O a) Fed Batch
We can imagine the system to share water
flouring in with heat being supplied to
the stored water

Far, Tin

There is no flow out because it is a storage geyser

b) Variably: Fir, hyane Trave, Tin, Q

Manipulated : # Fin, Q (where fin variables: # Fin, Q (where fin added is the heat added is flow in, and Q is the heat added it will be that a can be modified) to the

Disturbance Tin (Enlet temperature of variables water is directed by outside conditions)

-s controlled . Trank (temperature of water is the beach

9 Feedback system: Measure the temperature of tank (Trank) and manipulate Fire and Q awardingly. Fir manipulated by a value of ly using a rheartate tangerotus set-point controller. (eg. thermowyll d) Feedforward system! We measure Tis (the distribune) and accordingly charge the manipulated variable. Trank st point Finial Suyu Track Disturbance (Tin)

2 a) At steady state dy - dy -0 3 yet) yss = bo uss. ______ Consider the ODE dt + andy + any (t) = bounct) d29 (y-yrs) + a1 de (y-yss) + a. (y(t)-yrs) = 60 (ult) - 4'8) (": dyss. 0 -> yss is a that) But (1 3 90485 = 6048) · · d² y + a1 dy + a0 y() = b0 y (t) (This is expected because the ODE is linear) 485= 60 H852 Y85 3 X MS 3 => ao 3'ss = bo 4'ss (@ steadystate) · 3 3/2 220 = 60 ~ 1 m = 2 × 15 Edura OT - NV [E

Sometituting In (6)= Kc (2-4 (t)) is you, 129 andy + anglt) = bokc (2-9(t)) $= 3 \frac{d^2 \tilde{y}}{dt^2} + \alpha_1 d\tilde{y} + \tilde{y}(t) (a_0 + b_0 k_0) = 2b_0 k_0$ Now to answer whether the eystern will allieve the control objective is eget to asking whether the system the system in 4 raturates (whether it is stable) To analyse the stability we can see the poles of tail new rystem. Also dig | -0 & dig | -0 & 5'(+) | =0

dig | +0 | dt | +0 because the system is initially amoned to be in steady state. So & \{ \langle \degree \degre and I { dy } = sy(s)

of taking Laplace transfer, 3 Y(s) +915 Y(s) + 20 Y(s) = 200 Kc + 60 Kc Y(s) 7 9(3) 4= 2 bo Kc By Fral Value fam, we need the conditions SY(s) to be stable. ≥ 'root of 52+ a15+a0 the < 0 - - a 1 = Vai - 4 (a 0 + b 0 1 Kc) < 0 When the > ¿ai - 4 (ao - 1 bo Kc) < ai \Rightarrow Kc $\leq \frac{\alpha^2 - 4a_0}{4b_0}$ and $|CC\rangle - \frac{4a_0}{b_0}$ 1) Kc \(\frac{1}{3} \) and \(\chi_{\eta} \) \(7 - 5 \) 3-5 LKc = 1/3 3 0 CKC = 1/3 under such conditions we apply FVT

to get y(4) let = 14 5 9 (5)

7 t + 3 9(t) = lt \$10 2 ho Kc
3+100 \$ (3+915+90+50 Kc) Require d'objecture is attained for o LKc & 1/3 d) (3) dry + 9, dry + 90 y(t) = bo M(t) -Differentiets urb til d³ý paid²ý taodý = bodí dt³ dt² dt dt = bo (Kc(- day) + kg to notational convenience, ~ is dropped (2-y)) (90 + lo Kc) 3 dy + (0, nbooke) d2y + gody + boykg dt2 ddt bo k2y Smiles to previous part, take Lupland transform (83+ a152-1 (a0+ bokc) S+ 50 KI) Y(3)

2 Kz bo => Y(s) = S(53+ a152+ 60+ 50 KJ 5-1 50 KI) Let We want the poly (5 Y (5)) to be stable of roots (554 a 15t + (ao + hoke) 5+ hoke) Co 2) roots (53+852+ (15+3Kc) 5+3KI) (0 Assuming roots obey that property, apply FUT - Objective is achieved. Conclusion: The objective can't le actieved for and of Kc, FIZ, it is achieved only when 3 is satisfixed. -3.9+1.141 eg. Kc = Kz=1, roots al -3 objecture is not achieved. 0.181 +0.000 But for KC = 0.25 1 KI = 0.5 roits are -4.25, 1-3.14, -0.1 objective is achieved.

= - (L-1Va) w + - Va Z 25981 dz = - Lw - (L+1/9) 2 + 1/2+ At slendy 46 ats 1 L= LSS-4, V = VSS. = 200 O 3 -65 W + 2 .5 Z = 0 33. 4w - 6.5Z = -0.5 - - 19 Solving 3 4 4 1 Was 0.038 and Zes = 0.1008 0) Steady state values: w= 0.0388 In this model, statu = [w] Enputs = [] Let div = f(·) & diz -g(·) 6 4 9.T (1-12) 81 at + 3+ (m- ma) 9+ (5-24)

$$a_{12} = \frac{\partial f}{\partial w} = \frac{V}{M}$$

$$a_{21} = \frac{\partial f}{\partial z} = \frac{V}{M}$$

$$a_{21} = \frac{\partial g}{\partial z} = \frac{L}{M}; \quad a_{22} = \frac{d}{M} = \frac{-\omega}{M}$$

$$b_{11} = \frac{\partial f}{\partial z} = \frac{\omega}{M}; \quad b_{12} = \frac{d}{dz} = \frac{-\omega}{M} + \frac{24}{M}$$

$$b_{21} = \frac{\partial g}{\partial z} = \frac{\omega}{M}; \quad b_{22} = \frac{d}{M} = \frac{d}{M}$$

$$\therefore A = \begin{bmatrix} -6.5 & 2.5 \\ 4 & -6.5 \end{bmatrix}$$

$$(all value) we heated at the endy shall
$$B^{2} = \begin{bmatrix} -0.0019 & 0.0016 \\ -0.0031 & 0.0025 \end{bmatrix}$$

$$\therefore \begin{bmatrix} \frac{dw}{dz} \\ \frac{dz}{dz} \end{bmatrix} = A \begin{bmatrix} we sy \\ w - ws \\ w - 2.2ss \\ w -$$$$

$$\frac{3}{3} \times (5) = \frac{(1+5)e^{-35}}{5^{2}} = 25+11$$

$$3 \le t \le 4$$

$$4 \le 5 \le \frac{38}{5} = \frac{1}{2} = \frac{38}{5} = \frac{1}{2} = \frac{38}{5} = \frac{1}{2} = \frac{38}{5} = \frac{1}{2} = \frac$$

$$\frac{9\pi^{2}}{5^{2}} + 1$$

Q3 Part d)

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linsys =
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A =
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Integ1 Integ2

Integ1 -6.5 2.5

Integ2 4 -6.5

B =

FR FR1

Integ1 -0.001938 0.00155

Integ2 -0.003101 0.002481

C =

Integ1 Integ2

Out1 1 0

Out2 0 1

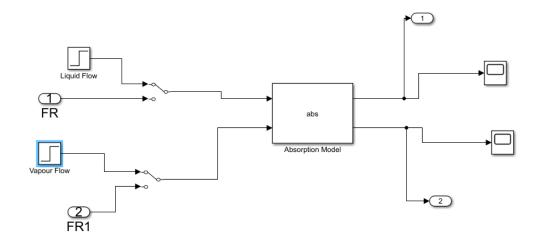
D =

FR FR1

Out1 0 0

Out2 0 0

Continuous-time state-space model.

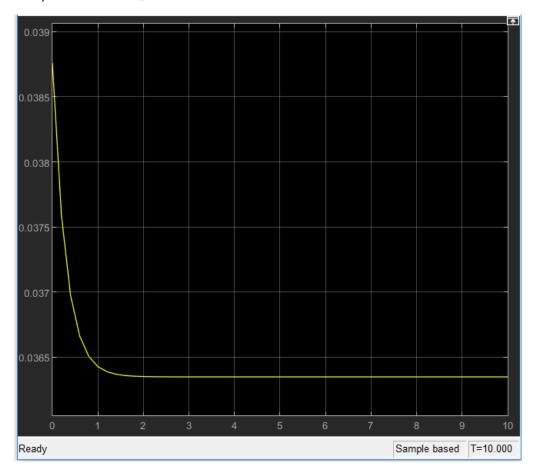


Part e)

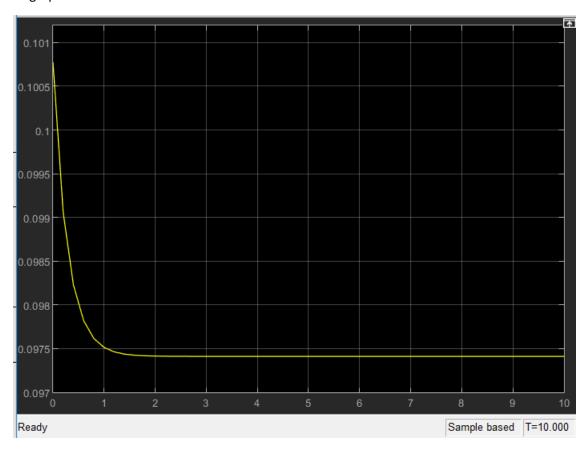
Since if we change both the flow rates, steady state values are same as original, I am changing only L in both cases.

ALL GRAPHS ARE FROM NON LINEAR MODEL. I DID NOT PLOT FOR LINEAR MODEL.

i) $L = 1.05L_{ss}$

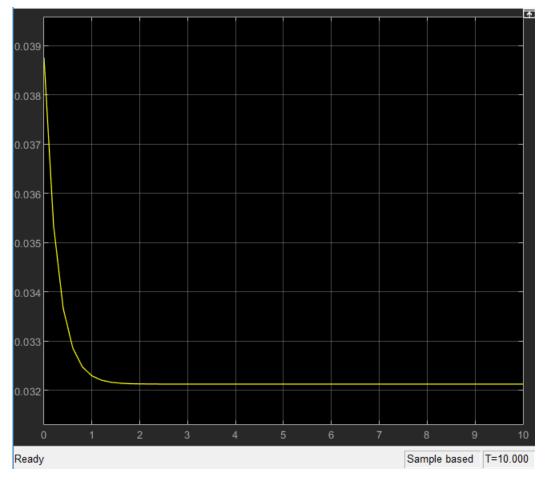


W graph

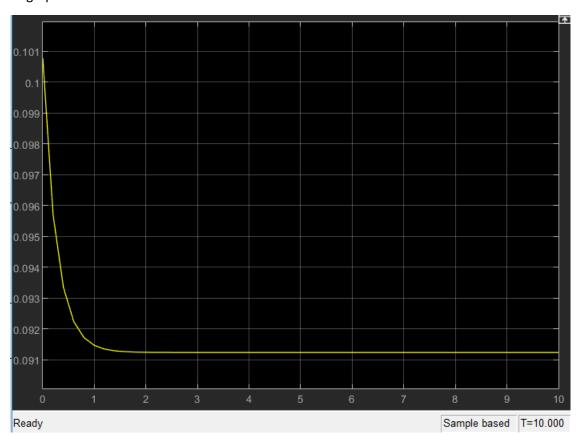


Z graph

ii) L= 1.15L_{ss}



W graph



```
Code:
clear; close all;
%% System charecterstics
Lss = 80; Vss = 100;
M = 20; a=0.5; zf = 0.1;
%% Part a) Finding steady state (by hand)
% Equate derivatives to zero, solve the linear eqn
Ass = [-(a*Vss+Lss)/M Vss*a/M;Lss/M - (a*Vss+Lss)/M];
bss = [0; -Vss*zf/M];
x_s = inv(Ass)*bss;
%% Part b) Linearisation (by Taylor Expansion)
w_s = x_s(1); z_s = x_s(2);
A = [-(Vss*a+Lss)/M Vss*a/M;Lss/M -(Lss+Vss*a)/M];
B = [-w_ss/M (-a*w_ss+a*z_ss)/M;(w_ss-z_ss)/M -a*z_ss/M+zf/M];
%% Part c) Finding the eigenvalues-eignvectors of the system
[V,D] = eig(A);
% Second eigen value is faster (more negative)
%% Part d) Find steady-state and linearise
open_system('Q3_model')
% Read the operating conditions into an object
opc = operspec('Q3_model');
% Operating conditions
opc.Inputs(1).u = 80;
opc.Inputs(2).u = 100;
opc.Inputs(1).Known = 1;
opc.Inputs(2).Known = 1;
% Constraints
opc.States(1).Min = 0;opc.States(2).Min = 0;
```

```
% Find the steady state point
ss_point = findop('Q3_model',opc);
% Linearize
linsys = linearize('Q3_model',ss_point)
%% Part e) Give step changes and plot
% Done in SIMULINK. Use the manual switch to step input(s)
[Y,T,X]=step(linsys);
plot()
```