# Module Interface Specification for Solar Water Heating Systems Incorporating Phase Change Material

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# Contents

1	Introduction 4								
2	Not	ation	4						
3	Mod	dule Decomposition	5						
4	MIS	S of Control Module	7						
	4.1	Module	7						
	4.2	Uses	7						
	4.3	Syntax	7						
	1.0	4.3.1 Exported Access Programs	7						
	4.4	Semantics	7						
	4.4	4.4.1 State Variables	7						
			-						
		4.4.2 Environment Variables	7						
		4.4.3 Access Routine Semantics	8						
5	MIS	S of Input Parameters Module	9						
	5.1	Module	9						
	5.2	Uses	9						
	5.3	Syntax	9						
	5.4	Semantics	9						
	0.4								
		5.4.1 Environment Variables	9						

		5.4.2 State Variables	10
		5.4.3 Assumptions	11
		5.4.4 Access Routine Semantics	11
	5.5	Considerations	13
6	MIS	S of Input Format Module	14
	6.1	Module	14
	6.2	Uses	14
	6.3	Syntax	14
	6.4	Exported Access Programs	14
	6.5	Semantics	14
		6.5.1 Environment Variables	14
		6.5.2 Assumptions	14
		6.5.3 Access Routine Semantics	14
		6.5.4 Local Functions	15
7	MIS	S of Input Verification Module	17
	7.1	Module	17
	7.2	Uses	17
	7.3	Syntax	17
		7.3.1 Exported Access Programs	17
	7.4	Semantics	17
		7.4.1 Assumptions	17
		7.4.2 Access Routine Semantics	17
	7.5	Considerations	19
8	MIS	S of Temperature ODEs Module	20
_	8.1	Module	20
	8.2	Uses	20
	8.3	Syntax	20
		8.3.1 Exported Access Programs	20
	8.4	Semantics	$\frac{1}{20}$
			20
			20
		8.4.3 Access Routine Semantics	20

9	MIS	of ODE Solver Module	22
	9.1	Module	22
	9.2	Uses	22
	9.3	Syntax	22
		9.3.1 Exported Constants	22
		9.3.2 Exported Access Programs	22
	9.4	<u>.</u>	22
			22
			23
10	MIS	of Energy Module 2	24
			 24
			 24
			 24
	20.0		24
	10.4		24
	10.1		24
			 25
		1	-0 27
			- · 28
11	MIS	of Output Verification Module	29
		<del>-</del>	29
			29
			29
	11.0		29
	11 4	1	29 29
	11.1		29 29
			20 30
			30 30
		11.4.0 Local Functions	οU
<b>12</b>		0	32
			32
	12.2	Uses	32
	12.3	Syntax	32

		12.3.1	Exported A	Access Pro	ogram	<b>S</b> .						 . 32
1	2.4	Seman	tics									 . 32
		12.4.1	State Varia	bles								 . 32
		12.4.2	Environmen	nt Variab	les .							 . 32
		12.4.3	Assumption	ns								 32
		12.4.4	Access Rou	itine Sem	antics							 33
13 N	MIS	of Ou	tput Mod	ule								34
1	3.1	Modul	e									 . 34
1	3.2	Uses										 . 34
1	3.3	Syntax										 34
		13.3.1	Exported C	Constants								 34
		13.3.2	Exported A	Access Pro	ogram							 34
1	3.4	Seman	tics									 34
		13.4.1	State Varia	bles								 34
		13.4.2	Environmen	nt Variab	les .							 34
		13.4.3	Access Rou	itine Sem	antics							 35
<b>14</b> <i>A</i>	<b>A</b> pp	endix										36

# 1 Introduction

The following document details the Module Interface Specifications for the implemented modules in a program simulating a Solar Water Heating System with Phase Change Material. It is intended to ease navigation through the program for design and maintenance purposes.

Complementary documents include the System Requirement Specifications and Module Guide.

# 2 Notation

The structure of the MIS for modules comes from Hoffman and Strooper (1995), with the addition that template modules have been adapted from Ghezzi et al. (2003). The mathematical notation comes from Chapter 3 of Hoffman and Strooper (1995). For instance, the symbol := is used for a multiple assignment statement and conditional rules follow the form  $(c_1 \Rightarrow r_1|c_2 \Rightarrow r_2|...|c_n \Rightarrow r_n)$ .

The following table summarizes the primitive data types used by SWHS.

Data Type	Notation	Description
character	char	a single symbol or digit
integer	$\mathbb Z$	a number without a fractional component in $(-\infty, \infty)$
natural number	$\mathbb{N}$	a number without a fractional component in $[1, \infty)$
real	$\mathbb{R}$	any number in $(-\infty, \infty)$

The specification of SWHS uses some derived data types: sequences, strings, and tuples. Sequences are lists filled with elements of the same data type. Strings are sequences of characters. Tuples contain a list of values, potentially of different types. In addition, SWHS uses functions, which are defined by the data types of their inputs and outputs. Functions are described by showing their input data types separated by multiplication symbols on the left side of an arrow, and their output data type on the right side.

# 3 Module Decomposition

The following table is taken directly from the Module Guide document for this project.

Level 1	Level 2
Hardware-Hiding Module	
Behaviour-Hiding Module	Input Format Module Input Parameters Module Input Verification Module Output Format Module Output Verification Module Temperature ODEs Module Energy Equations Module Control Module
Software Decision Module	Sequence Data Structure Module ODE Solver Module Plotting Module

Table 1: Module Hierarchy

# 4 MIS of Control Module

### 4.1 Module

main

### 4.2 Uses

parameters (Section 5), load\_params (Section 6), verify\_params (Section 7), temperature (Section 8), ODE Solvers Module (Section 9), energy (Section 10), verify\_output (Section 11), plot (Section 12), output (Section 13)

# 4.3 Syntax

### 4.3.1 Exported Access Programs

Name	In	Out	Exceptions
main	string	-	-

# 4.4 Semantics

#### 4.4.1 State Variables

time: array of  $\mathbb{R}$ tempW: array of  $\mathbb{R}$ tempP: array of  $\mathbb{R}$ latHeat: array of  $\mathbb{R}$ eW: array of  $\mathbb{R}$ eP: array of  $\mathbb{R}$ eTot: array of  $\mathbb{R}$ 

#### 4.4.2 Environment Variables

win: 2D array of pixels displayed on the screen

### 4.4.3 Access Routine Semantics

main(s): transition: time, tempW, tempP, latHeat, eW, eP, eTot, win := results[0],

 $results[1], \ results[2], \ results[3], \ eW1 \\ \|eW2 \\ \|eW3, \ eP1 \\ \|eP2 \\ \|eP3, \ eP4 \\ \|eP4 \\ \|$ 

 $(\forall i \in [0..|post(eW)|-1]) (post(eW[i]) + post(eP[i]))$ , Prints infor-

mation about the melting of PCM.

exception: none

# 5 MIS of Input Parameters Module

The secrets of this module are the data structure for input parameters, how the values are input and how the values are verified. The load and verify secrets are isolated to their own access programs.

## 5.1 Module

Param

## 5.2 Uses

N/A

# 5.3 Syntax

Name	In	Out	Exceptions
load_params verify_params	string -	- B	FileError badLength, badDiam, badPCMVolume, bad- PCMAndTankVol, badPCMArea, badPCMDen- sity, badMeltTemp, badCoilAndInitTemp, bad- CoilTemp, badPCMHeatCapSolid, badPCMHeat- CapLiquid, badHeatFusion, badCoilArea, badWa- terDensity, badWaterHeatCap, badCoilCoeff, bad- PCMCoeff, badInitTemp, badFinalTime, badIni- tAndMeltTemp
L	-	$\mathbb{R}$	1
D	-	$\mathbb R$	
$V_P$	-	$\mathbb{R}$	
$A_P$	_	$\mathbb{R}$	
	-		

## 5.4 Semantics

# 5.4.1 Environment Variables

f: sequence of string #f[i] is the ith string in the text file f

# 5.4.2 State Variables

```
\# From R1
L: \mathbb{R}
D \colon \mathbb{R}
V_P: \mathbb{R}
A_P: \mathbb{R}
\rho_P:\mathbb{R}
T_{\mathrm{melt}}^{P}: \mathbb{R}
C_P^S: \mathbb{R}
C_P^L: \mathbb{R}
H_f: \mathbb{R}
A_C: \mathbb{R}
T_C: \mathbb{R}
\rho_W: \mathbb{R}
C_W: \mathbb{R}
h_C: \mathbb{R}
h_P: \mathbb{R}
T_{\text{init}}: \mathbb{R}
t_{\text{step}}: \mathbb{R}
t_{\text{final}}: \mathbb{R}
AbsTol: \mathbb{R}
RelTol: \mathbb{R}
 ConsTol: \mathbb{R}
\# From R2
V_{\text{tank}}: \mathbb{R}
m_W: \mathbb{R}
m_P: \mathbb{R}
\# From R3
\tau_W: \mathbb{R}
```

```
\begin{split} \eta \colon \mathbb{R} \\ \tau_P^S \colon \mathbb{R} \\ \tau_P^L \colon \mathbb{R} \\ \end{split}
\# \text{ To Support IM4} \\ E_{P\text{melt}}^{\text{init}} \colon \mathbb{R} \\ E_{P\text{melt}}^{\text{all}} \colon \mathbb{R} \\ \end{split}
\# \text{ To Support Testing} \\ \tau_P^L \ m_W^{\text{noPCM}} \colon \mathbb{R} \\ \tau_W^{\text{noPCM}} \colon \mathbb{R} \end{split}
```

## 5.4.3 Assumptions

load\_params will be called before the values of any state variables will be accessed.

#### 5.4.4 Access Routine Semantics

init():

- transition: L, diam, Vp, Ap, ..., tau\_w\_no\_PCM := 0, 0, 0, 0, ..., 0
- output: out := self
- exception: none

getL():

- $\bullet$  output: out := L
- exception: none

get\_diam():

- output: out := diam
- exception: none

getVp():

```
\bullet output: out := Vp
```

• exception: none

## getAp():

 $\bullet$  output: out := Ap

• exception: none

. . .

## get\_tau\_w\_no\_PCM():

 $\bullet$  output:  $out := tau_w_no_PCM$ 

• exception: none

## setL(x):

 $\bullet$  transition: L := x

• exception: none

## $set_diam(x)$ :

• transition: diam := x

• exception: none

## setVp(x):

 $\bullet$  transition: Vp := x

• exception: none

### setAp(x):

• transition: Ap := x

• exception: none

. . .

## $set_tau_w_no_PCM(x)$ :

• transition:  $tau_w_no_PCM := x$ 

• exception: none

## 5.5 Considerations

The value of each state variable can be accessed through its name (getter). An access program is available for each state variable. There are no setters for the state variables, since the values will be set and checked by load params and not changed for the life of the program.

# 6 MIS of Input Format Module

### 6.1 Module

Load\_params

### 6.2 Uses

Param (Section 5)

## 6.3 Syntax

## 6.4 Exported Access Programs

Name	In	Out	Exceptions	
load_params	string	-	-	

#### 6.5 Semantics

#### 6.5.1 Environment Variables

f: sequence of string #f[i] is the ith string in the text file f

#### 6.5.2 Assumptions

The input string corresponds to an existing filename. The name will be relative to the current directory. The input file is assumed to be formatted correctly. The file contains the string equivalents of the numeric values for each input parameter in order, each on a new line. The order is the same as in the table in R1 of the SRS. Any comments in the input file should be denoted with a '#' symbol.

#### 6.5.3 Access Routine Semantics

 $load_params(s)$ :

• transition: The filename s is first associated with the file f. File f is then used to modify the state of Param (Section 5) as follows:

- 1. Param.init()
- 2. Read data sequentially from f to populate the state variables of Param from L to ConsTol.
- 3. Calculate the derived quantities in Param as follows:
  - Param.setVt(calcVt(Param.getL(), Param.get\_diam()))
  - Param.setMw(calcMw(Param.getVp(), Param.get\_rho\_w(), Param.getVt()))
  - Param.set\_tau\_w(calcTauw(Param.getMw(), Param.getC\_w(), Param.get\_hc(), Param.getAc()))
  - Param.set\_eta(calcEta(Param.get\_hp(), Param.getAp(), Param.get\_hc(), Param.getAc()))
  - Param.setMp(calcMp(Param.get\_rho\_p(), Param.getVp()))
  - Param.set\_tau\_ps(calcTaups(Param.getMp(), Param.getC\_ps(), Param.get\_hp(), Param.getAp()))
  - Param.set\_taul\_pl(calcTaupl(Param.getMp(), Param.getC\_pl(), Param.get\_hp(), Param.getAp()))
  - Param.setEpmelt\_init(calcEpmeltinit(Param.getC\_ps(), Param.getMp(), Param.getTmelt(), Param.getTinit()))
  - $-\ Param.setEp\_melt3(calcEpmelt3(Param.getHf(), Param.getMp()))$
  - $-\ \operatorname{Param.setMw\_noPCM}(\operatorname{calcMwno}(\operatorname{Param.get\_rho\_w}, \operatorname{Param.getVt}()))$
  - Param.set\_tau\_no\_PCM(calcTauwnoPCM(Param.getMw\_noPCM(), Param.getC\_w(), Param.get\_hc(), Param.getAc()))
- exception: none

#### 6.5.4 Local Functions

calcVt: 
$$\mathbb{R} \times \mathbb{R} \to \mathbb{R}$$
  
calcVt $(L, d) \equiv \pi \times L \times (\frac{d}{2})^2$   
calcMw:  $\mathbb{R} \times \mathbb{R} \times \mathbb{R} \to \mathbb{R}$   
calcMw $(V_p, \rho_w, V_t) \equiv \rho_w(V_t - V_p)$   
calcTauw:  $\mathbb{R} \times \mathbb{R} \times \mathbb{R} \times \mathbb{R} \to \mathbb{R}$   
calcTauw $(m_w, C_w, h_c, A_c) \equiv \frac{m_w C_w}{A_c h_c}$   
calcEta:  $\mathbb{R} \times \mathbb{R} \times \mathbb{R} \times \mathbb{R} \to \mathbb{R}$ 

calcEta
$$(h_p, A_p, h_c, A_c) \equiv \frac{h_p A_p}{h_c A_c}$$

calcMp: 
$$\mathbb{R} \times \mathbb{R} \to \mathbb{R}$$
  
calcMp $(\rho_p, V_p) \equiv \rho_p V_p$ 

calcTaups: 
$$\mathbb{R} \times \mathbb{R} \times \mathbb{R} \times \mathbb{R} \to \mathbb{R}$$
  
calcTaups $(M_p, C_{ps}, h_p, A_p) \equiv \frac{M_p C_{ps}}{h_p A_p}$ 

calcTaupl: 
$$\mathbb{R} \times \mathbb{R} \times \mathbb{R} \times \mathbb{R} \to \mathbb{R}$$
  
calcTaupl $(M_p, C_{pl}, h_p, A_p) \equiv \frac{M_p C_{pl}}{h_p A_p}$ 

calcEpmeltinit: 
$$\mathbb{R} \times \mathbb{R} \times \mathbb{R} \times \mathbb{R} \to \mathbb{R}$$
  
calcEpmeltinit( $C_{ps}$ ,  $M_p$ ,  $T_{\text{melt}}$ ,  $T_{\text{init}}$ )  $\equiv C_{ps}M_p(T_{\text{melt}} - T_{\text{init}})$ 

calcEpmelt3: 
$$\mathbb{R} \times \mathbb{R} \to \mathbb{R}$$
  
calcEpmelt3( $H_f, M_p$ )  $\equiv H_f M_p$ 

calcMwnoPCM: 
$$\mathbb{R} \times \mathbb{R} \to \mathbb{R}$$
  
calcMwnoPCM( $\rho_w, V_t$ )  $\equiv \rho_w V_t$ 

calcTauwnoPCM: 
$$\mathbb{R} \times \mathbb{R} \times \mathbb{R} \times \mathbb{R} \to \mathbb{R}$$
 calcTauwnoPCM $(M_{w\text{noPCM}}, C_w, h_c, A_c) \equiv \frac{M_{w\text{noPCM}}C_w}{h_cA_c}$ 

# 7 MIS of Input Verification Module

# 7.1 Module

 $verify\_params$ 

## 7.2 Uses

Param (Section 5)

# 7.3 Syntax

## 7.3.1 Exported Access Programs

Name	In	Out	Exceptions
verify_valid	-	-	badLength, badDiam, badPCMVolume, bad-PCMAndTankVol, badPCMArea, badPCMDensity, badMeltTemp, badCoilAndInitTemp, bad-CoilTemp, badPCMHeatCapSolid, badPCMHeat-CapLiquid, badHeatFusion, badCoilArea, badWaterDensity, badWaterHeatCap, badCoilCoeff, bad-
			PCMCoeff, badInitTemp, badFinalTime, badInitAndMeltTemp
verify_recommend	d -	_	-

## 7.4 Semantics

## 7.4.1 Assumptions

All of the fields Param have been assigned values before any of the access routines for this module are called.

### 7.4.2 Access Routine Semantics

verify\_valid():

• transition: none

```
• exceptions: exc := (
  Param.getL() \le 0 \Rightarrow badLength
  Param.get_diam() \leq 0 \Rightarrow \text{badDiam}
  Params.get_Vp() \leq 0 \Rightarrow \text{badPCMVolume}
  Params.getVp() \ge Params.Vt \Rightarrow badPCMAndTankVol
  Params.getAp() \leq 0 \Rightarrow \text{badPCMArea}
  Params.get_rho_p() \leq 0 \Rightarrow \text{badPCMDensity}
  Params.getTmelt() \leq 0 \Rightarrow \text{badMeltTemp}
  Params.getTmelt() > Params.getTc() \Rightarrow badMeltTemp
  Params.getTc() \leq Params.getTinit() \Rightarrow badCoilAndInitTemp
  Params.getTc() > 100 \lor Params.getTc() < 0 \Rightarrow badCoilTemp
  Params.getC_ps() \leq 0 \Rightarrow \text{badPCMHeatCapSolid}
  Params.getC_pl() \leq 0 \Rightarrow \text{badPCMHeatCapLiquid}
  Params.getHf() \leq 0 \Rightarrow \text{badHeatFusion} \mid
  Params.getAc() \leq 0 \Rightarrow \text{badCoilArea}
  Params.get_rho()_w \leq 0 \Rightarrow \text{badWaterDensity} \mid
  Params.getC_w() \leq 0 \Rightarrow \text{badWaterHeatCap}
  Params.get_hc() \leq 0 \Rightarrow \text{badCoilCoeff}
  Params.get_hp() \leq 0 \Rightarrow \text{badPCMCoeff}
  Params.getTinit() < 0 \lor Params.getTinit() > 100 \Rightarrow badInitTemp
  Params.get_tfinal() \leq 0 \Rightarrow \text{badFinalTime}
  Params.getTinit() \ge Params.getTmelt() \Rightarrow badInitAndMeltTemp)
verify_recommend():
• transition: none
\bullet exceptions: exc := (
  Params.getL() < 0.1 \lor Params.getL() > 50 \Rightarrow warnLength
  Params.getdiam() / Params.getL() < 0.002 \times Params.getdiam() / Params.getL()
  > 200 \Rightarrow \text{warnDiam}
  Params.getVp() < Params.getVt() \times 10^{-}6 \Rightarrow warnPCMVol |
  Params.getVp() > Params.getAp() \vee Params.getAp > (2/0.001) \times Params.getVp()
  ⇒ warnVolArea |
  (Params.get\_rho\_p() < 500) \lor (Params.get\_rho\_p() > 20000) \Rightarrow warn-
  PCMDensity | ... )
  # Need to continue for the rest of the example - tabular form? # Should
  add a module (Configuration Module) to store symbolic constants
```

# 7.5 Considerations

See Appendix (Section 14) for the complete list of exceptions and associated error messages.

# 8 MIS of Temperature ODEs Module

### 8.1 Module

temperature

### 8.2 Uses

Param (Section 5)

# 8.3 Syntax

### 8.3.1 Exported Access Programs

Name	In	Out	Exceptions
ODE_SolidPCM	=	sequence[2] of $\mathbb{R} \to \text{sequence}[2]$ of $\mathbb{R}$	-
ODE_MeltingPCM	_	sequence[3] of $\mathbb{R} \to \text{sequence}[3]$ of $\mathbb{R}$	-
ODE_LiquidPCM	_	sequence[2] of $\mathbb{R} \to \text{sequence}[2]$ of $\mathbb{R}$	-
event_StartMelt	_	sequence[2] of $\mathbb{R} \to \mathbb{R}$	-
event_EndMelt	_	sequence[3] of $\mathbb{R} \to \mathbb{R}$	-

#### 8.4 Semantics

#### 8.4.1 State Variables

none

#### 8.4.2 Assumptions

none

#### 8.4.3 Access Routine Semantics

ODE\_SolidPCM():

• output: 
$$out := \frac{d}{dt} \begin{bmatrix} T_W \\ T_P \end{bmatrix} = \begin{bmatrix} \frac{1}{\tau_W} [(T_C - T_W(t)) + \eta(T_P(t) - T_W(t))] \\ \frac{1}{\tau_P^S} (T_W(t) - T_P(t)) \end{bmatrix}$$

• exception: none

ODE\_MeltingPCM():

• output: 
$$out := \frac{d}{dt} \begin{bmatrix} T_W \\ T_P \\ Q_P \end{bmatrix} = \begin{bmatrix} \frac{1}{\tau_W} [(T_C - T_W(t)) + \eta(T_P(t) - T_W(t))] \\ 0 \\ h_P A_P (T_W(t) - T_{\text{melt}}^P) \end{bmatrix}$$

• exception: none

ODE\_LiquidPCM():

• output: 
$$out := \frac{d}{dt} \begin{bmatrix} T_W \\ T_P \end{bmatrix} = \begin{bmatrix} \frac{1}{\tau_W} [(T_C - T_W(t)) + \eta(T_P(t) - T_W(t))] \\ \frac{1}{\tau_P^L} (T_W(t) - T_P(t)) \end{bmatrix}$$

• exception: none

event\_StartMelt():

- output:  $out := g([T_W, T_P]^T) = T_{\text{melt}}^P T_P$
- exception: none

event\_EndMelt():

- output:  $out := g([T_W, T_P, Q_P]^T) = 1 \phi$ , where  $\phi = \frac{Q_P}{H_f m_P}$
- exception: none

# 9 MIS of ODE Solver Module

# 9.1 Module

ODE Solver Module

## 9.2 Uses

N/A

# 9.3 Syntax

## 9.3.1 Exported Constants

MaxStep: natural number

N: natural number

# 9.3.2 Exported Access Programs

Name	In	Out	Exceptions
solve	function, array of $\mathbb{R}$ , array of $\mathbb{R}$ , function, $\mathbb{R}$ , $\mathbb{R}$	array of $\mathbb{R}$ (N of them)	ODE_BAD_INPUT, ODE_MAXSTEP, ODE_ACCURACY

## 9.4 Semantics

### 9.4.1 State Variables

results: array of  $\mathbb{R}$  (N of them)

#### 9.4.2 Access Routine Semantics

 $\mbox{solve}(f,\,domain,\,ics,\,events,\,abstol,\,reltol) \quad \mbox{out := } results, \mbox{ where } \\ results \mbox{ holds the solution to } \\ \mbox{the ODE system generated } \\ \mbox{by the solver.}$ 

exceptions: exc := (Invalid input parameters  $\Rightarrow$  ODE\_BAD\_INPUT | MaxStep steps taken and no solution found  $\Rightarrow$  ODE\_MAXSTEP | reltol and abstol not satisfied for a step  $\Rightarrow$  ODE\_ACCURACY)

# 10 MIS of Energy Module

# 10.1 Module

energy

## 10.2 Uses

Param (Section 5)

# 10.3 Syntax

# 10.3.1 External Access Programs

Name	In	Out	Exceptions
energy1Wat	array of $\mathbb{R}$ , parameters	array of $\mathbb{R}$	-
energy1PCM	array of $\mathbb{R}$ , parameters	array of $\mathbb{R}$	-
energy2Wat	array of $\mathbb{R}$ , parameters	array of $\mathbb{R}$	-
energy2PCM	array of $\mathbb{R}$ , parameters	array of $\mathbb{R}$	-
energy3Wat	array of $\mathbb{R}$ , parameters	array of $\mathbb{R}$	-
energy3PCM	array of $\mathbb{R}$ , parameters	array of $\mathbb{R}$	-

# 10.4 Semantics

### 10.4.1 State Variables

eW1: array of  $\mathbb{R}$  eP1: array of  $\mathbb{R}$  eW2: array of  $\mathbb{R}$  eP2: array of  $\mathbb{R}$  eW3: array of  $\mathbb{R}$  eP3: array of  $\mathbb{R}$ 

# 10.4.2 Assumptions

All of the fields of the input parameters structure have been assigned a value. The values have been properly constrained.

#### 10.4.3 Access Routine Semantics

energy1Wat(Tw1, params): transition:  $(\forall i \in [0..|Tw1|-1]) (eW1[i] := [0..|Tw1|-1])$ 

watEnergy(Tw1[i], params))

output: out := eW1

exception: none

energy1PCM(Tp1, params): transition:  $(\forall i \in [0..|Tp1| - 1]) (eP1[i] :=$ 

pcmEnergy1(Tp1[i], params))

output: out := eP1

exception: none

energy2Wat(Tw2, params): transition:  $(\forall i \in [0..|Tw2|-1]) (eW2[i] :=$ 

watEnergy(Tw2[i], params))

output: out := eW2

exception: none

energy2PCM(Qp2, params): transition:  $(\forall i \in [0..|Qp2|-1]) (eP2[i] := 0...$ 

pcmEnergy2(Qp2[i], params))

output: out := eP2

exception: none

energy3Wat(Tw3, params): transition:  $(\forall i \in [0..|Tw3| - 1]) (eW3[i] :=$ 

watEnergy(Tw3[i], params))

output: out := eW3

exception: none

energy3PCM(Tp3, params): transition:  $(\forall i \in [0..|Tp3|-1]) (eP3[i] :=$ 

27

pcmEnergy3(Tp3[i], params))

output: out := eP3

exception: none

#### 10.4.4 Local Functions

```
watEnergy: \mathbb{R} \times \text{parameters} \to \mathbb{R}

watEnergy(Tw, params) \equiv params.C_{-}w \times params.Mw \times (Tw-params.Tinit)

pcmEnergy1: \mathbb{R} \times \text{parameters} \to \mathbb{R}

pcmEnergy1(Tp, params) \equiv params.C_{-}ps \times params.Mp \times (Tp-params.Tinit)

pcmEnergy2: \mathbb{R} \times \text{parameters} \to \mathbb{R}

pcmEnergy2(Qp, params) \equiv params.Epmelt\_init + Qp

pcmEnergy3: \mathbb{R} \times \text{parameters} \to \mathbb{R}

pcmEnergy3(Tp, params) \equiv params.Epmelt\_init + params.Ep\_melt3 + params.C_{-}pl \times params.Mp \times (Tp-params.Tmelt)
```

# 11 MIS of Output Verification Module

## 11.1 Module

verify\_output

#### 11.2 Uses

Param (Section 5)

## 11.3 Syntax

### 11.3.1 Exported Access Programs

Name	In	Out	Exceptions
verify_output	array of $\mathbb{R}$ , parameters	-	-

### 11.4 Semantics

#### 11.4.1 State Variables

expEPCM: array of  $\mathbb{R}$  expEWat: array of  $\mathbb{R}$ 

 $errorWater: \mathbb{R}$   $errorPCM: \mathbb{R}$ 

### 11.4.2 Environment Variables

win: 2D array of pixels displayed on the screen

#### 11.4.3 Local Variables

#### 11.4.4 Assumptions

All of the fields of the input parameters structure have been assigned a value. The values have been properly constrained. The input arrays are not empty.

#### 11.4.5 Access Routine Semantics

verify\_output(t, Tw, Tp, Ew, Ep, params): transition: expEPCM, expEWat, errorWater, errorPCM,  $win := (\forall i)$ [1..|t| - 1] $\in$ (expectedEp(traprule(delta(t[i t[i]),Tw[i],Tp[i],Tw[i-1], Tp[i-1], params), $(\forall i \in [1..|t|-1])$  (expectedEw (expectedEc(traprule(delta(t[i params.Tc,1], t[i]),params.Tc, Tw[i]1]),post(expEPCM))),params), $\operatorname{error}(\operatorname{sum}(\operatorname{post}(expEWat)),$ Ew[|Ew|]1]), $\operatorname{error}(\operatorname{sum}(\operatorname{post}(expEPCM)),$ Ep[|Ep|-1]), (errorWater > $ConsTol \lor errorPCM$ ConsTol $\Rightarrow$  Prints warning message(s)

exception:  $(errorWater > ConsTol \Rightarrow warnWaterError | errorPCM > ConsTol \Rightarrow warnPCMError)$ 

These exceptions do not termi-

nate the program.

#### 11.4.6 Local Functions

delta:  $\mathbb{R} \times \mathbb{R} \to \mathbb{R}$ delta $(t1, t2) \equiv t2 - t1$ 

traprule:  $\mathbb{R} \times \mathbb{R} \times \mathbb{R} \times \mathbb{R} \times \mathbb{R} \to \mathbb{R}$ traprule $(t, A1, B1, A2, B2) \equiv t \times (A1 - B1 + A2 - B2)/2$ 

expectedEc:  $\mathbb{R} \times \text{parameters} \to \mathbb{R}$ expectedEc(c, params)  $\equiv params.hc \times params.Ac \times c$  expectedEp:  $\mathbb{R} \times \text{parameters} \to \mathbb{R}$ expectedEp $(p, params) \equiv params.hp \times params.Ap \times p$ 

expectedEw:  $\mathbb{R} \times \mathbb{R} \to \mathbb{R}$ expectedEw(Ec, Ep)  $\equiv Ec - Ep$ 

sum: array of  $\mathbb{R}s \to \mathbb{R}$ sum $(a) \equiv \sum_{i=0}^{|a|-1} a[i]$ 

error:  $\mathbb{R} \times \mathbb{R} \to \mathbb{R}$ error $(exp, act) \equiv \frac{|exp-act|}{act} \times 100$ 

# 12 MIS of Plotting Module

# 12.1 Module

plot

## 12.2 Uses

N/A

# 12.3 Syntax

## 12.3.1 Exported Access Programs

Name	In	Out	Exceptions
plot	array of $\mathbb{R}$ , string	_	-

### 12.4 Semantics

## 12.4.1 State Variables

plotFilename: string

#### 12.4.2 Environment Variables

directory: The current directory of files from which the program is run.

## 12.4.3 Assumptions

The input arrays are all of the same size.

## 12.4.4 Access Routine Semantics

plot(t, Tw, Tp, Ew, Ep, filename): transition: directory: writes a .png file

named plotFilename containing

the graphs of the simulation re-

sults.

exception: none

# 13 MIS of Output Module

# 13.1 Module

output

## 13.2 Uses

Param (Section 5)

# 13.3 Syntax

## 13.3.1 Exported Constants

 $max\_width$ : integer

# 13.3.2 Exported Access Program

Name	In	Out	Exceptions
output	string, array of $\mathbb{R}$ , parameters	-	-

### 13.4 Semantics

### 13.4.1 State Variables

outFilename: string

### 13.4.2 Environment Variables

directory: The current directory of files from which the program is run.

#### 13.4.3 Access Routine Semantics

output(params, t, Tw, Tp, Ew, Ep, ETot, filename): transition: directory: writes

a .txt file named outFilename containing the input parameters, calculated parameters, and results of the

simulation.

exception: none

# References

Carlo Ghezzi, Mehdi Jazayeri, and Dino Mandrioli. Fundamentals of Software Engineering. Prentice Hall, Upper Saddle River, NJ, USA, 2nd edition, 2003.

Daniel M. Hoffman and Paul A. Strooper. Software Design, Automated Testing, and Maintenance: A Practical Approach. International Thomson Computer Press, New York, NY, USA, 1995.

# 14 Appendix

Table 2: Possible Exceptions

Message ID	Error Message
badLength	Error: Tank length must be $> 0$
badDiam	Error: Tank diameter must be $> 0$
${\it badPCMVolume}$	Error: PCM volume must be $> 0$
bad PCM And Tank Vol	Error: PCM volume must be < tank volume
badPCMArea	Error: PCM area must be $> 0$
badPCMDensity	Error: rho_p must be $> 0$
${\bf badMeltTemp}$	Error: Tmelt must be $> 0$ and $< Tc$
bad Coil And In it Temp	Error: Tc must be > Tinit
badCoilTemp	Error: Tc must be $> 0$ and $< 100$
${\it badPCMHeatCapSolid}$	Error: C <sub>-ps</sub> must be $> 0$
${\it badPCMHeatCapLiquid}$	Error: C <sub>-pl</sub> must be $> 0$
badHeatFusion	Error: Hf must be $> 0$
badCoilArea	Error: Ac must be $> 0$
badWaterDensity	Error: $rho_w$ must $be > 0$
${\bf badWaterHeatCap}$	Error: $C_{-}w$ must be $> 0$
badCoilCoeff	Error: hc must be $> 0$
badPCMCoeff	Error: hp must be $> 0$
${\bf badInitTemp}$	Error: Tinit must be $> 0$ and $< 100$
badFinalTime	Error: tfinal must be $> 0$
badInit And Melt Temp	Error: Tinit must be < Tmelt
ODE_ACCURACY	reltol and abstol were not satisfied by the ODE solver for a given solution step.
ODE_BAD_INPUT	Invalid input to ODE solver
$ODE\_MAXSTEP$	ODE solver took $MaxStep$ steps and did not find solution
warnLength	Warning: It is recommended that $0.1 \le L \le 50$
warnDiam	Warning: It is recommended that $0.002 \ll D/L \ll 200$

warnPCMVol	Warning: It is recommended that Vp be $>= 0.0001\%$ of Vt
warnVolArea	Warning: It is recommended that $Vp \le Ap \le (2/0.001) * Vp$
warnPCMDensity	Warning: It is recommended that $500 < \text{rho\_p} < 20000$
warn PCM Heat Cap Solid	Warning: It is recommended that $100 < C_ps < 4000$
warn PCM Heat Cap Liquid	Warning: It is recommended that $100 < C_{-}pl < 5000$
warnCoilArea	Warning: It is recommended that Ac $\leq$ pi * (D/2) $\wedge$ 2
warnWaterDensity	Warning: It is recommended that 950 < rho_w <= 1000
warnWaterHeatCap	Warning: It is recommended that $4170 < C_w < 4210$
warnCoilCoeff	Warning: It is recommended that $10 < hc < 10000$
warnPCMCoeff	Warning: It is recommended that $10 < hp < 10000$
warn Final Time	Warning: It is recommended that $0 < \text{tfinal} < 86400$
warnWaterError	Warning: There is greater than $x\%$ relative error between the energy in the water output and the expected output based on the law of conservation of energy. (Where $x$ is the value of $ConsTol$ )
warnPCMError	Warning: There is greater than $x\%$ relative error between the energy in the PCM output and the expected output based on the law of conservation of energy. (Where $x$ is the value of $ConsTol$ )