

INDIAN INSTITUTE OF TECHNOLOGY MADRAS
Department of Chemical Engineering

CH3050 Process Dynamics and Control
Assignment 1

Due: Tuesday, February 23, 2021 11:55 PM

Exercise

- Consider a household storage geyser that provides hot fluid stream to the user by heating the incoming cold water. Do / answer each of the following:
 - Classify the process as a continuous / batch / fed-batch process.
 - Identify the controlled variables, manipulated variables, and disturbance variables.
 - Propose a feedback control method and sketch the schematic diagram.
 - Suggest a feed-forward control method and sketch the schematic diagram.
- An input-output dynamical system is governed by

$$\frac{d^2y}{dt^2} + a_1 \frac{dy}{dt} + a_0 y(t) = b_0 u(t), \quad a_1 = 8, a_0 = 15, b_0 = 3$$

- Re-write the ODE in terms of deviations from steady-state, $\tilde{u}(t) = u(t) - u(0)$, $\tilde{y}(t) = y(t) - y(0)$, where $u(0)$ and $y(0)$ are the steady-state input and output, respectively.
 - AahaOohu wishes to increase the steady-state value of output by 2 units. To realize this objective, he decides to change the input by a fixed value. Determine the amount of change in input that is required.
 - Due to uncertainties in a_0 and b_0 , AahaOohu wishes to deploy a feedback strategy by changing the input proportional to the error $\tilde{u}(t) = K_c e(t)$, where $e(t) = 2 - \tilde{y}(t)$. Will the control objective be achieved for any finite value of $K_c > 0$?
 - In a different scheme of feedback control, AahaOohu changes the rate of input as $\dot{\tilde{u}}(t) = K_c \dot{e}(t) + K_I e(t)$. Will the control objective be achieved for any value of K_c and K_I ?
- Consider the following model of 2-stage absorption model:

$$\begin{aligned} \frac{dw}{dt} &= -\frac{L+Va}{M}w + \frac{Va}{M}z \\ \frac{dz}{dt} &= \frac{L}{M}w - \frac{L+Va}{M}z + \frac{V}{M}z_f \end{aligned}$$

where w and z are liquid concentrations on stage 1 and 2, respectively. L and V are the liquid and vapour molar flow rates, z_f is the concentration of the vapour stream entering the column. The steady-state input values are $L = 80$ gmol inert liquid/min and $V = 100$ gmol inert vapour/min. The parameter values are $M = 20$ gmol inert liquid, $a = 0.5$ and $z_f = 0.1$ gmol solute / gmol inert vapour.

Do / answer each of the following:

- (a) Find the steady-state values of w and z .
- (b) Obtain a linearized state-space model around the normal steady-state operation assuming that L and V are the inputs.
- (c) Find the eigenvalues of the system. What are the expected "slowest" and "fastest" initial condition directions of the system?
- (d) Set up the non-linear system in MATLAB. Solve for steady-state and obtain a linearized model using the linear analysis tools in MATLAB/SIMULINK.
- (e) Plot and compare the step responses of the non-linear system with that of the linearized model for two different magnitudes of steps (i) 5% and (ii) 15% change in the flow rate.

4. Answer the following

(a) Find the Laplace Transform of the signal $x(t) = \begin{cases} t - 2 & 0 \leq t < 3 \\ 1 & 3 \leq t < 4 \\ -\cos(3\pi(t - 4)) & 4 \leq t < 5 \\ e^{-2(t-5)} \cos(5\pi(t - 5)) & t \geq 5 \end{cases}$.

- (b) Find the inverse Laplace transform of $X(s) = \frac{(s - 2)}{s(\tau^2 s^2 + 2\zeta\tau s + 1)}$, where $\tau > 0$. Consider three different cases: (i) $\zeta > 1$, (ii) $\zeta = 1$ and (iii) $0 \leq \zeta < 1$