

# Supporting Information: Improvements and limitations of Mie $\lambda$ -6 potential for prediction of saturated and compressed liquid viscosity

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## SI.I. Input files

We provide example input files for simulating 2,2,4-trimethylpentane at 245 K with the Potoff force field in GROMACS (see attached .gro, .top, and .mdp files). Additionally, all files necessary to generate the results from this study can be found at [www.github.com/ramess101/IFPSC\\_10](http://www.github.com/ramess101/IFPSC_10).

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## SI.II. Systems simulated

Table [SI.I](#) enumerates the compounds, force fields, and viscosity types simulated in this study.

Table SI.I: Compounds, force fields, and state points. “X”: simulated, “O”: not simulated, “S” simulated with “short” parameters, “L” simulated with “long” parameters.

Compound	TraPPE (TraPPE-2)		Potoff (S/L)		AUA4		TAMie	
	$\eta_{\text{liq}}^{\text{sat}}$	$\eta_{\text{liq}}^{\text{comp}}$	$\eta_{\text{liq}}^{\text{sat}}$	$\eta_{\text{liq}}^{\text{comp}}$	$\eta_{\text{liq}}^{\text{sat}}$	$\eta_{\text{liq}}^{\text{comp}}$	$\eta_{\text{liq}}^{\text{sat}}$	$\eta_{\text{liq}}^{\text{comp}}$
ethane	X (X)	X (X)	X	X	X	X	X	X
propane	X	X	X	X	O	O	X	X
<i>n</i> -butane	X	X	X	X	O	O	X	X
<i>n</i> -octane	X	X	X	X	O	O	X	X
<i>n</i> -dodecane	X	O	X	O	O	O	X	O
<i>n</i> -hexadecane	X	O	X	O	O	O	X	O
2-methylpropane	X	X	S	S	O	O	X	X
2-methylbutane	X	X	S	S	O	O	X	X
2,2-dimethylpropane	X	X	S	S	X	X	O	O
2,3-dimethylbutane	X	X	S	S	O	O	X	X
2-methylpentane	X	X	L	L	O	O	X	X
3-methylpentane	X	X	L	L	O	O	X	X
2,2,4-trimethylpentane	X	X	L	L	O	O	O	O

### SI.III. Additional simulation details

Table [SI.II](#) lists the integrators, thermostats, and barostats used for each *NPT* or *NVT* stage.

Table SI.II: Integrator, thermostat and barostat specifications.

	<i>NPT</i> Equil.	<i>NPT</i> Prod.	<i>NVT</i> Equil.	<i>NVT</i> Prod.
Integrator	Velocity Verlet	Leap frog	Velocity Verlet	Velocity Verlet
Thermostat	Velocity rescale	Nosé-Hoover	Nosé-Hoover	Nosé-Hoover
Thermostat time-constant (ps)	1.0	1.0	1.0	1.0
Barostat	Berendsen	Parrinello-Rahman	N/A	N/A
Barostat time-constant (ps)	1.0	5.0	N/A	N/A
Barostat compressibility (1/bar)	4.5E-5	4.5E-5	N/A	N/A

## SI.IV. Simulation time

For less viscous systems, i.e., saturation and low pressures, a 1 ns simulation is typically sufficient for the Green-Kubo integral to reach a plateau. However, even when there is an apparent plateau, systematic bias in  $\eta$  may still exist if the simulation is too short [1, 2]. For this reason, Figure SI.1 compares the Green-Kubo integral for simulations with 0.5 ns, 1 ns, 2 ns, and 4 ns. We observe that the estimated viscosity obtained from a 1 ns trajectory is consistent with that from 2 ns and 4 ns simulations. Specifically, a plateau is observed at a similar value of  $\eta$  despite the large fluctuations at long times. We also note that 0.5 ns simulations are typically reliable but occasionally the plateau deviates considerably. For these reasons, the results presented in this study were obtained from 1 ns simulations.

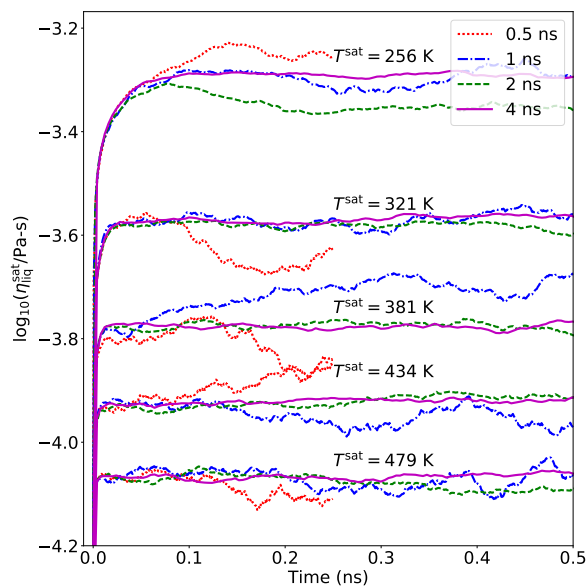


Figure SI.1: Simulation production time. Simulations were performed for *n*-octane using the TraPPE potential. Colors/line styles denote different simulation times (0.5 ns, 1 ns, 2 ns, and 4 ns).

For more viscous systems (greater than 0.02 Pa-s) a 1 ns simulation is too short to observe a plateau in the Green-Kubo integral. In these cases, we increase the simulation time to a value between 2 and 8 ns. Due to the increased computational cost of such simulations, we did not perform an exhaustive test with increasing simulation time. Instead, the choice of simulation time was determined primarily by the ability to detect a plateau region. Therefore, it is possible that even longer simulations are required for the most viscous systems.

Figure SI.2 depicts the Green-Kubo integral with respect to time for these highly viscous systems (note that the total simulation time is twice the maximum time plotted). For example, an 8 ns run appears to be sufficient to detect a plateau for 2,2,4-trimethylpentane with Potoff at 750 MPa, while 16 ns are required for 2,2,4-trimethylpentane with Potoff at 1000 MPa. This demonstrates that it is possible to obtain reasonable estimates for systems with viscosities much greater than 0.02 Pa-s. However, the bootstrap uncertainty is significantly larger for these more viscous systems.

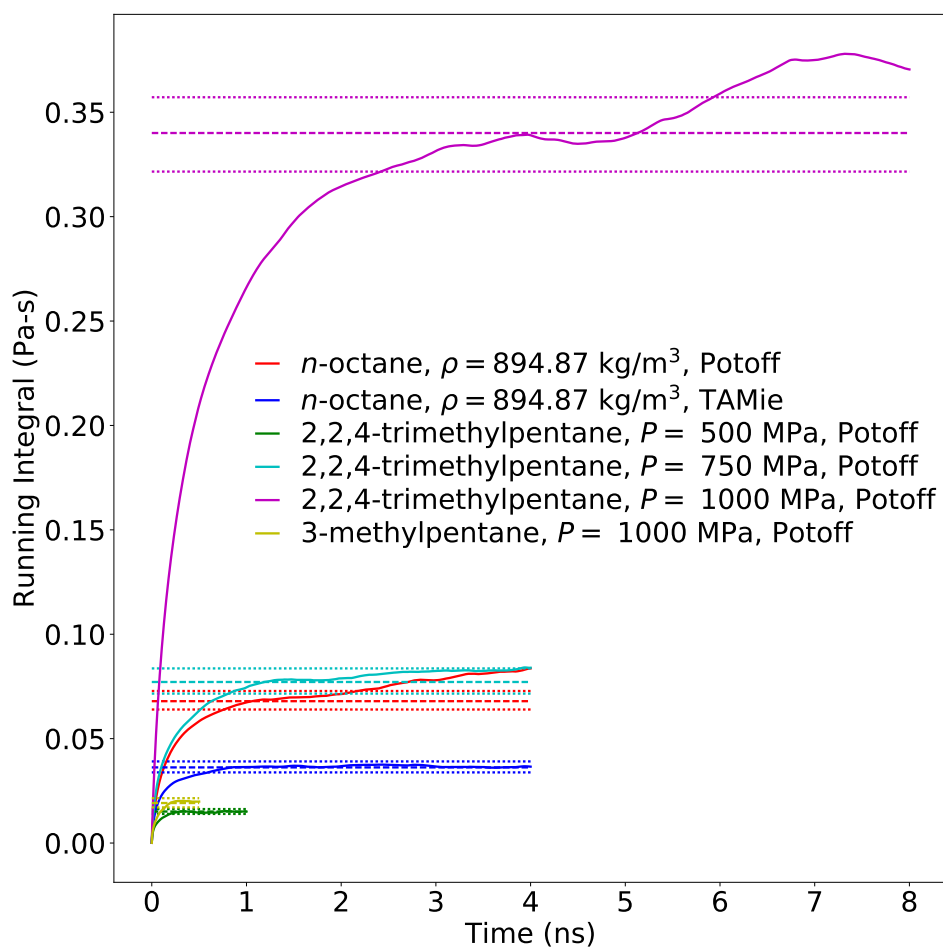


Figure SI.2: Green-Kubo integrals for the most viscous systems studied. Solid lines are the average of  $N_{\text{reps}}$  replicates. Dashed lines are the estimated  $\eta$  value after fitting. Dotted lines represent the 95 % bootstrapped uncertainties.

## SI.V. Fixed vs flexible bonds

Although static thermodynamic properties (e.g.,  $\rho_{\text{liq}}^{\text{sat}}$ ) are generally insensitive to the choice of fixed or flexible bonds, dynamic properties (e.g.,  $\eta$ ) can be much more sensitive. We perform simulations with flexible bonds to test how sensitive the results presented in this study are to the use of fixed bond-lengths. Specifically, we use the traditional harmonic bond potential:

$$u^{\text{bond}} = \frac{k_{\text{b}}}{2} (r - r_{\text{eq}})^2 \quad (1)$$

where  $u^{\text{bond}}$  is the bonded potential,  $k_{\text{b}}$  is the harmonic force constant, and  $r_{\text{eq}}$  is the equilibrium bond-length. We use an arbitrarily large value for the force constant,  $k_{\text{b}}/k_{\text{B}} = 60.43 \text{ K/pm}^2$ , as this should result in a fairly stiff bonded potential, i.e., the bond-lengths should not vary significantly.

Figure [SI.3](#) demonstrates that the difference between fixed and flexible bonds is negligible in certain cases. However, there is a small, but systematic, deviation towards higher viscosities for the stiff harmonic potential.

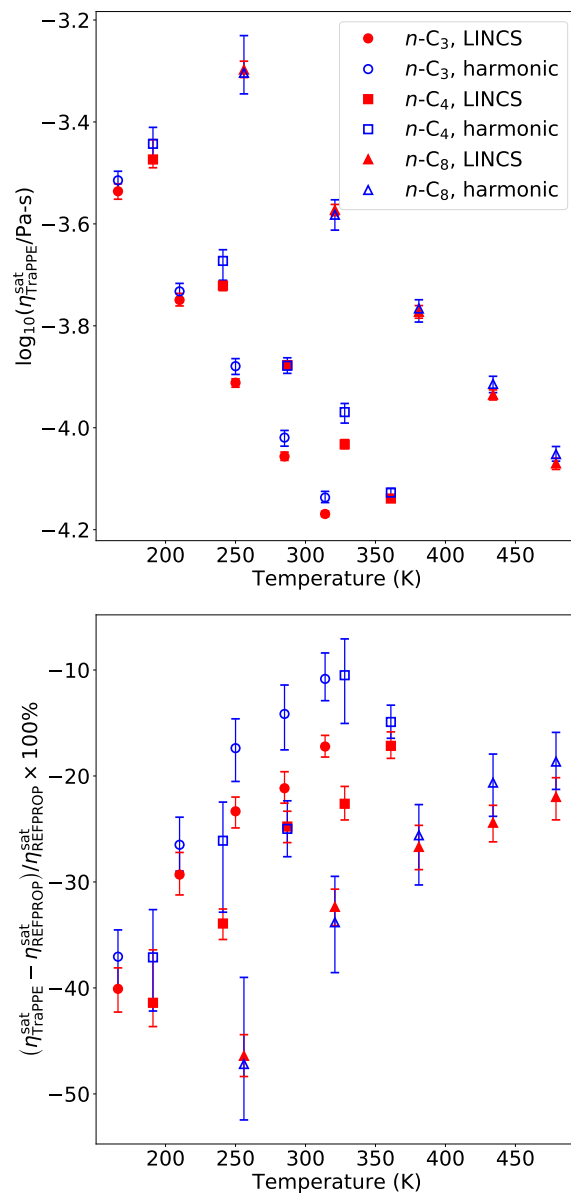


Figure SI.3: Fixed bond-lengths compared with an arbitrarily stiff harmonic bond potential. Simulations were performed using the TrapPE-UA force field. Colors/fill denote fixed or flexible bonds while symbol shape corresponds to different compounds.

## SI.VI. Green-Kubo analysis

This section provides a detailed example of how we obtain estimates for  $\eta$  and the corresponding uncertainty. The results depicted in Figures SI.4 through SI.7 are for propane with the Potoff model and  $T^{\text{sat}} = 166$  K. Figure SI.4 depicts a typical autocorrelation function (“enecorr.xvg” file) obtained by executing the GROMACS “energy -vis” command. By default, GROMACS partitions the complete simulation into twelve evenly sized time blocks. Therefore, the autocorrelation function in Figure SI.4 is the average of twelve different time origins.

GROMACS then performs a simple two-point trapezoidal integration of neighboring points to obtain the Green-Kubo integral. The Green-Kubo integral with respect to time is output in the “visco.xvg” file. Figure SI.5 presents the Green-Kubo integral from forty replicate simulations. Although a single replicate is often quite noisy at long times, the average of these replicates converges smoothly (see Figure SI.5).

Figure SI.6 shows that the fluctuations, or standard deviation, increases with time but is adequately modeled with  $At^b$ . The line labeled “cut-off” in Figures SI.5 and SI.6 is the time at which  $\sigma_\eta \approx 0.4 \times \eta^\infty$ . Data beyond this time are excluded from the fit of the double-exponential function.

Bootstrap re-sampling provides an estimate of the uncertainty. Figure SI.7 shows that, typically, the bootstrapped distribution is quite normal. The lines labeled “bootstraps” in Figure SI.5 are the lower and upper 95 % confidence interval.



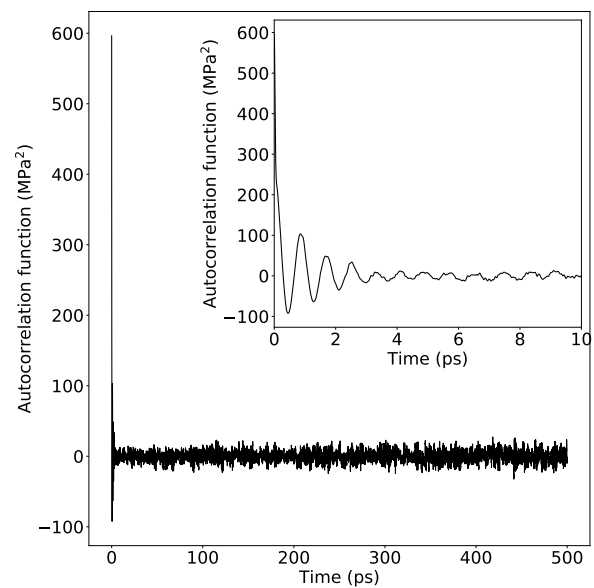


Figure SI.4: Autocorrelation function with respect to time.

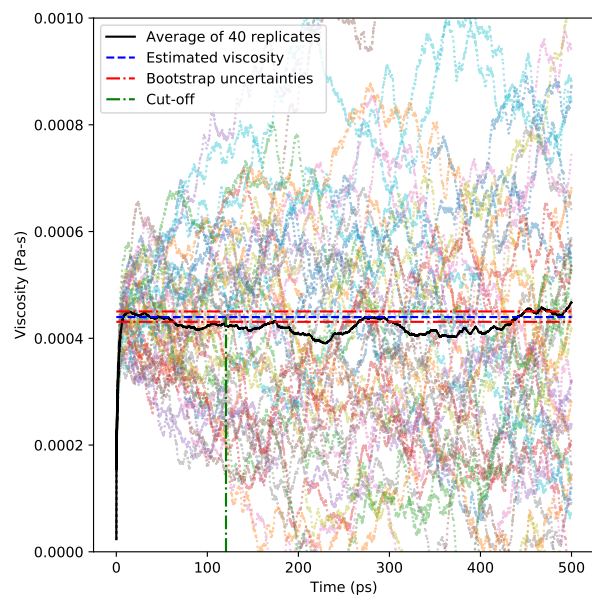


Figure SI.5: Replicate simulations, average, fit to average, bootstrap uncertainties, and cut-off.

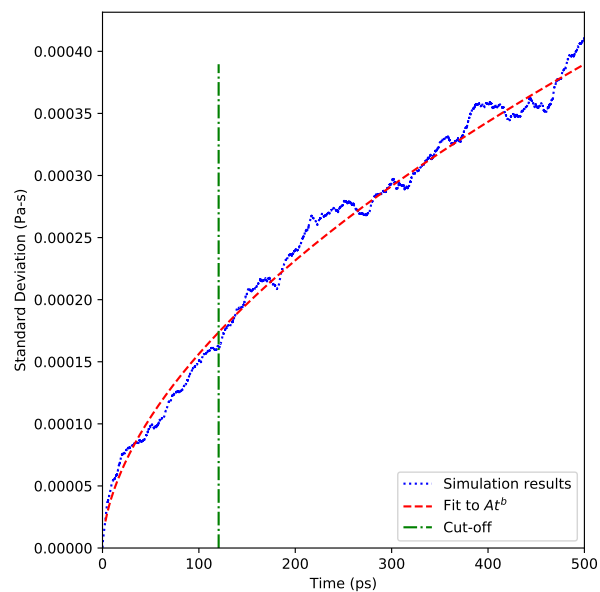


Figure SI.6: Standard deviation of replicate simulations with respect to time.

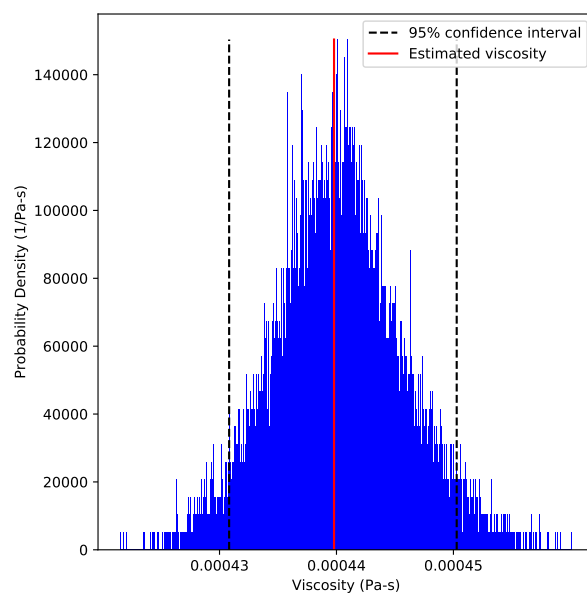


Figure SI.7: Bootstrap distribution of  $\eta$ .

## SI.VII. Validation Runs

To validate our approach, we attempt to replicate viscosity estimates available on the NIST Standard Reference Simulation Website [3] for TraPPE-UA ethane as well as literature values for TraPPE-UA *n*-octane [4, 5]. Figures SI.8 and SI.9 compare the ethane and *n*-octane results, respectively. The *n*-octane validation is somewhat more useful than the ethane validation for at least three reasons. First, *n*-octane includes angle and torsional contributions that are absent in ethane. Second, the literature provides values for both rigid and flexible bonds. Third, the *n*-octane results are at elevated pressures, which provides validation of our *NPT* ensemble results.

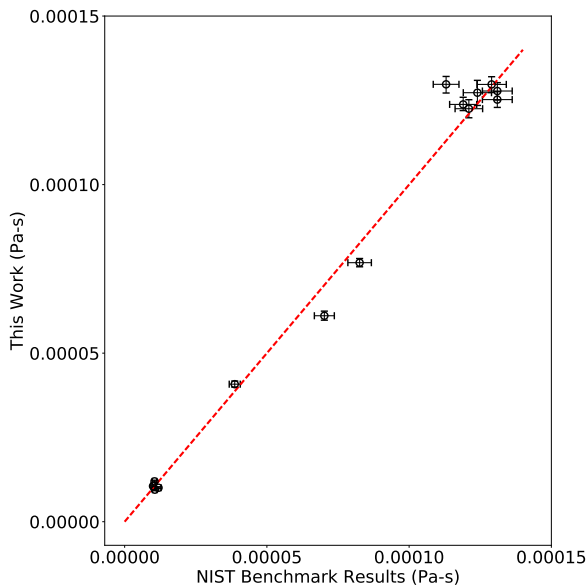


Figure SI.8: Comparison with NIST Standard Reference Simulation benchmark data for TraPPE ethane [3]. Red line corresponds to  $x = y$ , i.e., exact agreement between this work and the NIST values. A constant uncertainty of 4 % is assumed for NIST values.

Figure SI.8 demonstrates that our results are consistent with the NIST Reference Simulation Data at higher densities, with some discrepancies at lower densities. Note that the NIST Standard Reference Simulation benchmark data were obtained with the *NVE* ensemble, while our simulations were performed with the *NVT* ensemble at the average  $T$  reported on the NIST website. Also, the NIST simulations used 500 molecules, 250 ps production time, and a 0.5 fs time-step.

Figure SI.9 demonstrates that our results agree with the literature values for TraPPE *n*-octane at high pressures. Note that our flexible bond results utilize the same harmonic potential as Reference 4 ( $k_b/k_B = 45.29$  K/pm<sup>2</sup>, value actually reported in Reference 6). Thus, by comparing

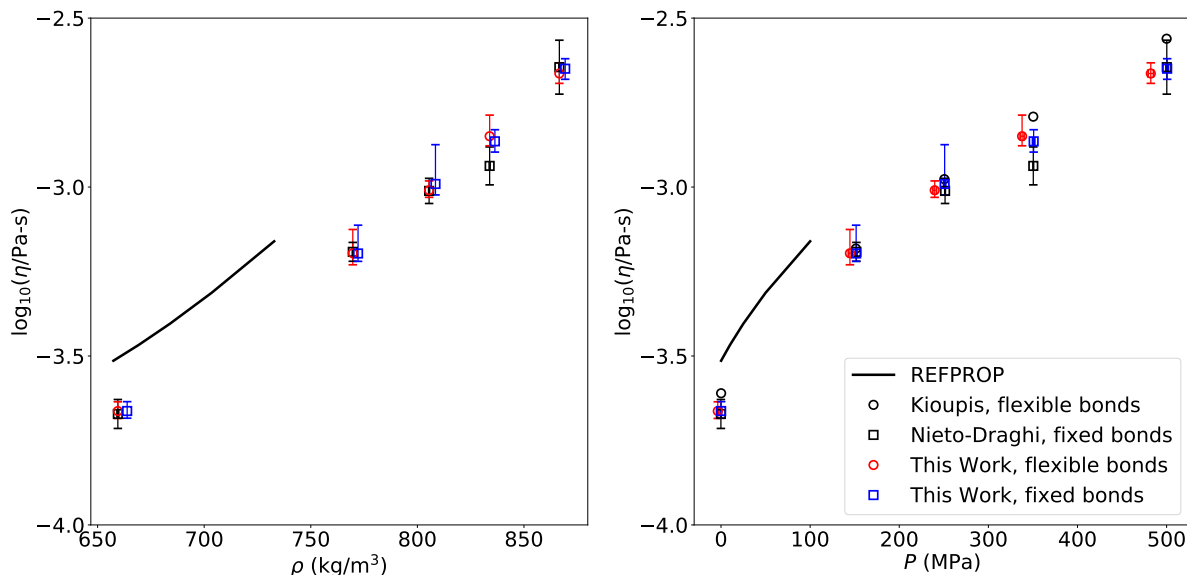


Figure SI.9: Comparison with Kioupis [4] and Nieto-Draghi [5] results for TraPPE *n*-octane. Circle symbols were obtained with the same harmonic potential, while square symbols denote fixed bond-lengths.

the circular points, there is an apparent positive bias between the Reference 4 values and those from this work. We note that Reference 4 utilizes NEMD simulations, where extrapolation to zero shear is necessary. From this result, we suggest that the extrapolation tends to over estimate the true viscosity. Furthermore, by comparing the fixed and flexible bond results we see a small shift towards higher viscosities for the harmonic potential. This is investigated further in Section SI.V.

It is important to note that Reference 5 utilizes a 1.0 nm cut-off, whereas we use a 1.4 nm cut-off. As demonstrated in Section 4 of the manuscript, the results for a 1.0 nm and 1.4 nm cut-off can become significant for larger molecules. However, due to the good agreement between our values and those from Reference 5, the 1.0 nm cut-off appears to be sufficient for *n*-octane at elevated pressures. It is also worth noting that Reference 5 performed 10 to 20 ns simulations, while our simulation production time was only 1 ns.

Note that there appears to be a slight bias towards smaller box-sizes (higher  $\rho$ ) for a given pressure when comparing the fixed bond-lengths from this work with the values of Reference 5. Also, small discrepancies exist between the state points reported in Reference 4 and Reference 5. This should not impact our validation, but it is somewhat curious.

## SI.VIII. RDF in real units

Figure SI.10 presents the same data as Figure 13 of the main text, but with the non-bonded distance in real units.

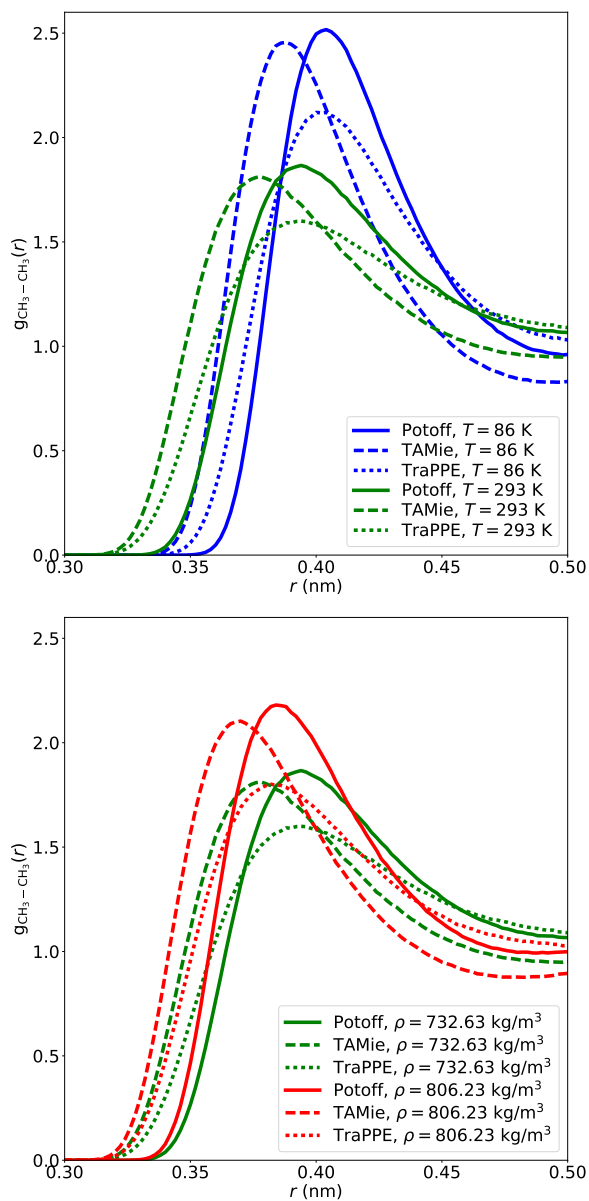


Figure SI.10: Comparison of radial distribution functions for  $\text{CH}_3\text{-CH}_3$  interactions ( $g_{\text{CH}_3\text{-CH}_3}(r)$ ) with  $r$  in real units. The top panel compares two different temperatures along the triple point isochore. The bottom panel compares two different densities along the 293 K isotherm. Colors correspond to different state points while line styles denote different force fields.

## SI.IX. Tabulated values

Table SI.III: Saturated liquid viscosity values for ethane.

		Potoff	TAMie	TraPPE	AUA4	TraPPE-2
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
137	600.04	0.516 <sub>0.024</sub>	0.389 <sub>0.013</sub>	0.313 <sub>0.014</sub>	0.321 <sub>0.011</sub>	0.2981 <sub>8.5E-3</sub>
174	557.16	0.2338 <sub>4.8E-3</sub>	0.2046 <sub>4.0E-3</sub>	0.1714 <sub>3.7E-3</sub>	0.1741 <sub>4.1E-3</sub>	0.1773 <sub>3.3E-3</sub>
207	514.33	0.1499 <sub>3.3E-3</sub>	0.1360 <sub>3.0E-3</sub>	0.1123 <sub>2.5E-3</sub>	0.1185 <sub>3.6E-3</sub>	0.1204 <sub>2.1E-3</sub>
236	471.45	0.0991 <sub>2.4E-3</sub>	0.0976 <sub>2.1E-3</sub>	0.0844 <sub>1.8E-3</sub>	0.0837 <sub>2.2E-3</sub>	0.0876 <sub>1.2E-3</sub>
260	428.60	0.0732 <sub>1.3E-3</sub>	0.0709 <sub>1.3E-3</sub>	0.0623 <sub>1.1E-3</sub>	0.0629 <sub>1.9E-3</sub>	0.0661 <sub>1.3E-3</sub>

Table SI.IV: Saturated liquid viscosity values for propane.

		Potoff	TAMie	TraPPE
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
86	732.21	10.7 <sub>1.5</sub>	5.31 <sub>0.40</sub>	2.47 <sub>0.16</sub>
90	728.03	8.34 <sub>0.96</sub>	4.42 <sub>0.22</sub>	2.01 <sub>0.12</sub>
100	717.71	3.56 <sub>0.22</sub>	2.53 <sub>0.18</sub>	1.243 <sub>0.049</sub>
110	707.53	2.17 <sub>0.12</sub>	1.500 <sub>0.060</sub>	0.898 <sub>0.039</sub>
130	687.26	1.003 <sub>0.033</sub>	0.844 <sub>0.026</sub>	0.517 <sub>0.013</sub>
166	651.14	0.439 <sub>0.011</sub>	0.389 <sub>0.013</sub>	0.2967 <sub>8.3E-3</sub>
210	604.63	0.2482 <sub>9.4E-3</sub>	0.2361 <sub>9.5E-3</sub>	0.1800 <sub>4.0E-3</sub>
250	558.12	0.1513 <sub>4.9E-3</sub>	0.1498 <sub>5.3E-3</sub>	0.1234 <sub>3.1E-3</sub>
285	511.61	0.1040 <sub>3.2E-3</sub>	0.1055 <sub>3.8E-3</sub>	0.0874 <sub>1.5E-3</sub>
314	465.10	0.0761 <sub>1.9E-3</sub>	0.0797 <sub>2.6E-3</sub>	0.0676 <sub>1.2E-3</sub>

Table SI.V: Saturated liquid viscosity values for *n*-butane.

		Potoff	TAMie	TraPPE
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
191	341.27	0.551 <sub>0.019</sub>	0.604 <sub>0.030</sub>	0.336 <sub>0.029</sub>
241	316.89	0.286 <sub>0.013</sub>	0.2664 <sub>6.2E-3</sub>	0.1900 <sub>4.3E-3</sub>
287	292.52	0.1690 <sub>3.6E-3</sub>	0.1640 <sub>3.7E-3</sub>	0.1327 <sub>2.7E-3</sub>
328	268.14	0.1147 <sub>2.2E-3</sub>	0.1168 <sub>1.8E-3</sub>	0.0928 <sub>2.0E-3</sub>
361	243.76	0.0858 <sub>1.6E-3</sub>	0.0849 <sub>2.1E-3</sub>	0.0726 <sub>1.2E-3</sub>

Table SI.VI: Saturated liquid viscosity values for *n*-octane.

		Potoff	TAMie	TraPPE
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
256	732.07	0.830 <sub>0.041</sub>	0.870 <sub>0.029</sub>	0.504 <sub>0.019</sub>
321	679.78	0.373 <sub>0.011</sub>	0.373 <sub>0.010</sub>	0.2675 <sub>7.0E-3</sub>
381	627.49	0.2231 <sub>0.010</sub>	0.2378 <sub>5.9E-3</sub>	0.1689 <sub>4.9E-3</sub>
434	575.20	0.1385 <sub>5.9E-3</sub>	0.1416 <sub>3.5E-3</sub>	0.1161 <sub>2.8E-3</sub>
479	522.91	0.1053 <sub>4.7E-3</sub>	0.1024 <sub>7.4E-3</sub>	0.0851 <sub>2.4E-3</sub>

Table SI.VII: Saturated liquid viscosity values for *n*-dodecane.

		Potoff	TAMie	TraPPE
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
296	747.27	1.056 <sub>0.065</sub>	1.009 <sub>0.048</sub>	0.691 <sub>0.049</sub>
362	698.31	0.487 <sub>0.024</sub>	0.487 <sub>0.014</sub>	0.349 <sub>0.014</sub>
427	647.90	0.2768 <sub>8.1E-3</sub>	0.2868 <sub>8.7E-3</sub>	0.2180 <sub>7.0E-3</sub>
493	590.68	0.1799 <sub>5.5E-3</sub>	0.1780 <sub>7.0E-3</sub>	0.1442 <sub>5.0E-3</sub>
559	520.47	0.1066 <sub>2.8E-3</sub>	0.1114 <sub>4.3E-3</sub>	0.0937 <sub>2.1E-3</sub>

Table SI.VIII: Saturated liquid viscosity values for *n*-hexadecane.

		Potoff	TAMie	TraPPE
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
325	751.26	1.225 <sub>0.092</sub>	1.217 <sub>0.094</sub>	0.794 <sub>0.047</sub>
397	700.84	0.572 <sub>0.027</sub>	0.568 <sub>0.023</sub>	0.439 <sub>0.017</sub>
469	648.85	0.364 <sub>0.025</sub>	0.329 <sub>0.017</sub>	0.264 <sub>0.010</sub>
541	592.22	0.1956 <sub>6.4E-3</sub>	0.1917 <sub>6.9E-3</sub>	0.1752 <sub>6.1E-3</sub>
613	524.45	0.1296 <sub>3.5E-3</sub>	0.1249 <sub>4.0E-3</sub>	0.1114 <sub>4.7E-3</sub>

Table SI.IX: Saturated liquid viscosity values for *n*-docosane.

		Potoff	TAMie	TraPPE
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
435	700.85	0.626 <sub>0.028</sub>	0.677 <sub>0.046</sub>	0.529 <sub>0.026</sub>
514	647.14	0.384 <sub>0.016</sub>	0.381 <sub>0.014</sub>	0.341 <sub>0.016</sub>
594	588.70	0.2422 <sub>8.6E-3</sub>	0.246 <sub>0.010</sub>	0.1901 <sub>7.1E-3</sub>
673	521.32	0.1368 <sub>4.5E-3</sub>	0.1540 <sub>5.5E-3</sub>	0.1267 <sub>4.3E-3</sub>

Table SI.X: Saturated liquid viscosity values for 2-methylpropane.

		Potoff	TAMie	TraPPE
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
184	673.41	0.546 <sub>0.017</sub>	0.3630 <sub>9.7E-3</sub>	0.347 <sub>0.019</sub>
232	625.31	0.2706 <sub>6.6E-3</sub>	0.2189 <sub>5.2E-3</sub>	0.2016 <sub>4.5E-3</sub>
276	577.21	0.1612 <sub>3.5E-3</sub>	0.1403 <sub>3.1E-3</sub>	0.1316 <sub>2.3E-3</sub>
315	529.11	0.1175 <sub>2.1E-3</sub>	0.1028 <sub>2.9E-3</sub>	0.0941 <sub>1.8E-3</sub>
347	481.01	0.0845 <sub>1.8E-3</sub>	0.0761 <sub>1.4E-3</sub>	0.0737 <sub>1.6E-3</sub>

Table SI.XI: Saturated liquid viscosity values for 2-methylbutane.

		Potoff	TAMie	TraPPE
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
207	700.98	0.648 <sub>0.019</sub>	0.475 <sub>0.014</sub>	0.396 <sub>0.021</sub>
261	650.91	0.3056 <sub>8.8E-3</sub>	0.2647 <sub>9.3E-3</sub>	0.2134 <sub>8.4E-3</sub>
312	600.84	0.1815 <sub>4.3E-3</sub>	0.1700 <sub>5.0E-3</sub>	0.1452 <sub>6.7E-3</sub>
356	550.77	0.1190 <sub>2.6E-3</sub>	0.1201 <sub>3.7E-3</sub>	0.1022 <sub>3.9E-3</sub>
392	500.70	0.0897 <sub>1.5E-3</sub>	0.0883 <sub>2.5E-3</sub>	0.0771 <sub>3.4E-3</sub>



Table SI.XII: Saturated liquid viscosity values for 2-methylpentane.

		Potoff	TAMie	TraPPE
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
224	713.87	0.572 <sub>0.016</sub>	0.501 <sub>0.019</sub>	0.330 <sub>0.014</sub>
282	662.88	0.2848 <sub>9.6E-3</sub>	0.2551 <sub>7.6E-3</sub>	0.2069 <sub>5.9E-3</sub>
337	611.89	0.1763 <sub>4.3E-3</sub>	0.1690 <sub>4.5E-3</sub>	0.1371 <sub>3.1E-3</sub>
384	560.90	0.1219 <sub>3.0E-3</sub>	0.1196 <sub>2.6E-3</sub>	0.0998 <sub>2.1E-3</sub>
423	509.91	0.101 <sub>0.010</sub>	0.0868 <sub>2.0E-3</sub>	0.0748 <sub>1.4E-3</sub>

Table SI.XIII: Saturated liquid viscosity values for 3-methylpentane.

		Potoff	TAMie	TraPPE
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
227	723.49	0.587 <sub>0.024</sub>	0.545 <sub>0.019</sub>	0.392 <sub>0.012</sub>
278	678.27	0.341 <sub>0.016</sub>	0.3090 <sub>8.6E-3</sub>	0.2423 <sub>7.3E-3</sub>
328	632.19	0.2060 <sub>5.6E-3</sub>	0.1913 <sub>5.0E-3</sub>	0.1700 <sub>9.3E-3</sub>
379	579.98	0.1325 <sub>2.6E-3</sub>	0.1282 <sub>2.7E-3</sub>	0.1131 <sub>2.5E-3</sub>
430	515.73	0.0882 <sub>1.6E-3</sub>	0.0895 <sub>1.9E-3</sub>	0.0778 <sub>1.4E-3</sub>

Table SI.XIV: Saturated liquid viscosity values for 2,2-dimethylpropane.

		Potoff	AUA4	TraPPE
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
257	627.44	0.325 <sub>0.024</sub>	0.1694 <sub>3.6E-3</sub>	0.2172 <sub>5.5E-3</sub>
300	582.62	0.1780 <sub>4.8E-3</sub>	0.1212 <sub>2.3E-3</sub>	0.1404 <sub>3.4E-3</sub>
337	537.80	0.1219 <sub>1.9E-3</sub>	0.0919 <sub>3.4E-3</sub>	0.1006 <sub>1.9E-3</sub>
368	492.99	0.0889 <sub>1.6E-3</sub>	0.0746 <sub>4.1E-3</sub>	0.0782 <sub>1.4E-3</sub>
393	448.17	0.0667 <sub>1.2E-3</sub>	0.0572 <sub>1.2E-3</sub>	0.0591 <sub>1.4E-3</sub>

Table SI.XV: Saturated liquid viscosity values for 2,3-dimethylbutane.

		Potoff	TAMie	TraPPE
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
225	719.43	0.898 <sub>0.035</sub>	0.579 <sub>0.019</sub>	0.478 <sub>0.013</sub>
275	677.37	0.410 <sub>0.013</sub>	0.332 <sub>0.015</sub>	0.2756 <sub>7.1E-3</sub>
325	632.13	0.270 <sub>0.011</sub>	0.218 <sub>0.010</sub>	0.1938 <sub>5.6E-3</sub>
375	580.70	0.1621 <sub>6.3E-3</sub>	0.1466 <sub>6.3E-3</sub>	0.1324 <sub>2.4E-3</sub>
425	517.24	0.1076 <sub>4.4E-3</sub>	0.0926 <sub>2.3E-3</sub>	0.0869 <sub>1.6E-3</sub>

Table SI.XVI: Saturated liquid viscosity values for 2,2,4-trimethylpentane.

		Potoff	TraPPE
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
245	730.93	0.807 <sub>0.046</sub>	0.450 <sub>0.023</sub>
309	678.72	0.390 <sub>0.014</sub>	0.255 <sub>0.013</sub>
369	626.51	0.245 <sub>0.013</sub>	0.1654 <sub>7.8E-3</sub>
421	574.30	0.1488 <sub>3.2E-3</sub>	0.1199 <sub>6.8E-3</sub>
464	522.09	0.1035 <sub>1.6E-3</sub>	0.1009 <sub>5.8E-3</sub>

Table SI.XVII: Saturated liquid viscosity values for *n*-butane at force field saturated liquid densities.

Potoff			TAMie			TraPPE		
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
260	610.98	0.2259 <sub>5.9e-3</sub>	260	608.86*	0.2247 <sub>8.6e-3</sub>	262	613.00	0.1716 <sub>4.8e-3</sub>

\* The value of 608.86 kg/m<sup>3</sup> is reported in Reference 7 but for the optimized UA LJ 12-6 potential. The actual density for TAMie (AUA Mie 14-6) should have been 605.91 kg/m<sup>3</sup>. We did not notice this mistake before the submission deadline. However, the percent deviations in  $\rho_{\text{liq}}^{\text{sat}}$  relative to the REFPROP value (614.65 kg/m<sup>3</sup>) are approximately -0.94 % and -1.4 % for the values of 608.86 kg/m<sup>3</sup> and 605.91 kg/m<sup>3</sup>, respectively. Considering the large uncertainties in  $\eta_{\text{liq}}^{\text{sat}}$  and that the 608.86 kg/m<sup>3</sup> viscosity deviation is consistent with other TAMie viscosity deviations, we did not deem it necessary to repeat this state point in the limited time available.

Table SI.XVIII: Saturated liquid viscosity values for 3-methylpentane at force field saturated liquid densities.

Potoff			TraPPE		
$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]	$T^{\text{sat}}$ [K]	$\rho_{\text{liq}}^{\text{sat}}$ [kg/m <sup>3</sup> ]	$\eta_{\text{liq}}^{\text{sat}}$ [mPa-s]
330	624.00	0.1844 <sub>4.5e-3</sub>	330	631.60	0.1643 <sub>4.5e-3</sub>

Table SI.XIX: Compressed liquid viscosity values for propane.

$T$ [K]	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	Potoff		TAMie		TraPPE	
		$P$ [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]	$P$ [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]	$P$ [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]
293	500.28	-0.11 <sub>0.39</sub>	0.0987 <sub>2.4E-3</sub>	0.54 <sub>0.35</sub>	0.0966 <sub>4.3E-3</sub>	0.71 <sub>0.45</sub>	0.0831 <sub>3.0E-3</sub>
293	559.78	40.48 <sub>0.45</sub>	0.1595 <sub>4.2E-3</sub>	41.14 <sub>0.53</sub>	0.183 <sub>0.024</sub>	32.51 <sub>0.56</sub>	0.1211 <sub>2.2E-3</sub>
293	629.11	156.03 <sub>0.63</sub>	0.318 <sub>0.015</sub>	154.23 <sub>0.58</sub>	0.316 <sub>0.023</sub>	117.77 <sub>0.74</sub>	0.2185 <sub>7.9E-3</sub>
293	654.75	228.00 <sub>0.96</sub>	0.3950 <sub>8.0E-3</sub>	223.73 <sub>0.81</sub>	0.364 <sub>0.013</sub>	168.77 <sub>0.79</sub>	0.2720 <sub>8.3E-3</sub>
293	681.80	328.1 <sub>1.8</sub>	0.579 <sub>0.020</sub>	318.8 <sub>1.4</sub>	0.525 <sub>0.027</sub>	237.7 <sub>1.1</sub>	0.3346 <sub>8.8E-3</sub>
293	710.37	466.6 <sub>1.4</sub>	0.840 <sub>0.022</sub>	449.4 <sub>1.0</sub>	0.676 <sub>0.027</sub>	330.85 <sub>0.98</sub>	0.420 <sub>0.010</sub>
293	740.56	658.7 <sub>1.2</sub>	1.291 <sub>0.072</sub>	627.74 <sub>0.72</sub>	1.22 <sub>0.11</sub>	455.94 <sub>0.86</sub>	0.618 <sub>0.024</sub>
293	772.48	925.08 <sub>0.72</sub>	2.370 <sub>0.096</sub>	871.66 <sub>0.69</sub>	1.611 <sub>0.076</sub>	624.13 <sub>0.72</sub>	0.842 <sub>0.031</sub>
293	806.26	1295.21 <sub>0.81</sub>	5.23 <sub>0.28</sub>	1205.57 <sub>0.63</sub>	2.68 <sub>0.12</sub>	849.83 <sub>0.91</sub>	1.360 <sub>0.070</sub>

Table SI.XX: Compressed liquid viscosity values for *n*-butane.

$T$ [K]	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	Potoff		TAMie		TraPPE	
		$P$ [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]	$P$ [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]	$P$ [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]
293	578.76	1.51 <sub>0.43</sub>	0.1568 <sub>4.0E-3</sub>	4.92 <sub>0.44</sub>	0.1611 <sub>8.6E-3</sub>	-0.05 <sub>0.49</sub>	0.1339 <sub>7.4E-3</sub>
293	618.15	38.98 <sub>0.53</sub>	0.2242 <sub>4.7E-3</sub>	43.98 <sub>0.51</sub>	0.2362 <sub>5.2E-3</sub>	28.12 <sub>0.54</sub>	0.1754 <sub>7.7E-3</sub>
293	661.20	110.51 <sub>0.62</sub>	0.3633 <sub>9.7E-3</sub>	116.62 <sub>0.46</sub>	0.377 <sub>0.017</sub>	80.01 <sub>0.55</sub>	0.249 <sub>0.010</sub>
293	708.33	242.33 <sub>0.73</sub>	0.695 <sub>0.034</sub>	247.68 <sub>0.62</sub>	0.628 <sub>0.019</sub>	171.74 <sub>0.76</sub>	0.351 <sub>0.015</sub>
293	760.06	481.6 <sub>1.1</sub>	1.483 <sub>0.061</sub>	479.67 <sub>0.98</sub>	1.317 <sub>0.061</sub>	330.31 <sub>0.79</sub>	0.643 <sub>0.036</sub>

Table SI.XXI: Compressed liquid viscosity values for *n*-octane.

<i>T</i> [K]	Potoff			TAMie			TraPPE		
	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	<i>P</i> [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]	<i>P</i> [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]	<i>P</i> [MPa]	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	<i>P</i> [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]
293	702.44	1.15 <sub>0.65</sub>	0.508 <sub>0.034</sub>	13.64 <sub>0.63</sub>	0.505 <sub>0.020</sub>	-6.37 <sub>0.47</sub>	—	-6.37 <sub>0.47</sub>	0.324 <sub>0.014</sub>
293	764.16	123.47 <sub>0.83</sub>	1.435 <sub>0.076</sub>	142.97 <sub>0.98</sub>	1.148 <sub>0.070</sub>	77.88 <sub>0.59</sub>	—	77.88 <sub>0.59</sub>	0.657 <sub>0.024</sub>
293	832.65	405.1 <sub>7.6</sub>	6.28 <sub>0.53</sub>	426.7 <sub>2.8</sub>	6.02 <sub>0.41</sub>	260.9 <sub>1.1</sub>	—	260.9 <sub>1.1</sub>	1.790 <sub>0.084</sub>
293	894.90	870.6 <sub>1.4</sub>	68.0 <sub>4.9</sub>	881.09 <sub>0.81</sub>	36.2 <sub>2.9</sub>	548.29 <sub>0.99</sub>	—	548.29 <sub>0.99</sub>	6.13 <sub>0.41</sub>
293	921.79	—	—	—	—	719.6 <sub>1.1</sub>	—	719.6 <sub>1.1</sub>	11.7 <sub>1.1</sub>

Table SI.XXII: Compressed liquid viscosity values for 2-methylpropane.

<i>T</i> [K]	Potoff			TAMie			TraPPE		
	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	<i>P</i> [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	<i>P</i> [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	<i>P</i> [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]
293	558.6 <sub>1.2</sub>	-0.03 <sub>0.91</sub>	0.1501 <sub>6.3E-3</sub>	—	—	—	559.1 <sub>2.1</sub>	0.1 <sub>1.3</sub>	0.1167 <sub>2.6E-3</sub>
293	626.45 <sub>0.53</sub>	69.9 <sub>1.3</sub>	0.287 <sub>0.016</sub>	636.45 <sub>0.93</sub>	62.7 <sub>5.6</sub>	0.2338 <sub>8.9E-3</sub>	640.08 <sub>0.95</sub>	70.1 <sub>1.9</sub>	0.2227 <sub>7.7E-3</sub>
293	752.08 <sub>0.25</sub>	500.2 <sub>2.3</sub>	1.676 <sub>0.066</sub>	770.48 <sub>0.39</sub>	491.1 <sub>2.4</sub>	1.077 <sub>0.034</sub>	786.19 <sub>0.33</sub>	500.3 <sub>2.2</sub>	1.029 <sub>0.037</sub>
293	787.35 <sub>0.18</sub>	750.2 <sub>2.6</sub>	3.53 <sub>0.17</sub>	806.17 <sub>0.25</sub>	723.3 <sub>2.5</sub>	1.87 <sub>0.20</sub>	827.97 <sub>0.28</sub>	750.8 <sub>2.6</sub>	1.844 <sub>0.073</sub>
293	813.97 <sub>0.19</sub>	1001.1 <sub>2.4</sub>	6.90 <sub>0.42</sub>	833.55 <sub>0.14</sub>	952.0 <sub>2.2</sub>	3.25 <sub>0.12</sub>	860.07 <sub>0.21</sub>	1000.7 <sub>2.4</sub>	3.17 <sub>0.17</sub>

Table SI.XXIII: Compressed liquid viscosity values for 2-methylbutane.

$T$ [K]	Potoff			TAMie			TraPPE		
	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	$P$ [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	$P$ [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	$P$ [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]
293	617.83 <sub>0.58</sub>	-0.17 <sub>0.75</sub>	0.2233 <sub>9.6E-3</sub>	622.94 <sub>0.59</sub>	-0.21 <sub>0.71</sub>	0.1968 <sub>4.0E-3</sub>	622.35 <sub>0.83</sub>	-0.20 <sub>0.66</sub>	0.1618 <sub>3.3E-3</sub>
293	741.30 <sub>0.21</sub>	249.9 <sub>1.2</sub>	0.925 <sub>0.039</sub>	751.79 <sub>0.19</sub>	250.0 <sub>1.2</sub>	0.816 <sub>0.028</sub>	767.87 <sub>0.23</sub>	250.1 <sub>1.1</sub>	0.667 <sub>0.028</sub>
293	792.67 <sub>0.19</sub>	500.1 <sub>1.4</sub>	2.32 <sub>0.10</sub>	805.79 <sub>0.17</sub>	499.8 <sub>1.5</sub>	1.90 <sub>0.11</sub>	828.04 <sub>0.17</sub>	500.2 <sub>1.4</sub>	1.461 <sub>0.060</sub>
293	827.36 <sub>0.21</sub>	749.9 <sub>2.3</sub>	5.73 <sub>0.50</sub>	842.47 <sub>0.20</sub>	748.8 <sub>2.2</sub>	4.09 <sub>0.22</sub>	869.12 <sub>0.18</sub>	750.3 <sub>1.7</sub>	2.91 <sub>0.12</sub>
293	854.00 <sub>0.20</sub>	1000 <sub>2.9</sub>	12.4 <sub>1.1</sub>	869.29 <sub>0.38</sub>	982.7 <sub>4.0</sub>	8.54 <sub>0.84</sub>	900.99 <sub>0.14</sub>	1000.3 <sub>2.4</sub>	5.29 <sub>0.29</sub>

Table SI.XXIV: Compressed liquid viscosity values for 3-methylpentane.

$T$ [K]	Potoff			TAMie			TraPPE		
	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	$P$ [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	$P$ [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	$P$ [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]
293	647.42 <sub>0.68</sub>	-0.18 <sub>0.86</sub>	0.2312 <sub>5.7E-3</sub>	660.41 <sub>0.46</sub>	-0.08 <sub>0.60</sub>	0.2528 <sub>6.8E-3</sub>	667.88 <sub>0.50</sub>	-0.21 <sub>0.61</sub>	0.2145 <sub>4.6E-3</sub>
293	768.20 <sub>0.22</sub>	250.0 <sub>1.3</sub>	1.079 <sub>0.049</sub>	778.92 <sub>0.24</sub>	250.1 <sub>1.0</sub>	1.099 <sub>0.048</sub>	800.52 <sub>0.25</sub>	250.1 <sub>1.3</sub>	0.833 <sub>0.067</sub>
293	819.29 <sub>0.20</sub>	500.3 <sub>1.8</sub>	2.61 <sub>0.13</sub>	831.42 <sub>0.18</sub>	500.5 <sub>1.6</sub>	2.78 <sub>0.19</sub>	858.95 <sub>0.18</sub>	500.2 <sub>1.5</sub>	1.94 <sub>0.12</sub>
293	854.04 <sub>0.22</sub>	750.2 <sub>2.4</sub>	8.71 <sub>0.97</sub>	867.56 <sub>0.22</sub>	750.5 <sub>2.3</sub>	6.53 <sub>0.55</sub>	899.32 <sub>0.19</sub>	750.4 <sub>1.7</sub>	3.80 <sub>0.45</sub>
293	880.81 <sub>0.31</sub>	1000 <sub>4.3</sub>	19.2 <sub>2.3</sub>	895.60 <sub>0.30</sub>	999.9 <sub>4.0</sub>	18.0 <sub>2.1</sub>	930.76 <sub>0.20</sub>	1000.0 <sub>2.4</sub>	8.50 <sub>0.66</sub>

Table SI.XXV: Compressed liquid viscosity values for 2,2,4-trimethylpentane.

$T$ [K]	Potoff			TraPPE		
	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	$P$ [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]	$\rho_{\text{liq}}^{\text{comp}}$ [kg/m <sup>3</sup> ]	$P$ [MPa]	$\eta_{\text{liq}}^{\text{comp}}$ [mPa-s]
293	691.60 <sub>0.64</sub>	-1.88 <sub>0.98</sub>	0.432 <sub>0.013</sub>	704.21 <sub>0.84</sub>	-1.7 <sub>1.0</sub>	0.3299 <sub>8.5E-3</sub>
293	788.98 <sub>0.33</sub>	207.1 <sub>1.6</sub>	2.24 <sub>0.11</sub>	817.59 <sub>0.33</sub>	206.9 <sub>1.3</sub>	1.455 <sub>0.069</sub>
293	848.66 <sub>0.34</sub>	499.9 <sub>2.8</sub>	15.1 <sub>1.2</sub>	887.40 <sub>0.28</sub>	499.7 <sub>1.8</sub>	4.91 <sub>0.20</sub>
293	881.93 <sub>0.59</sub>	750.5 <sub>6.0</sub>	77.2 <sub>6.5</sub>	926.81 <sub>0.29</sub>	750.5 <sub>2.4</sub>	15.02 <sub>0.78</sub>
293	907.61 <sub>0.90</sub>	994.1 <sub>9.7</sub>	315 <sub>17</sub>	957.44 <sub>0.44</sub>	1000.5 <sub>4.3</sub>	49.5 <sub>5.4</sub>

## References

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