# Module Interface Specification for Solar Water Heating Systems Incorporating Phase Change Material

Brooks MacLachlan and Spencer Smith

May 7, 2018

## Contents

1	Syn	nbols, Abbreviations and Acronyms	1										
2	Inti	roduction	1										
3	Not	tation	1										
4	Mo	dule Decomposition	1										
5	MIS	S of Control Module	3										
	5.1	Module	3										
	5.2	Uses	3										
	5.3	Syntax	3										
		5.3.1 Exported Access Programs	3										
	5.4	Semantics	3										
		5.4.1 State Variables	3										
		5.4.2 Access Routine Semantics	3										
6	MIS	S of Input Parameters Module	5										
	6.1	Module	5										
	6.2	Uses	5										
	6.3	Syntax	5										
	6.4	Semantics	5										
		6.4.1 Environment Variables	5										
		6.4.2 State Variables	6										
		6.4.3 Assumptions	7										
		6.4.4 Access Routine Semantics	7										
	6.5	Considerations	9										
7	MIS	S of Temperature ODEs Module	10										
	7.1	Module	10										
	7.2	Uses	10										
	7.3	Syntax	10										
		7.3.1 Exported Access Programs	10										
	7.4	Semantics	10										
		7.4.1 State Variables	10										
		7.4.2 Assumptions	10										
		7.4.3 Access Routine Semantics	10										
8	MIS of ODE Solver Module												
	8.1	Module	12										
	8.2	Uses	12										
	8.3	Syntax	12										

		8.3.1	Exported Access Programs					. 1
	8.4	Seman	ntics					. 1
		8.4.1	State Variables					. 1
		8.4.2	Access Routine Semantics					. 1
9	MIS	of En	nergy Module					1
	9.1	Modul	<u>le</u>					. 1
	9.2	Uses						. 1
	9.3	Syntax	x					. 1
			External Access Programs					
	9.4		$egin{array}{c} egin{array}{c} \egin{array}{c} \egin{array}{c} \egin{array}{c} \egin{array}$					
		9.4.1	State Variables					
		9.4.2	Assumptions					
		9.4.3	Access Routine Semantics					
		5.4.0	recess redunic semantics	•	•	•	•	. 1
10	MIS	of Ou	utput Verification Module					1
			le					. 1
			X					
	10.0		Exported Constant					
			Exported Access Programs					
	10.4		ntics					
	10.4		State Variables					
			Assumptions					
			Access Routine Semantics					
		10.4.4	Local Functions	•	•	•	•	. 1
11	мтс	of Dl	lotting Module					1
11			le					
	11.5	•	X					
	11 /		Exported Access Programs					
	11.4							
			State Variables					
			Environment Variables					
			Assumptions					
		11.4.4	Access Routine Semantics		•			. 1
10	ТИТС	1 -6 0	orterest N.C. deels					-1
12			utput Module					1
			le					
	12.3		x		•			
		19 2 1	Exported Constants					1

		12.3.2	$\mathbf{E}$	xp	$\operatorname{ort}_{m{\epsilon}}$	$\operatorname{ed}$	A	$cc\epsilon$	ess	P	$^{ m rc}$	ogi	aı	m								 					19
	12.4	Seman																									19
		12.4.1	$S_1$	tat	e V	'ari	iab	oles	$\mathbf{S}$													 					19
		12.4.2	$\mathbf{E}$	nvi	ror	nm	en	t J	Va:	ria	abl	les	;									 					19
		12.4.3	A	.cce	ess	Ro	out	ine	e S	Sei	ma	an	tic	cs				•			•	 	•				19
13	MIS	of Sp	ec	ific	cat	ior	n l	Pa	ra	m	ıeı	te	$\mathbf{r}\mathbf{s}$	,													20
	13.1	Modul	le .																			 					20
	13.2	Uses																				 					20
	13.3	Syntax	κ.																			 					20
		13.3.1	$\mathbf{E}$	хp	orte	$\operatorname{ed}$	$\mathbf{C}$	ons	sta	n	ts											 					20
	13.4	Seman	ıtic	$\mathbf{S}$																		 					21
14	App	endix																									22

## 1 Symbols, Abbreviations and Acronyms

See SRS Documentation at https://github.com/smiths/swhs

## 2 Introduction

The following document details the Module Interface Specifications for the implemented modules in a program simulating a Solar Water Heating System with Phase Change Material. It is intended to ease navigation through the program for design and maintenance purposes.

Complementary documents include the System Requirement Specifications and Module Guide. The full documentation and implementation can be found at https://github.com/smiths/swhs.

The specification is given in terms of functions, rather than sequences. For instance, the predicted temperature of the water is given as a function of time  $(\mathbb{R} \to \mathbb{R})$ , not as a sequence  $(\mathbb{R}^n)$ . This approach is more straightforward for the specification, but in the implementation stage, it will likely be necessary to introduce a sequence, assuming that a numerical solver is used for the system of ODEs.

## 3 Notation

The structure of the MIS for modules comes from ?, with the addition that template modules have been adapted from ?. The mathematical notation comes from Chapter 3 of ?. For instance, the symbol := is used for a multiple assignment statement and conditional rules follow the form  $(c_1 \Rightarrow r_1 | c_2 \Rightarrow r_2 | ... | c_n \Rightarrow r_n)$ .

The following table summarizes the primitive data types used by SWHS.

Data Type	Notation	Description
character	char	a single symbol or digit
integer	$\mathbb{Z}$	a number without a fractional component in $(-\infty, \infty)$
natural number	N	a number without a fractional component in $[1, \infty)$
real	$\mathbb{R}$	any number in $(-\infty, \infty)$

The specification of SWHS uses some derived data types: sequences, strings, and tuples. Sequences are lists filled with elements of the same data type. Strings are sequences of characters. Tuples contain a list of values, potentially of different types. In addition, SWHS uses functions, which are defined by the data types of their inputs and outputs. Local functions are described by giving their type signature followed by their specification.

## 4 Module Decomposition

The following table is taken directly from the Module Guide document for this project.

Level 1	Level 2
Hardware-Hiding	
Behaviour-Hiding	Input Parameters Output Format Output Verification Temperature ODEs Energy Equations Control Module Specification Parameters Module
Software Decision	Sequence Data Structure ODE Solver Plotting

Table 1: Module Hierarchy

## 5 MIS of Control Module

## 5.1 Module

main

#### 5.2 Uses

Param (Section 6), Temperature (Section 7), Solver (Section 8), Energy (Section 9), verify\_output (Section 10), plot (Section 11), output (Section 12)

## 5.3 Syntax

#### 5.3.1 Exported Access Programs

Name	In	Out	Exceptions
main	=	-	-

#### 5.4 Semantics

#### 5.4.1 State Variables

None

#### 5.4.2 Access Routine Semantics

main():

• transition: Modify the state of Param module and the environment variables for the Plot and Output modules by following these steps

Get (filenameIn: string) and (filenameOut: string) from user

load\_params(filenameIn)

#Find temperature function  $(T_W^{\text{Solid}}, T_W^{\text{Melting}}, T_W^{\text{Liquid}}, T_P^{\text{Solid}}, T_P^{\text{Melting}}, T_P^{\text{Liquid}})$ , and energy  $(Q_P)$  and times of transition between solid, melting and liquid phases  $(t_{\text{melt}}^{\text{init}}, t_{\text{melt}}^{\text{final}})$ 

 $t_{\mathrm{melt}}^{\mathrm{init}}, [T_W^{\mathrm{Solid}}, T_P^{\mathrm{Solid}}]^T := \mathrm{solve}(\mathrm{ODE\_SolidPCM}, 0.0, [T_{\mathrm{init}}, T_{\mathrm{init}}]^T, \mathrm{event\_StartMelt}, t_{\mathrm{final}})$ 

 $t_{\mathrm{melt}}^{\mathrm{final}}, [T_W^{\mathrm{Melting}}, T_P^{\mathrm{Melting}}, Q_p]^T := \mathrm{solve}(\mathrm{ODE\_MeltingPCM}, t_{\mathrm{melt}}^{\mathrm{init}}, [T_W^{\mathrm{Solid}}(t_{\mathrm{melt}}^{\mathrm{init}}), T_P^{\mathrm{Solid}}(t_{\mathrm{melt}}^{\mathrm{init}}), 0.0]^T,$  event\\_EndMelt,  $t_{\mathrm{final}}$ )

 $[T_W^{\text{Liquid}}, T_P^{\text{Liquid}}]^T := \text{solveNoE}(\text{ODE\_LiquidPCM}, \, t_{\text{melt}}^{\text{final}}, \, [T_W^{\text{Melting}}(t_{\text{melt}}^{\text{final}}), \, T_P^{\text{Melting}}(t_{\text{melt}}^{\text{final}})]^T, \, t_{\text{final}})$ 

 $\#Combine\ temperatures\ for\ 0 \le t \le t_{final}$ 

$$T_W(t) = (0 \leq t < t_{\text{melt}}^{\text{init}} \Rightarrow T_W^{\text{Solid}} | t_{\text{melt}}^{\text{init}} \leq t < t_{\text{melt}}^{\text{final}} \Rightarrow T_W^{\text{Melting}} | t_{\text{melt}}^{\text{final}} \leq t \leq t_{\text{final}} \Rightarrow T_W^{\text{Liquid}})$$

$$T_P(t) = (0 \leq t < t_{\rm melt}^{\rm init} \Rightarrow T_P^{\rm Solid} | t_{\rm melt}^{\rm init} \leq t < t_{\rm melt}^{\rm final} \Rightarrow T_P^{\rm Melting} | t_{\rm melt}^{\rm final} \leq t \leq t_{\rm final} \Rightarrow T_P^{\rm Liquid})$$

#Energy values  $(E_W(t), E_P(t))$  for  $0 \le t \le t_{\text{final}}$ 

$$E_W(t) = (0 \le t < t_{\rm melt}^{\rm init} \Rightarrow {\rm energyWater}(T_W^{\rm Solid}) | t_{\rm melt}^{\rm init} \le t < t_{\rm melt}^{\rm final} \Rightarrow {\rm energyWater}(T_W^{\rm Melting}) | t_{\rm melt}^{\rm final} \le t \le t_{\rm final} \Rightarrow {\rm energyWater}(T_W^{\rm Liquid}))$$

$$E_P(t) = (0 \le t < t_{\rm melt}^{\rm init} \Rightarrow {\rm energySolidPCM}(T_P^{\rm Solid}) | t_{\rm melt}^{\rm init} \le t < t_{\rm melt}^{\rm final} \Rightarrow {\rm energyMeltingPCM}(Q_P) | t_{\rm melt}^{\rm final} \le t \le t_{\rm final} \Rightarrow {\rm energyLiquidPCM}(T_P^{\rm Liquid}))$$

#Output calculated values to a file and to a plot. Verify calculated values obey conservation of energy.

verify\_output $(T_w, T_p, E_w, E_p, t_{final})$ 

$$plot(T_w, T_p, E_w, E_p, t_{final})$$

output(filenameOut,  $T_w$ ,  $T_p$ ,  $E_w$ ,  $E_p$ ,  $t_{final}$ )

## 6 MIS of Input Parameters Module

The secrets of this module are the data structure for input parameters, how the values are input and how the values are verified. The load and verify secrets are isolated to their own access programs.

## 6.1 Module

Param

## 6.2 Uses

SpecParam (Section 13)

## 6.3 Syntax

Name	In	Out	Exceptions
load_params	string	-	FileError
verify_params	-	-	badLength, badDiam, badPCMVolume,
			badPCMAndTankVol, badPCMArea,
			badPCMDensity, badMeltTemp,
			badCoilAndInitTemp, badCoilTemp,
			badPCMHeatCapSolid, badPCMHeatCapLiquid,
			badHeatFusion, badCoilArea, badWaterDensity,
			badWaterHeatCap, badCoilCoeff, badPCMCoeff,
			badInitTemp, badFinalTime,
			${\it badInitAndMeltTemp}$
L	-	$\mathbb{R}$	
D	-	$\mathbb{R}$	
$V_P$	-	$\mathbb{R}$	
$A_P$	-	$\mathbb{R}$	
$m_W^{ m noPCM}$	-	$\mathbb{R}$	
$ au_W^{ ext{noPCM}}$	_	$\mathbb{R}$	

Should verify\_params have a boolean output?

## 6.4 Semantics

#### 6.4.1 Environment Variables

input File: sequence of string #f[i] is the ith string in the text file f

## 6.4.2 State Variables

# From R1  $L \colon \mathbb{R}$ D:  $\mathbb{R}$  $V_P$ :  $\mathbb{R}$  $A_P$ :  $\mathbb{R}$  $\rho_P: \mathbb{R}$  $T_{\mathrm{melt}}^{P} \colon \mathbb{R}$  $C_P^S$ :  $\mathbb{R}$  $C_P^L$ :  $\mathbb{R}$  $H_f$ :  $\mathbb{R}$  $A_C$ :  $\mathbb{R}$  $T_C$ :  $\mathbb{R}$  $\rho_W$ :  $\mathbb{R}$  $C_W$ :  $\mathbb{R}$  $h_C$ :  $\mathbb{R}$  $h_P$ :  $\mathbb{R}$  $T_{\text{init}}$ :  $\mathbb{R}$  $t_{\text{step}}$ :  $\mathbb{R}$  $t_{\text{final}}$ :  $\mathbb{R}$  $AbsTol: \mathbb{R}$  $RelTol: \mathbb{R}$ ConsTol:  $\mathbb{R}$ # From R2  $V_{\text{tank}}$ :  $\mathbb{R}$  $m_W$ :  $\mathbb{R}$  $m_P$ :  $\mathbb{R}$ # From R3  $\tau_W$ :  $\mathbb{R}$  $\eta$ :  $\mathbb{R}$  $\tau_P^S$ :  $\mathbb{R}$ 

 $\tau_P^L\colon\thinspace\mathbb{R}$ 

```
# To Support IM4
E_{P \text{melt}}^{\text{init}} \colon \mathbb{R}
E_{P \text{melt}}^{\text{all}} \colon \mathbb{R}
# To Support Testing
m_W^{\text{noPCM}} \colon \mathbb{R}
\tau_W^{\text{noPCM}} \colon \mathbb{R}
```

## 6.4.3 Assumptions

- load\_params will be called before the values of any state variables will be accessed.
- The file contains the string equivalents of the numeric values for each input parameter in order, each on a new line. The order is the same as in the table in R1 of the SRS. Any comments in the input file should be denoted with a '#' symbol.

#### 6.4.4 Access Routine Semantics

Param.L:

 $\bullet$  output: out := L

• exception: none

Param.D:

• output: out := D

• exception: none

. . .

Param. $m_W^{\text{noPCM}}$ :

• output:  $out := m_W^{\text{noPCM}}$ 

• exception: none

Param. $\tau_W^{\text{noPCM}}$ :

• output:  $out := \tau_W^{\text{noPCM}}$ 

• exception: none

 $load_params(s)$ :

- transition: The filename s is first associated with the file f. inputFile is used to modify the state variables using the following procedural specification:
  - 1. Read data sequentially from inputFile to populate the state variables from R1 (L to ConsTol).
  - 2. Calculate the derived quantities (all other state variables) as follows:

$$\begin{split} &-V_{\text{tank}} := \pi \times L \times (\frac{D}{2})^2 \\ &-m_W := \rho_w (V_t - V_p) \\ &-m_P := \rho_p V_p \\ &-\tau_W := \frac{m_w C_w}{A_c h_c} \\ &-\eta := \frac{h_p A_p}{h_c A_c} \\ &-\tau_P^S := \frac{m_p C_{ps}}{h_p A_p} \\ &-\tau_P^L := \frac{m_p C_{pl}}{h_p A_p} \\ &-E_{P\text{melt}}^{\text{init}} := C_{ps} m_p (T_{\text{melt}} - T_{\text{init}}) \\ &-E_{P\text{melt}}^{\text{milt}} := H_f m_p \\ &-m_W^{\text{noPCM}} := \rho_w V_t \\ &-\tau_W^{\text{noPCM}} := \frac{m_W^{\text{noPCM}} C_w}{h_c A_c} \end{split}$$

- 3. verify\_params()
- exception: exc := a file name s cannot be found OR the format of inputFile is incorrect  $\Rightarrow$  FileError

## verify\_params():

- out: out := none
- exception: exc :=

etc. See Appendix (Section 14) for the complete list of exceptions and associated error messages.

## 6.5 Considerations

The value of each state variable can be accessed through its name (getter). An access program is available for each state variable. There are no setters for the state variables, since the values will be set and checked by load params and not changed for the life of the program.

## 7 MIS of Temperature ODEs Module

## 7.1 Module

Temperature

## 7.2 Uses

Param (Section 6)

## 7.3 Syntax

## 7.3.1 Exported Access Programs

Name	In	Out	Exceptions
ODE_SolidPCM	_	$(\mathbb{R}^3  o \mathbb{R})^2$	-
ODE_MeltingPCM	_	$(\mathbb{R}^4 \to \mathbb{R})^3$	_
ODE_LiquidPCM	_	$(\mathbb{R}^3 \to \mathbb{R})^2$	_
event_StartMelt	_	$\mathbb{R}^2  o \mathbb{R}$	_
event_EndMelt	_	$\mathbb{R}^3  o \mathbb{R}$	-

## 7.4 Semantics

#### 7.4.1 State Variables

none

### 7.4.2 Assumptions

none

#### 7.4.3 Access Routine Semantics

ODE\_SolidPCM():

• output: 
$$out := \frac{d}{dt} \begin{bmatrix} T_W \\ T_P \end{bmatrix} = \begin{bmatrix} \frac{1}{\tau_W} [(T_C - T_W(t)) + \eta(T_P(t) - T_W(t))] \\ \frac{1}{\tau_P^S} (T_W(t) - T_P(t)) \end{bmatrix}$$

• exception: none

ODE\_MeltingPCM():

• output: 
$$out := \frac{d}{dt} \begin{bmatrix} T_W \\ T_P \\ Q_P \end{bmatrix} = \begin{bmatrix} \frac{1}{\tau_W} [(T_C - T_W(t)) + \eta(T_P(t) - T_W(t))] \\ 0 \\ h_P A_P (T_W(t) - T_{\text{melt}}^P) \end{bmatrix}$$

• exception: none

ODE\_LiquidPCM():

• output: 
$$out := \frac{d}{dt} \begin{bmatrix} T_W \\ T_P \end{bmatrix} = \begin{bmatrix} \frac{1}{\tau_W} [(T_C - T_W(t)) + \eta(T_P(t) - T_W(t))] \\ \frac{1}{\tau_P^L} (T_W(t) - T_P(t)) \end{bmatrix}$$

• exception: none

event\_StartMelt():

- output:  $out := g([T_W, T_P]^T) = T_{\text{melt}}^P T_P$
- exception: none

event\_EndMelt():

- output:  $out := g([T_W, T_P, Q_P]^T) = 1 \phi$ , where  $\phi = \frac{Q_P}{E_{\text{melt}}^{\text{all}}}$
- exception: none

## 8 MIS of ODE Solver Module

#Bold font is used to indicate variables that are a sequence type

### 8.1 Module

Solver $(n : \mathbb{N}) \# n$  is the length of the sequences

### 8.2 Uses

None

## 8.3 Syntax

### 8.3.1 Exported Access Programs

Name	In	Out	Except.
solve	$\mathbf{f}: (\mathbb{R}^{n+1} \to \mathbb{R})^n, t_0: \mathbb{R}, \mathbf{y}_0: \mathbb{R}^n, g: \mathbb{R}^n \to \mathbb{R}, t_{\text{fin}}: \mathbb{R}$		ODE_ERR, NO_EVENT
solveNoE	$\mathbf{f}:(\mathbb{R}^{n+1}\to\mathbb{R})^n,t_0:\mathbb{R},\mathbf{y}_0:\mathbb{R}^n,t_{\mathrm{fin}}:\mathbb{R}$	$\mathbf{y}:(\mathbb{R} o\mathbb{R})^n$	ODE_ERR

### 8.4 Semantics

#### 8.4.1 State Variables

None

#### 8.4.2 Access Routine Semantics

 $\#Solving \frac{d}{dt}\mathbf{y} = \mathbf{f}(t, \mathbf{y}(t))$ 

solve( $\mathbf{f}, t_0, \mathbf{y}_0, g, t_{\text{fin}}$ ):

• output:  $out := t_1, \mathbf{y}(t)$  where

$$\mathbf{y}(t) = \mathbf{y}_0 + \int_{t_0}^t \mathbf{f}(s, \mathbf{y}(s)) ds$$

with  $t_1$  determined by the first time where  $g(\mathbf{y}(t_1)) = 0$ .  $\mathbf{y}(t)$  is calculated from  $t = t_0$  to  $t = t_1$ .

• exception:  $exc := (\neg(\exists t : \mathbb{R}|t_0 \le t \le t_{\text{fin}} : g(\mathbf{y}(t)) = 0) \Rightarrow \text{NO\_EVENT} \mid \text{ODE Solver Fails} \Rightarrow \text{ODE\_ERR})$ 

solveNoE( $\mathbf{f}, t_0, \mathbf{y}_0, t_{fin}$ ):

ullet output:  $out := \mathbf{y}(t)$  where

$$\mathbf{y}(t) = \mathbf{y}_0 + \int_{t_0}^{t_{\text{fin}}} \mathbf{f}(s, \mathbf{y}(s)) ds$$

y(t) is calculated from  $t=t_0$  to  $t=t_{\rm fin}$ .

 $\bullet$  exception: exc := ( ODE Solver Fails  $\Rightarrow$  ODE\_ERR)

## 9 MIS of Energy Module

## 9.1 Module

Energy

## 9.2 Uses

Param (Section 6)

## 9.3 Syntax

## 9.3.1 External Access Programs

Name	In	Out	Exceptions
energyWater	$\mathbb{R}  o \mathbb{R}$	$\mathbb{R}  o \mathbb{R}$	-
energySolidPCM	$\mathbb{R}  o \mathbb{R}$	$\mathbb{R}  o \mathbb{R}$	_
energyMeltingPCM	$\mathbb{R}  o \mathbb{R}$	$\mathbb{R}  o \mathbb{R}$	-
energyLiquidPCM	$\mathbb{R}  o \mathbb{R}$	$\mathbb{R}  o \mathbb{R}$	_

## 9.4 Semantics

#### 9.4.1 State Variables

None

## 9.4.2 Assumptions

None

## 9.4.3 Access Routine Semantics

energyWater $(T_W)$ :

- output:  $out := C_W m_W (T_W T_{\text{init}})$
- exception: none

energySolidPCM $(T_P)$ :

- output:  $out := C_P^S m_P (T_P T_{\text{init}})$
- exception: none

energyMeltingPCM $(Q_P)$ :

• output:  $out := E_{P \text{melt}}^{\text{init}} + Q_P$ 

 $\bullet$  exception: none

## energyLiquidPCM $(T_P)$ :

• output:  $out := E_{P \text{melt}}^{\text{init}} + H_f m_p + C_P^L m_P (T_P(t) - T_{\text{melt}}^P)$ 

• exception: none

## 10 MIS of Output Verification Module

## 10.1 Module

 $verify\_output$ 

#### 10.2 Uses

Param (Section 6)

## 10.3 Syntax

#### 10.3.1 Exported Constant

 $ADMIS\_ER = 1 \times 10^{-6}$ 

## 10.3.2 Exported Access Programs

Name	In	Out	Exceptions
$verify\_output$	$T_W(t): \mathbb{R} \to \mathbb{R}, T_P(t): \mathbb{R} \to \mathbb{R}, E_W(t): \mathbb{R} \to \mathbb{R}, E_P(t): \mathbb{R} \to \mathbb{R}, t_{\text{final}}: \mathbb{R}$	-	EWAT_NOT_CONSERVE, EPCM_NOT_CONSERVE

## 10.4 Semantics

#### 10.4.1 State Variables

None

#### 10.4.2 Assumptions

All of the fields of the input parameters structure have been assigned a value.

#### 10.4.3 Access Routine Semantics

verify\_output( $T_W, T_P, E_W, E_P, t_{\text{final}}$ ):

• exception: exc := (

$$\begin{array}{l} (\forall t|0\leq t\leq t_{\rm final}: {\rm relErr}(E_W, \int_0^t h_C A_C (T_C-T_W(t)) dt - \int_0^t h_P A_P (T_W(t)-T_P(t)) dt) < {\rm ADMIS\_ER}) \Rightarrow {\rm EWAT\_NOT\_CONSERVE} \\ |\\ (\forall t|0\leq t\leq t_{\rm final}: {\rm relErr}(E_P, \int_0^t h_P A_P (T_W(t)-T_P(t)) dt) < {\rm ADMIS\_ER}) \Rightarrow {\rm EPCM\_NOT\_CONSERVE} \\ ) \end{array}$$

## 10.4.4 Local Functions

relErr: 
$$\mathbb{R} \times \mathbb{R} \to \mathbb{R}$$
  
relErr $(t, e) \equiv \frac{|t-e|}{|t|}$ 

## 11 MIS of Plotting Module

## 11.1 Module

plot

### 11.2 Uses

N/A

## 11.3 Syntax

## 11.3.1 Exported Access Programs

Name	In	Out	Exceptions
plot	$T_W(t): \mathbb{R} \to \mathbb{R}, T_P(t): \mathbb{R} \to \mathbb{R}, E_W(t): \mathbb{R} \to \mathbb{R}, E_P(t): \mathbb{R} \to \mathbb{R}, t_{\text{final}}: \mathbb{R}$	-	-

### 11.4 Semantics

#### 11.4.1 State Variables

None

#### 11.4.2 Environment Variables

win: 2D sequence of pixels displayed on the screen

#### 11.4.3 Assumptions

None

#### 11.4.4 Access Routine Semantics

 $plot(T_w, T_p, E_w, E_p, t_{final})$ :

- transition: Modify win to display a plot where the vertical axis is time and one horizontal axis is temperature and the other horizontal axis is energy. The time should run from 0 to  $t_{\rm final}$
- exception: none

## 12 MIS of Output Module

#### 12.1 Module

output

#### 12.2 Uses

Param (Section 6)

## 12.3 Syntax

## 12.3.1 Exported Constants

 $max\_width$ : integer

## 12.3.2 Exported Access Program

Name	In	Out	Exceptions
output	fname: string, $T_W(t): \mathbb{R} \to \mathbb{R}, T_P(t): \mathbb{R} \to \mathbb{R}, E_W(t): \mathbb{R} \to \mathbb{R}, E_P(t): \mathbb{R} \to \mathbb{R}, t_{\text{final}}: \mathbb{R}$	-	-

### 12.4 Semantics

#### 12.4.1 State Variables

None

#### 12.4.2 Environment Variables

file: A text file

## 12.4.3 Access Routine Semantics

output(fname,  $T_w$ ,  $T_p$ ,  $E_w$ ,  $E_p$ ,  $t_{\text{final}}$ ):

- transition: Write to environment variable named fname the following: the input parameters from Param, and the calculated values  $T_w$ ,  $T_p$ ,  $E_w$ ,  $E_p$  from times 0 to  $t_{\text{final}}$ . The functions will be output as sequences in this file. The spacing between points in the sequence should be selected so that the heating behaviour is captured in the data.
- exception: none

## 13 MIS of Specification Parameters

The secrets of this module is the value of the specification parameters.

## 13.1 Module

SpecParam

## 13.2 Uses

N/A

## 13.3 Syntax

### 13.3.1 Exported Constants

```
# From Table 2 in SRS
L_{\min} := 0.1
L_{\text{max}} := 50
\frac{D}{L_{\min}} := 0.002
\frac{D}{L_{\text{max}}} := 200
minfrac := 10^{-6}
h_{\min} := 0.001

\rho_P^{\min} := 500

\rho_P^{\text{max}} := 20000
C_{P\min}^S := 100
C_{P\mathrm{max}}^S := 4000
C_{P\min}^{L} := 100
C_{P\max}^L := 5000
A_C^{\max} := \pi(\frac{D}{2})^2

\rho_W^{\min} := 950

\rho_W^{\text{max}} := 1000

C_W^{\min} := 4170
C_W^{\max} := 4210
h_C^{\min} := 10
h_C^{\text{max}} := 10000
h_P^{\min} := 10
h_P^{\text{max}} := 10000
t_{\text{final}}^{\text{max}} := 86400
```

 $[A_C^{\rm max}$  shouldn't be in this table of constants —SS]

## 13.4 Semantics

N/A

# 14 Appendix

Table 2: Possible Exceptions

Message ID	Error Message
badLength	Error: Tank length must be $> 0$
badDiam	Error: Tank diameter must be $> 0$
badPCMVolume	Error: PCM volume must be $> 0$
bad PCM And Tank Vol	Error: PCM volume must be < tank volume
badPCMArea	Error: PCM area must be $> 0$
badPCMDensity	Error: rho_p must be $> 0$
${\bf badMeltTemp}$	Error: Tmelt must be $> 0$ and $< Tc$
bad Coil And In it Temp	Error: Tc must be > Tinit
badCoilTemp	Error: Tc must be $> 0$ and $< 100$
${\it badPCMHeatCapSolid}$	Error: C <sub>-ps</sub> must be $> 0$
${\it badPCMHeatCapLiquid}$	Error: C_pl must be $> 0$
${\bf bad Heat Fusion}$	Error: Hf must be $> 0$
badCoilArea	Error: Ac must be $> 0$
badWaterDensity	Error: rho_w must be $> 0$
${\bf badWaterHeatCap}$	Error: $C_{-w}$ must be $> 0$
badCoilCoeff	Error: hc must be $> 0$
badPCMCoeff	Error: hp must be $> 0$
badInitTemp	Error: Tinit must be $> 0$ and $< 100$
badFinalTime	Error: tfinal must be $> 0$
badInit And Melt Temp	Error: Tinit must be < Tmelt
ODE_ACCURACY	reltol and abstol were not satisfied by the ODE solver for a given solution step.
ODE_BAD_INPUT	Invalid input to ODE solver
ODE_MAXSTEP	ODE solver took $MaxStep$ steps and did not find solution
warnLength	Warning: It is recommended that $0.1 \le L \le 50$
warnDiam	Warning: It is recommended that $0.002 \le D/L \le 200$
warnPCMVol	Warning: It is recommended that Vp be $>= 0.0001\%$ of Vt
warn Vol Area	Warning: It is recommended that Vp $<=$ Ap $<=$ $(2/0.001)$ * Vp
warnPCMDensity	Warning: It is recommended that $500 < \text{rho\_p} < 20000$
warn PCM Heat Cap Solid	Warning: It is recommended that $100 < C_{-ps} < 4000$

warn PCM Heat Cap Liquid	Warning: It is recommended that $100 < C_pl < 5000$
warnCoilArea	Warning: It is recommended that Ac <= pi * (D/2) $\wedge$ 2
warnWaterDensity	Warning: It is recommended that $950 < \text{rho\_w} <= 1000$
warn Water Heat Cap	Warning: It is recommended that $4170 < C_w < 4210$
warnCoilCoeff	Warning: It is recommended that $10 < hc < 10000$
warnPCMCoeff	Warning: It is recommended that $10 < hp < 10000$
warn Final Time	Warning: It is recommended that $0 < \text{tfinal} < 86400$
warnWaterError	Warning: There is greater than $x\%$ relative error between the energy in the water output and the expected output based on the law of conservation of energy. (Where $x$ is the value of $ConsTol$ )
warnPCMError	Warning: There is greater than $x\%$ relative error between the energy in the PCM output and the expected output based on the law of conservation of energy. (Where $x$ is the value of $ConsTol$ )