

## **Objective:**

To simulate the Exhaust manifold in Ansys fluent for analysing the heat transfer and the flow of fluid inside.

## **Conjugate heat transfer:**

The term Conjugate heat transfer is used to describe that when there is a heat transfer between solid to fluid and vice versa.

The conjugate heat transfer (CHT) analysis is an iterative way to simulate the heat transfer between solid and liquid surfaces.

## **Applications of CHT:**

Heat exchanger, cooling fins with natural or forced convection, etc. . . .

## **K Omega model:**

More accurate for near-wall interactions than k-epsilon models. Ability to predict flow separation and accurate prediction for internal flow, curvatures.

Needs small inflation layer which increases the total cell count.

For this model,  $Y^+$  should be below 10 ( $Y^+ < 10$ ).

Using Matlab code total thickness is calculated with a desirable  $y^+$  of 3.

```
clear all
close all
clc

u = 5; %m/s
L = 0.15; %m
rho = 1.225; %kg/m3
mu = 0.000018375; %kg/m.s
Y_plus = input('enter desired value of Y+: ');

Re = u*L*rho/mu; %reynolds number

cf = 0.026/(Re^(1/7)); %skin friction coefficient

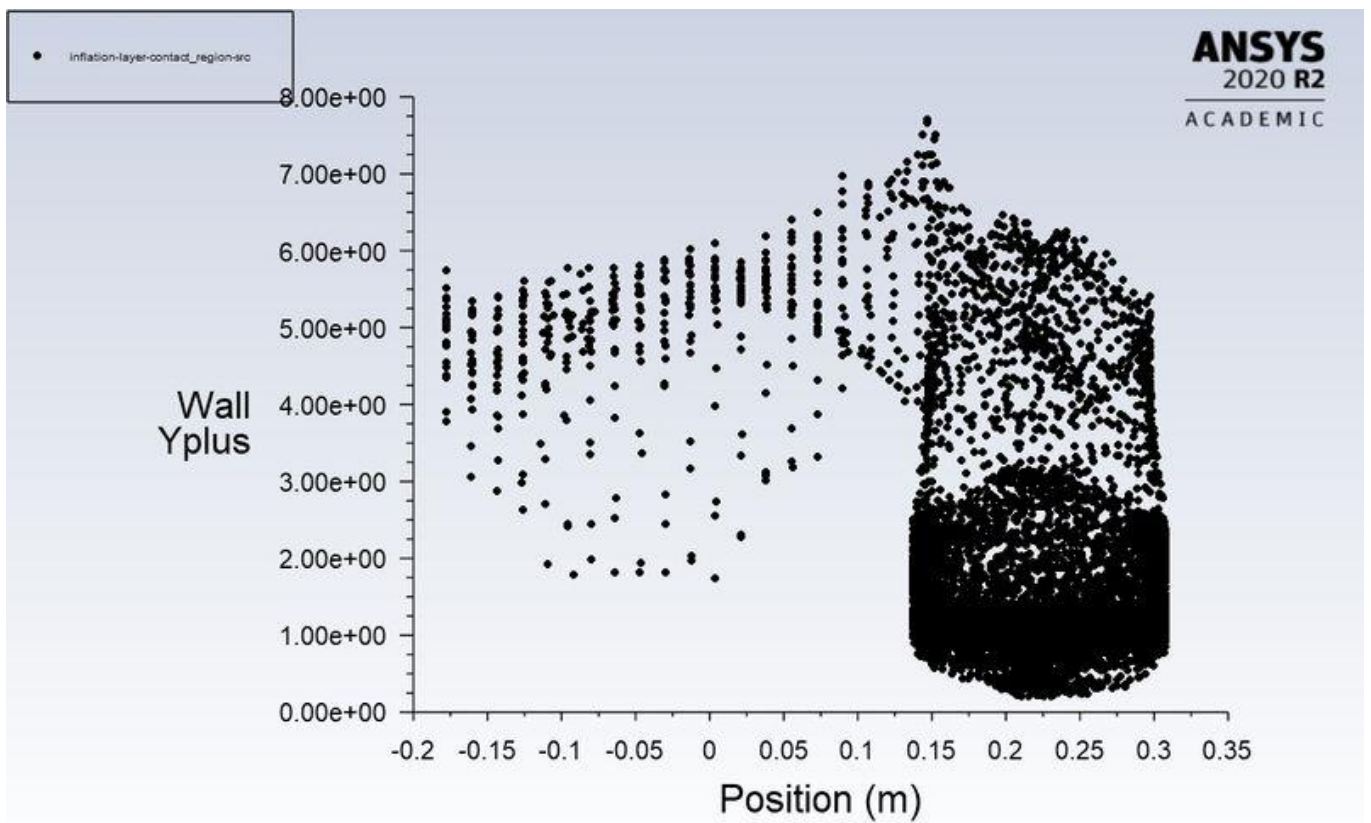
T_wall = 0.5*cf*rho*u^2; %wall shear stress

U_fri = sqrt(T_wall/rho); %friction velocity

del_s = Y_plus*mu/(U_fri*rho);

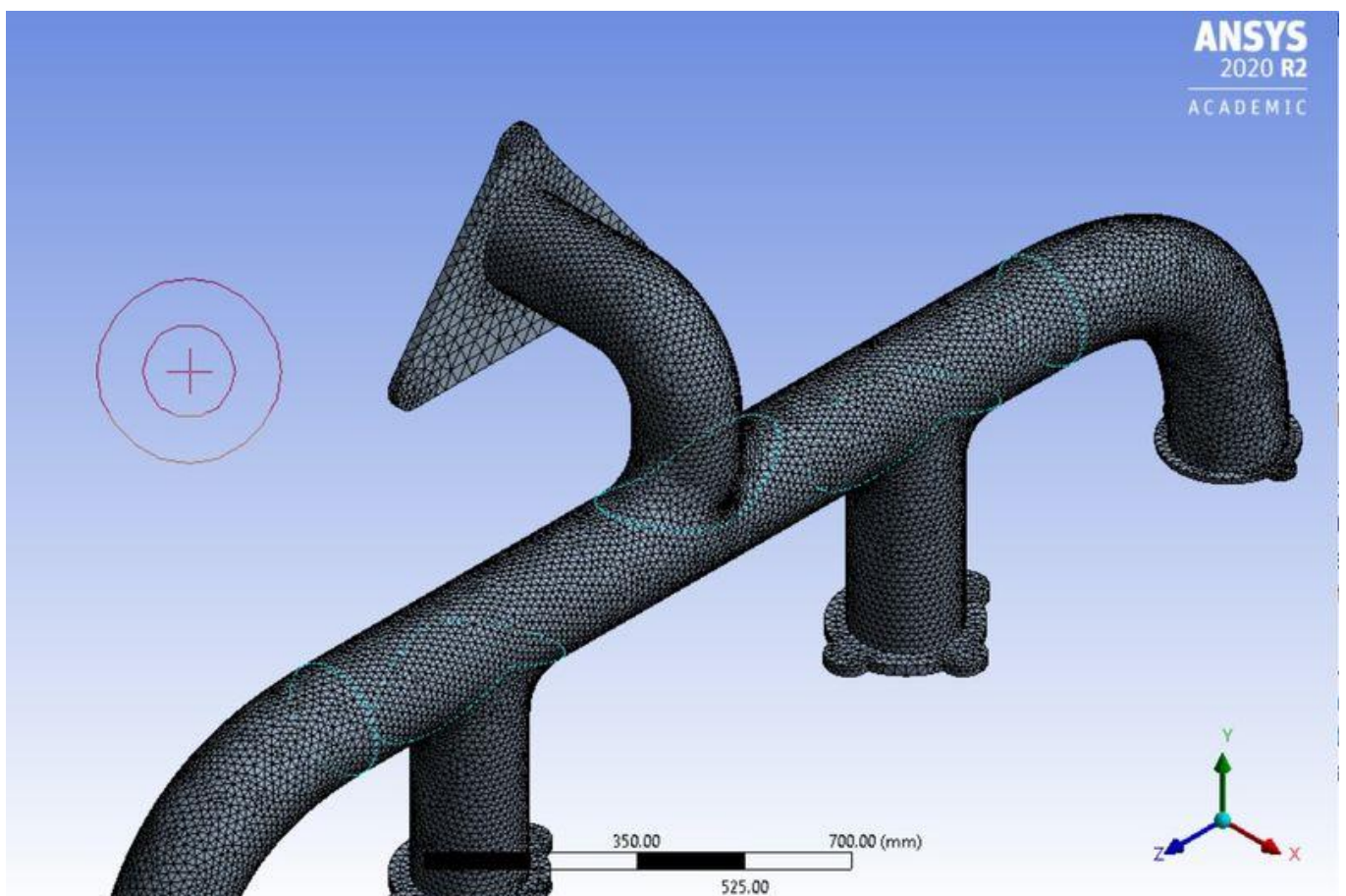
growthrate = 1.2; %growth rate of next cell from previous cell
no_layer = 6; % no of cells
tot_thick = del_s*2*1.2^(no_layer-1);

fprintf('n Reynolds number is %d n n',Re);
fprintf(' first wall thickness is %d in mn n',del_s);
fprintf(' Total thickness of the cell %d in mn', tot_thick);
```

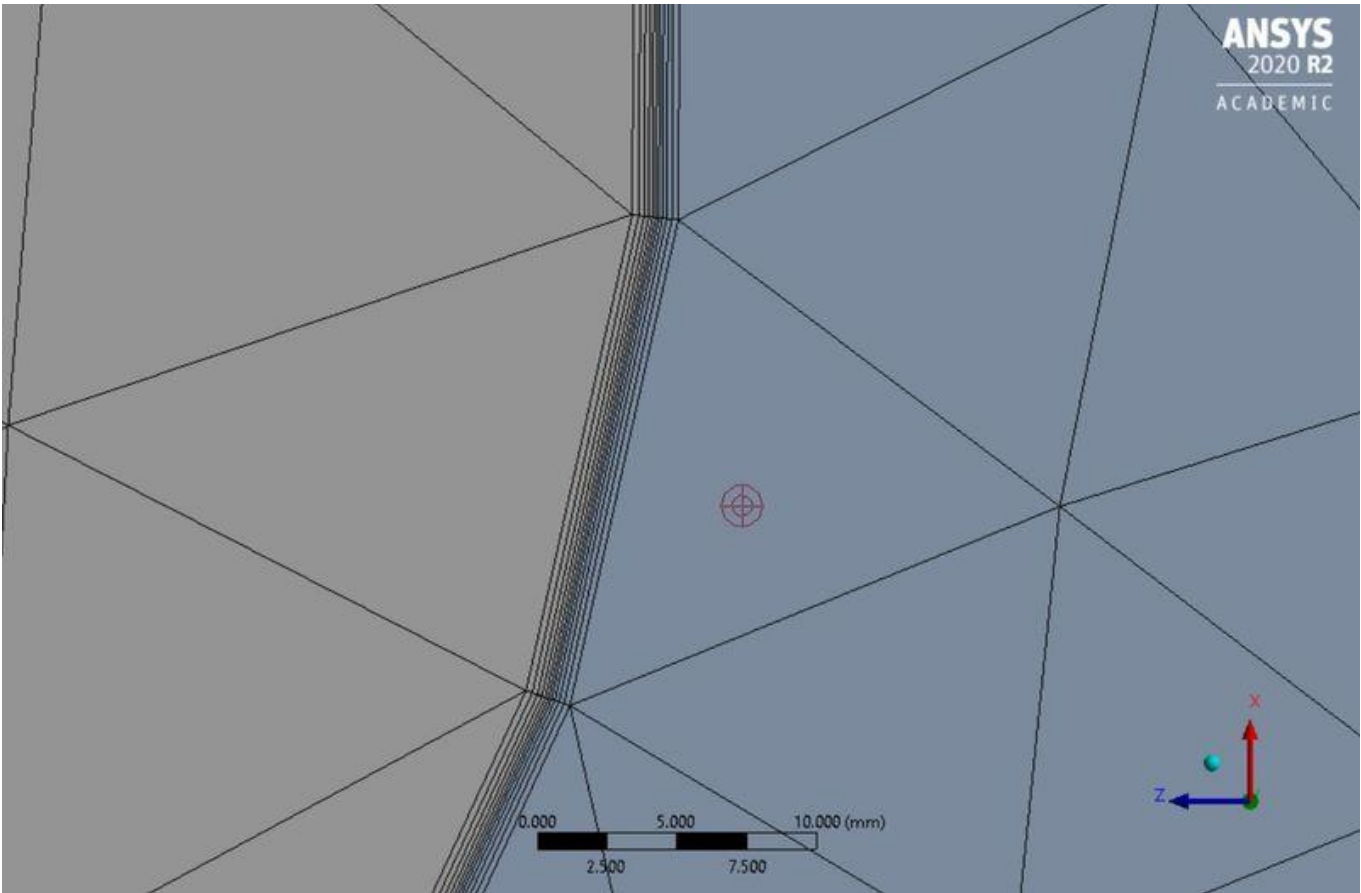


from the above chart, we can say that the  $y^+$  value is within 10. so we can use the K-omega model.

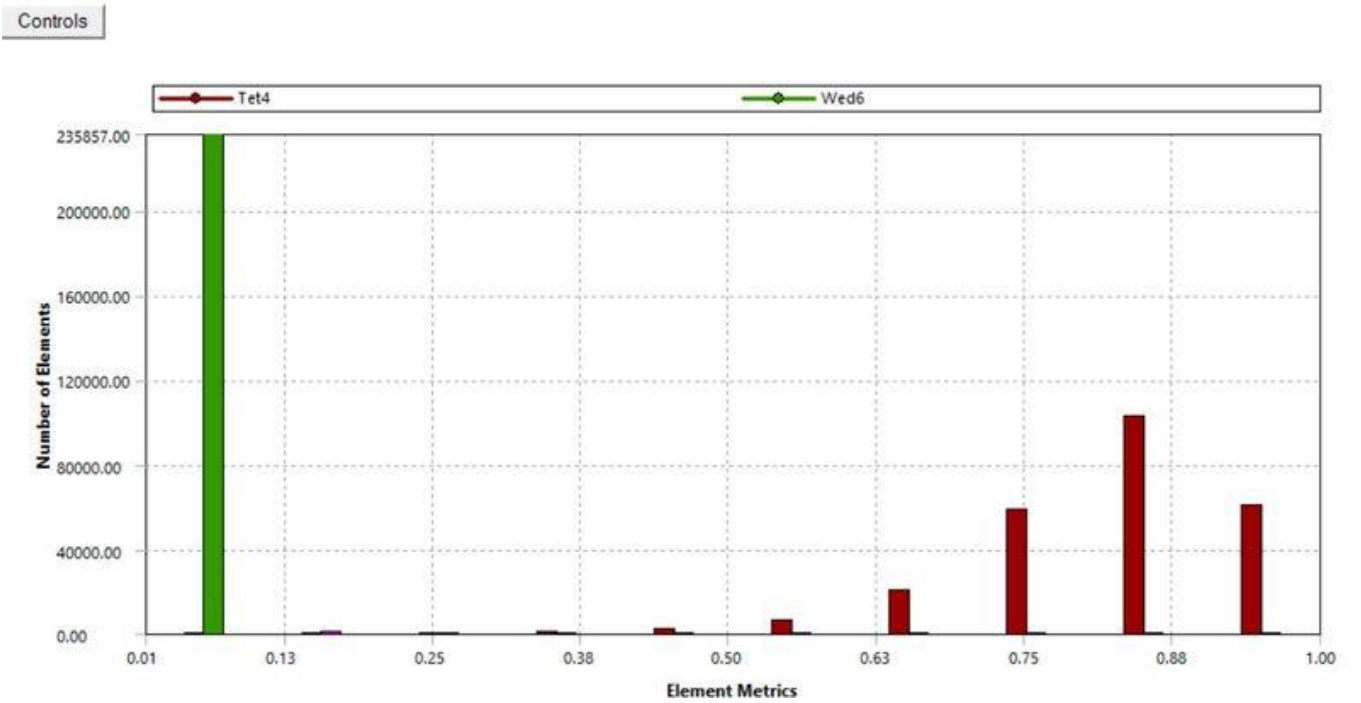
### Meshing:



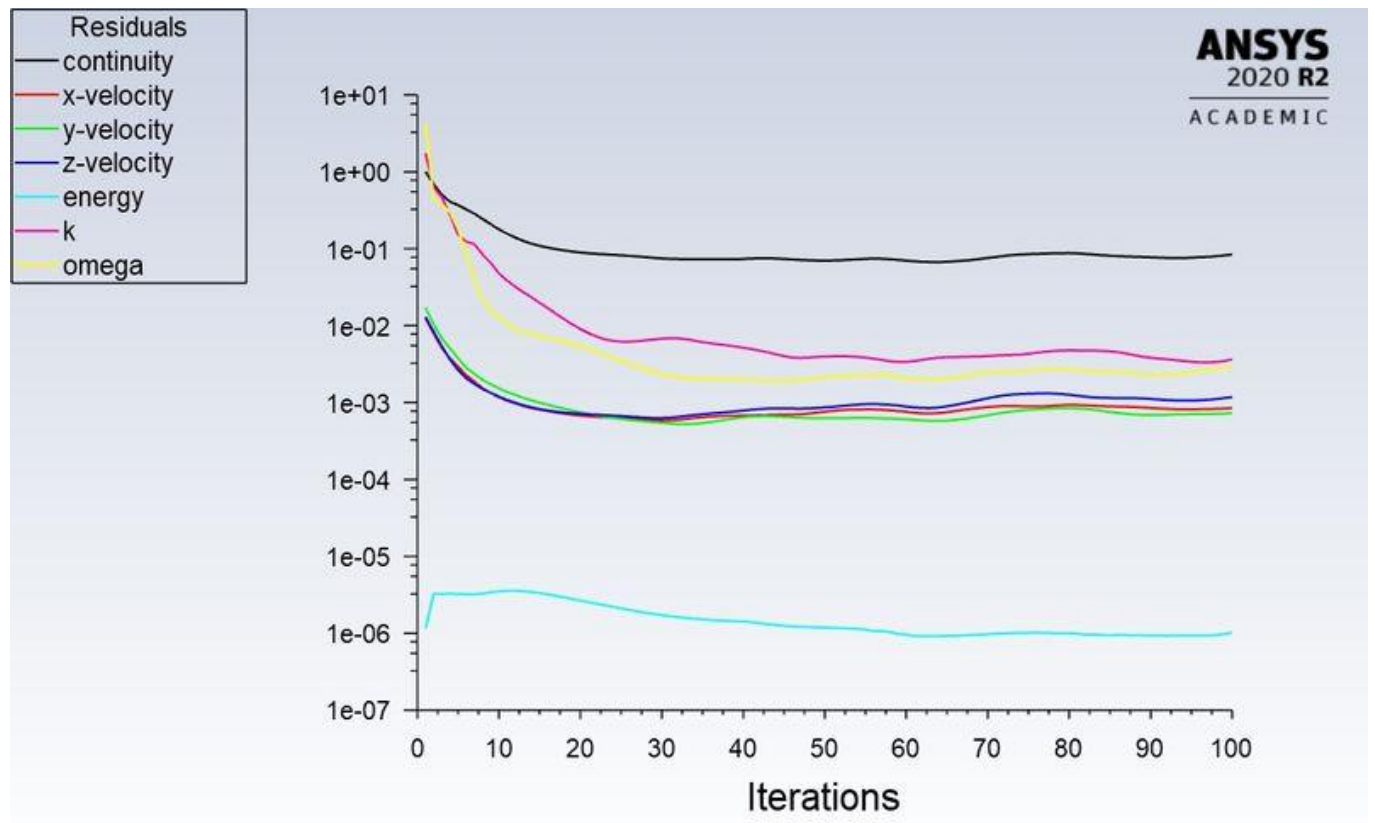
Inflation layer:



Element Quality:



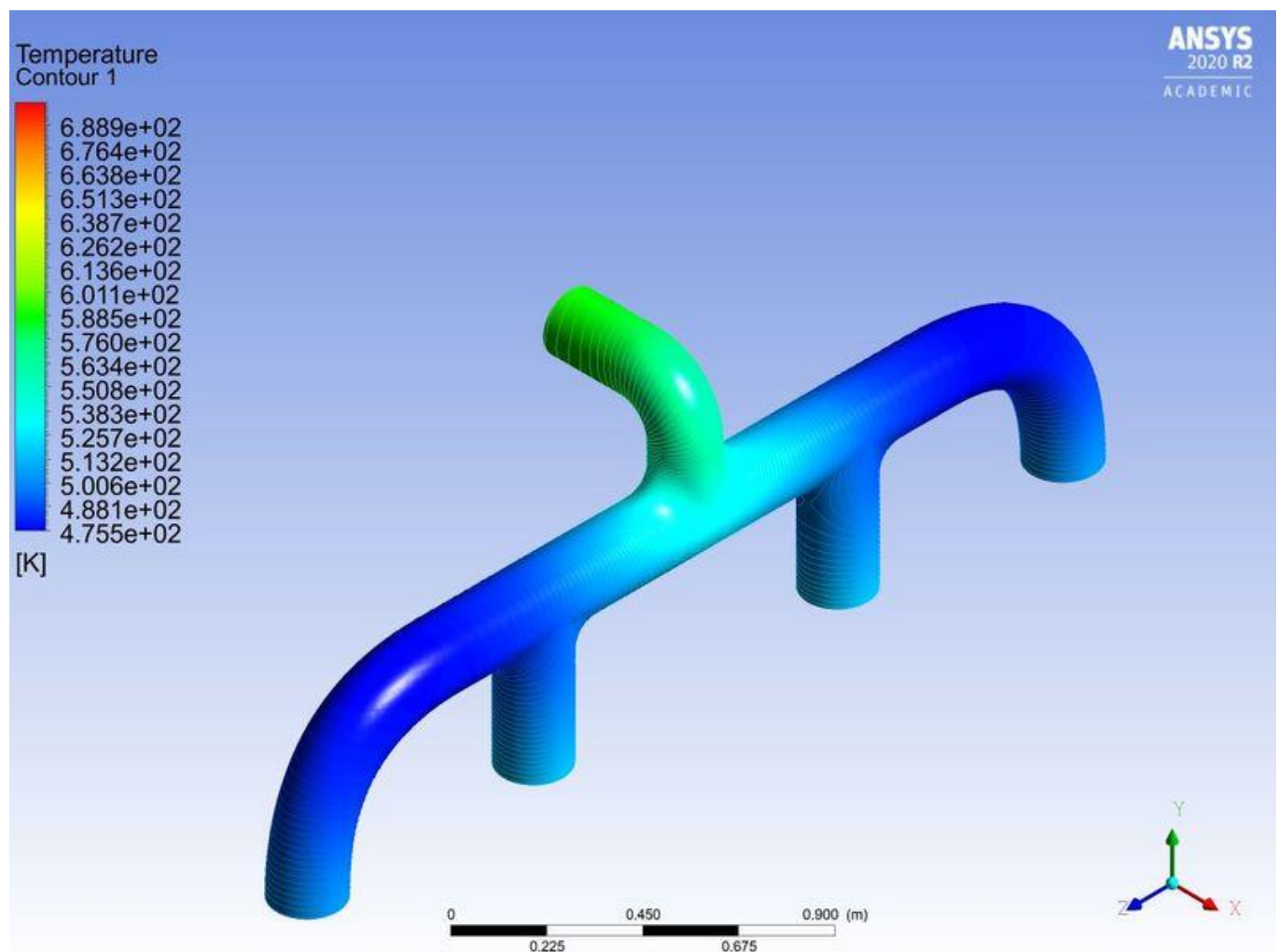
## Residuals:



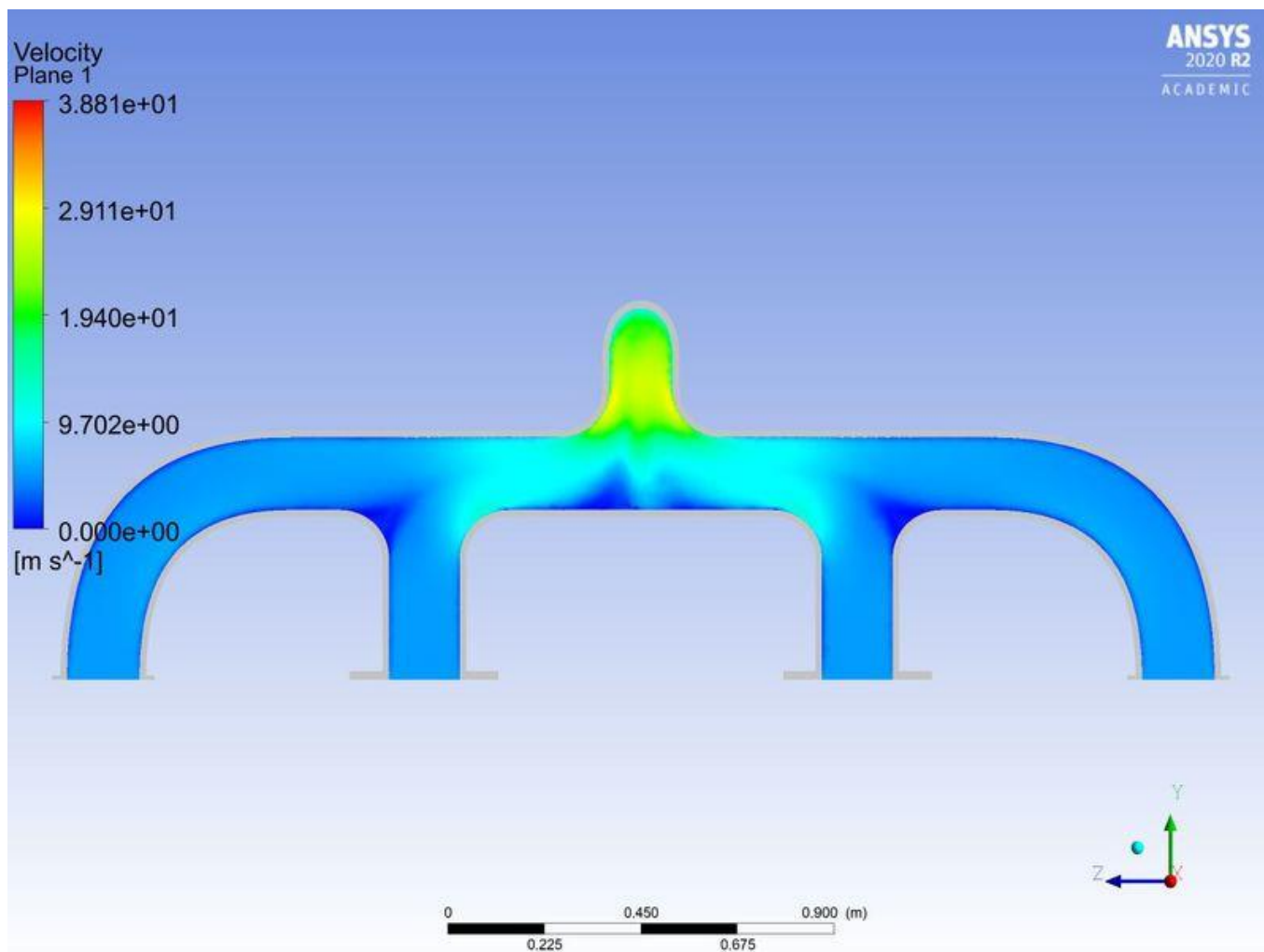
Since there is not much change in residual values and temperature variation in the temperature contour, thus the solution is converged.

## Post-processing:

Temperature contour:



Velocity contour:



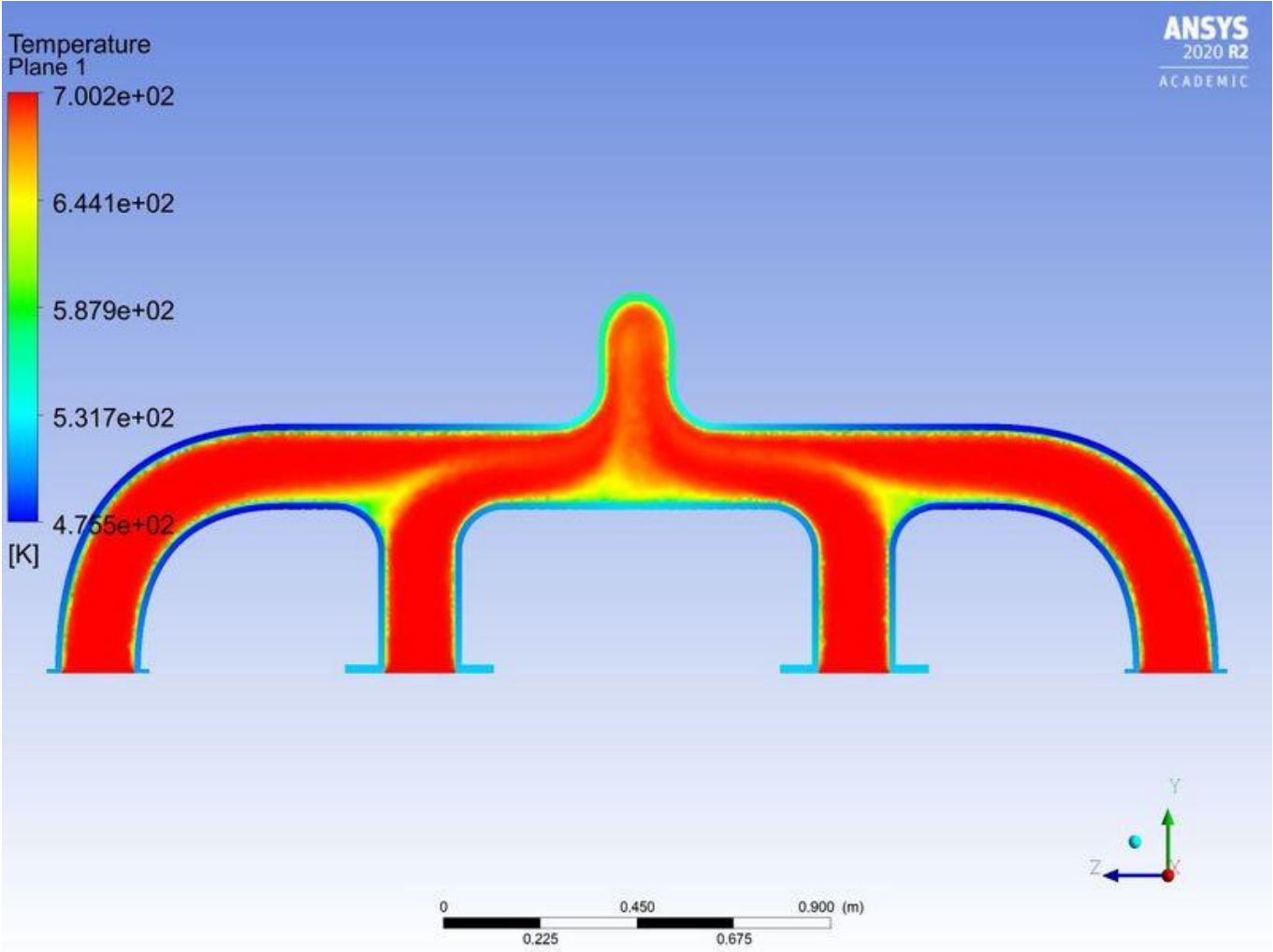


Velocity  
Plane 1  
3.881e+01  
2.911e+01  
1.940e+01  
9.702e+00  
0.000e+00  
[m s<sup>-1</sup>]

0 0.050 0.100 0.150 0.200 (m)

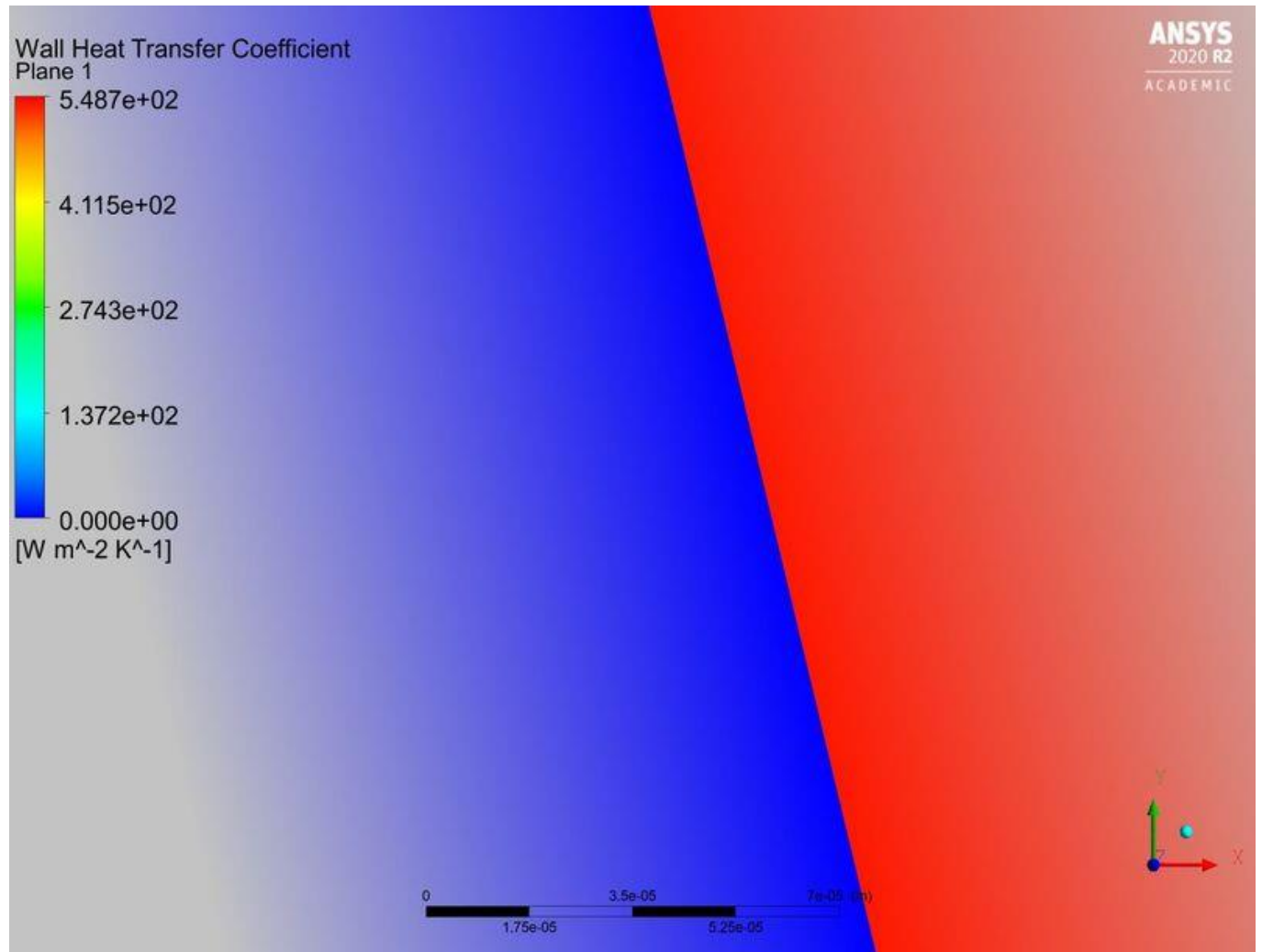


Temperature contour:





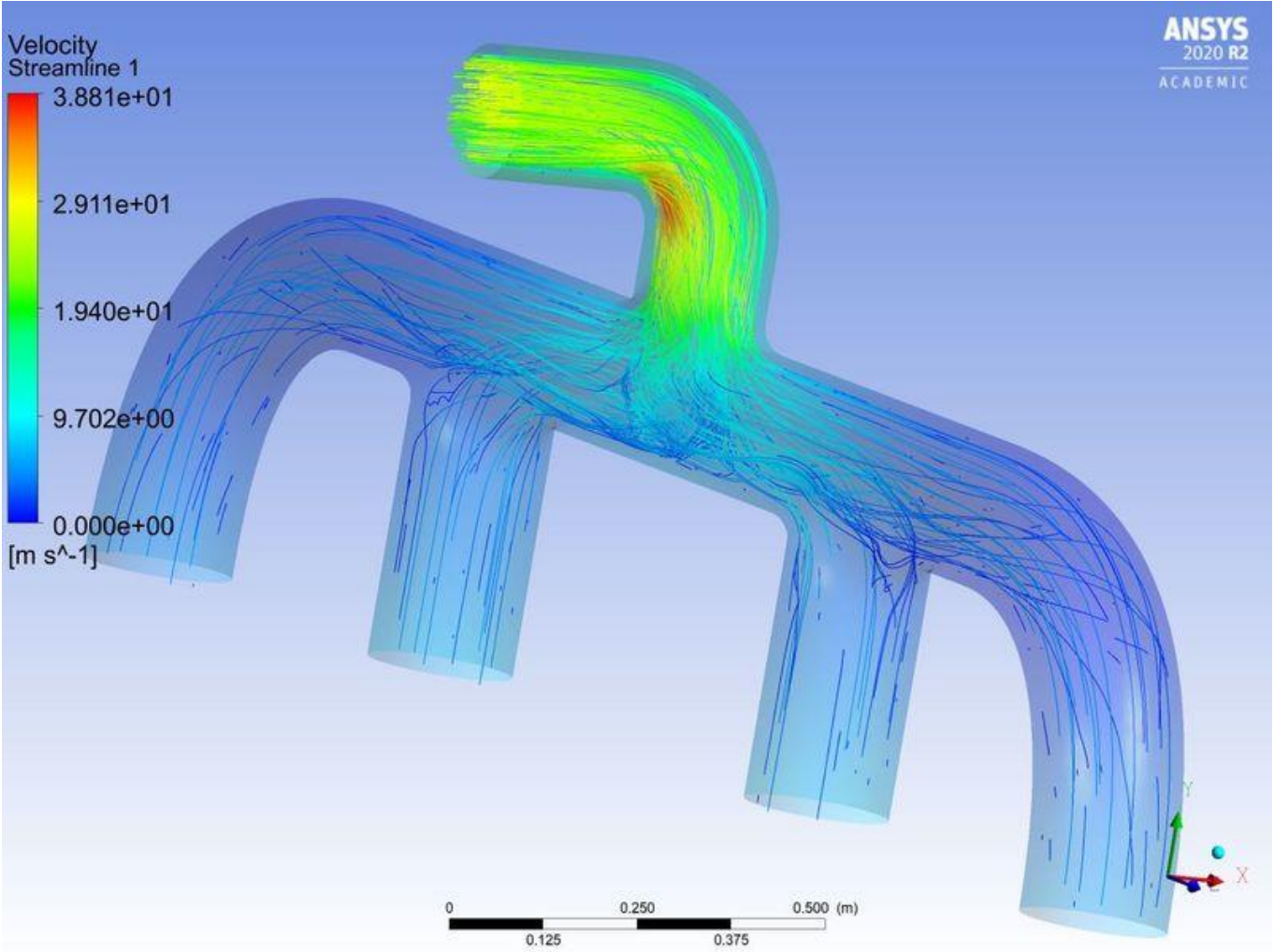
Wall heat transfer coefficient:

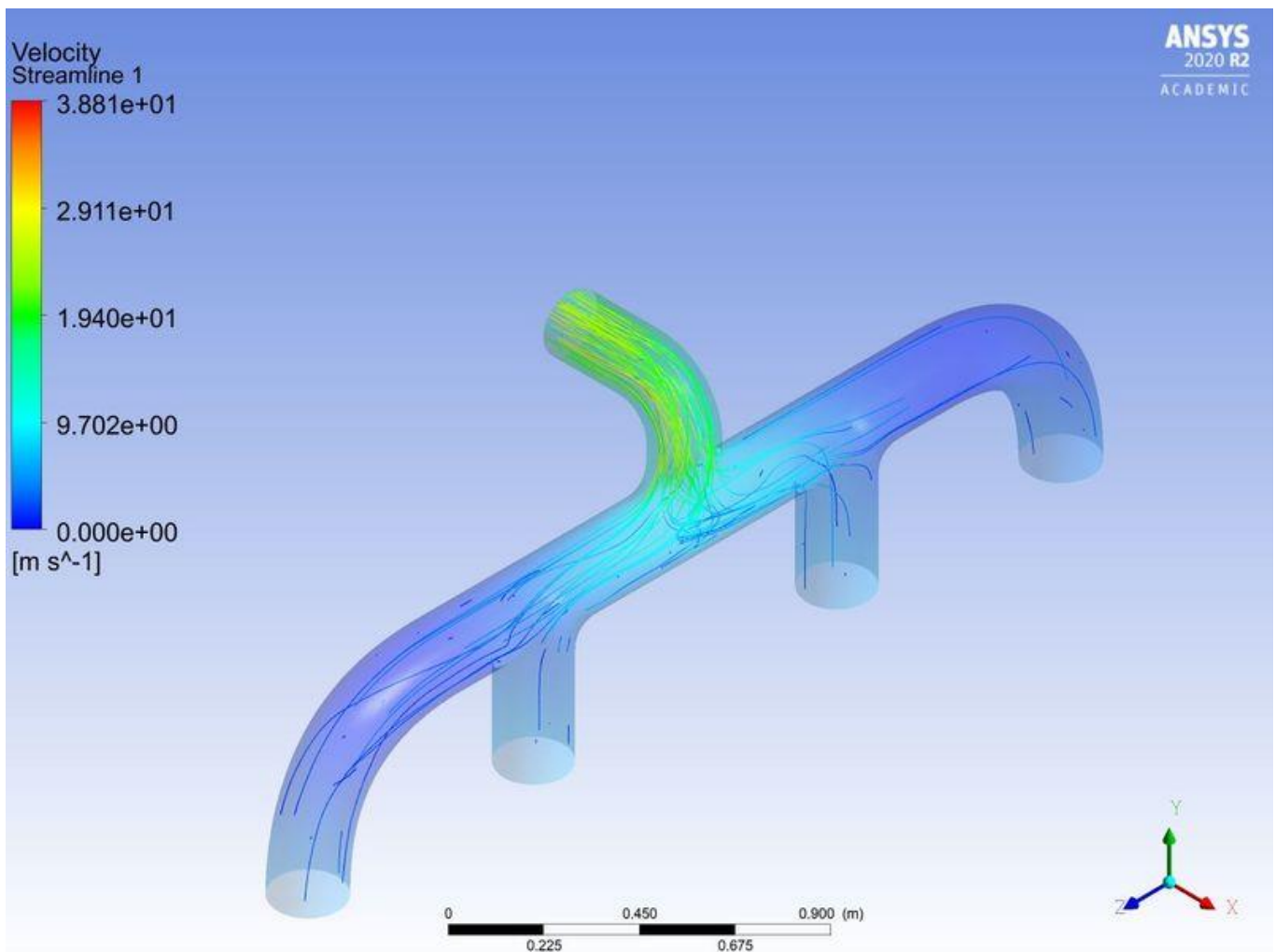


**Area Average of Wall Heat Transfer Coefficient on inflation\_layer**

435.84 [W m<sup>-2</sup> K<sup>-1</sup>]

Streamline:





### To Verify the result:

Assuming the air as the fluid flowing in the pipe

For temperature  $t_{\text{air}} = 700\text{K}$ , from data book

Properties of air:

density =  $0.524 \text{ (kg)/m}^3$

Kinematic viscosity =  $63\text{e-}6 \text{ m}^2/\text{s}$

Prandtl number = 0.678

Conductivity =  $0.0521 \text{ W/m.K}$

Reynold's number =  $(u.L)/\nu$   
 $= (5 \times 0.166)/(63.03\text{e-}6)$

Thus,  $Re = 13.17\text{e}3$

For internal flow Reynold's number  $> 10000$

Nusselt number  $Nu = 0.036 [Re]^{0.8} [Pr]^{0.3}$

Thus,  $Nu = 63.31378$

We know that,  $Nu = (h.D)/k$

Thus which gives  $h = 19.8591 \text{ W/m}^2\text{.K}$

thus the  $h = 20 \text{ W/m}^2\text{.K}$  is used in the simulation

and it proves that the simulation is accurate.

(ii) as per the mass conservation law

we can say that the outlet velocity should be 4 times the inlet since there are 4 inlet and also the Inlet and outlet diameter are same.

Area Average of Velocity on outlet  $25.2434 [\text{m s}^{-1}]$

Thus the velocity is approximately  $25 [\text{m s}^{-1}]$

### **Conclusion:**

Thus the simulation has successfully run in Ansys fluent.