of the system have negative real parts for all the possible values of the proportional gain  $k_p$ , however they may become real if  $k_p$  is larger than 379.

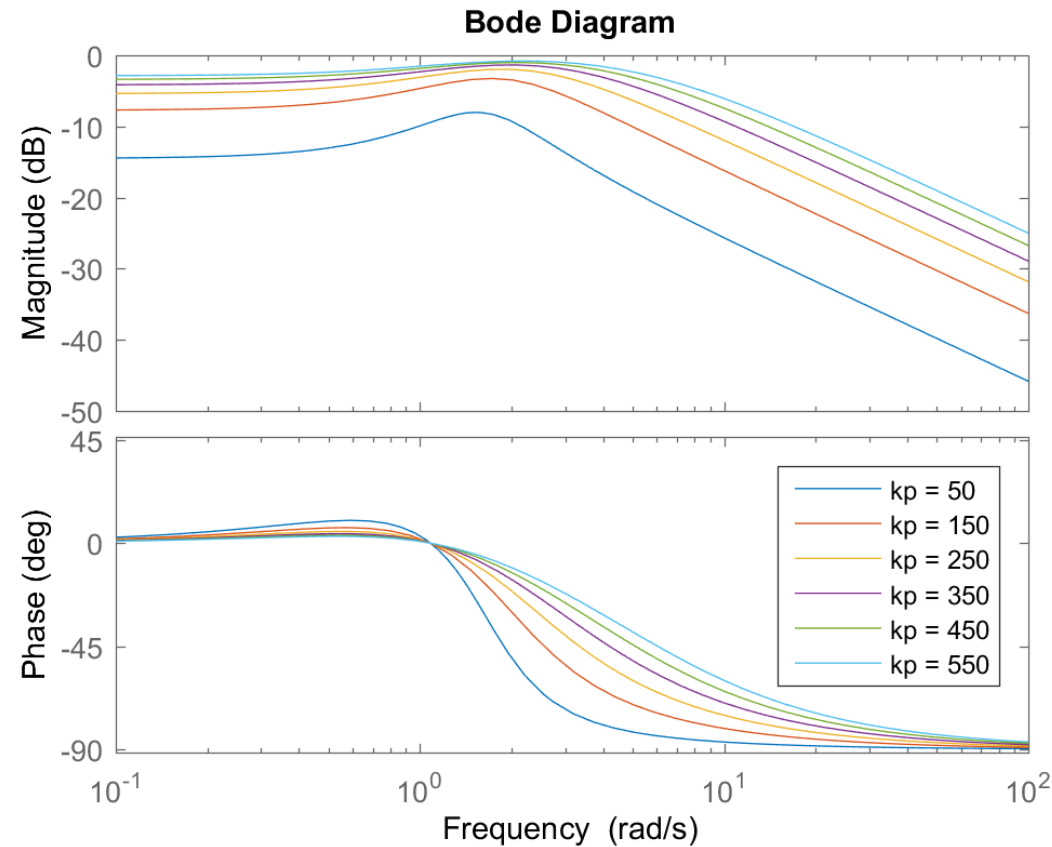




$k = 250 \text{ N/m}$  (zero before the c.c. poles)

9

Bode diagram of the closed loop transfer function  $L(s)$

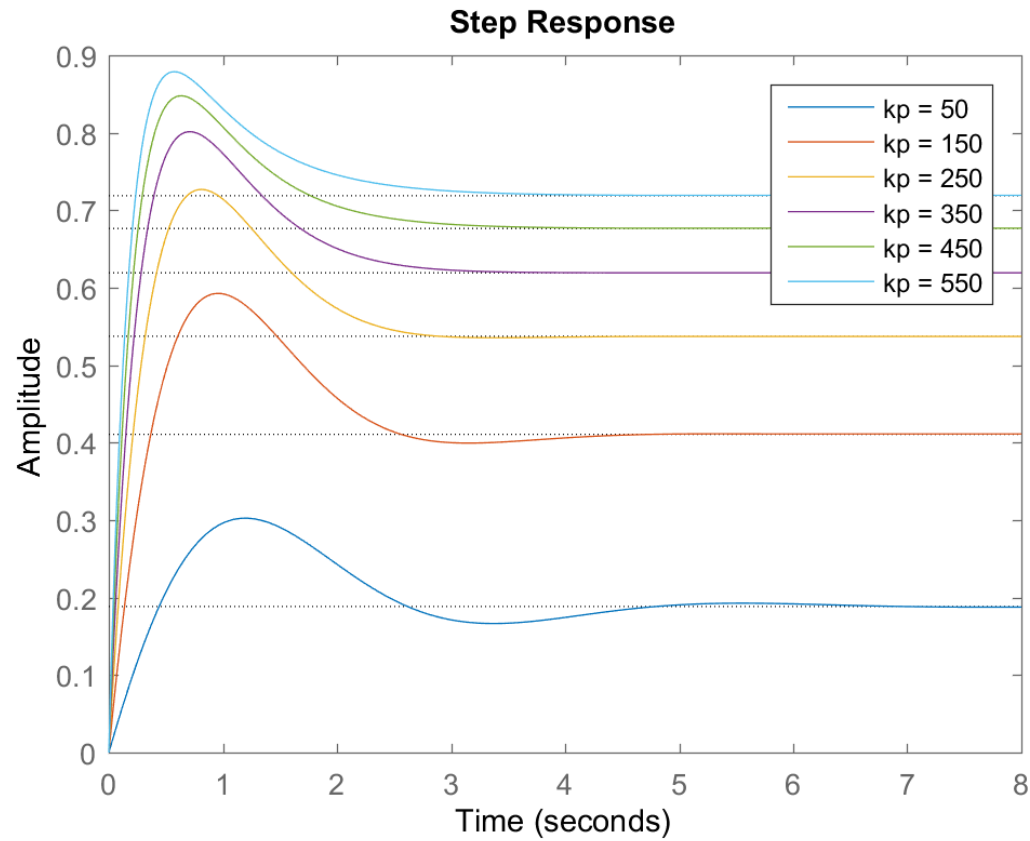


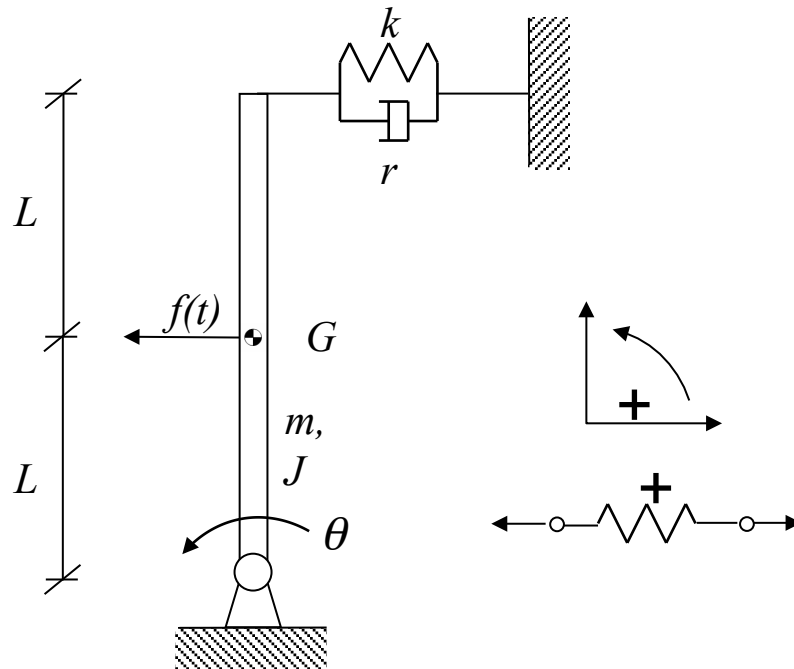


$k = 250 \text{ N/m}$  (zero before the c.c. poles)

Step response

10





$$\begin{aligned} L &= 1 \text{ m} \\ m &= 80 \text{ kg} \\ J &= 20 \text{ kgm}^2 \\ k &= 250 \text{ N/m (or 125 N/m)} \\ r &= 25 \text{ Ns/m} \end{aligned}$$

$$(mL^2 + J)\ddot{\vartheta} + 4rL^2\dot{\vartheta} + (4kL^2 - mgL)\vartheta = f(t)L = F(t)$$

$$m^*\ddot{\vartheta} + r^*\dot{\vartheta} + k^*\vartheta = F(t)$$

$$F(t) = k_p(\vartheta_{ref} - \vartheta) + k_i \int_0^t (\vartheta_{ref} - \vartheta) dt$$

$$m^*\ddot{\vartheta} + r^*\dot{\vartheta} + k^*\vartheta = k_p(\vartheta_{ref} - \vartheta) + k_i \int_0^t (\vartheta_{ref} - \vartheta) dt$$

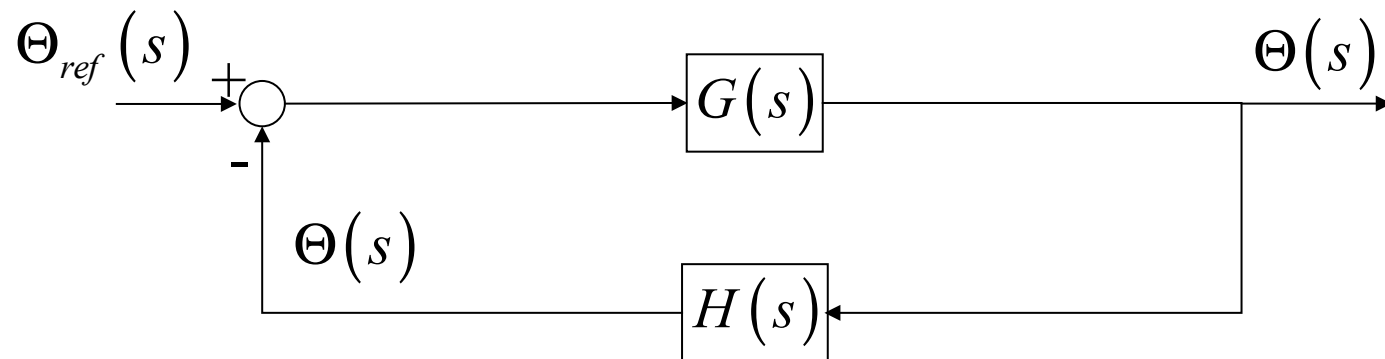
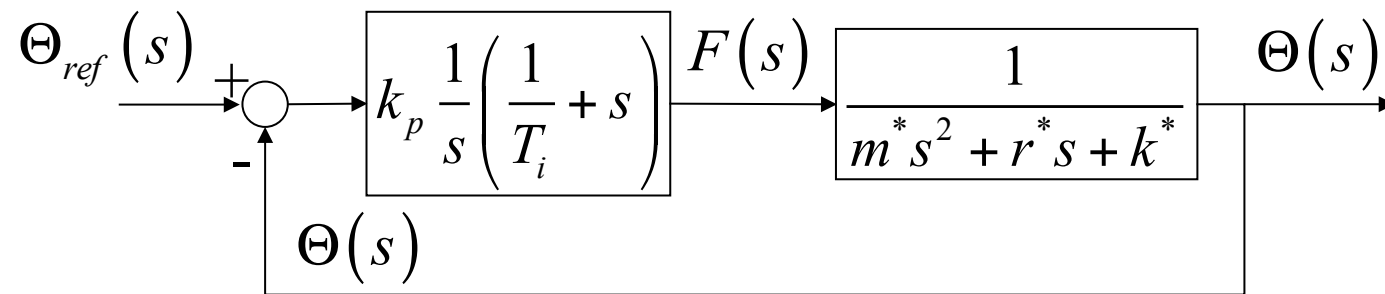


$$m^* \ddot{\vartheta} + r^* \dot{\vartheta} + k^* \vartheta = k_p (\vartheta_{ref} - \vartheta) + k_i \int_0^t (\vartheta_{ref} - \vartheta) dt$$

$$(m^* s^2 + r^* s + k^*) \Theta(s) = k_p \frac{1}{s} \left( \frac{1}{T_i} + s \right) (\Theta_{ref}(s) - \Theta(s))$$

Input

Output





$$GH(s) = G(s)H(s) = \frac{k_p \left( \frac{1}{T_i} + s \right)}{s(m^*s^2 + r^*s + k^*)}$$

open loop transfer function

$$L(s) = \frac{G(s)}{1 + G(s)H(s)} = \frac{k_p \left( \frac{1}{T_i} + s \right)}{s(m^*s^2 + r^*s + k^*) + k_p \left( \frac{1}{T_i} + s \right)}$$

closed loop transfer function

The stability analysis can be performed:

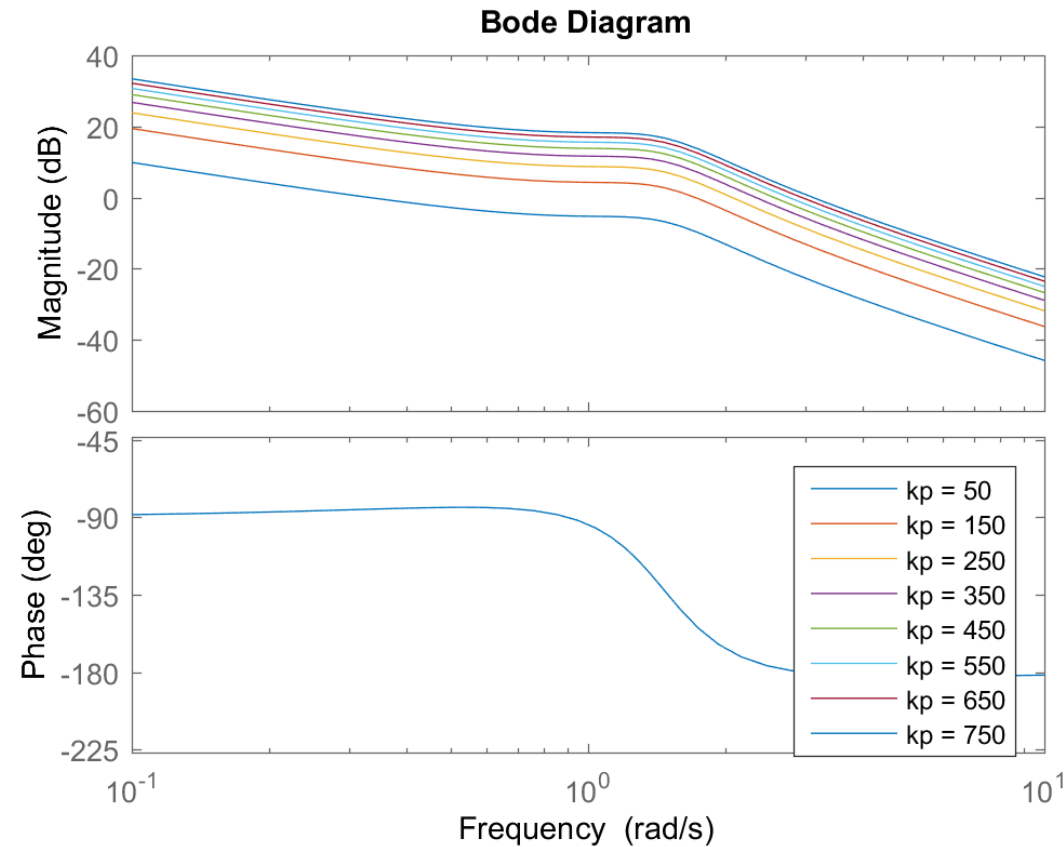
- 1) studying the poles of the closed loop transfer function  $L(s)$ ;
- 2) using Nyquist criterion (we must draw the Nyquist diagram of  $GH(s)$ );
- 3) using Bode criterion, if and only if the uncontrolled system is stable (we must draw the Bode diagram of  $GH(s)$ ).



$k = 250 \text{ N/m}$  (zero just before the c.c. poles)

14

Bode diagram of the open loop transfer function  $GH(s)$

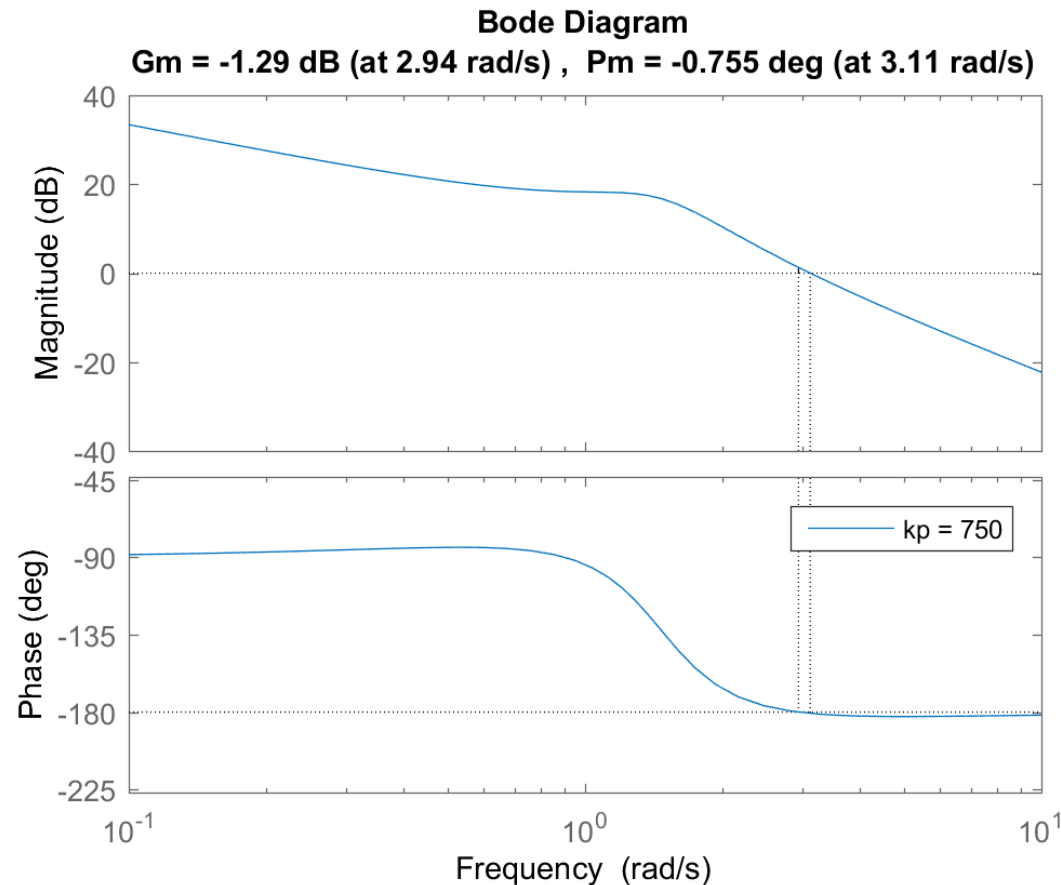




$k = 250 \text{ N/m}$  (zero just before the c.c. poles)

15

## Bode diagram of the open loop transfer function $GH(s)$



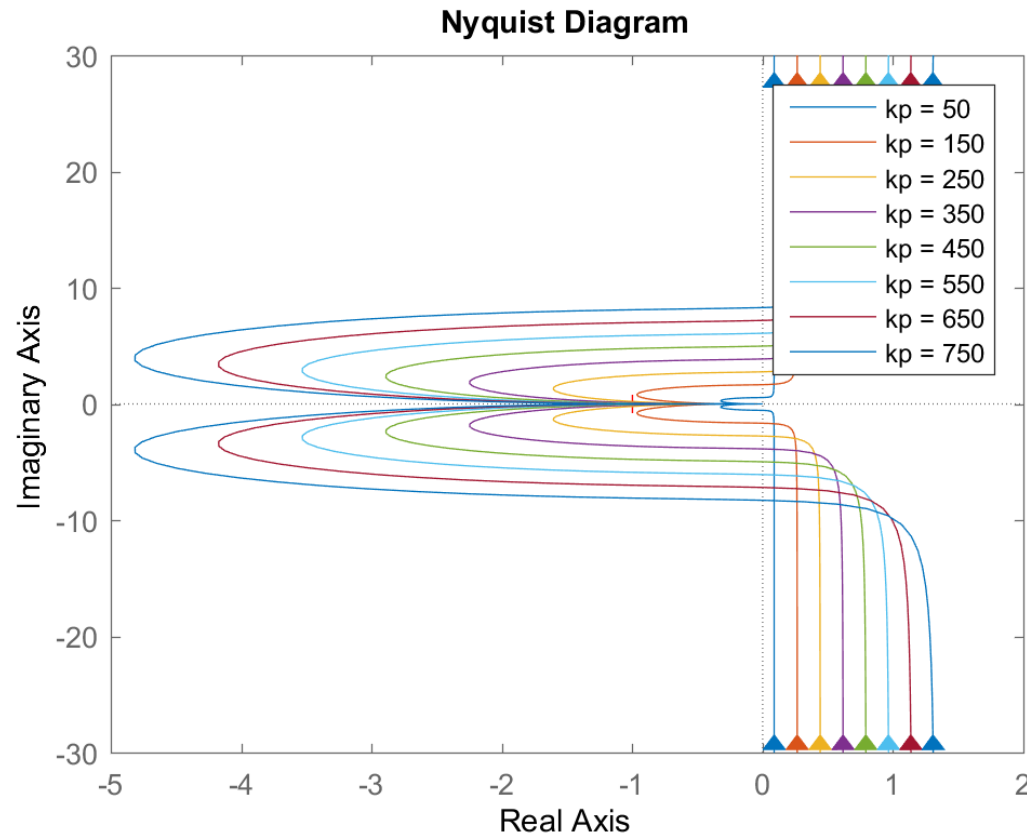
Using Bode criterion, being  $P_m < 0$  and  $G_m < 0$  we can say that the controlled system is unstable when  $k_p$  is equal to 750.



$k = 250 \text{ N/m}$  (zero just before the c.c. poles)

16

Nyquist diagram of the open loop transfer function  $GH(s)$



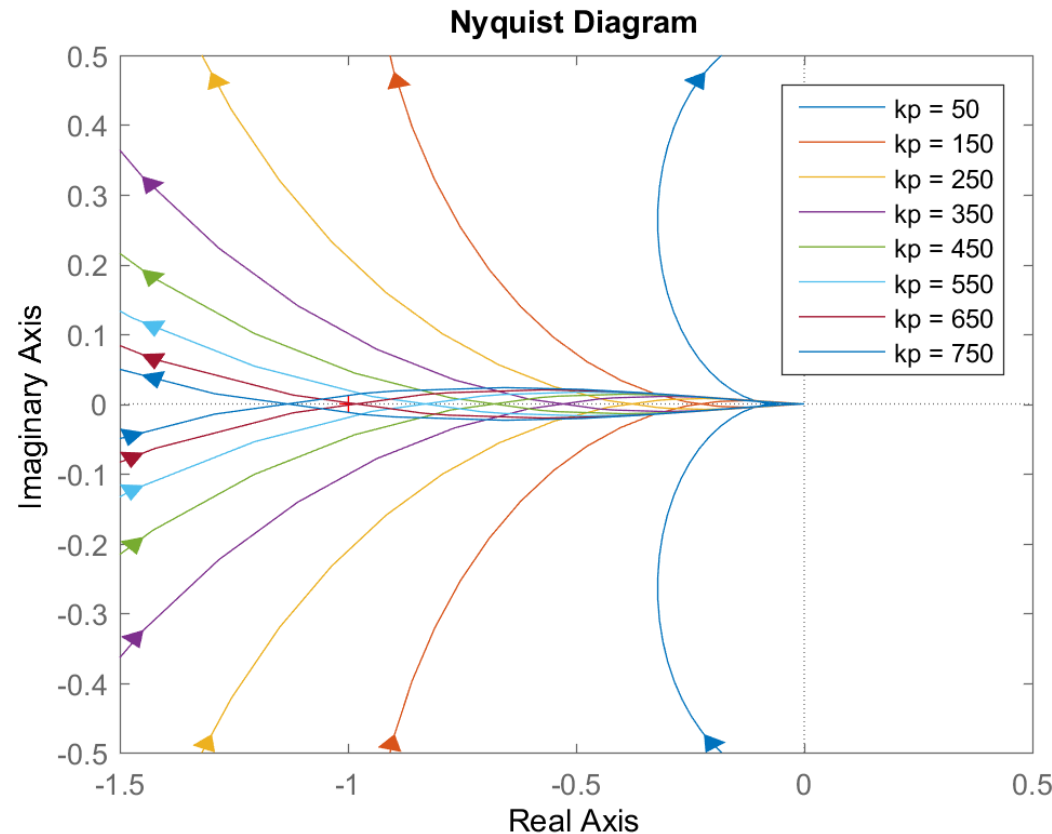




$k = 250 \text{ N/m}$  (zero just before the c.c. poles)

17

Nyquist diagram of the open loop transfer function  $GH(s)$



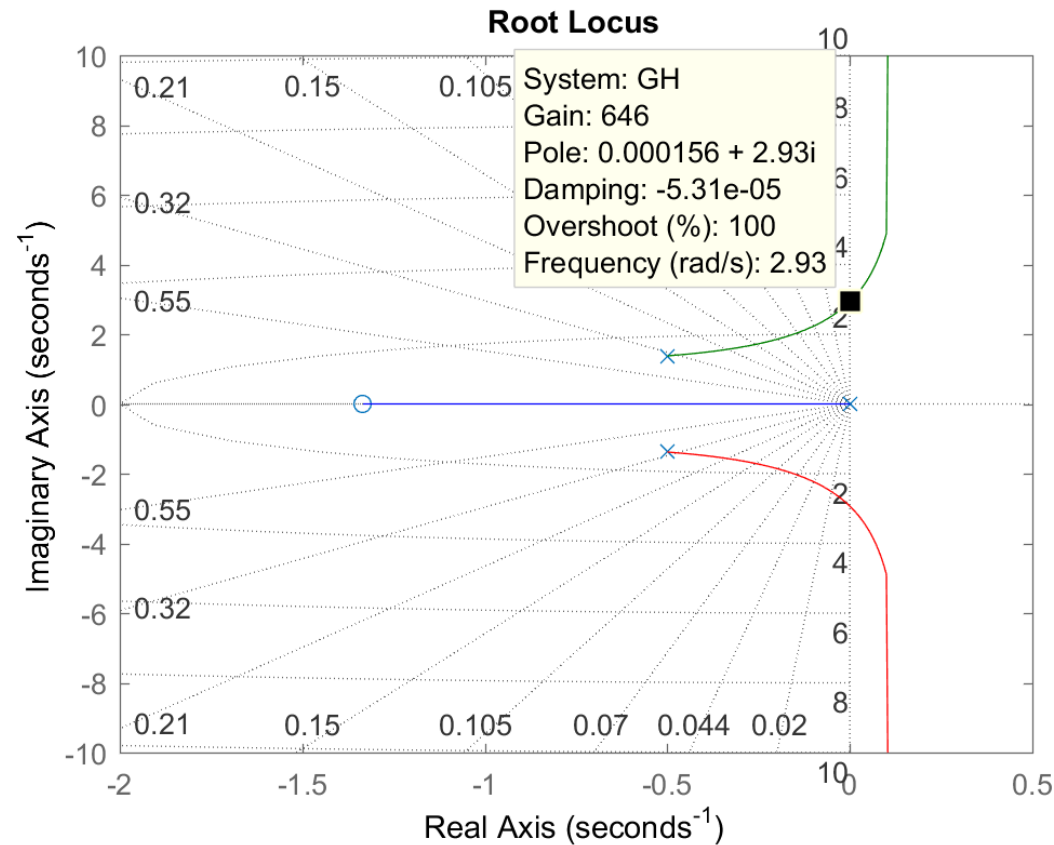
No encirclement of the point  $(-1,0)$  is found when  $k_p$  is smaller than 650. If  $k_p$  is equal to 650 and 750 one encirclement is found. For these two cases, using Nyquist criterion we can say that the controlled system is unstable.



$k = 250 \text{ N/m}$  (zero just before the c.c. poles)

## Root locus

18



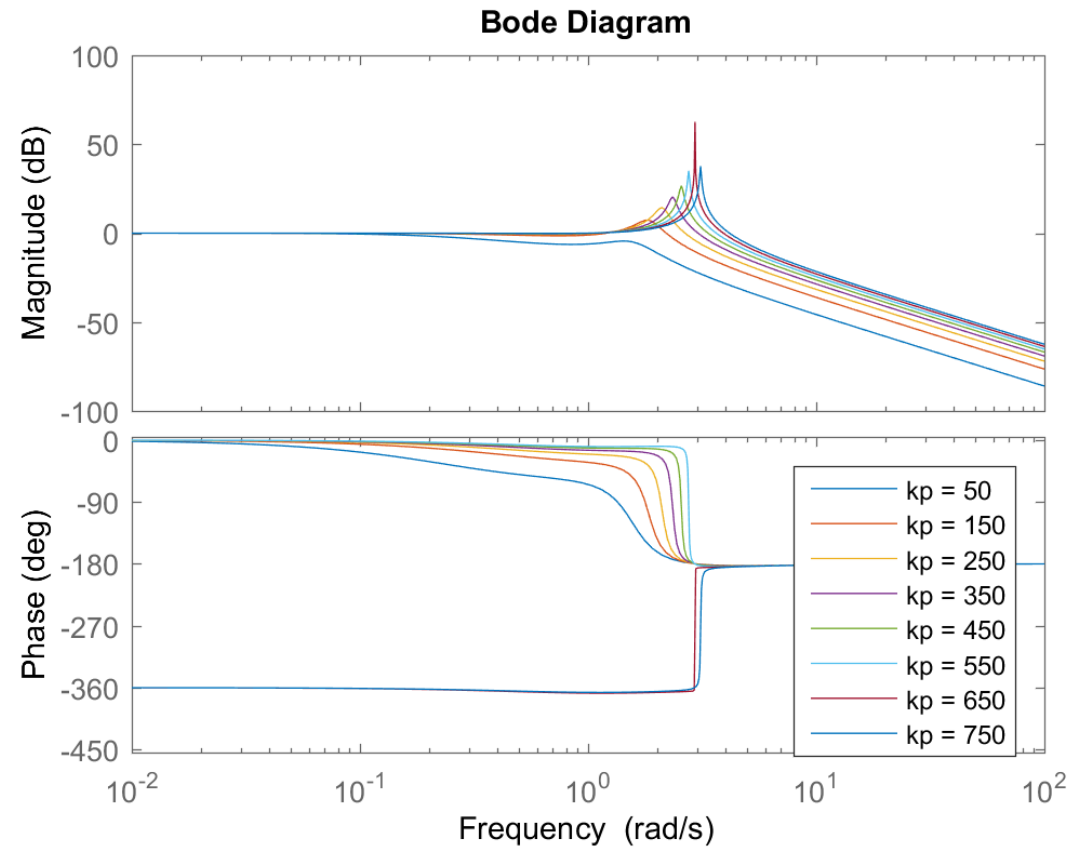
The poles of the system have negative real parts if the proportional gain  $k_p$  is smaller than 646.



$k = 250 \text{ N/m}$  (zero just before the c.c. poles)

19

Bode diagram of the closed loop transfer function  $L(s)$

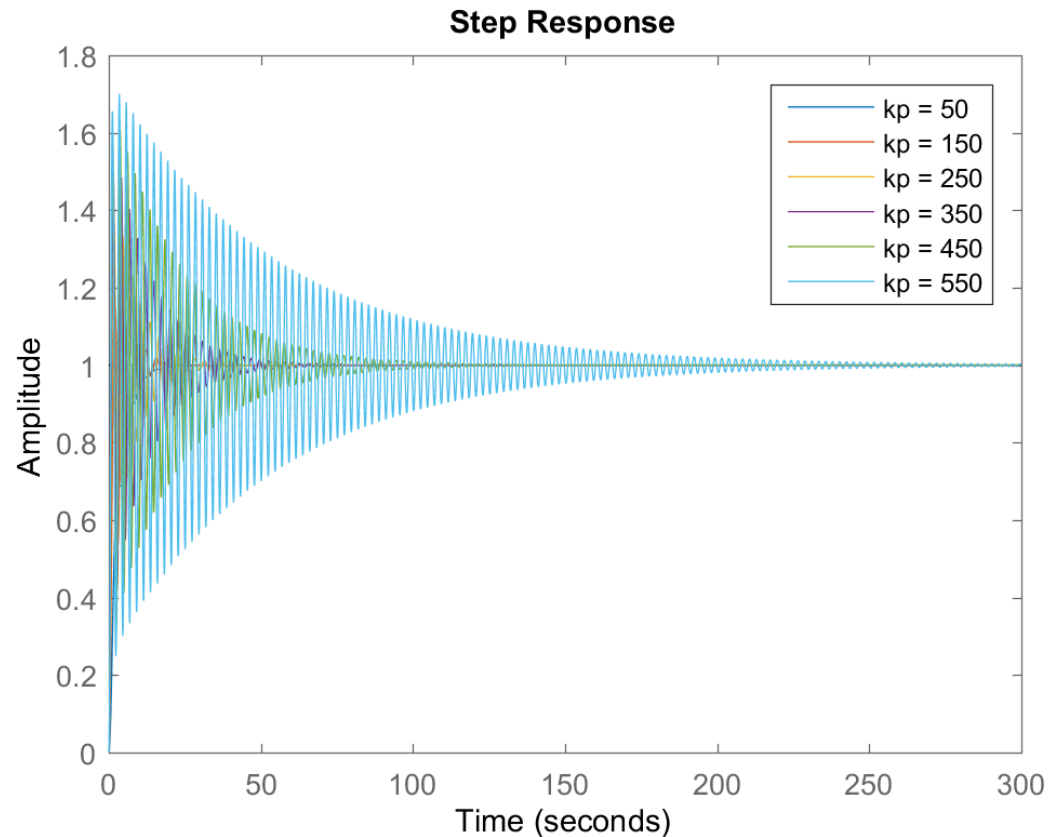




$k = 250 \text{ N/m}$  (zero just before the c.c. poles)

## Step response

20



Increasing the proportional gain  $k_p$  the damping ratio of the poles of the controlled system decreases thus increasing the maximum overshoot. The steady state error is null for any value of the gain.