Tyche Example

Set up.

One only needs to execute the following line once, in order to make sure recent enough packages are installed.

```
In [ ]: !pip install 'numpy>=1.17.2' 'pandas>=0.25.1'
```

Import packages.

```
In [1]: import numpy
                                  as np
        import matplotlib.pyplot as pl
        import pandas
                                 as pd
        import re
                                 as re
        import scipy.stats
                                 as st
        import seaborn
                                 as sb
        # The `tyche` package is located at <https://github.com/NREL/portfolio/tree/master/production-func
        tion/framework/code/tyche/>.
        import tyche
                                  as ty
        from copy import deepcopy
```

Load data.

The data are stored in a set of tab-separated value files in a folder.

```
In [2]: designs = ty.Designs("../data")
In [3]: investments = ty.Investments("../data")
```

Compile the production and metric functions for each technology in the dataset.

```
In [4]: designs.compile()
```

Examine the data.

The functions table specifies where the Python code for each technology resides.



Right now, only the style $\ \ numpy \ \ is \ supported.$

The indices table defines the subscripts for variables.

In [6]: designs.indices

Out[6]:

| | | | Offset | Description | Notes |
|---------------------|-----------------|-------------|--------|--------------------------|-------|
| Technology | Type | Index | | | |
| | Capital | Catalyst | 0 | Catalyst | |
| | Fixed | Rent | 0 | Rent | |
| | Input Metric | Electricity | 1 | Electricity | |
| | | Water | 0 | Water | |
| Simple electrolysis | | Cost | 0 | Jobs | |
| | | GHG | 2 | Greenhouse gas emissions | |
| | | Jobs | 1 | Jobs | |
| | Output | Hydrogen | 1 | Hydrogen | |
| | Output | Oxygen | 0 | Oxygen | |

The designs table contains the cost, input, efficiency, and price data for a scenario.

In [7]: designs.designs

Out[7]:

| | | | | Value | Units | Notes |
|------------------------|----------------------------------|--------------|-------------|--|----------|---------------------------------------|
| Technology | Scenario | Variable | Index | | | |
| Simple electrolysis | | Input | Electricity | 279 | kJ/mole | |
| electiolysis | | iliput | Water | 19.04 | g/mole | |
| | | Input | Electricity | 0.85 | 1 | |
| | | efficiency | Water | 0.95 | 1 | |
| | | Input price | Electricity | 3.33e-5 | USD/kJ | |
| | | F F | Water | 4.8e-3 | USD/mole | |
| | Base Electrolysis | Lifetime | Catalyst | 3 | yr | Effective lifetime of Al-Ni catalyst. |
| | | Output | Hydrogen | 0.90 | 1 | |
| | | efficiency | Oxygen | 0.90 | 1 | |
| | | Output price | Hydrogen | 1.0e-2 | USD/g | |
| | | | Oxygen | 3.0e-3 | USD/g | |
| | | Scale | NaN | 6650 | mole/yr | Rough estimate for a 50W setup. |
| | Fast Progress on Electrolysis | Input | Electricity | 279 | kJ/mole | |
| | Lieuwiyale | | Water | 19.04 | g/mole | |
| | | Input | Electricity | st.truncnorm(-3, 0.75, loc=0.97, scale=0.04) | 1 | |
| | | efficiency | Water | st.truncnorm(-3, 2, loc=0.97, scale=0.01) | 1 | |
| | | Input price | Electricity | 3.33e-5 | USD/kJ | |
| | | input price | Water | 4.8e-3 | USD/mole | |
| | | Lifetime | Catalyst | 3 | yr | Effective lifetime of Al-Ni catalyst. |
| | | Output | Hydrogen | st.beta(3, 2, loc=0.90, scale=0.03) | 1 | |
| | | efficiency | Oxygen | st.beta(3, 2, loc=0.90, scale=0.06) | 1 | |
| | | Output price | Hydrogen | 1.0e-2 | USD/g | |
| | | Salpat piloo | Oxygen | 3.0e-3 | USD/g | |

| | | | | | Value | Units | Notes |
|-----|--------------|----------------------------------|--------------|-------------------------------------|--|----------|---------------------------------------|
| Tec | chnology | Scenario | Variable | Index | | | |
| | | | Scale | NaN | 6650 | mole/yr | Rough estimate for a 50W setup. |
| | | | Input | Electricity | 279 | kJ/mole | |
| | | | iliput | Water | 19.04 | g/mole | |
| | | | Input | Electricity | st.truncnorm(-2, 1.75, loc=0.93, scale=0.04) | 1 | |
| | | | efficiency | Water | st.truncnorm(-2, 3, loc=0.97, scale=0.01) | 1 | |
| | | | Input price | Electricity | 3.33e-5 | USD/kJ | |
| | | Moderate Progress on | input price | Water | 4.8e-3 | USD/mole | |
| | Electrolysis | Electrolysis | Lifetime | Catalyst | 3 | yr | Effective lifetime of Al-Ni catalyst. |
| | | | Output | Hydrogen | st.beta(2, 2, loc=0.90, scale=0.03) | 1 | |
| | | efficiency | Oxygen | st.beta(2, 2, loc=0.90, scale=0.06) | 1 | | |
| | | | Output price | Hydrogen | 1.0e-2 | USD/g | |
| | | | Catput prioc | Oxygen | 3.0e-3 | USD/g | |
| | | | Scale | NaN | 6650 | mole/yr | Rough estimate for a 50W setup. |
| | | Slow Progress on Electrolysis | Input | Electricity | 279 | kJ/mole | |
| | | Licotrolysis | mpat | Water | 19.04 | g/mole | |
| | | | Input | Electricity | st.truncnorm(-1, 2.75, loc=0.89, scale=0.04) | 1 | |
| | | | efficiency | Water | st.truncnorm(-1, 4, loc=0.96, scale=0.01) | 1 | |
| | | | Input price | Electricity | 3.33e-5 | USD/kJ | |
| | | | input price | Water | 4.8e-3 | USD/mole | |
| | | | Lifetime | Catalyst | 3 | yr | Effective lifetime of Al-Ni catalyst. |
| | | | Output | Hydrogen | st.beta(1, 2, loc=0.90, scale=0.03) | 1 | |
| | | | efficiency | Oxygen | st.beta(1, 2, loc=0.90, scale=0.06) | 1 | |

| Notes | Units | Value | | | | |
|---------------------------------|---------|--------|----------|--------------|----------|------------|
| | | | Index | Variable | Scenario | Technology |
| | USD/g | 1.0e-2 | Hydrogen | Output price | | |
| | USD/g | 3.0e-3 | Oxygen | Output price | | |
| Rough estimate for a 50W setup. | mole/yr | 6650 | NaN | Scale | | |

The parameters table contains additional techno-economic parameters for each technology.

In [8]: designs.parameters

Out[8]:

| | | | Offset | Value | Units | Notes |
|--------------|-------------------------------|-------------------------------------|--------|---------|----------|---|
| Technology | Scenario | Parameter | | | | |
| Simple | | Electricity consumption | 3 | 237 | kJ | |
| electrolysis | | GHG factor for electricity | 9 | 0.138 | gCO2e/kJ | based on 1 kWh = 0.5 kg CO2e |
| | | GHG factor for water | 8 | 0.00108 | gCO2e/g | based on 244,956 gallons = 1 Mg CO2e |
| | | Hydrogen production | 1 | 2.00 | g | |
| | Base Electrolysis | Jobs | 4 | 1.5e-4 | job/mole | |
| | Dase Liectiolysis | Oxygen production | 0 | 16.00 | g | |
| | | Reference capital cost for catalyst | 6 | 0.63 | USD | |
| | | Reference fixed cost for rent | 7 | 1000 | USD/yr | |
| | | Reference scale | 5 | 6650 | mole/yr | |
| | | Water consumption | 2 | 18.08 | g | |
| | | Electricity consumption | 3 | 237 | kJ | |
| | | GHG factor for electricity | 9 | 0.138 | gCO2e/kJ | based on 1 kWh = 0.5 kg CO2e |
| | | GHG factor for water | 8 | 0.00108 | gCO2e/g | based on 244,956 gallons = 1 Mg CO2e |
| | | Hydrogen production | 1 | 2.00 | g | |
| | Foot Drogropp on Flootrolygic | Jobs | 4 | 1.5e-4 | job/mole | |
| | Fast Progress on Electrolysis | Oxygen production | 0 | 16.00 | g | |
| | | Reference capital cost for catalyst | 6 | 0.63 | USD | |
| | | Reference fixed cost for rent | 7 | 1000 | USD/yr | |
| | | Reference scale | 5 | 6650 | mole/yr | |
| | | Water consumption | 2 | 18.08 | g | |
| | Moderate Progress on | Electricity consumption | 3 | 237 | kJ | |
| | Electrolysis | GHG factor for electricity | 9 | 0.138 | gCO2e/kJ | based on 1 kWh = 0.5 kg CO2e |
| | | GHG factor for water | 8 | 0.00108 | gCO2e/g | based on 244,956 gallons = 1 Mg CO2e |

| | | Offset | Value | Units | Notes |
|-------------------------------|--|--------|---------|----------|---|
| Technology Scenario | Parameter | | | | |
| | Hydrogen production | 1 | 2.00 | g | |
| | Jobs | 4 | 1.5e-4 | job/mole | |
| | Oxygen production | 0 | 16.00 | g | |
| | Reference capital cost for catalyst | 6 | 0.63 | USD | |
| | Reference fixed cost for rent | 7 | 1000 | USD/yr | |
| | Reference scale | 5 | 6650 | mole/yr | |
| | Water consumption | 2 | 18.08 | g | |
| | Electricity consumption | 3 | 237 | kJ | |
| | GHG factor for electricity | 9 | 0.138 | gCO2e/kJ | based on 1 kWh = 0.5 kg CO2e |
| | GHG factor for water | 8 | 0.00108 | gCO2e/g | based on 244,956 gallons = 1 Mg CO2e |
| | Hydrogen production | 1 | 2.00 | g | |
| Slow Progress on Electrolysis | Jobs | 4 | 1.5e-4 | job/mole | |
| Slow Flogress on Electrorysis | Oxygen production | 0 | 16.00 | g | |
| | Reference capital cost for catalyst | 6 | 0.63 | USD | |
| | Reference fixed cost for rent | 7 | 1000 | USD/yr | |
| | Reference scale | 5 | 6650 | mole/yr | |
| | Water consumption | 2 | 18.08 | g | |

The results table specifies the units of measure for results of computations.

| Technology | Variable | Index | |
|-----------------------|---------------|----------|-----------|
| | Cost | Cost | USD/mole |
| | | Cost | USD/gH2 |
| Circula ala atrabiaia | Metric | GHG | gCO2e/gH2 |
| Simple electrolysis | | Jobs | job/gH2 |
| | Outerut | Hydrogen | g/mole |
| | Output Oxygen | Oxygen | g/mole |

The tranches table specifies multually exclusive possibilities for investments: only one $\, Tranch \, may \, be \, selected for each <math>\, Cateogry \, .$

In [10]: investments.tranches
Out[10]:

Notes

| Scenario | Tranche | Category |
|-----------------------------------|-------------------------|------------------|
| Fast Progress on Electrolysis | High Electrolysis R&D | |
| Slow Progress on Electrolysis | Low Electrolysis R&D | Flacture in DOD |
| Moderate Progress on Electrolysis | Medium Electrolysis R&D | Electrolysis R&D |
| Base Electrolysis | No Electrolysis R&D | |

The investments table bundles a consistent set of tranches (one per category) into an overall investment.

```
In [11]: investments.investments
```

Amount Notes

Out[11]:

| Investment | Category | Tranche | |
|---------------------|------------------|-------------------------|-----------|
| High R&D Spending | Electrolysis R&D | High Electrolysis R&D | 5000000.0 |
| Low R&D Spending | Electrolysis R&D | Low Electrolysis R&D | 1000000.0 |
| Medium R&D Spending | Electrolysis R&D | Medium Electrolysis R&D | 2500000.0 |
| No R&D Spending | Electrolysis R&D | No Electrolysis R&D | 0.0 |

Evaluate the scenarios in the dataset.

```
In [12]: scenario_results = designs.evaluate_scenarios(sample_count=50)
```

In [13]: scenario_results.xs(1, level="Sample", drop_level=False)

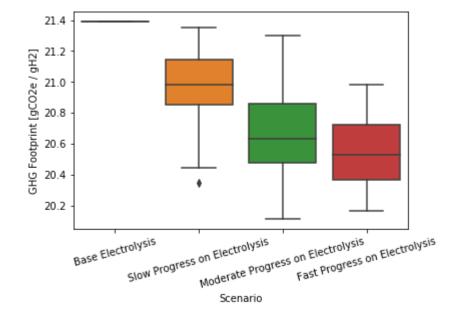
Out[13]:

| | | | | | Value | Units |
|---------------------|-----------------------------------|--------|----------|----------|-----------|-----------|
| Technology | Scenario | Sample | Variable | Index | | |
| | | | Cost | Cost | 0.183900 | USD/mole |
| | | | | Cost | 0.102121 | USD/gH2 |
| | Daga Flactrolynia | 4 | Metric | GHG | 21.391959 | gCO2e/gH2 |
| | Base Electrolysis | 1 | | Jobs | 0.000083 | job/gH2 |
| | | | Output | Hydrogen | 1.800796 | g/mole |
| | | | Output | Oxygen | 14.406372 | g/mole |
| | | | Cost | Cost | 0.182463 | USD/mole |
| | | | | Cost | 0.097287 | USD/gH2 |
| | Fast Progress on Electrolysis | 1 | Metric | GHG | 20.539648 | gCO2e/gH2 |
| | rast Flogress on Electrolysis | 1 | | Jobs | 0.000080 | job/gH2 |
| | | | Output | Hydrogen | 1.875522 | g/mole |
| Simple electrolysis | | | Output | Oxygen | 15.780807 | g/mole |
| Simple electrolysis | | | Cost | Cost | 0.182335 | USD/mole |
| | | | | Cost | 0.096208 | USD/gH2 |
| | Moderate Progress on Electrolysis | 1 | Metric | GHG | 20.326215 | gCO2e/gH2 |
| | Woderate Frogress on Electrorysis | ' | | Jobs | 0.000079 | job/gH2 |
| | | | Output | Hydrogen | 1.895216 | g/mole |
| | | | Output | Oxygen | 15.558470 | g/mole |
| | | | Cost | Cost | 0.184527 | USD/mole |
| | | | | Cost | 0.098531 | USD/gH2 |
| | Slow Progress on Electrolysis | 1 | Metric | GHG | 20.569724 | gCO2e/gH2 |
| | Clow i Togress on Electrorysis | ' | | Jobs | 0.000080 | job/gH2 |
| | | | Output | Hydrogen | 1.872780 | g/mole |
| | | | Output | Oxygen | 14.612968 | g/mole |

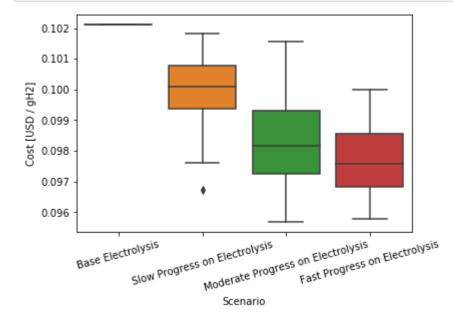
Save results.

```
In [14]: scenario_results.to_csv("example-scenario.csv")
```

Plot GHG metric.

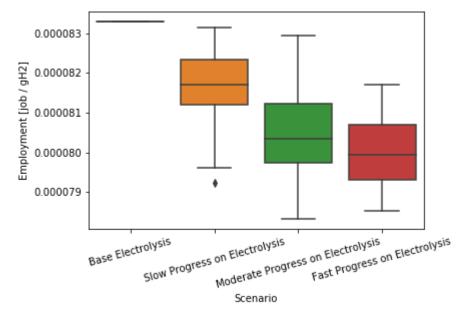


Plot cost metric.



Plot employment metric.

```
In [17]: g = sb.boxplot(
    x="Scenario",
    y="Value",
    data=scenario_results.xs(
        ["Metric", "Jobs"],
        level=["Variable", "Index"]
    ).reset_index()[["Scenario", "Value"]],
    order=["Base Electrolysis", "Slow Progress on Electrolysis", "Moderate Progress on Electrolysis",
    s", "Fast Progress on Electrolysis"]
)
g.set(ylabel="Employment [job / gH2]")
g.set_xticklabels(g.get_xticklabels(), rotation=15);
```



Evaluate the investments in the dataset.

```
In [18]: investment_results = investments.evaluate_investments(designs, sample_count=50)
```

Costs of investments.

In [19]: investment_results.amounts

Out[19]:

Amount

 Investment

 High R&D Spending
 5000000.0

 Low R&D Spending
 1000000.0

 Medium R&D Spending
 2500000.0

 No R&D Spending
 0.0

Benefits of investments.

In [20]: investment_results.metrics.xs(1, level="Sample", drop_level=False)

Out[20]:

| | | Index | Technology | Sample | Scenario | Tranche | Category | Investment | | | | |
|-----------|-----------|-------|------------------------|--------|----------------------------------|--------------------------------------|----------------------------|----------------------|---|---|--|------------------------|
| USD/gH2 | 0.102121 | Cost | | | | | | | | | | |
| gCO2e/gH2 | 21.391959 | GHG | Simple electrolysis | 1 | Base Electrolysis | No Electrolysis R&D | Electrolysis R&D | No R&D Spending | | | | |
| job/gH2 | 0.000083 | Jobs | | | | | | | | | | |
| USD/gH2 | 0.097203 | Cost | | | | | | | | | | |
| gCO2e/gH2 | 20.509349 | GHG | Simple electrolysis | 1 | Fast Progress on Electrolysis | High Electrolysis R&D | Electrolysis R&D | High R&D Spending | | | | |
| job/gH2 | 0.000080 | Jobs | , | | , | | | Openang | | | | |
| USD/gH2 | 0.097801 | Cost | | | | | | | | | | |
| gCO2e/gH2 | 20.505051 | GHG | Simple electrolysis | 1 | , | Moderate Progress on Electrolysis | Medium Electrolysis R&D | Electrolysis R&D | • | , | | Medium R&D Spending |
| job/gH2 | 0.000080 | Jobs | 0.000.0.90.0 | | , | . 13.2 | . 10.2 | Gpeag | | | | |
| USD/gH2 | 0.100331 | Cost | | | | | | | | | | |
| gCO2e/gH2 | 21.160737 | GHG | Simple electrolysis | 1 | Slow Progress on Electrolysis | Low Electrolysis R&D | Electrolysis R&D | Low R&D Spending | | | | |
| job/gH2 | 0.000082 | Jobs | S.Soli Gry Glo | | Licotrolydio | Nab | Ναυ | Spending | | | | |

Value

Units

```
In [21]: investment_results.summary.xs(1, level="Sample", drop_level=False)
```

Out[21]:

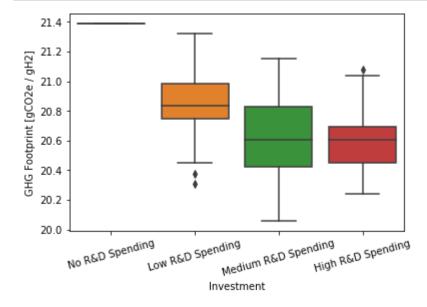
| | | | Value | Units |
|---------------------|--------|-------|-----------|-----------|
| Investment | Sample | Index | | |
| | | Cost | 0.102121 | USD/gH2 |
| No R&D Spending | 1 | GHG | 21.391959 | gCO2e/gH2 |
| | | Jobs | 0.000083 | job/gH2 |
| | | Cost | 0.097203 | USD/gH2 |
| High R&D Spending | 1 | GHG | 20.509349 | gCO2e/gH2 |
| | | Jobs | 0.000080 | job/gH2 |
| | | Cost | 0.097801 | USD/gH2 |
| Medium R&D Spending | 1 | GHG | 20.505051 | gCO2e/gH2 |
| | | Jobs | 0.000080 | job/gH2 |
| | | Cost | 0.100331 | USD/gH2 |
| Low R&D Spending | 1 | GHG | 21.160737 | gCO2e/gH2 |
| | | Jobs | 0.000082 | job/gH2 |

Save results.

```
In [22]: investment_results.amounts.to_csv("example-investment-amounts.csv")
In [23]: investment_results.metrics.to_csv("example-investment-metrics.csv")
```

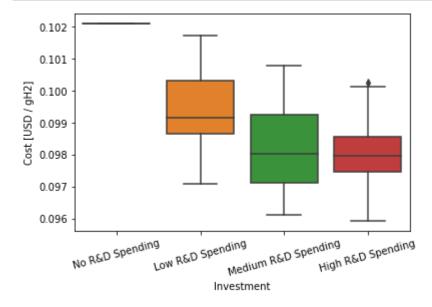
Plot GHG metric.

```
In [24]: 
g = sb.boxplot(
    x="Investment",
    y="Value",
    data=investment_results.metrics.xs(
        "GHG",
        level="Index"
    ).reset_index()[["Investment", "Value"]],
    order=["No R&D Spending", "Low R&D Spending", "Medium R&D Spending", "High R&D Spending"]
)
g.set(ylabel="GHG Footprint [gCO2e / gH2]")
g.set_xticklabels(g.get_xticklabels(), rotation=15);
```



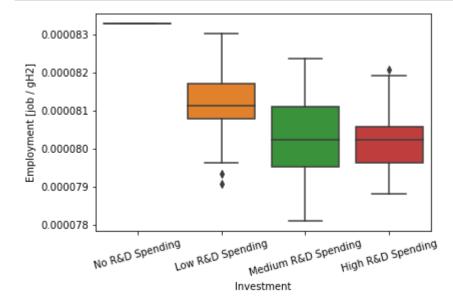
Plot cost metric.

```
In [25]: g = sb.boxplot(
    x="Investment",
    y="Value",
    data=investment_results.metrics.xs(
        "Cost",
        level="Index"
    ).reset_index()[["Investment", "Value"]],
    order=["No R&D Spending", "Low R&D Spending", "Medium R&D Spending", "High R&D Spending"]
)
    g.set(ylabel="Cost [USD / gH2]")
    g.set_xticklabels(g.get_xticklabels(), rotation=15);
```



Plot employment metric.

```
In [26]: g = sb.boxplot(
    x="Investment",
    y="Value",
    data=investment_results.metrics.xs(
        "Jobs",
        level="Index"
    ).reset_index()[["Investment", "Value"]],
    order=["No R&D Spending", "Low R&D Spending", "Medium R&D Spending", "High R&D Spending"]
)
    g.set(ylabel="Employment [job / gH2]")
    g.set_xticklabels(g.get_xticklabels(), rotation=15);
```



Sensitity analysis.

Vary the four efficiencies in the design.

Start from the base case.

In [29]: base_design = designs.designs.xs("Base Electrolysis", level=1, drop_level=False)
base_design

Out[29]:

| | | | | Value | Units | Notes |
|---------------------|-------------------|-------------------|-------------|---------|----------|---------------------------------------|
| Technology | Scenario | Variable | Index | | | |
| | Base Electrolysis | Input | Electricity | 279 | kJ/mole | |
| | | | Water | 19.04 | g/mole | |
| | | Input efficiency | Electricity | 0.85 | 1 | |
| | | | Water | 0.95 | 1 | |
| | | Input price | Electricity | 3.33e-5 | USD/kJ | |
| Simple electrolysis | | | Water | 4.8e-3 | USD/mole | |
| Simple electrolysis | | Lifetime | Catalyst | 3 | yr | Effective lifetime of Al-Ni catalyst. |
| | | Output efficiency | Hydrogen | 0.90 | 1 | |
| | | | Oxygen | 0.90 | 1 | |
| | | Output price | Hydrogen | 1.0e-2 | USD/g | |
| | | | Oxygen | 3.0e-3 | USD/g | |
| | | Scale | NaN | 6650 | mole/yr | Rough estimate for a 50W setup. |

In [30]: base_parameters = designs.parameters.xs("Base Electrolysis", level=1, drop_level=False)
base_parameters

Out[30]:

| | | | Offset | Value | Units | Notes |
|---------------------|-------------------|-------------------------------------|--------|---------|----------|--------------------------------------|
| Technology | Scenario | Parameter | | | | |
| | Base Electrolysis | Electricity consumption | 3 | 237 | kJ | |
| | | GHG factor for electricity | 9 | 0.138 | gCO2e/kJ | based on 1 kWh = 0.5 kg CO2e |
| | | GHG factor for water | 8 | 0.00108 | gCO2e/g | based on 244,956 gallons = 1 Mg CO2e |
| | | Hydrogen production | 1 | 2.00 | g | |
| Simple electrolysis | | Jobs | 4 | 1.5e-4 | job/mole | |
| Simple electrolysis | | Oxygen production | 0 | 16.00 | g | |
| | | Reference capital cost for catalyst | 6 | 0.63 | USD | |
| | | Reference fixed cost for rent | 7 | 1000 | USD/yr | |
| | | Reference scale | 5 | 6650 | mole/yr | |
| | | Water consumption | 2 | 18.08 | g | |

Generate the new scenarios and append them to the previous ones.

```
In [31]: sensitivities = deepcopy(designs)
    sensitivities.designs = sensitivities.designs[0:0]
    sensitivities.parameters = sensitivities.parameters[0:0]
```

```
In [32]: # Iterate over variables and efficiencies.
for variable, index in variables:
    for efficiency in efficiencies:

# Name the scenario.
        scenario = "Let " + variable + " @ " + index + " = " + str(round(efficiency, 3))

# Alter the base case.
        vary_design = base_design.rename(index={"Base Electrolysis" : scenario}, level=1)
        vary_design.loc[("Simple electrolysis", scenario, variable, index), "Value"] = efficiency

# Keep the parameters the same.
        vary_parameters = base_parameters.rename(index={"Base Electrolysis" : scenario}, level=1)

# Append the results to the existing table of scenarios.
        sensitivities.designs = sensitivities.designs.append(vary_design)
        sensitivities.parameters = sensitivities.parameters.append(vary_parameters)
```

Remember to compile the design, since we've added scenarios.

```
In [33]: sensitivities.compile()
```

See how many rows there are in the tables now.

```
In [34]: sensitivities.designs.shape
Out[34]: (480, 3)
In [35]: sensitivities.parameters.shape
Out[35]: (400, 4)
```

In [36]: sensitivities.designs

Out[36]:

| | | | | Value | Units | Notes |
|---------------------|--|-------------------|-------------|---------|---------|---------------------------------|
| Technology | Scenario | Variable | Index | | | |
| | | Input | Electricity | 279 | kJ/mole | |
| | Let Input efficiency @ Water = 0.75 | | Water | 19.04 | g/mole | |
| | | Input efficiency | Electricity | 0.85 | 1 | |
| Simple electrolysis | | | Water | 0.75 | 1 | |
| | | Input price | Electricity | 3.33e-5 | USD/kJ | |
| | | | | | | |
| | Let Output efficiency @ Hydrogen = 0.975 | Output efficiency | Hydrogen | 0.975 | 1 | |
| | | | Oxygen | 0.90 | 1 | |
| | | Output price | Hydrogen | 1.0e-2 | USD/g | |
| | | | Oxygen | 3.0e-3 | USD/g | |
| | | Scale | NaN | 6650 | mole/yr | Rough estimate for a 50W setup. |

480 rows × 3 columns

Compute the results.

```
In [37]: results = sensitivities.evaluate_scenarios(1)
results
```

Out[37]:

| | | | | | Value | Units |
|---------------------|---|--------|----------|----------|-----------|-----------|
| Technology | Scenario | Sample | Variable | Index | | |
| | Let Input efficiency @ Electricity = 0.75 | 1 | Cost | Cost | 0.190164 | USD/mole |
| | | | Metric | Cost | 0.119657 | USD/gH2 |
| | | | | GHG | 24.239606 | gCO2e/gH2 |
| | | | | Jobs | 0.000094 | job/gH2 |
| | | | Output | Hydrogen | 1.589241 | g/mole |
| Simple electrolysis | | | | | | |
| | | | | Cost | 0.100121 | USD/gH2 |
| | Let Output efficiency @ Oxygen = 0.975 | | Metric | GHG | 21.391959 | gCO2e/gH2 |
| | | 1 | | Jobs | 0.000083 | job/gH2 |
| | | | Output | Hydrogen | 1.800796 | g/mole |
| | | | | Oxygen | 15.606903 | g/mole |

240 rows × 2 columns

Plot the cost results.

```
In [38]: cost_results = results.xs("Cost", level="Variable").reset_index()[["Scenario", "Value"]]
```

```
In [39]: cost_results[0:10]
```

Out[39]:

```
ScenarioValue0Let Input efficiency @ Electricity = 0.750.1901641Let Input efficiency @ Electricity = 0.7750.1885952Let Input efficiency @ Electricity = 0.80.1870263Let Input efficiency @ Electricity = 0.8250.1854574Let Input efficiency @ Electricity = 0.850.1839005Let Input efficiency @ Electricity = 0.8750.1841326Let Input efficiency @ Electricity = 0.90.1843647Let Input efficiency @ Electricity = 0.9250.1845978Let Input efficiency @ Electricity = 0.950.1848299Let Input efficiency @ Electricity = 0.9750.185061
```

```
In [41]: cost_results = cost_results[["Variable", "Efficiency", "Cost [USD/mole]"]]
cost_results[0:10]
```

Out[41]:

| | Variable | Efficiency | Cost [USD/mole] |
|---|-------------------------------|------------|-----------------|
| 0 | Input efficiency[Electricity] | 0.750 | 0.190164 |
| 1 | Input efficiency[Electricity] | 0.775 | 0.188595 |
| 2 | Input efficiency[Electricity] | 0.800 | 0.187026 |
| 3 | Input efficiency[Electricity] | 0.825 | 0.185457 |
| 4 | Input efficiency[Electricity] | 0.850 | 0.183900 |
| 5 | Input efficiency[Electricity] | 0.875 | 0.184132 |
| 6 | Input efficiency[Electricity] | 0.900 | 0.184364 |
| 7 | Input efficiency[Electricity] | 0.925 | 0.184597 |
| 8 | Input efficiency[Electricity] | 0.950 | 0.184829 |
| 9 | Input efficiency[Electricity] | 0.975 | 0.185061 |

Out[42]: <matplotlib.axes._subplots.AxesSubplot at 0x7ff0148837f0>

