

# Ordinary differential equations

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## ⑥ Conclusion

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D. K. ...

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## D. L. 151

Global

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# Ordinary differential equations

An equation containing a function of one independent variable and its derivatives, in contrast to a *partial differential equation*, which contains derivatives with respect to more independent variables.

accurately and efficiently?

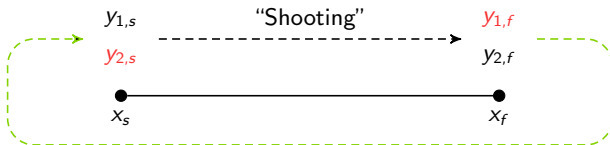
- Algebraic equation:



$$\frac{dc}{dx} = -\frac{1}{\mathcal{D}}y$$
$$\frac{dy}{dx} = \frac{kc}{1 + Kc}$$



$$\frac{dz}{dx} = r(x) - q(x)z(x)$$



- Explicit methods

- First order: forward Euler
- Second order: improved Euler (RK2)
- Fourth order: Runge-Kutta 4 (RK4)
- Step size control
- Implicit methods
  - First order: backward Euler
  - Second order: midpoint rule

- Explicit methods

- Explicit methods

- Shooting method

151

D. K. ...

### Conclusions

## D. L. 151

CL  $\rightarrow$   $\frac{1}{2}$   $\rightarrow$   $\frac{1}{2}$   $\rightarrow$   $\frac{1}{2}$

Get it?

Gifford, J. D. 1995. CODE.

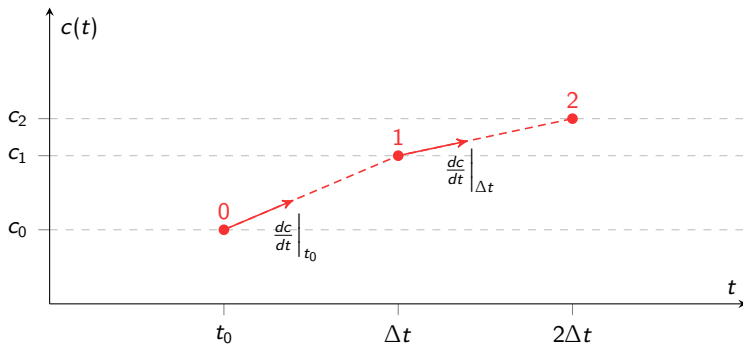
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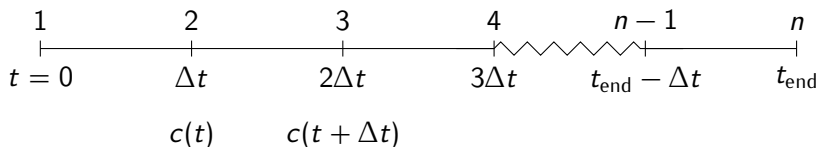
$$c(t_0 + \Delta t) \approx c(t_0) + \left. \frac{dc}{dt} \right|_{t_0} \Delta t + \frac{1}{2} \left. \frac{d^2c}{dt^2} \right|_{t_0} (\Delta t)^2 + \mathcal{O}(\Delta t^3)$$

$$\frac{c(t_0 + \Delta t) - c(t_0)}{\Delta t} = f(c_0, t_0) \Rightarrow c(t_0 + \Delta t) = c(t_0) + \Delta t f(c_0, t_0)$$



Start with  $t = t_0$ ,  $c = c_0$ , then calculate at discrete points in time:  
 $c(t_1 = t_0 + \Delta t) = c(t_0) + \Delta t f(c_0, t_0)$ .

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 $c(t_1 = t_0 + \Delta t) = c(t_0) + \Delta t f(c_0, t_0)$ .

- 1 Initialize variables, functions; set  $h = \frac{x_1 - x_0}{N}$
- 2 Set  $x = x_0, y = y_0$
- 3 While  $x < x_{\text{end}}$  do  
 $x_{i+1} = x_i + h; \quad y_{i+1} = y_i + hf(x_i, y_i)$



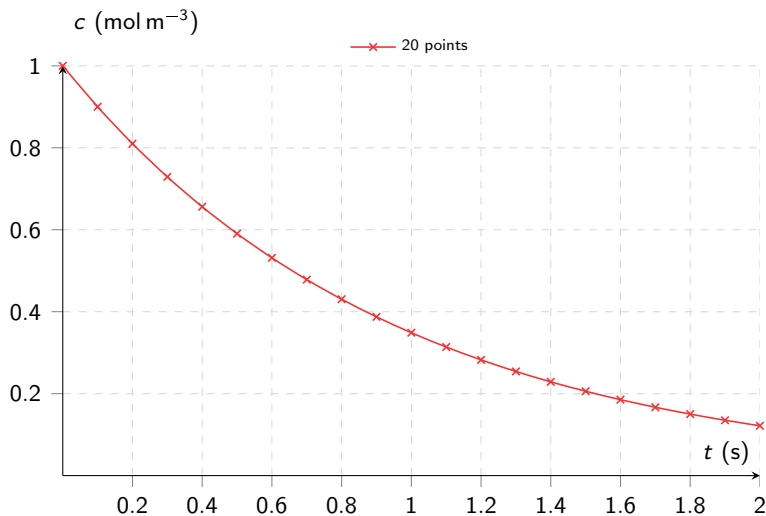
$$\frac{dc}{dt} = -kc \quad \text{with} \quad c(t=0) = 1 \text{ mol m}^{-3}, \quad k = 1 \text{ s}^{-1}, \quad t_{\text{end}} = 2 \text{ s}$$

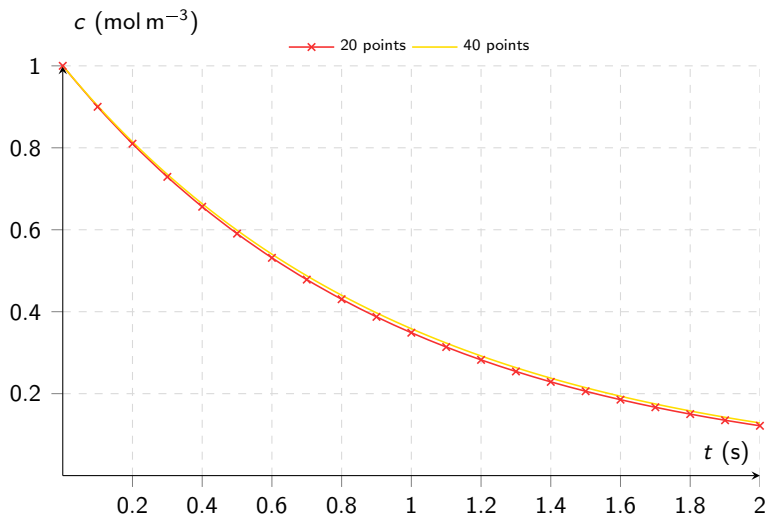
## Euler's method - example

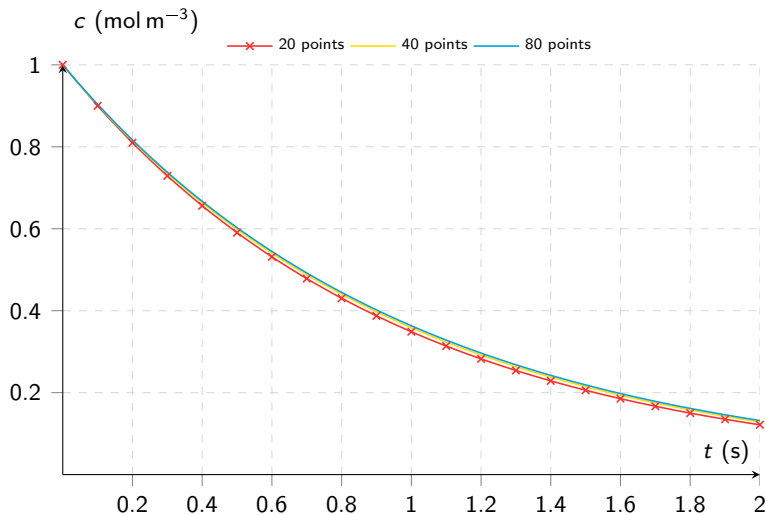
First order reaction in a batch reactor:

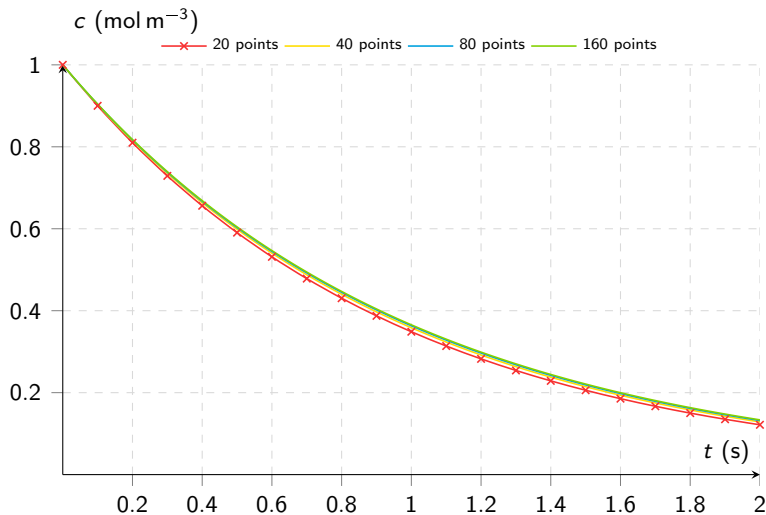
$$\frac{dc}{dt} = -kc \quad \text{with} \quad c(t=0) = 1 \text{ mol m}^{-3}, \quad k = 1 \text{ s}^{-1}, \quad t_{\text{end}} = 2 \text{ s}$$

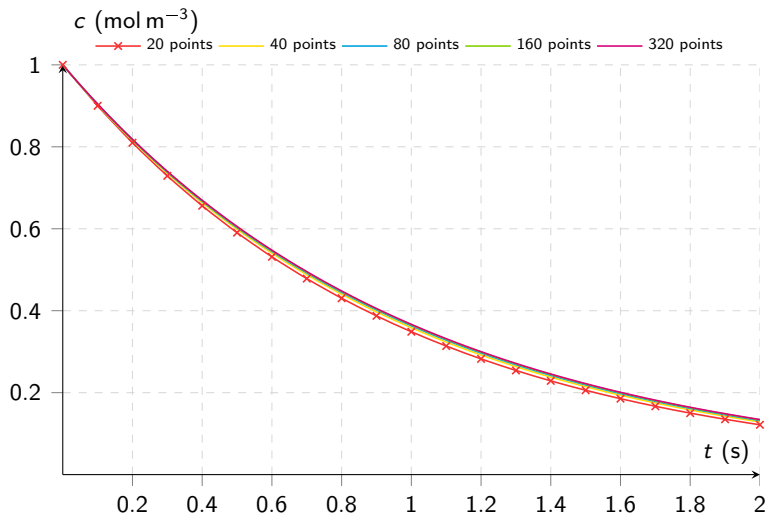
Time [s]	Concentration [mol m <sup>-3</sup> ]
$t_0 = 0$	$c_0 = 1.00$
$t_1 = t_0 + \Delta t$ $= 0 + 0.1 = 0.1$	$c_1 = c_0 + \Delta t \cdot (-kc_0)$ $= 1 + 0.1 \cdot (-1 \cdot 1) = 0.9$
$t_2 = t_1 + \Delta t$ $= 0.1 + 0.1 = 0.2$	$c_2 = c_1 + \Delta t \cdot (-kc_1)$ $= 0.9 + 0.1 \cdot (-1 \cdot 0.9) = 0.81$
$t_3 = t_2 + \Delta t$ $= 0.2 + 0.1 = 0.3$	$c_3 = c_2 + \Delta t \cdot (-kc_2)$ $= 0.81 + 0.1 \cdot (-1 \cdot 0.81) = 0.729$
...	...
$t_{i+1} = t_i + \Delta t$	$c_{i+1} = c_i + \Delta t \cdot (-kc_i)$
...	...
$t_{20} = 2.0$	$c_{20} = c_{19} + \Delta t \cdot (-kc_{19}) = 0.1211577$







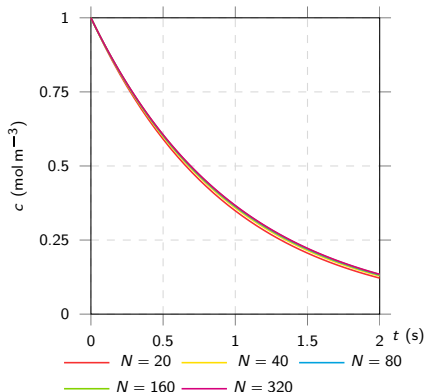




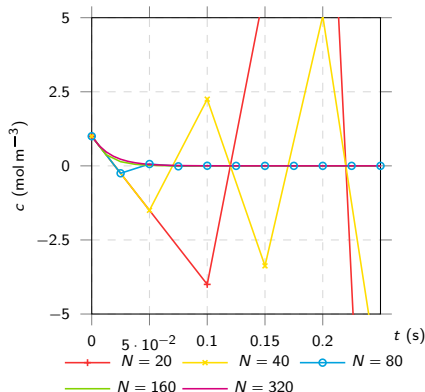
# Problems with Euler's method

The question is: What step size, or how many steps to use?

- 1 *Accuracy*  $\Rightarrow$  need information on numerical error!
- 2 *Stability*  $\Rightarrow$  need information on stability limits!



Reaction rate:  $k = 1 \text{ s}^{-1}$



Reaction rate:  $k = 50 \text{ s}^{-1}$

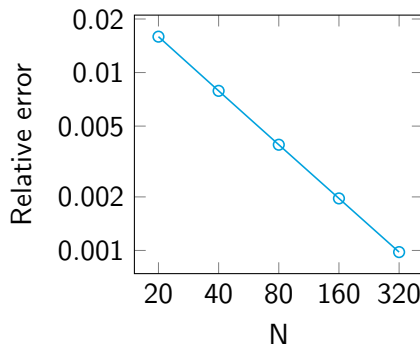


## Accuracy

Comparison with analytical solution for  $k = 1 \text{ s}^{-1}$ :

$$c(t) = c_0 \exp(-kt) \Rightarrow \zeta = 1 - \exp(-kt) \Rightarrow \zeta_{\text{analytical}} = 0.864665$$

$N$	$\zeta$	$\frac{\zeta_{\text{numerical}} - \zeta_{\text{analytical}}}{\zeta_{\text{analytical}}}$
20	0.878423	0.015912
40	0.871488	0.007891
80	0.868062	0.003929
160	0.866360	0.001961
320	0.865511	0.000979



## Accuracy

For Euler's method: Error halves when the number of grid points is doubled, i.e. error is proportional to  $\Delta t$ : first order method.

Error estimate:

$$\left. \frac{dx}{dt} \right|_{t_0} = \frac{x(t_0 + \Delta t) - x(t_0)}{\Delta t} + \frac{1}{2} \left. \frac{d^2 x}{dt^2} \right|_{t_0} (\Delta t) + \mathcal{O}(\Delta t)^2$$

$$\frac{x(t_0 + \Delta t) - x(t_0)}{\Delta t} = f(x_0, t_0) - \frac{1}{2} \frac{d^2 x}{dt^2} \bigg|_{t_0} (\Delta t) + \mathcal{O}(\Delta t)^2$$

## Errors and convergence rate

## $L_2$ norm (Euclidean norm)

$$\|\mathbf{v}\|_2 = \sqrt{v_1^2 + v_2^2 + \dots + v_n^2} = \sqrt{\sum_{i=1}^n v_i^2}$$

### $L_\infty$ norm (maximum norm)

$$\|\mathbf{v}\|_\infty = \max(|v_1|, \dots, |v_n|)$$

## Absolute difference

$$\epsilon_{\text{abs}} = \|\mathbf{y}_{\text{numerical}} - \mathbf{y}_{\text{analytical}}\|_{2,\infty}$$

## Relative difference

$$\epsilon_{\text{rel}} = \frac{\|\mathbf{y}_{\text{numerical}} - \mathbf{y}_{\text{analytical}}\|_{2,\infty}}{\|\mathbf{y}_{\text{analytical}}\|_{2,\infty}}$$

## What to do when there is no analytical solution available?

## Errors and convergence rate

Convergence rate (or: order of convergence)  $r$

$$\epsilon = \lim_{\Delta t \rightarrow 0} c(\Delta x)^r$$

- A first order method reduces the error by a factor 2 when increasing the number of steps by a factor 2
- A second order method reduces the error by a factor 4 when increasing the number of steps by a factor 2

What to do when there is no analytical solution available? Compare to calculations with different number of steps:  $\epsilon_1 = c(\Delta x_1)^r$  and  $\epsilon_2 = c(\Delta x_2)^r$  and solve for  $r$ :

$$\frac{\epsilon_2}{\epsilon_1} = \frac{c(\Delta x_2)^r}{c(\Delta x_1)^r} = \left( \frac{\Delta x_2}{\Delta x_1} \right)^r \Rightarrow \log \left( \frac{\epsilon_2}{\epsilon_1} \right) = \log \left( \frac{\Delta x_2}{\Delta x_1} \right)^r$$

$$\Rightarrow r = \frac{\log\left(\frac{\epsilon_2}{\epsilon_1}\right)}{\log\left(\frac{\Delta x_2}{\Delta x_1}\right)} = \frac{\log\left(\frac{\epsilon_2}{\epsilon_1}\right)}{\log\left(\frac{N_1}{N_2}\right)} \quad \text{in the limit of } \Delta x \rightarrow 0 \quad \text{or} \quad N \rightarrow \infty$$

$N$	$\zeta$	$\frac{\zeta_{\text{numerical}} - \zeta_{\text{analytical}}}{\zeta_{\text{analytical}}}$	$r = \frac{\log\left(\frac{\epsilon_j}{\epsilon_{j-1}}\right)}{\log\left(\frac{N_{j-1}}{N_j}\right)}$
20	0.878423	0.015912	—
40	0.871488	0.007891	1.011832
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## Example: Euler's method — order of convergence

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Wouldn't it be great to have a method that can give the answer using much less steps?



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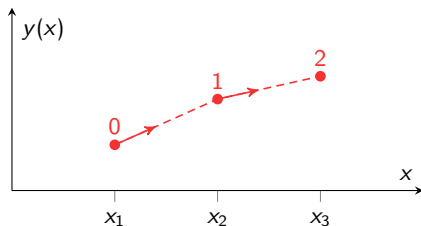
Wouldn't it be great to have a method that can give the answer using much less steps? ⇒ Higher order methods

# Runge-Kutta methods

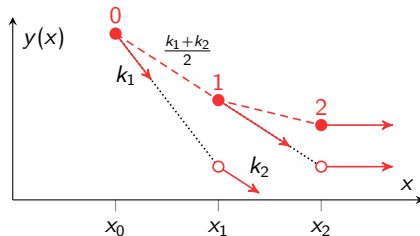
Propagate a solution by combining the information of several Euler-style steps (each involving one function evaluation) to match a Taylor series expansion up to some higher order.

Euler:  $y_{i+1} = y_i + hf(x_i, y_i)$  with  $h = \Delta x$ , i.e.  
slope =  $k_1 = f(x_i, y_i)$ .

Euler's method



RK2 method



# Classical second order Runge-Kutta (RK2) method

This method is also called Heun's method, or improved Euler method:

- 1 Approximate the slope at  $x_i$ :  $k_1 = f(x_i, y_i)$
- 2 Approximate the slope at  $x_{i+1}$ :  $k_2 = f(x_{i+1}, y_{i+1})$  where we use Euler's method to approximate  $y_{i+1} = y_i + hf(x_i, y_i) = y_i + hk_1$
- 3 Perform an Euler step with the average of the slopes:  

$$y_{i+1} = y_i + h\frac{1}{2}(k_1 + k_2)$$

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- 3 Perform an Euler step with the average of the slopes:  

$$y_{i+1} = y_i + h\frac{1}{2}(k_1 + k_2)$$

In pseudocode:

```

x = x0, y = y0
while x < xend do
  xi+1 = xi + h
  k1 = f(xi, yi)
  k2 = f(xi + h, yi + hk1)
  yi+1 = yi + h1/2 (k1 + k2)
end while
  
```

# Runge-Kutta methods — derivation

$$\frac{dy}{dx} = f(x, y(x))$$

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Using Taylor series expansion:  $y_{i+1} = y_i + h \left. \frac{dy}{dx} \right|_i + \frac{h^2}{2} \left. \frac{d^2y}{dx^2} \right|_i + \mathcal{O}(h^3)$

$$\left. \frac{dy}{dx} \right|_i = f(x_i, y_i) \equiv f_i$$

$$\left. \frac{d^2y}{dx^2} \right|_i = \left. \frac{d}{dx} f(x, y(x)) \right|_i = \left. \frac{\partial f}{\partial x} \right|_i + \left. \frac{\partial f}{\partial y} \right|_i \left. \frac{dy}{dx} \right|_i = \left. \frac{\partial f}{\partial x} \right|_i + \left. \frac{\partial f}{\partial y} \right|_i f_i \quad (\text{chain rule})$$

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Substitution gives:

$$y_{i+1} = y_i + hf_i + \frac{h^2}{2} \left( \left. \frac{\partial f}{\partial x} \right|_i + \left. \frac{\partial f}{\partial y} \right|_i f_i \right) + \mathcal{O}(h^3)$$

$$y_{i+1} = y_i + \frac{h}{2} f_i + \frac{h}{2} \left( f_i + h \left. \frac{\partial f}{\partial x} \right|_i + hf_i \left. \frac{\partial f}{\partial y} \right|_i \right) + \mathcal{O}(h^3)$$

# Runge-Kutta methods — derivation

Note multivariate Taylor expansion:

$$f(x_i + h, y_i + k) = f_i + h \left. \frac{\partial f}{\partial x} \right|_i + k \left. \frac{\partial f}{\partial y} \right|_i + \mathcal{O}(h^2)$$

$$\Rightarrow \frac{h}{2} \left( f_i + h \left. \frac{\partial f}{\partial x} \right|_i + hf_i \left. \frac{\partial f}{\partial y} \right|_i \right) = \frac{h}{2} f(x_i + h, y_i + kf_i) + \mathcal{O}(h^3)$$

Concluding:

$$y_{i+1} = y_i + \frac{h}{2} f_i + \frac{h}{2} f(x_i + h, y_i + kf_i) + \mathcal{O}(h^3)$$

Rewriting:

$$k_1 = f(x_i, y_i)$$

$$k_2 = f(x_i + h, y_i + hk_1)$$

$$\Rightarrow y_{i+1} = y_i + \frac{h}{2}(k_1 + k_2)$$



# Runge-Kutta methods — derivation

Generalization:  $y_{i+1} = y_i + h(b_1 k_1 + b_2 k_2) + \mathcal{O}(h^3)$

with  $k_1 = f_i$ ,  $k_2 = f(x_i + c_2 h, y_i + a_{2,1} h k_1)$

(Note that classical RK2:  $b_1 = b_2 = \frac{1}{2}$  and  $c_2 = a_{2,1} = 1$ .)

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Bivariate Taylor expansion:

$$f(x_i + c_2 h, y_i + a_{2,1} h k_1) = f_i + c_2 h \left. \frac{\partial f}{\partial x} \right|_i + a_{2,1} h k_1 \left. \frac{\partial f}{\partial y} \right|_i + \mathcal{O}(h^2)$$

$$y_{i+1} = y_i + h(b_1 k_1 + b_2 k_2) + \mathcal{O}(h^3)$$

$$= y_i + h[b_1 f_i + b_2 f(x_i + c_2 h, y_i + a_{2,1} h k_1)] + \mathcal{O}(h^3)$$

$$= y_i + h \left[ b_1 f_i + b_2 \left\{ f_i + c_2 h \left. \frac{\partial f}{\partial x} \right|_i + a_{2,1} h k_1 \left. \frac{\partial f}{\partial y} \right|_i + \mathcal{O}(h^2) \right\} \right] + \mathcal{O}(h^3)$$

$$= y_i + h(b_1 + b_2) f_i + h^2 b_2 \left( c_2 \left. \frac{\partial f}{\partial x} \right|_i + a_{2,1} f_i \left. \frac{\partial f}{\partial y} \right|_i \right) + \mathcal{O}(h^3)$$

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Comparison with Taylor:

$$y_{i+1} = y_i + h f_i + \frac{h^2}{2} \left( \left. \frac{\partial f}{\partial x} \right|_i + \left. \frac{\partial f}{\partial y} \right|_i f_i \right) + \mathcal{O}(h^3)$$

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$$= y_i + h \left[ b_1 f_i + b_2 f(x_i + c_2 h, y_i + a_{2,1} h k_1) \right] + \mathcal{O}(h^3)$$

$$= y_i + h \left[ b_1 f_i + b_2 \left\{ f_i + c_2 h \left. \frac{\partial f}{\partial x} \right|_i + a_{2,1} h k_1 \left. \frac{\partial f}{\partial y} \right|_i + \mathcal{O}(h^2) \right\} \right] + \mathcal{O}(h^3)$$

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Comparison with Taylor:

$$y_{i+1} = y_i + h f_i + \frac{h^2}{2} \left( \left. \frac{\partial f}{\partial x} \right|_i + \left. \frac{\partial f}{\partial y} \right|_i f_i \right) + \mathcal{O}(h^3)$$

# Runge-Kutta methods — derivation

$$y_{i+1} = y_i + h(b_1 + b_2)f_i + h^2 b_2 \left( c_2 \left. \frac{\partial f}{\partial x} \right|_i + a_{2,1} f_i \left. \frac{\partial f}{\partial y} \right|_i \right) + \mathcal{O}(h^3)$$

$$y_{i+1} = y_i + hf_i + \frac{h^2}{2} \left( \left. \frac{\partial f}{\partial x} \right|_i + \left. \frac{\partial f}{\partial y} \right|_i f_i \right) + \mathcal{O}(h^3)$$

$\Rightarrow$  3 eqns and 4 unknowns  $\Rightarrow$  multiple possibilities!

- 1 Classical RK2:

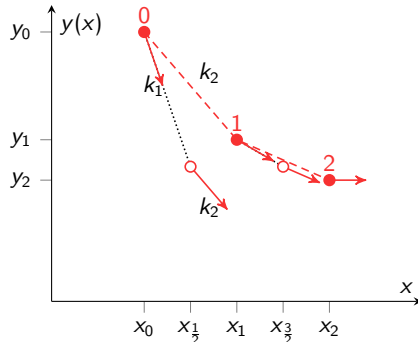
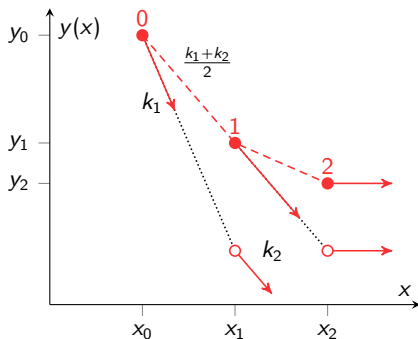
$$b_1 = b_2 = \frac{1}{2} \text{ and } c_2 = a_{2,1} = 1$$

- 2 Midpoint rule (modified Euler):

$$b_1 = 0, b_2 = 1, c_2 = a_{2,1} = \frac{1}{2}$$

# Second order Runge-Kutta methods

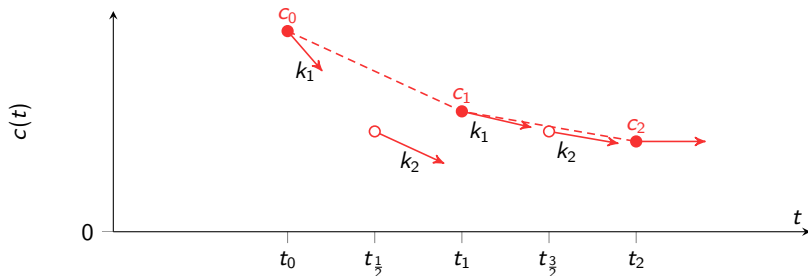
Classical RK2 method (= Heun's method, improved Euler method)	Explicit midpoint rule (modified Euler method)
$k_1 = f_i$	$k_1 = f_i$
$k_2 = f(x_i + h, y_i + hk_1)$	$k_2 = f(x_i + \frac{1}{2}h, y_i + \frac{1}{2}hk_1)$
$y_{i+1} = y_i + \frac{1}{2}h(k_1 + k_2)$	$y_{i+1} = y_i + hk_2$



## Second order Runge-Kutta method — Example

First order reaction in a batch reactor:  $\frac{dc}{dt} = -kc$  with  
 $c(t = 0) = 1 \text{ mol m}^{-3}$ ,  $k = 1 \text{ s}^{-1}$ ,  $t_{\text{end}} = 2 \text{ s}$ .

Time [s]	C [mol m <sup>-3</sup> ]	$k_1 = hf(x_i, y_i)$	$k_2 = hf(x_i + \frac{1}{2}h, y_n + \frac{1}{2}k_1)$
0	1.00	$0.1 \cdot (-1 \cdot 1) = -0.1$	$0.1 \cdot (-1 \cdot (1 - 0.5 \cdot 0.1)) = -0.095$
0.1	$1 - 0.095 = 0.905$	$0.1 \cdot (-1 \cdot 0.905) = -0.0905$	$0.1 \cdot (-1 \cdot (0.905 - 0.5 \cdot 0.0905)) = -0.085975$
...	...	...	...
2	0.1358225	-0.0135822	-0.0129031



# RK2 method — order of convergence

$N$	$\zeta$	$\frac{\zeta_{\text{numerical}} - \zeta_{\text{analytical}}}{\zeta_{\text{analytical}}}$	$r = \frac{\log\left(\frac{\epsilon_i}{\epsilon_{i-1}}\right)}{\log\left(\frac{N_{i-1}}{N_i}\right)}$
20	0.864178	$5.634 \times 10^{-4}$	—
40	0.864548	$1.355 \times 10^{-4}$	2.056
80	0.864636	$3.323 \times 10^{-5}$	2.028
160	0.864658	$8.229 \times 10^{-6}$	2.014
320	0.864663	$2.048 \times 10^{-6}$	2.007



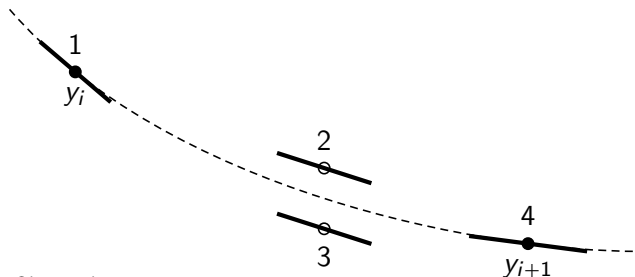
# RK2 method — order of convergence

$N$	$\zeta$	$\frac{\zeta_{\text{numerical}} - \zeta_{\text{analytical}}}{\zeta_{\text{analytical}}}$	$r = \frac{\log\left(\frac{\epsilon_i}{\epsilon_{i-1}}\right)}{\log\left(\frac{N_{i-1}}{N_i}\right)}$
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320	0.864663	$2.048 \times 10^{-6}$	2.007

$\Rightarrow$  RK2 is a second order method. Doubling the number of cells reduces the error by a factor 4!

Can we do even better?

# RK4 method (classical fourth order Runge-Kutta method)



$$k_1 = f(x_i, y_i)$$

$$k_2 = f\left(x_i + \frac{1}{2}h, y_i + \frac{1}{2}hk_1\right)$$

$$k_3 = f\left(x_i + \frac{1}{2}h, y_i + \frac{1}{2}hk_2\right)$$

$$k_4 = f(x_i + h, y_i + hk_3)$$

$$y_{i+1} = y_i + h \left( \frac{1}{6}k_1 + \frac{1}{3}(k_2 + k_3) + \frac{1}{6}k_4 \right)$$

# RK4 method — order of convergence

$N$	$\zeta$	$\frac{\zeta_{\text{numerical}} - \zeta_{\text{analytical}}}{\zeta_{\text{analytical}}}$	$r = \frac{\log\left(\frac{\epsilon_i}{\epsilon_{i-1}}\right)}{\log\left(\frac{N_{i-1}}{N_i}\right)}$
20	0.864664472	$2.836 \times 10^{-7}$	—
40	0.864664702	$1.700 \times 10^{-8}$	4.060
80	0.864664716	$1.040 \times 10^{-9}$	4.030
160	0.864664717	$6.435 \times 10^{-11}$	4.015
320	0.864664717	$4.001 \times 10^{-12}$	4.007

# RK4 method — order of convergence

$N$	$\zeta$	$\frac{\zeta_{\text{numerical}} - \zeta_{\text{analytical}}}{\zeta_{\text{analytical}}}$	$r = \frac{\log\left(\frac{\epsilon_i}{\epsilon_{i-1}}\right)}{\log\left(\frac{N_{i-1}}{N_i}\right)}$
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160	0.864664717	$6.435 \times 10^{-11}$	4.015
320	0.864664717	$4.001 \times 10^{-12}$	4.007

$\Rightarrow$  RK4 is a fourth order method: Doubling the number of cells reduces the error by a factor 16!

Can we do even better?

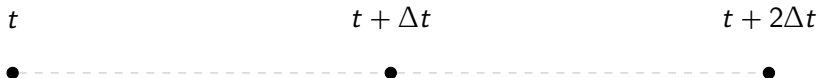
# Adaptive step size control

The step size (be it either position, time or both (PDEs)) cannot be decreased indefinitely to favour a higher accuracy, since each additional grid point causes additional computation time. It may be wise to adapt the step size according to the computation requirements.

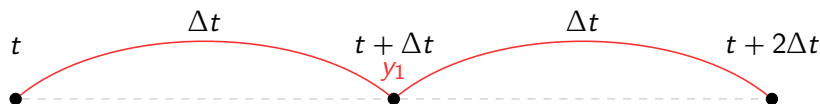
Globally two different approaches can be used:

- 1 Step doubling: compare solutions when taking one full step or two consecutive halve steps
- 2 Embedded methods: Compare solutions when using two approximations of different order

## Adaptive step size control: step doubling

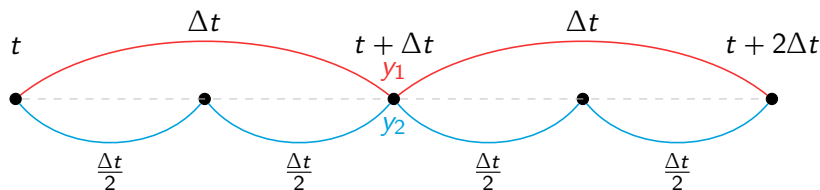


## Adaptive step size control: step doubling



- RK4 with one large step of  $h$ :  $y_{i+1} = y_1 + ch^5 + \mathcal{O}(h^6)$

# Adaptive step size control: step doubling



- RK4 with one large step of  $h$ :  $y_{i+1} = y_1 + ch^5 + \mathcal{O}(h^6)$
- RK4 with two steps of  $\frac{1}{2}h$ :  $y_{i+1} = y_2 + 2c(\frac{1}{2}h)^5 + \mathcal{O}(h^6)$



## Adaptive step size control: step doubling

- Estimation of truncation error by comparing  $y_1$  and  $y_2$ :

$$\Delta = y_2 - y_1$$

- If  $\Delta$  too large, reduce step size for accuracy
- If  $\Delta$  too small, increase step size for efficiency.

- Ignoring higher order terms and solving for  $c$ :

$$\Delta = \frac{15}{16}ch^5 \Rightarrow ch^5 = \frac{16}{15}\Delta \Rightarrow y_{i+1} = y_2 + \frac{\Delta}{15} + \mathcal{O}(h^6)$$

(local Richardson extrapolation)

Note that when we specify a tolerance  $tol$ , we can estimate the maximum allowable step size as:  $h_{\text{new}} = \alpha h_{\text{old}} \left| \frac{tol}{\Delta} \right|^{\frac{1}{5}}$  with  $\alpha$  a safety factor (typically  $\alpha = 0.9$ ).

## Adaptive step size control: embedded methods

Use a special fourth and a fifth order Runge Kutta method to approximate  $y_{i+1}$

- The fourth order method is special because we want to use the same positions for the evaluation for computational efficiency.
- RK45 is there preferred method (minimum number of function evaluations) (this is built in Matlab as [ode45](#)).

# Today's outline

## ① Introduction

## ② Explicit methods

Forward Euler

Convergence rate

Runge-Kutta methods

Step size control

## ③ Implicit methods

Backward Euler

Implicit midpoint method

## ④ Boundary value problems

Shooting method

## ⑤ Systems of ODEs

Solution methods for systems of ODEs

Stiff systems of ODEs

Solving systems of ODEs in Matlab

## ⑥ Conclusion



Where to evaluate the function  $f$ ?

- 1 Evaluation at  $x_i$ : Explicit Euler method (forward Euler)
- 2 Evaluation at  $x_{i+1}$ : Implicit Euler method (backward Euler)

- This is an explicit equation for  $y_{i+1}$  in terms of  $y_i$ .
- It can give instabilities with large function values.

$$\frac{dc}{dt} = -kc \Rightarrow c_{i+1} = c_i - k c_i \Delta t \Rightarrow \frac{c_{i+1}}{c_i} = 1 - k \Delta t$$



(but probably accuracy requirements are more stringent here!)

## Problems with Euler's method: instability – backward Euler

Implicit Euler method (backward Euler):

- Use values at  $x_{j+1}$ :

$$\frac{y_{i+1}-y_i}{\Delta x} = f(x_{i+1}, y_{i+1}) \Rightarrow y_{i+1} = y_i + hf(x_{i+1}, y_{i+1}).$$

- This is an implicit equation for  $y_{i+1}$ , because it also depends on terms of  $y_{i+1}$ .

Problems with Euler's method: instability – backward Euler

Implicit Euler method (backward Euler):

- Use values at  $x_{j+1}$ :

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- This is an implicit equation for  $y_{i+1}$ , because it also depends on terms of  $y_{i+1}$ .

Consider the first order batch reactor:

$$\frac{dc}{dt} = -kc \Rightarrow c_{i+1} = c_i - k c_{i+1} \Delta t \Rightarrow \frac{c_{i+1}}{c_i} = \frac{1}{1 + k \Delta t}$$

The implicit Euler method is *unconditionally stable* (but maybe not very accurate or efficient).

## Semi-implicit Euler method

Usually  $f$  is a non-linear function of  $y$ , so that linearization is required (recall Newton's method).

$$\frac{dy}{dx} = f(y) \Rightarrow y_{i+1} = y_i + hf(y_{i+1}) \quad \text{using} \quad f(y_{i+1}) = f(y_i) + \left. \frac{df}{dy} \right|_i (y_{i+1} - y_i) + \dots$$

$$\Rightarrow y_{i+1} = y_i + h \left[ f(y_i) + \frac{df}{dy} \Big|_i (y_{i+1} - y_i) \right]$$

$$\Rightarrow \left(1 - h \left. \frac{df}{dy} \right|_i\right) y_{i+1} = \left(1 - h \left. \frac{df}{dy} \right|_i\right) y_i + hf(y_i)$$

$$\Rightarrow y_{i+1} = y_i + h \left( 1 - h \frac{df}{dy} \Big|_i \right)^{-1} f(y_i)$$

$$y_{i+1} = y_i + hf(x_{i+1}, y_{i+1}) \Rightarrow y_{i+1} = y_i + h \left( 1 - h \frac{df}{dy} \Big|_i \right)^{-1} f(x_{i+1}, y_i)$$

## Semi-implicit Euler method - example

Second order reaction in a batch reactor:

$$\frac{dc}{dt} = -kc^2 \text{ with } c_0 = 1 \text{ mol m}^{-3}, k = 1 \text{ m}^3 \text{ mol}^{-1} \text{ s}^{-1}, t_{\text{end}} = 2 \text{ s}$$

Analytical solution:  $c(t) = \frac{c_0}{1+kc_0t}$

# Semi-implicit Euler method - example

Second order reaction in a batch reactor:

$$\frac{dc}{dt} = -kc^2 \text{ with } c_0 = 1 \text{ mol m}^{-3}, k = 1 \text{ m}^3 \text{ mol}^{-1} \text{ s}^{-1}, t_{\text{end}} = 2 \text{ s}$$

Analytical solution:  $c(t) = \frac{c_0}{1+kc_0t}$

Define  $f = -kc^2$ , then  $\frac{df}{dc} = -2kc \Rightarrow c_{i+1} = c_i - \frac{hkc_i^2}{1+2hkc_i}$ .



$N$	$\zeta$	$\frac{\zeta_{\text{numerical}} - \zeta_{\text{analytical}}}{\zeta_{\text{analytical}}}$	$r = \frac{\log\left(\frac{\epsilon_i}{\epsilon_{i-1}}\right)}{\log\left(\frac{N_{i-1}}{N_i}\right)}$
20	0.654066262	$1.89 \times 10^{-2}$	—
40	0.660462687	$9.31 \times 10^{-3}$	1.02220
80	0.663589561	$4.62 \times 10^{-3}$	1.01162
160	0.665134433	$2.30 \times 10^{-3}$	1.00594
320	0.665902142	$1.15 \times 10^{-3}$	1.00300

$$f\left(\frac{1}{2}(y_i + y_{i+1})\right) = f_i + \left.\frac{df}{dy}\right|_i \left(\frac{1}{2}(y_i + y_{i+1}) - y_i\right) = f_i + \frac{1}{2} \left.\frac{df}{dy}\right|_i (y_{i+1} - y_i)$$

$$\Rightarrow y_{i+1} = y_i + h \left( 1 - \frac{h}{2} \frac{df}{dy} \bigg|_i \right)^{-1} f_i$$

$\frac{dc}{dt} = -kc^2$  with  $c_0 = 1 \text{ mol m}^{-3}$ ,  $k = 1 \text{ m}^3 \text{ mol}^{-1} \text{ s}^{-1}$ ,  $t_{\text{end}} = 2 \text{ s}$   
(Analytical solution:  $c(t) = \frac{c_0}{1+kc_0t}$ ).

Define  $f = -kc^2$ , then  $\frac{df}{dc} = -2kc$ .

$\frac{dc}{dt} = -kc^2$  with  $c_0 = 1 \text{ mol m}^{-3}$ ,  $k = 1 \text{ m}^3 \text{ mol}^{-1} \text{ s}^{-1}$ ,  $t_{\text{end}} = 2 \text{ s}$   
(Analytical solution:  $c(t) = \frac{c_0}{1+kc_0t}$ ).

$$\begin{aligned} c_{i+1} &= c_i + h \left( 1 - \frac{h}{2} \cdot (-2kc_i) \right)^{-1} \cdot (-kc_i^2) \\ &= c_i - \frac{hkc_i^2}{1 + hkc_i} = \frac{c_i + hkc_i^2 - hkc_i^2}{1 + hkc_i} \Rightarrow c_{i+1} = \frac{c_i}{1 + hkc_i} \end{aligned}$$

You will find that this method is exact for all step sizes  $h$  because of the quadratic source term!

$$C_{i+1} = \frac{C_i}{1 + hkc_i}$$



## Implicit midpoint method — example

Second order reaction in a batch reactor:

$$\frac{dc}{dt} = -kc^2 \text{ with } c_0 = 1 \text{ mol m}^{-3}, k = 1 \text{ m}^3 \text{ mol}^{-1} \text{ s}^{-1}, t_{\text{end}} = 2 \text{ s}$$

Analytical solution:  $c(t) = \frac{c_0}{1+kc_0t}$

$$C_{i+1} = \frac{C_i}{1 + hkc_i}$$

$N$	$\zeta$	$\frac{\zeta_{\text{numerical}} - \zeta_{\text{analytical}}}{\zeta_{\text{analytical}}}$	$r = \frac{\log\left(\frac{\epsilon_i}{\epsilon_{i-1}}\right)}{\log\left(\frac{N_{i-1}}{N_i}\right)}$
20	0.6666666667	$1.665 \times 10^{-16}$	—
40	0.6666666667	0	—
80	0.6666666667	0	—
160	0.6666666667	0	—
320	0.6666666667	0	—

$$C_{i+1} = C_i - \frac{hkc_i^3}{1 + \frac{3}{2}hkc_i^2}$$

## Implicit midpoint method — example

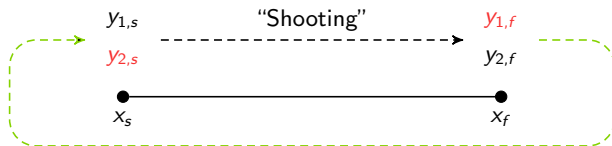
### Third order reaction in a batch reactor

Analytical solution:  $c(t) = \frac{c_0}{\sqrt{1+2kc_0^2t}}$

$$C_{i+1} = C_i - \frac{hkc_i^3}{1 + \frac{3}{2}hkc_i^2}$$

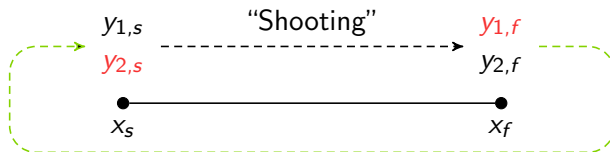
$N$	$\zeta$	$\frac{\zeta_{\text{numerical}} - \zeta_{\text{analytical}}}{\zeta_{\text{analytical}}}$	$r = \frac{\log\left(\frac{\epsilon_i}{\epsilon_{i-1}}\right)}{\log\left(\frac{N_{i-1}}{N_i}\right)}$
20	0.5526916174	$1.71 \times 10^{-4}$	—
40	0.5527633731	$4.17 \times 10^{-5}$	2.041
80	0.5527807304	$1.03 \times 10^{-5}$	2.021
160	0.5527849965	$2.55 \times 10^{-6}$	2.011
320	0.5527860538	$6.34 \times 10^{-7}$	2.005





## Shooting method

How to solve a BVP using the shooting method:



- Define the system of ODEs
- Provide an initial guess for the unknown boundary condition
- Solve the system and compare the resulting boundary condition to the expected value
- Adjust the guessed boundary value, and solve again. Repeat until convergence.
  - Of course, you can subtract the expected value from the computed value at the boundary, and use a non-linear root finding method

Question: compute the concentration profile in the film layer.

[illegible]

da

\_\_\_\_\_



## BVP: example in Excel

Consider a chemical reaction in a liquid film layer of thickness  $\delta$ :

$$\mathcal{D} \frac{d^2 c}{dx^2} = k_R c \text{ with } \begin{array}{ll} c(x=0) = C_{A,i,L} = 1 & \text{(interface concentration)} \\ c(x=\delta) = 0 & \text{(bulk concentration)} \end{array}$$

Question: compute the concentration profile in the film layer.

## Step 2: Set the boundary conditions

The boundary conditions for the concentrations at  $x = 0$  and  $x = \delta$  are known.

The flux at the interface, however, is not known, and should be solved for.

$$\frac{dc}{dx} = -\frac{1}{\mathcal{D}}q$$

$$\frac{dq}{dx} = -k_R C$$

## BVP: example in Excel


Solving the two first-order ODEs in Excel. First, the cells with constants:

	A	B	C
1	CAiL	1	ml/m3
2	D	1e-8	m2/s
3	kR	10	1/s
4	delta	1e-4	m
5	N	100	
6	dx	=B4/B5	

$$\frac{dc}{dx} = -\frac{1}{\mathcal{D}}q$$

$$\frac{dq}{dx} = -k_R C$$

\_\_\_\_\_



$$\frac{dc}{dx} = -\frac{1}{D}q$$

$$\frac{dq}{dx} = -k_R c$$

	A	B	C
10	x	c	q
11	0	=B1	10
12	=A11+\$B\$6	=B11+\$B\$6*(-1/\$B\$2*C11)	=C11+\$B\$6*(-\$B\$3*B11)
13	=A12+\$B\$6	=B12+\$B\$6*(-1/\$B\$2*C12)	=C12+\$B\$6*(-\$B\$3*B12)
...	...	...	...
111	=A110+\$B\$6	=B110+\$B\$6*(-1/\$B\$2*C110)	=C110+\$B\$6*(-\$B\$3*B110)

- We now have profiles for  $c$  and  $q$  as a function of position  $x$ .
- The concentration  $c(x = \delta)$  depends (eventually) on the boundary condition at the interface  $q(x = 0)$
- We can use the solver to change  $q(x = 0)$  such that the concentration at the bulk meets our requirement:  
 $c(x = \delta) = 0$

```
function [dxdt] = BVPODE(t,x,ps)
dxdt(1)=-1/ps.D*x(2);
dxdt(2)=-ps.kR*x(1);
dxdt=dxdt';
return
```

$$\frac{dq}{dx} = -k_R C$$

```
function f = RunBVP(bcq,ps)
[x,cq] = ode45(@BVPODE,[0 ps.delta],[1 bcq], [], ps);
f = cq(end,1) - 0;
plotyy(x,cq(:,1),x,cq(:,2));
return;
```





## BVP: example in Matlab

Finally, we should solve the system so that we obtain the right boundary condition  $q = \text{bcq}$  such that  $c(x = \delta) = 0$ . We can use the built-in function `fzero` to do this

```
% Parameter definition
```

```
ps.D=1e-8;  
ps.kR=10;  
ps.delta=1e-4;
```

```
% Solve for flux boundary condition (initial guess: 0)
opt = optimset('Display','iter');
flux = fzero(@RunBVP,0,opt,ps);
```

$$k_L = \frac{\mathcal{D}}{\delta} \quad (\text{mass transfer coefficient})$$

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*dyo*



$$\mathbf{y}_{i+1} = \mathbf{y}_i + h\mathbf{k}_2 \quad \text{using} \quad \begin{aligned} \mathbf{k}_1 &= \mathbf{f}(x_i, \mathbf{y}_i) \\ \mathbf{k}_2 &= \mathbf{f}\left(x_i + \frac{h}{2}, \mathbf{y}_i + \frac{h}{2}\mathbf{k}_1\right) \end{aligned}$$

## Systems of ODEs: Explicit methods

## Classical fourth order Runge-Kutta method (RK4)

$$\mathbf{y}_{i+1} = \mathbf{y}_i + h \left( \frac{\mathbf{k}_1}{6} + \frac{1}{3} (\mathbf{k}_2 + \mathbf{k}_3) + \frac{\mathbf{k}_4}{6} \right)$$

$$\mathbf{k}_1 = \mathbf{f}(x_j, \mathbf{y}_j)$$

$$\mathbf{k}_2 = \mathbf{f}(x_i + \frac{h}{2}, \mathbf{y}_i + \frac{h}{2}\mathbf{k}_1)$$

using

$$\mathbf{k}_3 = \mathbf{f}(x_i + \frac{h}{2}, \mathbf{y}_i + \frac{h}{2}\mathbf{k}_2)$$

$$\mathbf{k}_4 = \mathbf{f}(x_i + h, \mathbf{y}_i + h\mathbf{k}_3)$$

## Systems of ODEs: Implicit methods

## Backward Euler method

$$\mathbf{y}_{i+1} = \mathbf{y}_i + h \left( 1 - h \left. \frac{d\mathbf{f}}{d\mathbf{y}} \right|_i \right)^{-1} \mathbf{f}(\mathbf{y}_i)$$

## Implicit midpoint method

$$\mathbf{y}_{i+1} = \mathbf{y}_i + h \left( 1 - \frac{h}{2} \frac{d\mathbf{f}}{d\mathbf{y}} \Big|_i \right)^{-1} \mathbf{f}(\mathbf{y}_i)$$





For the explicit method we require  $\Delta t < 10^{-3}$  despite the fact that the term is completely negligible, but essential to keep stability.

The “disease” of stiff equations: we need to follow the solution on the shortest length scale to maintain stability of the integration, although accuracy requirements would allow a much larger time step.

$$\Rightarrow \begin{aligned} c_{1,i+1} &= (1 + 998\Delta t) c_{1,i} + 1998\Delta t c_{2,i} \\ c_{2,i+1} &= -999\Delta t c_{1,i} + (1 - 1999\Delta t) c_{2,i} \end{aligned}$$

## Demonstration with example

## Backward Euler (implicit)

$$\frac{dc_{1,i+1} - c_{1,i+1}}{dt} = 998c_{1,i+1} + 1998c_{2,i+1}$$

$$\frac{dc_{2,i+1} - c_{2,i+1}}{dt} = -999c_{1,i+1} - 1999c_{2,i+1}$$

$$\Rightarrow \begin{aligned} (1 - 998\Delta t) c_{1,i+1} - 1998\Delta t c_{2,i} &= c_{1,i} \\ 999\Delta t c_{1,i+1} + (1 + 999\Delta t) c_{2,i+1} &= c_{2,i} \end{aligned}$$





## Demonstration with example

Backward Euler (implicit)  $A\mathbf{c}_{i+1} = \mathbf{c}_i$  with

$$A = \begin{pmatrix} 1 - 998\Delta t & -1998\Delta t \\ 999\Delta t & 1 + 1999\Delta t \end{pmatrix} \quad \text{and} \quad \mathbf{b} = \begin{pmatrix} c_{1,i} \\ c_{2,i} \end{pmatrix}$$

Cramers rule:

$$c_{1,i+1} = \frac{\begin{vmatrix} c_{1,i} & -1998\Delta t \\ c_{2,i} & 1 + 1999\Delta t \end{vmatrix}}{\det(A)} = \frac{(1+1999\Delta t)c_{1,i} + 1998\Delta t c_{2,i}}{(1-998\Delta t)(1+1999\Delta t) + 1998 \cdot 999\Delta t^2}$$

$$c_{2,i+1} = \frac{\begin{vmatrix} 1 - 998\Delta t & c_{1,i} \\ 999\Delta t & c_{2,i} \end{vmatrix}}{\det(A)} = \frac{-999\Delta t c_{1,i} + (1-998\Delta t)c_{2,i}}{(1-998\Delta t)(1+1999\Delta t) + 1998 \cdot 999\Delta t^2}$$

Forward Euler:  $\Delta t \leq 0.001$  for stability

Backward Euler: always stable, even for  $\Delta t > 100$  (but then not very accurate!)



Cure for stiff problems: use implicit methods! To find out whether your system is stiff: check whether one of the eigenvalues have an imaginary part

- 1 Create a function that specifies the ODEs. Specifically, this function returns the  $\frac{dy}{dx}$  vector.
- 2 Initialise solver variables and settings (e.g. step size, initial conditions, tolerance), in a separate script
- 3 Call the ODE solver function, using a *function handle* to the ODE function described in point 1.
  - The ODE solver will return the vector for the independent variable, and a solution vector (matrix for systems of ODEs).

```
function [dxdt] = myODEFunction(t,x)
dxdt(1) = -x(1) - x(2);
dxdt(2) = x(1) - 2*x(2);
dxdt=dxdt'; % Transpose to column vector
return
```

## Solving systems of ODEs in Matlab: example

We solve the system:  $\frac{dx_1}{dt} = -x_1 - x_2, \quad \frac{dx_2}{dt} = x_1 - 2x_2$

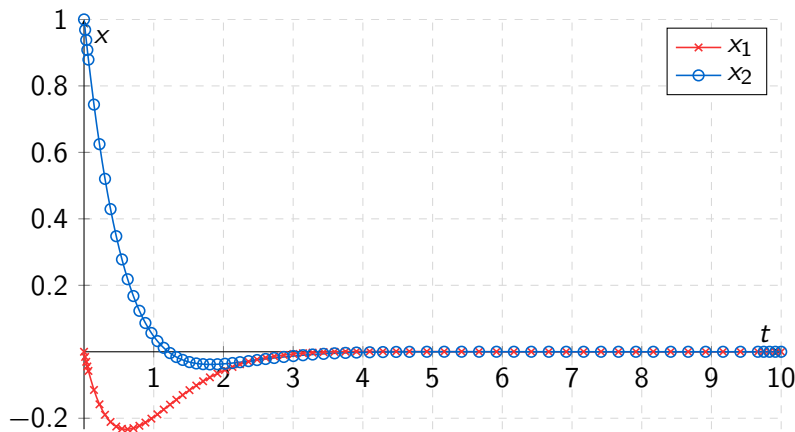
## Create an ODE function

```
function [dxdt] = myODEFunction(t,x)
dxdt(1) = -x(1) - x(2);
dxdt(2) = x(1) - 2*x(2);
dxdt=dxdt'; % Transpose to column vector
return
```

## Create a solution script

```
x_init = [0 1];           % Initial conditions
tspan = [0 10];          % Time span
options = odeset('RelTol',1e-4,'AbsTol',[1e-4 1e-4]);
[t,x] = ode45(@myODEfunction,tspan,x_init,options);
```

```
plot(t,x(:,1),'r-x',t,x(:,2),'b-o')
```



```
[t,x] = ode45(@myODE,tspan,x_0,options,a,b,c);
```

## Solving systems of ODEs in Matlab: example

A few notes on working with `ode45` and other solvers. If we want to give additional arguments (e.g. `a`, `b` and `c`) to our ODE function, we can list them in the function line:

```
function [dxdt] = myODE(t,x,a,b,c)
```

The additional arguments can now be set in the solver script by *adding them after the options*:

```
[t,x] = ode45(@myODE,tspan,x_0,options,a,b,c);
```

- Of course, in the solver script, the variables do not need to be called `a`, `b` and `c`:

```
[t,x] = ode45(@myODE,tspan,x_0,options,k1,phi,V);
```

- These variables may be of any type (vectors, matrix, struct). Especially a struct is useful to carry many values in 1 variable.



```
tspan = [0 10];
```

Note that you may affect the efficiency and accuracy of the solver algorithm by doing this!

# Today's outline

## ① Introduction

## ② Explicit methods

Forward Euler

Convergence rate

Runge-Kutta methods

Step size control

## ③ Implicit methods

Backward Euler

Implicit midpoint method

## ④ Boundary value problems

Shooting method

## ⑤ Systems of ODEs

Solution methods for systems of ODEs

Stiff systems of ODEs

Solving systems of ODEs in Matlab

## ⑥ Conclusion



- Several solution methods and their derivation were discussed:
  - Explicit solution methods: Euler, Improved Euler, Midpoint method, RK45
  - Implicit methods: Implicit Euler and Implicit midpoint method
  - A few examples of their spreadsheet implementation were shown
- We have paid attention to accuracy and instability, rate of convergence and step size
- Systems of ODEs can be solved by the same algorithms. Stiff problems should be treated with care.
- An example of solving ODEs with Matlab was demonstrated.