

# A Numerical Study of Mesh Adaptivity in Multiphase Flows with Non-Newtonian Fluids

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APS DFD meeting  
Monday 24<sup>th</sup> November 2014  
San Francisco, California

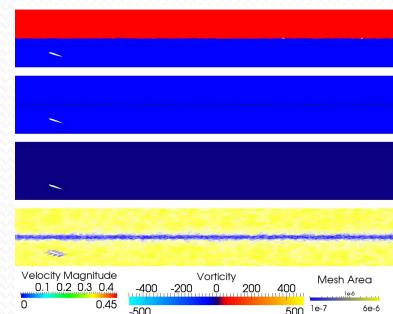
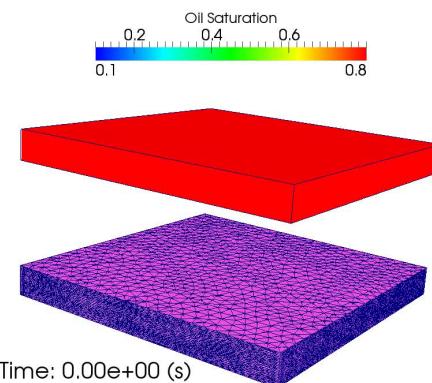
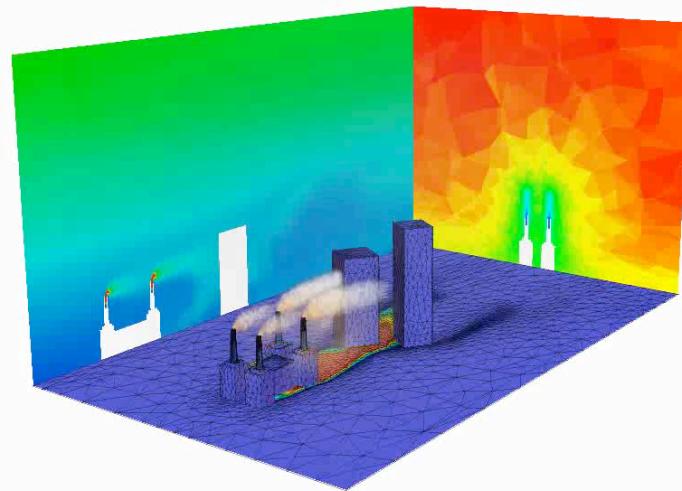




## Fluidity – a finite element flow simulator

- (CV)FEM based Navier-Stokes/Darcy flow solver framework
  - Mesh adaptivity capability on unstructured meshes
  - Parallelized [MPI/OpenMP]
  - Multimaterial & multiphase formulations (and both together)
  - Used for CFD, GFD and oil reservoir simulations

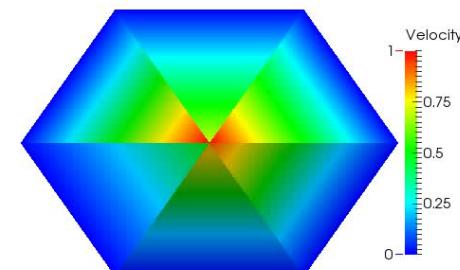
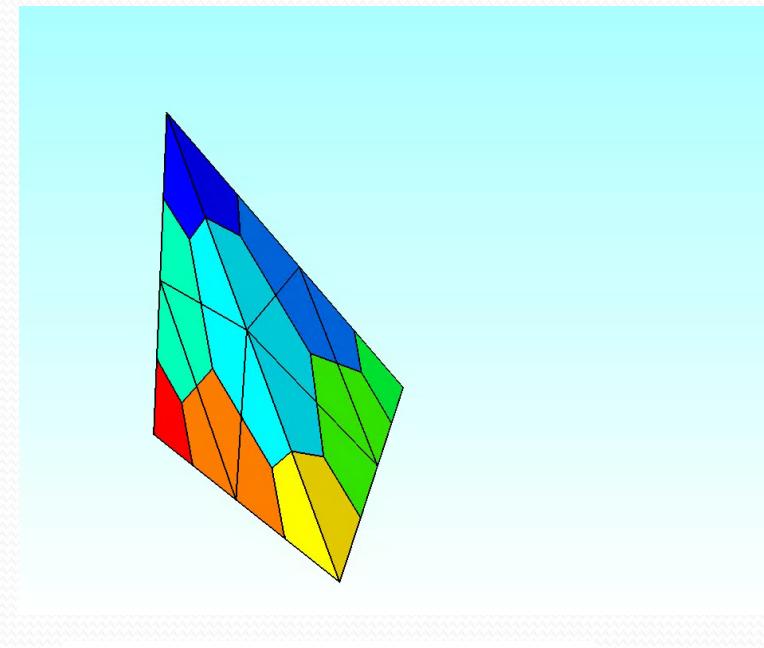
[www.fluidity-project.org](http://www.fluidity-project.org)





## Fluidity – multiphase implementation

- Volume of fluid (VOF) approach for interface capturing.
- Compressible advection for two phase ( $n$ -phase) indicator functions
- Optimized for unstructured mesh modeling on simplices (triangles & tetrahedra).
- Control volume- finite element method
  - Control volumes [phase indicator functions/phase volume fraction]
  - Finite elements [pressure/velocity]
- Surface tension also implemented  
[Z. Xie. **R33.1**]
- Multiple Rheologies:
  - Power law/Herschel Bulkley
  - Carreau
  - Viscoelastic (Oldroyd – B)



Pavlidis et. al *IJMF*(2014)  
Xie et al. *IJMF* (2014)  
Percival et al. *IJMF* (2014)

# Fluidity – multiphase implementation

## Equation Set

momentum

$$\frac{\partial \rho \mathbf{u}}{\partial t} + \rho \mathbf{u} \cdot \nabla \mathbf{u} = -\nabla p + \rho \mathbf{g} + \mathbf{F}_{\text{visc}}$$

mass continuity

$$\frac{\partial \rho}{\partial t} + \nabla \cdot \rho \mathbf{u} = 0$$

Indicator function

$$\begin{aligned} \rho &= \rho(\mathbf{I}) & \frac{\partial I_i}{\partial t} + \mathbf{u} \cdot \nabla I_i &= 0 \\ \mathbf{F}_{\text{visc}} &= \mathbf{F}_{\text{visc}}(\mathbf{I}) \end{aligned}$$

Implying either:

$$\nabla \cdot \mathbf{u} = 0$$

(incompressible)

$$p = \rho^2 \frac{\partial e}{\partial \rho}$$

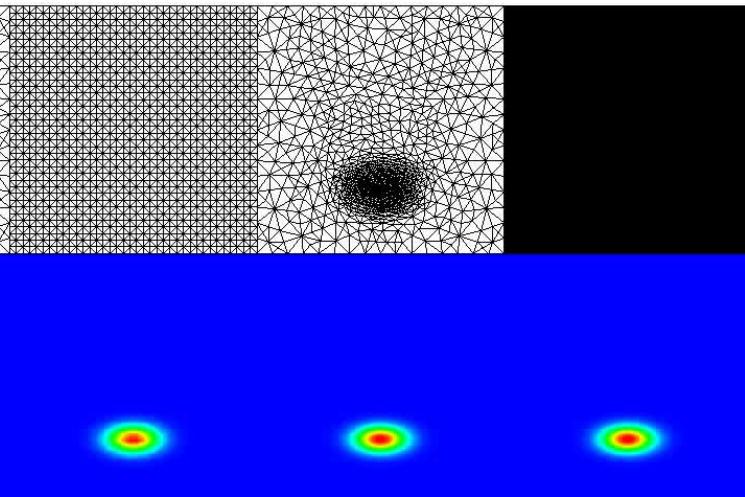
(compressible)

$$\mathbf{F}_{\text{visc}} = \begin{cases} \nabla \cdot \mu \mathcal{D} & \text{Newtonian} \\ \nabla \cdot \mu_{\text{eff}}(\mathcal{D}) \mathcal{D} & \text{Shear Dependent} \\ \nabla \cdot \underline{\tau} \quad \underline{\tau} := \underline{\tau}(t, \mathbf{x}, \mathbf{u}) & \text{Viscoelastic} \end{cases} \quad \mathcal{D}_{ij} = \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} - \frac{2\delta_{ij}}{3} \nabla \cdot \mathbf{u} \right)$$



## Mesh Adaptivity - examples

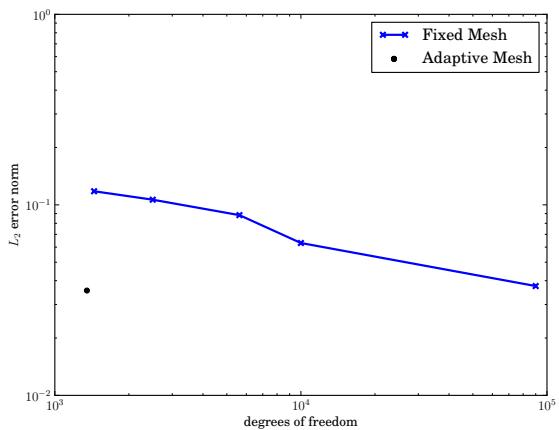
Initial adaptive mesh      Fixed mesh 1      Adaptive mesh      Fixed mesh 2



Analytic solution      Fixed mesh 1      Adaptive mesh

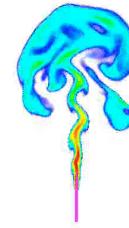
Fixed mesh 2

2 orders of magnitude smaller problem/half error



30x speed up

Time: 4.71



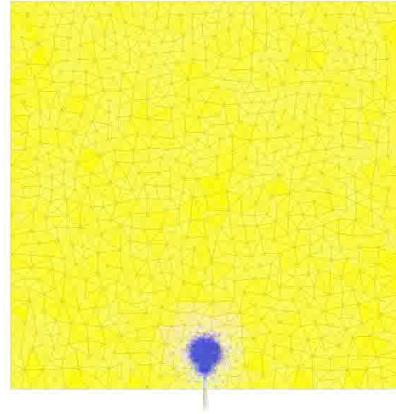
Helium Mass Fraction (g/g)  
0 0.25 0.5 0.75 1

Time: 5.45



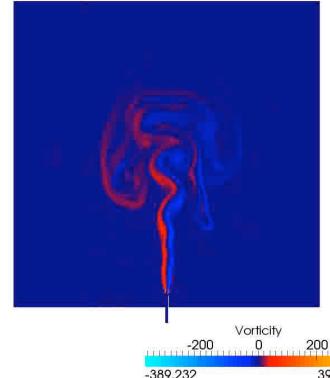
Potential Temperature (K)  
29.84591 100 200 301.0877

Time: 1.91



Element area  
0.0001 0.001 0.01  
6.788e-5 0.145369

Time: 5.23



Vorticity  
-389.232 0 390.8497



# Mesh Adaptivity– Interpolation Error estimates

Motivation: Céa's Lemma

$$\begin{aligned} \text{error} &:= \|\psi^{\text{exact}} - \psi^\delta\| \leq C_1 \|\psi^{\text{exact}} - \psi^{\text{proj}}\| \\ &\leq C_2 \sum_i h_i^2 \max_{x \in \Omega} \left| \frac{\partial^2 \psi}{\partial x^2} \right| \end{aligned}$$

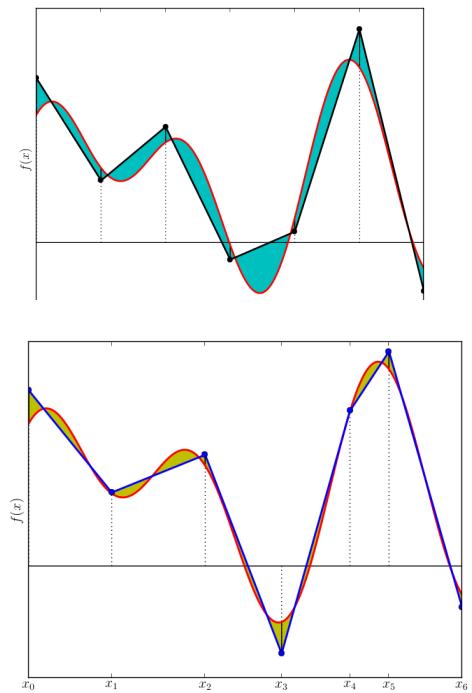
In higher dimensions, error estimate is a function of the Hessian matrix and the edge vectors.

$$\mathcal{H}(\psi) = \begin{pmatrix} \frac{\partial^2 \psi}{\partial x^2} & \frac{\partial^2 \psi}{\partial x \partial y} & \frac{\partial^2 \psi}{\partial x \partial z} \\ \frac{\partial^2 \psi}{\partial x \partial y} & \frac{\partial^2 \psi}{\partial y^2} & \frac{\partial^2 \psi}{\partial y \partial z} \\ \frac{\partial^2 \psi}{\partial x \partial z} & \frac{\partial^2 \psi}{\partial y \partial z} & \frac{\partial^2 \psi}{\partial z^2} \end{pmatrix}$$

$$\begin{aligned} \text{error} &\sim \sum_k \mathbf{v}_k^T \mathcal{M} \mathbf{v}_k \\ \mathcal{M} &= \mathcal{M}(\mathcal{H}(\psi)) \end{aligned}$$

“Mesh metric”

For sufficiently nice PDEs and linear (or better) elements





## Mesh Adaptivity – Interpolation Error Estimates

**Problem:** we don't know  $\psi^{\text{exact}}$

Answer: Use old  $\psi^\delta$  instead.

Estimate second derivatives  
from the finite element data

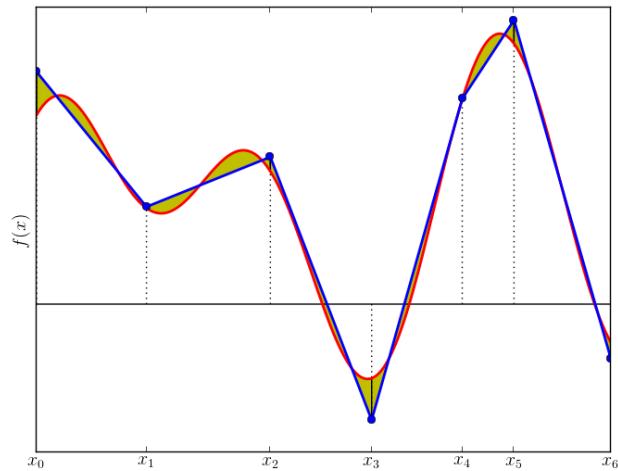
Try to extremize

$$I(\mathbf{v}) = \sum_k \frac{1}{\epsilon} \mathbf{v}_k^T \mathcal{M} \mathbf{v}_k - 1$$

Where the  $\mathbf{v}$ s are the edges of the mesh

Additional constraints for

- Bounds on min/max edge lengths
- Gradation of the increase
- Aspect ratios
- Metric advection



$$\mathcal{M} = \mathcal{M}(\mathcal{H}(\psi^\delta))$$

# Mesh Adaptvity: Error Estimate Optimization

Local remeshing algorithm. Preserve the old mesh in regions where it is adequate.

Apply  $hr$  adaptivity in the regions where fixing is necessary: Add, remove nodes, reconnect nodes and move nodes.

Algorithm works iteratively, attacking areas in which edge lengths are far from the ideal calculated from interpolation error estimate and freezing sufficiently good elements.

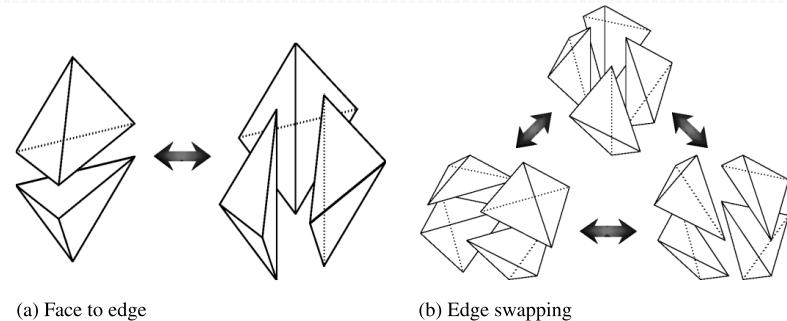


Fig. 1. Diagram showing: (a) edge to face and face to edge swapping; (b) edge to edge swapping with four elements.

Pain, Umpleby, de Oliveira & Goddard,(2001).  
Tetrahedral mesh optimisation and adaptivity for steady-state and transient finite element calculations,  
*Computer Method in Applied Mechanics & Engineering*

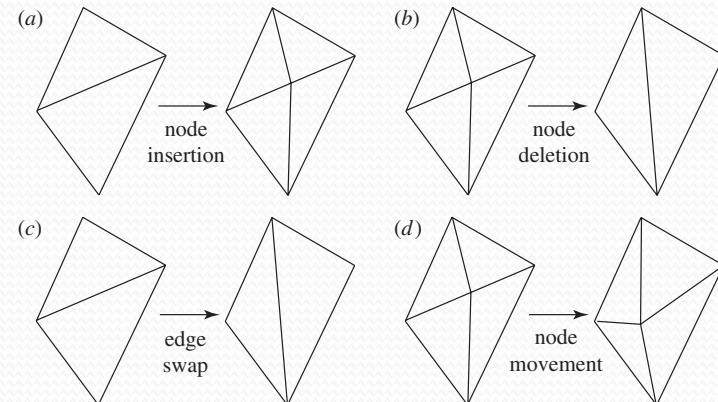
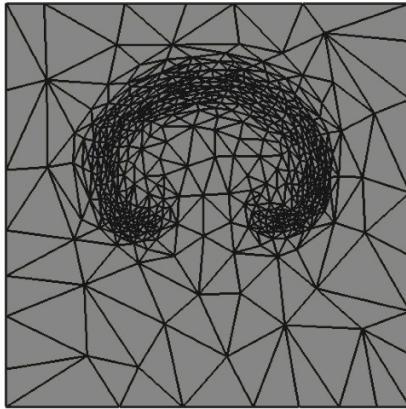
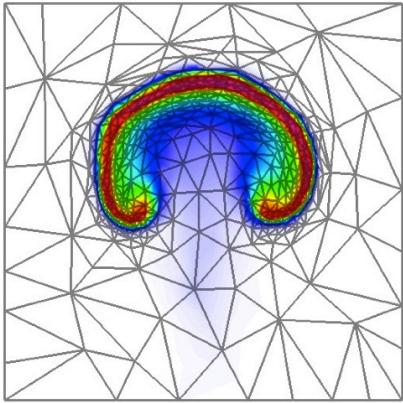


Figure 1. Local element operations used to optimize the mesh in two dimensions. (a) Node insertion or edge split. (b) Node deletion or edge collapse. (c) Edge swap. (d) Node movement.

Piggott, Farrell, Wilson, Gorman & Pain (2009)  
Anisotropic mesh adaptivity for multi-scale ocean modelling  
*Philosophical Transactions of the Royal Society A*



## Mesh to mesh interpolation - supermeshing



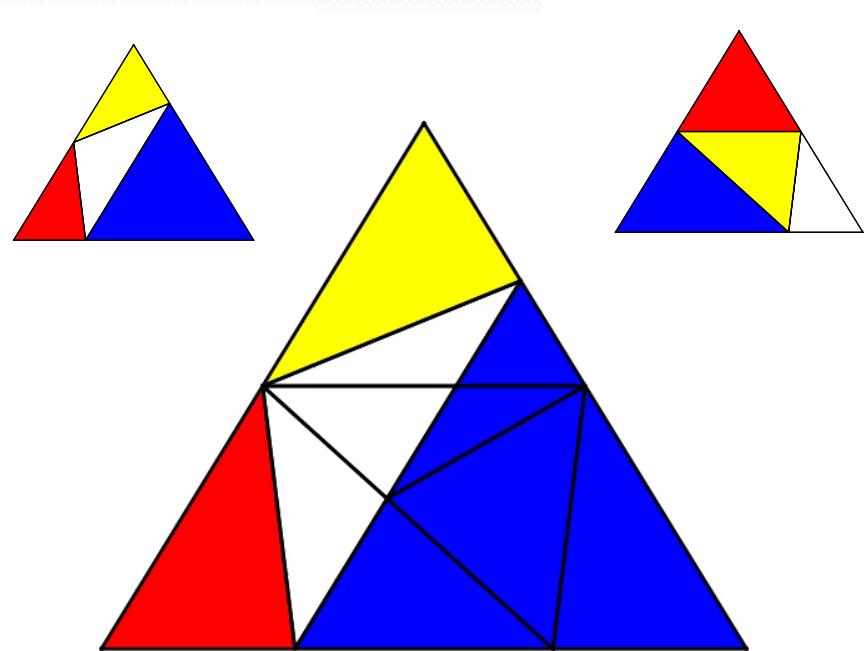
FE solutions/test functions piecewise smooth over mesh elements

Elements of supermesh: old variables and new test fns both smooth.

No jumps.

Allows efficient conservative mesh to mesh interpolation via projection methods

$$\sum_j \int_{\Omega} N_i^{\text{new}} N_j^{\text{new}} \psi_j^{\text{new}} dV = \sum_k \int_{\Omega} N_i^{\text{new}} N_k^{\text{old}} \psi_k^{\text{old}} dV$$



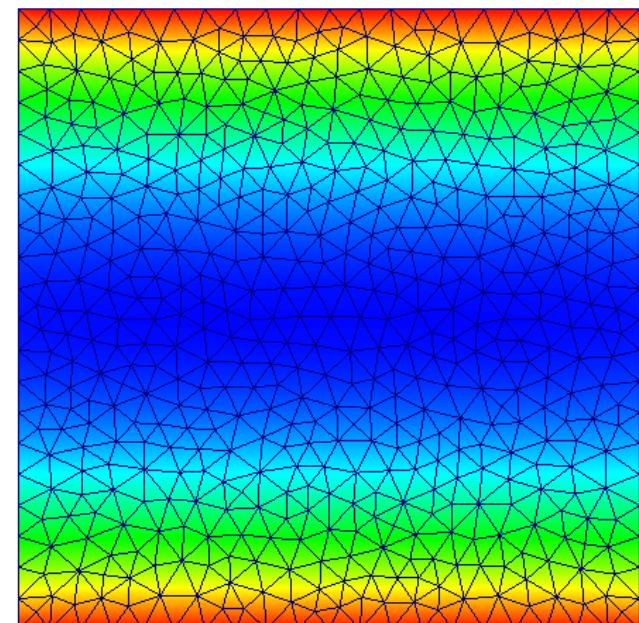
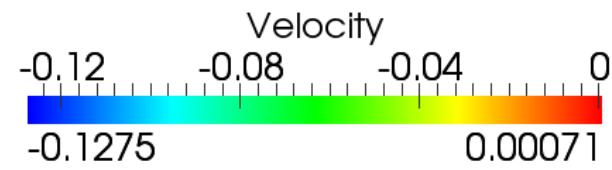
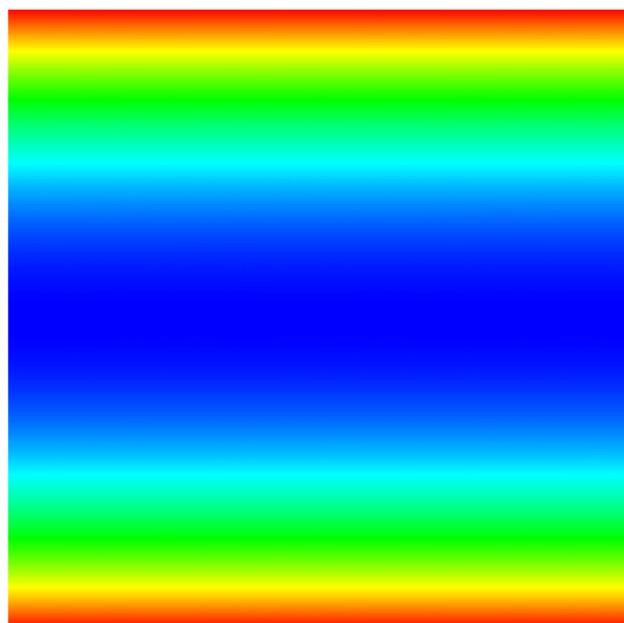
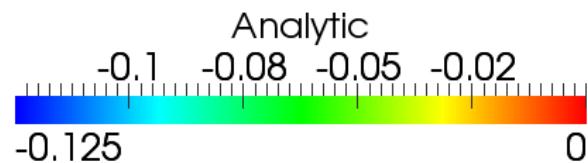
P. E. Farrell & J. R. Maddison (2011)  
Computer Methods in Applied Mechanics and Engineering

## Single Phase Newtonian flow

Spin up from  
Pressure differential

$$u(y) = -\frac{1}{2\mu} \frac{\partial p}{\partial x} (h^2 - y^2)$$

### Single phase laminar channel flow





## Two phase Newtonian flow

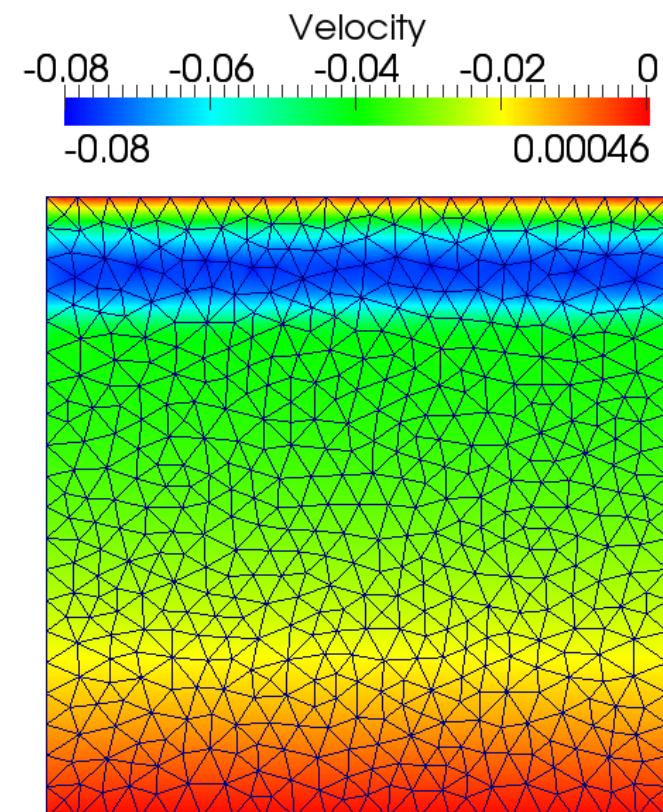
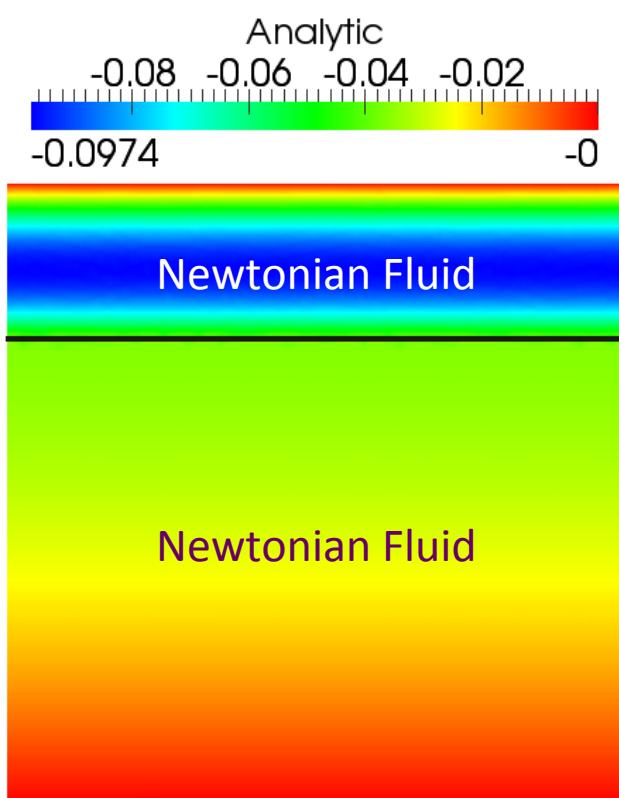
multiphase laminar channel flow

Spin up from  
Pressure differential

$$c_0 = \frac{1}{2} \left[ \frac{(\mu_1 - \mu_0) h_c^2 + \mu_0 h^2}{(\mu_1 - \mu_0) h_c + \mu_0 h} \right]$$

$$u(y) = -\frac{1}{2\mu_0} \frac{\partial p}{\partial x} [2c_0y - y^2]$$

$$u(y) = -\frac{1}{2\mu_1} \frac{\partial p}{\partial x} [2c_0(y-h) + h^2 - y^2]$$





## Two phase Newtonian flow

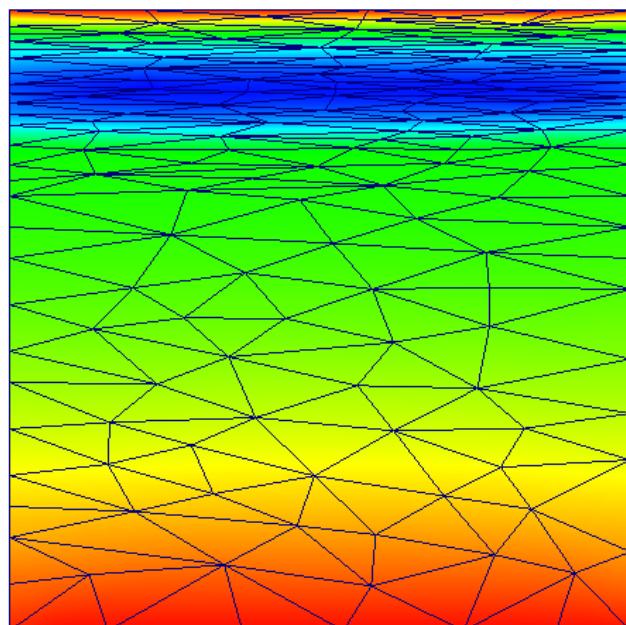
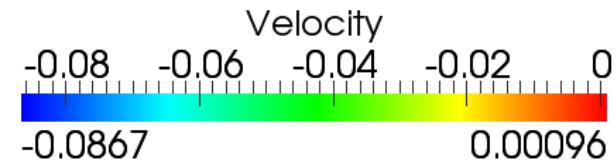
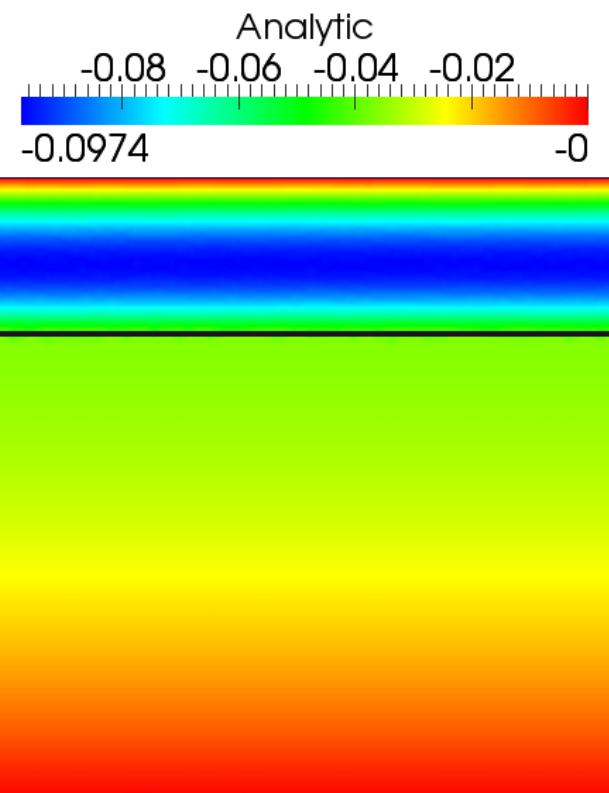
multiphase laminar channel flow

Spin up from  
Pressure differential

$$c_0 = \frac{1}{2} \left[ \frac{(\mu_1 - \mu_0) h_c^2 + \mu_0 h^2}{(\mu_1 - \mu_0) h_c + \mu_0 h} \right]$$

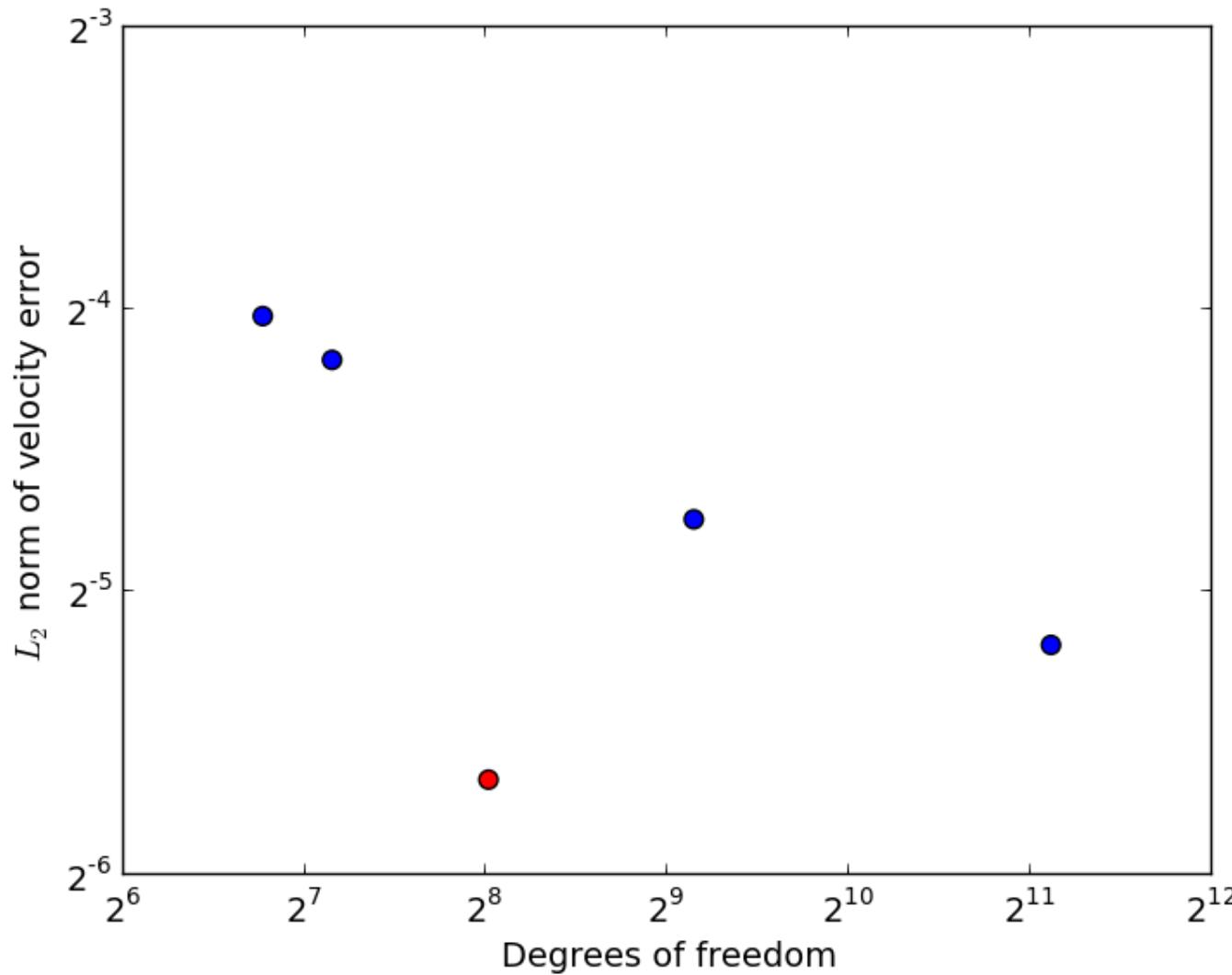
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$$u(y) = -\frac{1}{2\mu_1} \frac{\partial p}{\partial x} [2c_0(y-h) + h^2 - y^2]$$

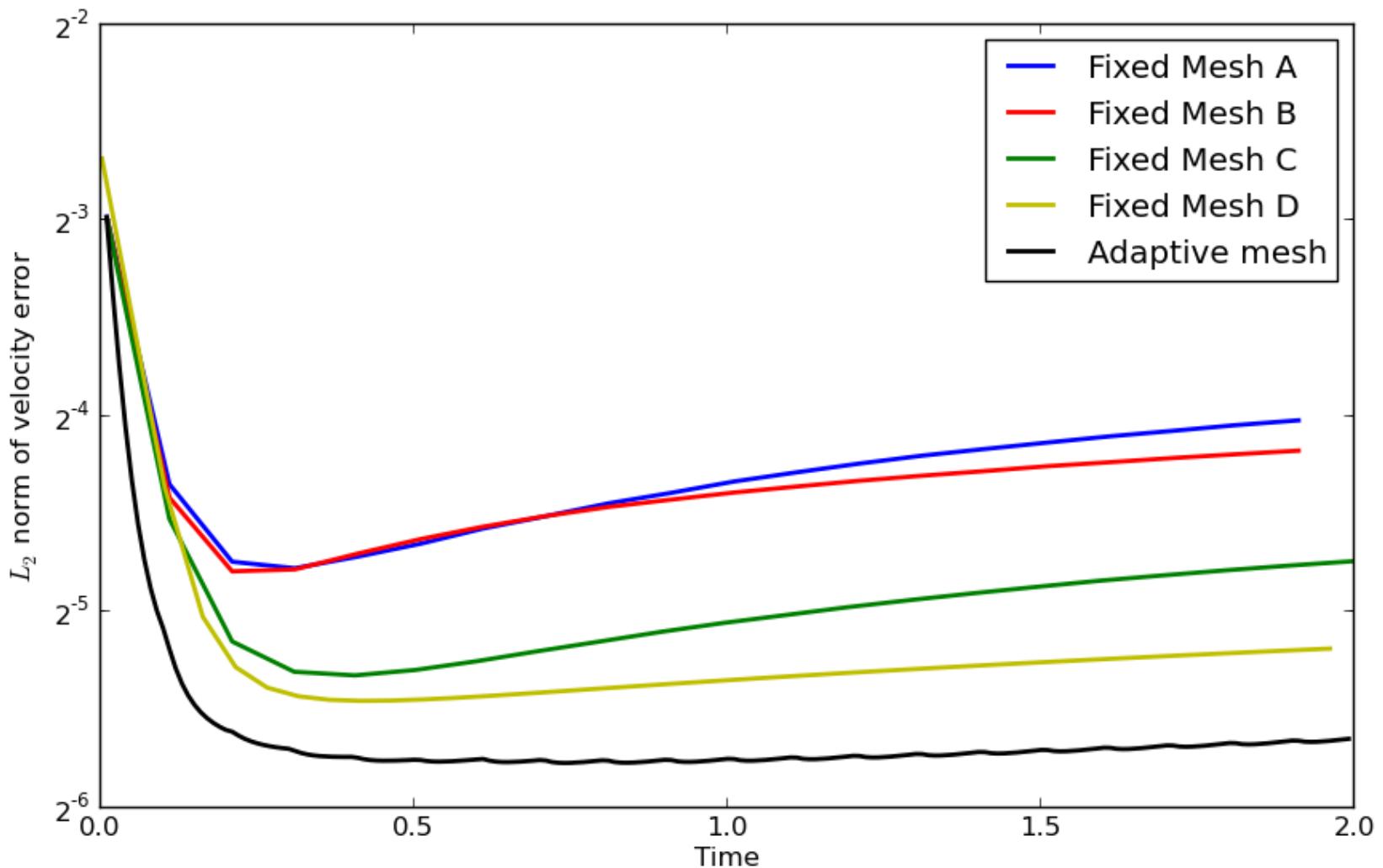




## Convergence rates and error reduction



## Temporal convergence to steady state

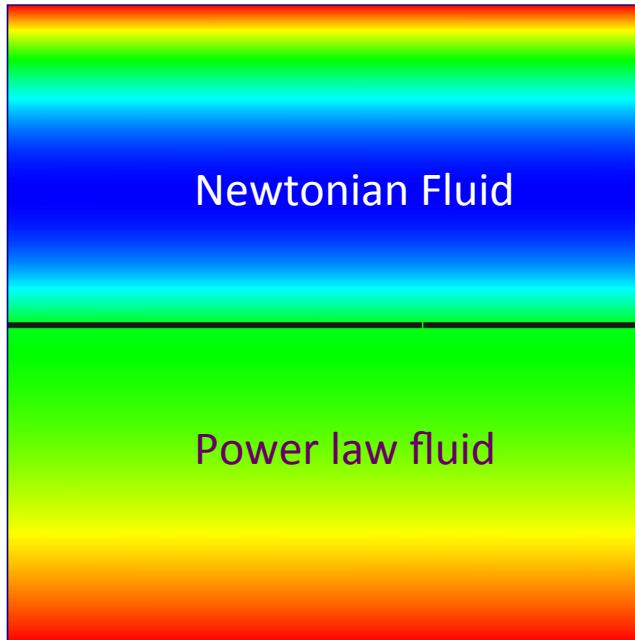
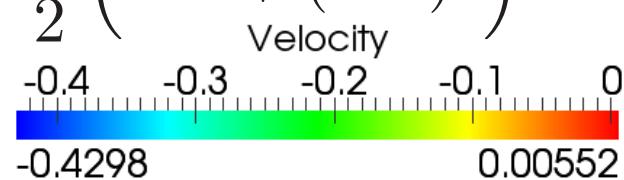
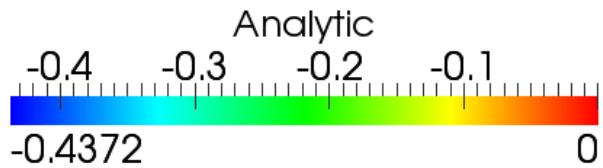




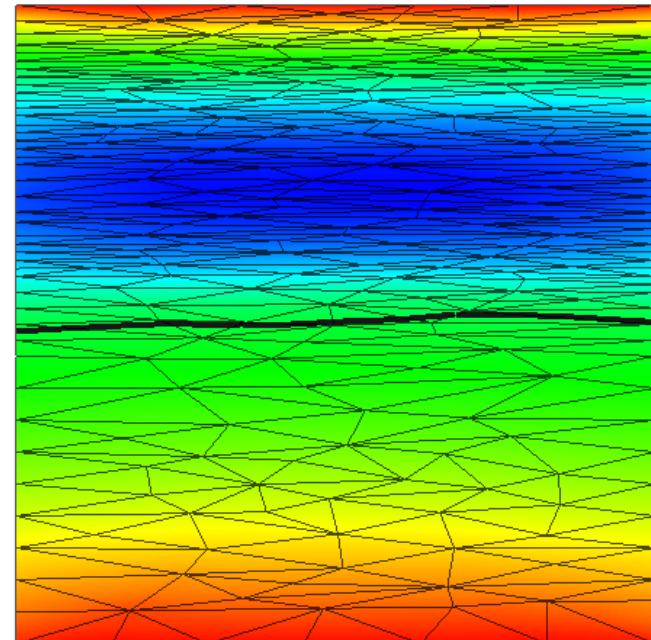
## Non-Newtonian Rheologies

multiphase laminar channel flow : power law

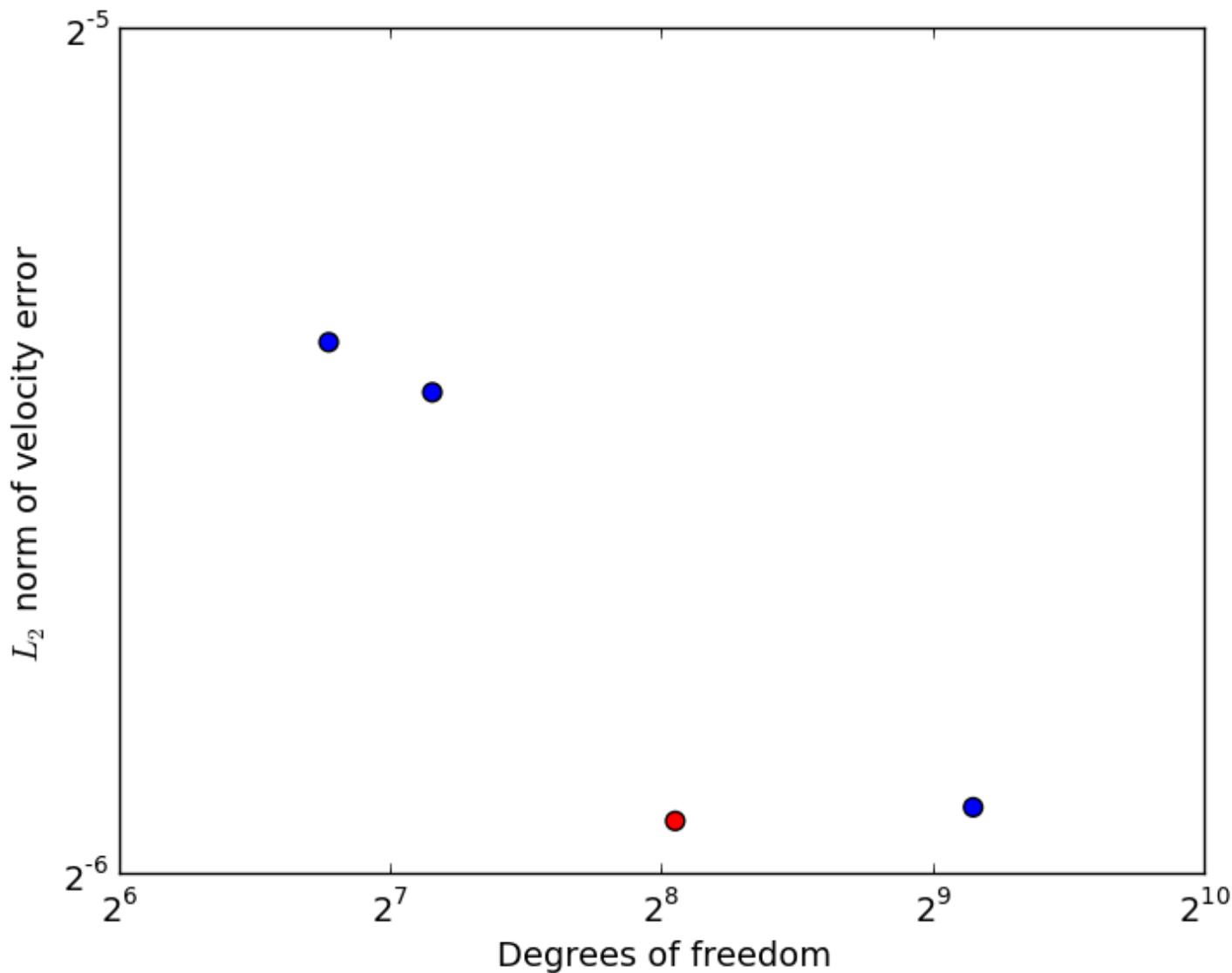
$$\mu_{\text{eff}} = k(2\mathcal{D}_{mn}\mathcal{D}^{mn})^{\frac{n-1}{2}} \quad \mathcal{D} = \frac{1}{2} \left( \nabla \mathbf{u} + (\nabla \mathbf{u})^T \right)$$



$$u(y) = \begin{cases} \frac{n}{n+1} \left[ \frac{1}{k} \frac{dp}{dx} \right]^{\frac{1}{n}} \left( |y - c|^{\frac{n+1}{n}} - |c|^{\frac{n+1}{n}} \right) & y \geq h_c \\ \frac{1}{\mu_b} \frac{dp}{dx} \left( \frac{(y^2 - h^2)}{2} - c(y - h) \right) & y < h_c \end{cases}$$



## Convergence rates and error reduction

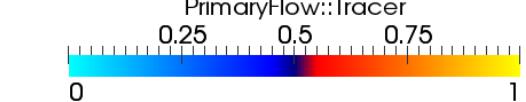
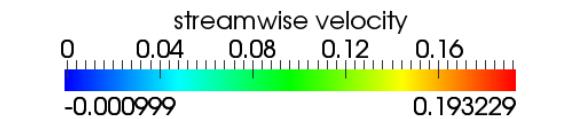
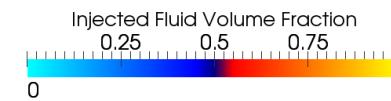
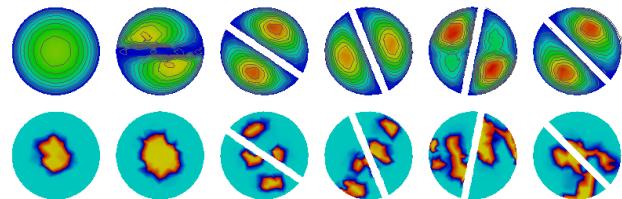
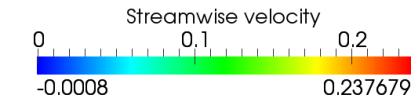
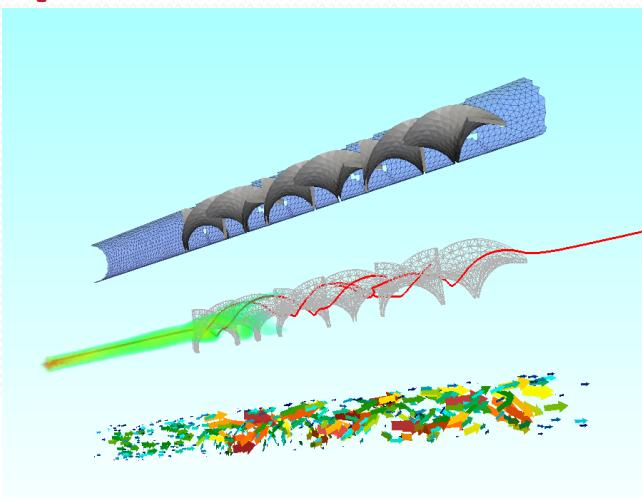
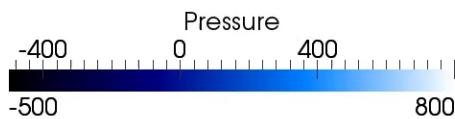




# Carreau fluids



## 3D problems in non-idealized geometries



# Other Rheologies

- viscoelastic stress model
    - Oldroyd B
      - Adds fluid memory term
      - Includes rotational terms for convection of local coordinate
- ## Polymers & Boger fluids

$$\frac{\partial}{\partial t} (\rho \mathbf{u}) + \nabla \cdot \rho \mathbf{u} \mathbf{u} = -\nabla p - \rho \mathbf{g} + \nabla \cdot \left( \mu_s \left[ \nabla \mathbf{u} + (\nabla \mathbf{u})^T - \frac{2}{3} \underline{\mathbf{I}} \nabla \cdot \mathbf{u} \right] + \underline{\boldsymbol{\tau}_p} \right)$$
$$\frac{\partial \underline{\boldsymbol{\tau}_p}}{\partial t} + \mathbf{u} \cdot \nabla \underline{\boldsymbol{\tau}_p} - \left[ (\nabla \mathbf{u})^T \cdot \underline{\boldsymbol{\tau}_p} + \underline{\boldsymbol{\tau}_p} \cdot \nabla \mathbf{u} \right] = \frac{1}{\lambda_1} \left[ \mu_p \left[ \nabla \mathbf{u} + (\nabla \mathbf{u})^T - \frac{2}{3} \underline{\mathbf{I}} \nabla \cdot \mathbf{u} \right] - \underline{\boldsymbol{\tau}_p} \right]$$



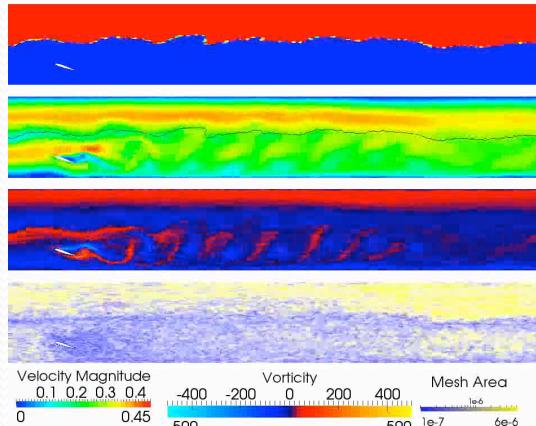
## Upcoming MEMPHIS talks @ APS-DFD



**Studies of Interfacial Perturbations  
in Two Phase Oil-Water Pipe Flows  
Induced by a Transverse Cylinder**

Dr. Maxime  
Chinaud

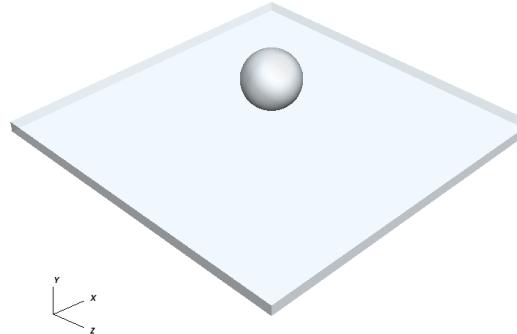
**M22.8**



**Numerical study of Taylor  
bubbles with adaptive  
unstructured meshes**

Dr. Zhihua  
Xie

**R33.1**



**Optimisation of sensor  
locations for falling film  
problems based on  
importance maps**

Dr. Zhizhao  
Che

**R35.9**

