O a) Fed Batch
We can imagine the system to share water
the can imagine with heat being supplied to
the stored water

Furthing Tick

There is no flow out because it is a storage geyser

b) Variably: Fin, hope, Trank, Tin, Q

-Interriphent of Fin, Q (where fin variables: Fin, Q (where fin added as the heat added as the heat added of the summer that Q can be modified) by the

Disturbance Tin (Enlet temperature of variables : Tin (Enlet temperature of variables : water is directed by outside conditions)

-s controlled . Trank (temperature of water is the beach

9 Feedback eystern: Measure the temperature of tank (Trank) and manipulate Fir and Q awardingly. Fin manipulated by a value of ly using a rheatate temperature set-point controller. Disturbance (eg. thermocouple d) Feedforward system! We measure Tis (the distribune) and accordingly charge the manipulated variable Trank st part Fin 12 Greyry Track Disturbance (Tim)

2 a) At steady state dy - dy -0 3 yet) yss = bo uss. ______ Consider the ODE It' + andy + any (t) = bom(t) d29 (y-yrs) + a1 de (y-yrs) + a. (y(t)-yrs) = 60 (ult) - 4:8) (-: dys, 0 -> 423 0 9 tot) But @ 3 90485 = 6048 · · d² y + a1 dy + a0 y(+) = b0 v (t) (This is expected because the ODE is linear) 485= 60 H85= 3 X MS 3 => ao 3ss = bo 4ss (@ steadystatt) · 3 3/2 220 = 60 % 1 M = 2 × 15 Edurate - MY

Soutstituting In (6)= Kc (2-3 (t)) in you, 129 andy + an 3/t) = bokc (2-5/t) a) deg + aidy + g(t) (ao + boke) = 2boke Now to answer whether the eystern will allieve the control objective is eget to asking whether the system the system in 4 raturates (whether it is stable) To analyse the stability we can see the poles of tail new rystem. Also dig | -0 & dig | =0 & 5'(+) | =0

His dig | -0 & dig | +0 because the system is initially amoned to be in steady state. So & \{ \langle \degree \degre and I { dy } = sy(s)

of taking Laplace transfer, 3 9(s) +9159(s) + 209(s) = 200 × c + box c 9(s) 7 9(s) 4 = 2 bo Kc By Frank Value term, we need the conditions SY(s) to be stable. ≥ 'root of 52+ a15+a0 thece o -) -ait Vai- 4 (ao+boxkc) Co When that > ¿a² - 4 (ao - 160 Kc) < a² \Rightarrow Kc $\leq \frac{\alpha^2 - 490}{450}$ and $|CC| > -\frac{490}{50}$ $3 \times c \leq \frac{1}{3}$ and $\times 3$, 7-53-5 LKc = 1/3 3 0 CKC = 1/3 under such conditions we apply FVT

to get y(+) Lt = 14 5 9 (5)

7 H & J(+) = H & 2 ho Kc 3+100 \$ (3+915+90+50 Kc) Require d'objecture is attained for o LKc & 1/3 d) (3) dry + 9, dry + 90 y (6) = 6. m(t) - Differentiets urt til, d³y + a1d²y + aody = body dt dt = bo (Kc/- day) + kg

ten notational convenience, ~ is dropped (2-y))

(90 + 10 Kc)

(90 + 10 Kc)

dy + (0, + bookse) d2y + 90 dy + 50 y kg

dt2 ddt bo k2y Smiles to previous part, take Leplane transform (83+ a152-1 (a0+ boxc) S+ 50 KI) YCS)

2 Kz 60 => Y(3) = S(53+ a152+ 60+ 50 K) 5-1 50 KI) Let We want the poly (5 Y (5)) to be stable of roots (54 a 15t + (ao + to Ke) 5+ to KI) (0 2 roots (53+852+ (15+3Kc) 5+3KI) (0 Assuming roots obey that property, apply FUT H ytt) = H 5x 2 K ± 60 6 30 5 (3 3 4 9 1 2 4 60 1 40 4 6) - Objective is achieved. Conclusion: The objective can't be achieved for any { Kc , F I }, it is achieved only when 3 is satisfixed. -3.9+1.141 eg. Kc = Kz = 1, roots al -3 objecture is not achieved. 0.181 +000 But for Kc = 0.25 1 K = = 0.5 rosts are -4.25, -3.14, -0.1 objective is achieved.

- - (L-149) w + - 49 2 M M - 0 252 81 dz = - Lw - (L+1/9) 2 + - 1/2+ At slendy thate , L= Lss -4, Y - 455 = 200 du =0 , d2 =0 O 3 -65 W + 2.5 Z = 0 - 3 33 4w - 6.52 = -0.5 - 19 Solving 3 4 4 1 was 0.038 and Zes = 0.1008 0) Steady stute relies: w= 0.0388 8001 0 In this model, state = [w] Enputs = [] Let die = f(·) & die -g(·) (+ 3t (1-12) 81 dt + 3+ (w- ww) 2+ (2-24)

$$\frac{3}{3} \times (5)^{2} = \frac{(1+5)e^{35} - 25 + 1}{5^{2}} = \frac{5}{3}$$

$$\frac{5}{3} = \frac{6}{9}$$

$$\frac{5}{3} = \frac{1}{9}$$

$$\frac$$

$$\frac{9\pi^{2}}{5^{2}} + 1$$

Food John No. + (5-2) (Db) 5-2 5 173-129TS+1) T25 (#12-12-91-11) Park of # 52-1 2 EX 5-1 Te = - 49 ± 59-1 (without)

Try our wit 4921 15 \$ (1 = 3-2 13(5+245+1) Box 3001 145=44 T2 $A2 = \frac{A-2}{+2} \cdot A3 - \frac{B-2}{-72}$

Q3 Part d)

```
linsys =
```

```
A =
```

Integ1 Integ2

Integ1 -6.5 2.5

Integ2 4 -6.5

B =

FR FR1

Integ1 -0.001938 0.00155

Integ2 -0.003101 0.002481

C =

Integ1 Integ2

Out1 1 0

Out2 0 1

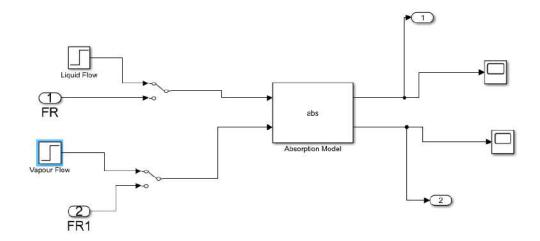
D =

FR FR1

Out1 0 0

Out2 0 0

Continuous-time state-space model.

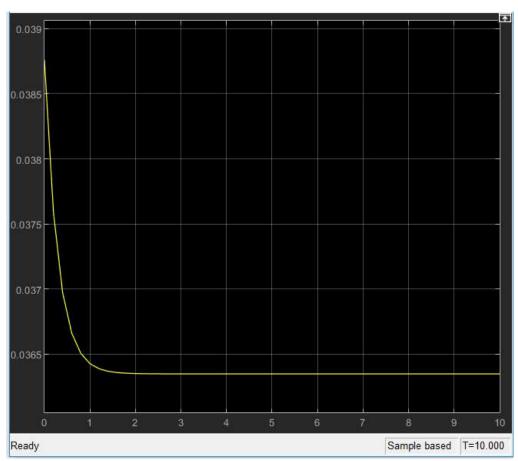


Part e)

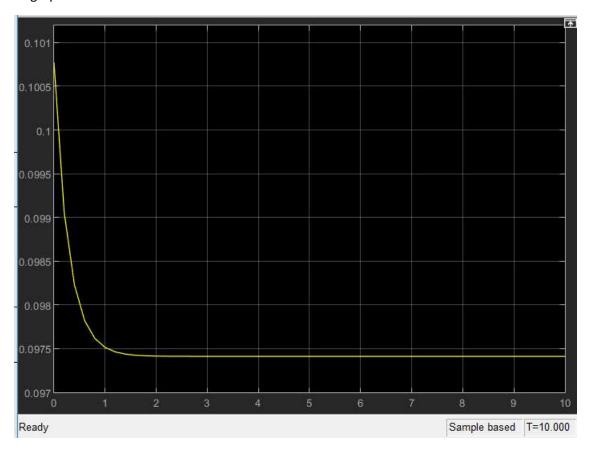
Since if we change both the flow rates, steady state values are same as original, I am changing only L in both cases.

ALL GRAPHS ARE FROM NON LINEAR MODEL. I DID NOT PLOT FOR LINEAR MODEL.

i) $L = 1.05L_{ss}$

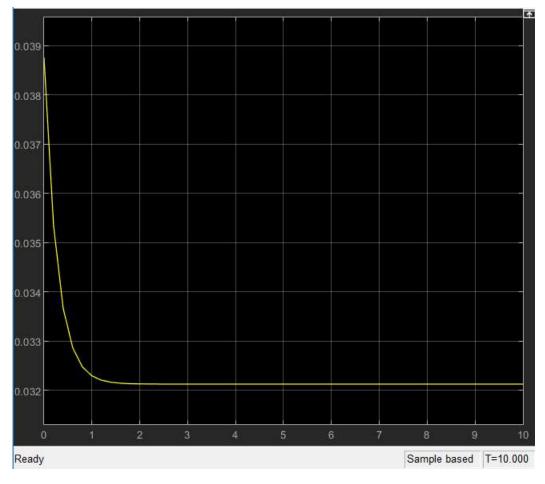


W graph

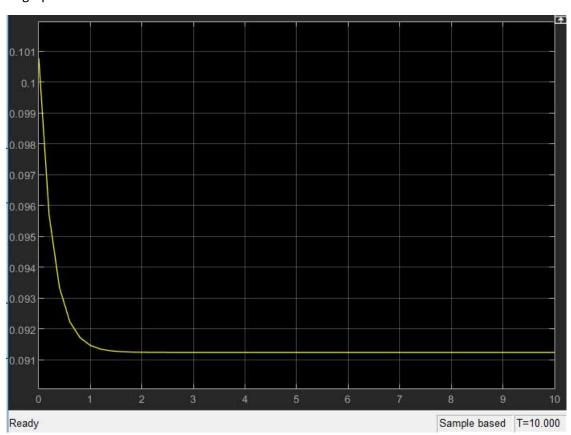


Z graph

ii) L= 1.15L_{ss}



W graph



```
Code:
clear; close all;
%% System charecterstics
Lss = 80; Vss = 100;
M = 20; a=0.5; zf = 0.1;
%% Part a) Finding steady state (by hand)
% Equate derivatives to zero, solve the linear eqn
Ass = [-(a*Vss+Lss)/M Vss*a/M;Lss/M - (a*Vss+Lss)/M];
bss = [0; -Vss*zf/M];
x_s = inv(Ass)*bss;
%% Part b) Linearisation (by Taylor Expansion)
w_s = x_s(1); z_s = x_s(2);
A = [-(Vss*a+Lss)/M Vss*a/M;Lss/M -(Lss+Vss*a)/M];
B = [-w_ss/M (-a*w_ss+a*z_ss)/M;(w_ss-z_ss)/M -a*z_ss/M+zf/M];
%% Part c) Finding the eigenvalues-eignvectors of the system
[V,D] = eig(A);
% Second eigen value is faster (more negative)
%% Part d) Find steady-state and linearise
open_system('Q3_model')
% Read the operating conditions into an object
opc = operspec('Q3_model');
% Operating conditions
opc.Inputs(1).u = 80;
opc.Inputs(2).u = 100;
opc.Inputs(1).Known = 1;
opc.Inputs(2).Known = 1;
% Constraints
opc.States(1).Min = 0;opc.States(2).Min = 0;
```

```
% Find the steady state point
ss_point = findop('Q3_model',opc);
% Linearize
linsys = linearize('Q3_model',ss_point)
%% Part e) Give step changes and plot
% Done in SIMULINK. Use the manual switch to step input(s)
[Y,T,X]=step(linsys);
plot()
```