### Ordinary differential equations 2

Implicit methods, systems of ODEs and boundary value problems

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# Today's outline

- Introduction
  - Backward Euler
  - Implicit midpoint method
- Systems of ODEs
  - Solution methods for systems of ODEs
  - Solving systems of ODEs in Python
  - Stiff systems of ODEs
- Boundary value problems
  - Shooting method
- Conclusion



#### Introduction

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## Problems with Euler's method: instability

Consider the ODE:

$$\frac{dy}{dx} = f(x, y(x)) \quad \text{with} \quad y(x = 0) = y_0$$



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First order approximation of derivative:  $\frac{dy}{dx} = \frac{y_{i+1} - y_i}{\lambda x}$ .

Where to evaluate the function *f*?



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First order approximation of derivative:  $\frac{dy}{dx} = \frac{y_{j+1} - y_j}{\Delta x}$ .

Where to evaluate the function *f*?

- 1 Evaluation at x<sub>i</sub>: Explicit Euler method (forward Euler)
- 2 Evaluation at  $x_{i+1}$ : Implicit Euler method (backward Euler)



## Problems with Euler's method: instability – forward Euler

Explicit Euler method (forward Euler):

- Use values at x<sub>i</sub>:  $\frac{y_{i+1}-y_i}{\Delta_{\times}}=f(x_i,y_i)\Longrightarrow y_{i+1}=y_i+hf(x_i,y_i).$
- This is an explicit equation for  $y_{i+1}$  in terms of  $y_i$ .
- It can give instabilities with large function values.



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Consider the first order batch reactor:

$$\frac{dc}{dt} = -kc \Rightarrow c_{i+1} = c_i - k\frac{c_i}{\Delta t} \Rightarrow \frac{c_{i+1}}{c_i} = 1 - k\Delta t$$



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It follows that unphysical results are obtained for  $k\Delta t \ge 1!!$ 

#### Stability requirement

 $k\Lambda t < 1$ 

(but probably accuracy requirements are more stringent here!)



#### Implicit Euler method (backward Euler):

- Use values at  $x_{i+1}$ :  $\frac{y_{i+1}-y_i}{\Delta v} = f(x_{i+1},y_{i+1}) \Rightarrow y_{i+1} = y_i + hf(x_{i+1},y_{i+1})$ .
- This is an implicit equation for  $y_{i+1}$ , because it also depends on terms of  $y_{i+1}$ .



Implicit Euler method (backward Euler):

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Consider the first order batch reactor:

$$\frac{dc}{dt} = -kc \Rightarrow c_{i+1} = c_i - kc_{i+1} \Delta t \Rightarrow \frac{c_{i+1}}{c_i} = \frac{1}{1 + k\Delta t}$$



### Problems with Euler's method: instability – backward Euler

Implicit Euler method (backward Euler):

- Use values at  $x_{i+1}$ :  $\frac{y_{i+1}-y_i}{A} = f(x_{i+1}, y_{i+1}) \Rightarrow y_{i+1} = y_i + hf(x_{i+1}, y_{i+1})$ .
- This is an implicit equation for  $y_{i+1}$ , because it also depends on terms of  $y_{i+1}$ .

Consider the first order batch reactor:

$$\frac{dc}{dt} = -kc \Rightarrow c_{i+1} = c_i - kc_{i+1} \Delta t \Rightarrow \frac{c_{i+1}}{c_i} = \frac{1}{1 + k\Delta t}$$

This equation does never give unphysical results! The implicit Euler method is unconditionally stable (but maybe not very accurate or efficient).



### Semi-implicit Euler method

Usually f is a non-linear function of y, so that linearization is required (recall Newton's method).

$$\frac{dy}{dx} = f(y) \Rightarrow y_{i+1} = y_i + hf(y_{i+1}) \quad \text{using} \quad f(y_{i+1}) = f(y_i) + \left. \frac{df}{dy} \right|_i (y_{i+1} - y_i) + \dots$$

$$\Rightarrow y_{i+1} = y_i + h \left[ f(y_i) + \left. \frac{df}{dy} \right|_i (y_{i+1} - y_i) \right]$$

$$\Rightarrow \left( 1 - h \left. \frac{df}{dy} \right|_i \right) y_{i+1} = \left( 1 - h \left. \frac{df}{dy} \right|_i \right) y_i + hf(y_i)$$

$$\Rightarrow y_{i+1} = y_i + h \left( 1 - h \frac{df}{dy} \Big|_i \right)^{-1} f(y_i)$$



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For the case that f(x,y(x)) we could add the variable x as an additional variable  $y_{n+1} = x$ . Or add one fully implicit Euler step (which avoids the computation of  $\frac{\partial f}{\partial x}$ ):

$$y_{i+1} = y_i + hf(x_{i+1}, y_{i+1}) \Rightarrow y_{i+1} = y_i + h\left(1 - h\left|\frac{df}{dy}\right|_i\right)^{-1} f(x_{i+1}, y_i)$$



### Implicit Euler's method - implementation

A basic function of the implicit Euler method is given in ode\_scalar\_implicit.py:

```
def implicit_euler(func, c0, t0, tend, n):
     h = 1e-8
     dt = (tend - t0)/n
     times = np.linspace(t0,tend,n+1)
     c = np.zeros(n+1)
     c[0] = c0
     for i,t in enumerate(times[:-1]):
        f = func(c[i],t)
        fh = func(c[i]+h,t)
        dfdc = (fh - f)/h
        c[i+1] = c[i] + dt*f/(1 - dt*dfdc)
        print(f"{t=:0.4f}, c: {c[i+1]:.8f}")
     print(f"t={times[-1]:0.4f}, c: {c[-1]:.8f}")
     return times, c
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```



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```
from ode_scalar_implcit import implicit_euler
t,c = implicit_euler(lambda c,t: -1.0*c**2, 1, 0, 2,
      10)
plt.plot(t.c.'-o'.label='Implicit Euler')
 print(f"Conversion = {conv_e}")
```

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```

```
t=0.0000. c: 0.85714286
t=0.2000, c: 0.74772036
t=0.4000, c: 0.66164680
t=0.6000. c: 0.59241445
t=0.8000, c: 0.53566997
t=1.0000. c: 0.48840819
t=1.2000, c: 0.44849689
t=1.4000, c: 0.41438638
t=1.6000, c: 0.38492630
t=1.8000, c: 0.35924657
t=2.0000. c: 0.35924657
Conversion = 0.64075343
```

# Semi-implicit Euler method - example

Second order reaction in a batch reactor:

$$\frac{dc}{dt} = -kc^2$$
 with  $c_0 = 1 \text{ mol m}^{-3}$ ,  $k = 1 \text{ m}^3 \text{ mol}^{-1} \text{ s}^{-1}$ ,  $t_{\text{end}} = 2 \text{ s}$ 

Analytical solution:  $c(t) = \frac{c_0}{1 + kc_0 t}$ 



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Analytical solution:  $c(t) = \frac{c_0}{1+kc_0t}$ 

$$1+\kappa c_0 t$$

Define 
$$f = -kc^2$$
, then  $\frac{df}{dc} = -2kc \Rightarrow c_{i+1} = c_i - \frac{hkc_i^2}{1+2hkc_i}$ .



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N	ζ	$rac{\zeta_{ m numerical} - \zeta_{ m analytical}}{\zeta_{ m analytical}}$	$r = \frac{\log\left(\frac{\epsilon_i}{\epsilon_{i-1}}\right)}{\log\left(\frac{N_{i-1}}{N_i}\right)}$
20	0.654066262	1.89 × 10 <sup>-2</sup>	_
40	0.660462687	9.31 × 10 <sup>-3</sup>	1.02220
80	0.663589561	$4.62 \times 10^{-3}$	1.01162
160	0.665134433	$2.30 \times 10^{-3}$	1.00594
320	0.665902142	$1.15 \times 10^{-3}$	1.00300



## Second order implicit method: Implicit midpoint method

Implicit midpoint rule	Explicit midpoint rule (modified Euler method)	
(second order)		
$y_{i+1} = y_i + hf\left(x_i + \frac{1}{2}h, \frac{1}{2}(y_i + y_{i+1})\right)$	$y_{i+1} = y_i + hf(x_i + \frac{1}{2}h, y_i + \frac{1}{2}hk_1)$	

in case f(y) then:

$$f\left(\frac{1}{2}(y_i + y_{i+1})\right) = f_i + \frac{df}{dy}\Big|_i \left(\frac{1}{2}(y_i + y_{i+1}) - y_i\right) = f_i + \frac{1}{2} \frac{df}{dy}\Big|_i (y_{i+1} - y_i)$$



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in case f(y) then:

$$f\left(\frac{1}{2}(y_i+y_{i+1})\right) = f_i + \left. \frac{df}{dy} \right|_i \left(\frac{1}{2}(y_i+y_{i+1}) - y_i\right) = f_i + \frac{1}{2} \left. \frac{df}{dy} \right|_i (y_{i+1} - y_i)$$

Implicit midpoint rule reduces to:

$$y_{i+1} = y_i + hf_i + \frac{h}{2} \frac{df}{dy} \Big|_i (y_{i+1} - y_i)$$

$$\Rightarrow \left( 1 - \frac{h}{2} \frac{df}{dy} \Big|_i \right) y_{i+1} = \left( 1 - \frac{h}{2} \frac{df}{dy} \Big|_i \right) y_i + hf_i$$

$$\Rightarrow y_{i+1} = y_i + h \left(1 - \frac{h}{2} \frac{df}{dy} \Big|_{i}\right)^{-1} f_i$$

Second order reaction in a batch reactor:

$$\frac{dc}{dt} = -kc^2$$
 with  $c_0 = 1 \text{ mol m}^{-3}$ ,  $k = 1 \text{ m}^3 \text{ mol}^{-1}$  s<sup>-1</sup>,  $t_{\text{end}} = 2 \text{ s}$  (Analytical solution:  $c(t) = \frac{c_0}{1 + kc_0 t}$ ).



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Define  $f = -kc^2$ , then  $\frac{df}{dc} = -2kc$ .

Substitution:

$$c_{i+1} = c_i + h \left( 1 - \frac{h}{2} \cdot (-2kc_i) \right)^{-1} \cdot (-kc_i^2)$$

$$= c_i - \frac{hkc_i^2}{1 + hkc_i} = \frac{c_i + hkc_i^2 - hkc_i^2}{1 + hkc_i} \Rightarrow c_{i+1} = \frac{c_i}{1 + hkc_i}$$



Second order reaction in a batch reactor:

$$\frac{dc}{dt} = -kc^2$$
 with  $c_0 = 1$  mol m<sup>-3</sup>,  $k = 1$  m<sup>3</sup> mol<sup>-1</sup> s<sup>-1</sup>,  $t_{end} = 2$  s (Analytical solution:  $c(t) = \frac{c_0}{1+kc_0t}$ ).

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Substitution:

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You will find that this method is exact for all step sizes h because of the quadratic source term!



Second order reaction in a batch reactor:

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Analytical solution: 
$$c(t) = \frac{c_0}{1+kc_0t}$$

$$c_{i+1} = \frac{c_i}{1 + hkc_i}$$



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N	ζ	$\frac{\zeta_{ ext{numerical}} - \zeta_{ ext{analytical}}}{\zeta_{ ext{analytical}}}$	$r = \frac{\log\left(\frac{\epsilon_i}{\epsilon_{i-1}}\right)}{\log\left(\frac{N_{i-1}}{N_i}\right)}$
20	0.6666666667	1.665 × 10 <sup>-16</sup>	_
40	0.6666666667	0	_
80	0.6666666667	0	_
160	0.6666666667	0	_
320	0.6666666667	0	_



Third order reaction in a batch reactor:  $\frac{dc}{dt} = -kc^3$ 

Analytical solution: 
$$c(t) = \frac{c_0}{\sqrt{1+2kc_0^2t}}$$

$$c_{i+1} = c_i - \frac{hkc_i^3}{1 + \frac{3}{2}hkc_i^2}$$



Third order reaction in a batch reactor:  $\frac{dc}{dt} = -kc^3$ 

Analytical solution: 
$$c(t) = \frac{c_0}{\sqrt{1+2kc_0^2t}}$$

$$c_{i+1} = c_i - \frac{hkc_i^3}{1 + \frac{3}{2}hkc_i^2}$$

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20	0.5526916174	1.71 × 10 <sup>-4</sup>	_
40	0.5527633731	$4.17 \times 10^{-5}$	2.041
80	0.5527807304	$1.03 \times 10^{-5}$	2.021
160	0.5527849965	$2.55 \times 10^{-6}$	2.011
320	0.5527860538	$6.34 \times 10^{-7}$	2.005



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### Systems of ODEs

A system of ODEs is specified using vector notation:

$$\frac{d\mathbf{y}}{dx} = \mathbf{f}(x, \mathbf{y}(x))$$

for

$$\frac{dy_1}{dx} = f_1(x, y_1(x), y_2(x)) \quad \text{or} \quad f_1(x, y_1, y_2)$$

$$\frac{dy_2}{dx} = f_2(x, y_1(x), y_2(x)) \quad \text{or} \quad f_2(x, y_1, y_2)$$



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$$\frac{dy_2}{dx} = f_2(x, y_1(x), y_2(x)) \quad \text{or} \quad f_2(x, y_1, y_2)$$

The solution techniques discussed before can also be used to solve systems of equations.



### Systems of ODEs: Explicit methods

#### Forward Euler method

$$\mathbf{y}_{i+1} = \mathbf{y}_i + h\mathbf{f}(x_i, \mathbf{y}_i)$$

#### Improved Euler method (classical RK2)

$$y_{i+1} = y_i + \frac{h}{2}(k_1 + k_2)$$
 using  $k_1 = f(x_i, y_i)$   
 $k_2 = f(x_i + h, y_i + hk_1)$ 

#### Modified Euler method (midpoint rule)

$$\mathbf{y}_{i+1} = \mathbf{y}_i + h\mathbf{k}_2$$
 using  $\mathbf{k}_1 = \mathbf{f}(x_i, \mathbf{y}_i)$   
 $\mathbf{k}_2 = \mathbf{f}(x_i + \frac{h}{2}, \mathbf{y}_i + \frac{h}{2}\mathbf{k}_1)$ 



# Systems of ODEs: Explicit methods

#### Classical fourth order Runge-Kutta method (RK4)

$$\mathbf{y}_{i+1} = \mathbf{y}_i + h \left( \frac{\mathbf{k}_1}{6} + \frac{1}{3} (\mathbf{k}_2 + \mathbf{k}_3) + \frac{\mathbf{k}_4}{6} \right)$$

$$\boldsymbol{k}_1 = \boldsymbol{f}(x_i, \boldsymbol{y}_i)$$

$$\boldsymbol{k}_2 = \boldsymbol{f}(x_i + \frac{h}{2}, \boldsymbol{y}_i + \frac{h}{2}\boldsymbol{k}_1)$$

using

$$\boldsymbol{k}_3 = \boldsymbol{f}(x_i + \frac{h}{2}, \boldsymbol{y}_i + \frac{h}{2}\boldsymbol{k}_2)$$

$$\boldsymbol{k_4} = \boldsymbol{f}(x_i + h, \boldsymbol{y}_i + h\boldsymbol{k}_3)$$



### Solving systems of ODEs in Python

Solving systems of ODEs in Python is completely analogous to solving a single ODE:

- **1** Create a function that specifies the ODEs. This function returns the  $\frac{dy}{dx}$  vector.
- Initialise solver variables and settings (e.g. step size, initial conditions, tolerance), in a separate script. Initial conditions and tolerances should be given per-equation, i.e. as a vector.
- 6 Call the ODE solver function, using a function argument to the ODE function described in point 1.
  - The ODE solver will return the vector for the independent variable (e.g. time), and a solution matrix, with a column as the solution for each equation in the system.



We solve the system  $\frac{dx_0}{dt} = ax_0 - x_1$ ,  $\frac{dx_1}{dt} = bx_1 + x_0$ , with a = -1 and b = -2:

Create an ODE function:

```
# Example scipy solve_ivp/Example scipy solve_ivp vector.py
def func(t, x, a, b):
    #output can be of list or np.array type:
    dxdt = np.zeros(2)
    dxdt[0] = a*x[0] - x[1]
    dxdt[1] = b*x[1] + x[0]
    return dxdt
```

Solve by calling solve\_ivp

```
from scipy.integrate import solve_ivp
x_init = [0.1]: % Initial conditions
stspan = [0,10]; % Time span
 sol = solve_ivp(func, tspan, x_init, args=(-1,-2), rtol=1e-12)
```



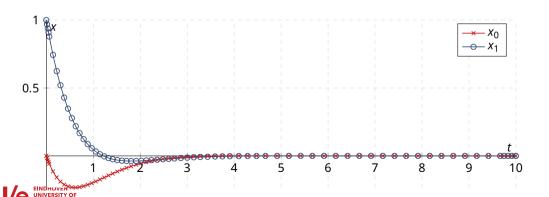
Plot the solution (note: the solution is attribute sol.v):

```
import matplotlib.pyplot as plt
plt.plot(sol.t, sol.y[0], 'r-x', linewidth=2)
plt.plot(sol.t, sol.v[1], 'b-o', linewidth=2)
```



Plot the solution (note: the solution is attribute sol.v):

```
import matplotlib.pyplot as plt
plt.plot(sol.t, sol.y[0], 'r-x', linewidth=2)
plt.plot(sol.t, sol.y[1], 'b-o', linewidth=2)
```



You may have noticed that the step size in *t* varies. This happens when only the begin and end times of the time span are defined, and <code>scipy.integrate.solve\_ivp</code> uses adaptive step size for efficiency:

tspan = [0, 10]



You may have noticed that the step size in t varies. This happens when only the begin and end times of the time span are defined, and scipy.integrate.solve\_ivp uses adaptive step size for efficiency:

```
tspan = [0, 10]
```

You can also retrieve the solution at specific steps, by supplying all steps explicitly as an additional argument to solve\_ivp, e.g.:

```
sol = solve_ivp(func, tspan, x_init, args=(-1,-2), t_eval=np.linspace(0, 10, 101), rtol=1e-12)
```

This example provides 101 explicit time steps between 0 and 10 seconds. It can be useful if you need a direct comparison with e.g. measurements at specific times.

Note that this is an interpolated result. The solver uses, in the background, still the adaptive step size functionality!



# Systems of ODEs: Implicit methods

#### Backward Euler method

$$\mathbf{y}_{i+1} = \mathbf{y}_i + h \left( \mathbf{I} - h \left. \frac{d\mathbf{f}}{d\mathbf{y}} \right|_i \right)^{-1} \mathbf{f}(\mathbf{y}_i)$$

#### Implicit midpoint method

$$\mathbf{y}_{i+1} = \mathbf{y}_i + h \left( \mathbf{I} - \frac{h}{2} \left. \frac{d\mathbf{f}}{d\mathbf{y}} \right|_i \right)^{-1} \mathbf{f}(\mathbf{y}_i)$$



A system of ODEs can be stiff and require a different solution method.



# Stiff systems of ODEs

A system of ODEs can be stiff and require a different solution method. For example:

$$\frac{dc_1}{dt} = 998c_1 + 1998c_2$$
  $\frac{dc_2}{dt} = -999c_1 - 1999c_2$ 

with boundary conditions  $c_1(t=0) = 1$  and  $c_2(t=0) = 0$ . The analytical solution is:

$$c_1 = 2e^{-t} - e^{-1000t}$$
  $c_2 = -e^{-t} + e^{-1000t}$ 

For the explicit method we require  $\Delta t < 10^{-3}$  despite the fact that the term is completely negligible, but essential to keep stability.



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$$c_1 = 2e^{-t} - e^{-1000t}$$
  $c_2 = -e^{-t} + e^{-1000t}$ 

For the explicit method we require  $\Delta t < 10^{-3}$  despite the fact that the term is completely negligible, but essential to keep stability.

> The "disease" of stiff equations: we need to follow the solution on the shortest length scale to maintain stability of the integration, although accuracy requirements would allow a much larger time step.



Forward Euler (explicit)

$$\begin{aligned} &\frac{c_{1,i+1} - c_{1,i}}{dt} = 998c_{1,i} + 1998c_{2,i} \\ &\frac{c_{2,i+1} - c_{2,i}}{dt} = -999c_{1,i} - 1999c_{2,i} \\ &\Rightarrow c_{1,i+1} = (1 + 998\Delta t)c_{1,i} + 1998\Delta tc_{2,i} \\ &c_{2,i+1} = -999\Delta tc_{1,i} + (1 - 1999\Delta t)c_{2,i} \end{aligned}$$



Backward Euler (implicit)

$$\begin{split} &\frac{c_{1,i+1}-c_{1,i}}{\Delta t} = 998c_{1,i+1} + 1998c_{2,i+1} \\ &\frac{c_{2,i+1}-c_{2,i}}{\Delta t} = -999c_{1,i+1} - 1999c_{2,i+1} \\ &\Rightarrow \frac{(1-998\Delta t)c_{1,i+1} - 1998\Delta tc_{2,i} = c_{1,i}}{999\Delta tc_{1,i+1} + (1+999\Delta t)c_{2,i+1} = c_{2,i}} \end{split}$$



Backward Euler (implicit)

$$\frac{c_{1,i+1} - c_{1,i}}{\Delta t} = 998c_{1,i+1} + 1998c_{2,i+1}$$

$$\frac{c_{2,i+1} - c_{2,i}}{\Delta t} = -999c_{1,i+1} - 1999c_{2,i+1}$$

$$\Rightarrow \frac{(1 - 998\Delta t)c_{1,i+1} - 1998\Delta tc_{2,i} = c_{1,i}}{999\Delta tc_{1,i+1} + (1 + 999\Delta t)c_{2,i+1} = c_{2,i}}$$

$$Ac_{i+1} = c_i \text{ with } A = \begin{pmatrix} 1 - 998\Delta t & -1998\Delta t \\ 999\Delta t & 1 + 1999\Delta t \end{pmatrix} \text{ and } b = \begin{pmatrix} c_{1,i} \\ c_{2,i} \end{pmatrix}$$



Backward Euler (implicit) 
$$A\mathbf{c}_{i+1} = \mathbf{c}_i$$
 with  $A = \begin{pmatrix} 1 - 998\Delta t & -1998\Delta t \\ 999\Delta t & 1 + 1999\Delta t \end{pmatrix}$  and  $\mathbf{b} = \begin{pmatrix} c_{1,i} \\ c_{2,i} \end{pmatrix}$ 



Backward Euler (implicit) 
$$A\mathbf{c}_{i+1} = \mathbf{c}_i$$
 with  $A = \begin{pmatrix} 1 - 998\Delta t & -1998\Delta t \\ 999\Delta t & 1 + 1999\Delta t \end{pmatrix}$  and  $\mathbf{b} = \begin{pmatrix} c_{1,i} \\ c_{2,i} \end{pmatrix}$ 

Cramers rule:

$$c_{1,i+1} = \frac{\begin{vmatrix} c_{1,i} & -1998\Delta t \\ c_{2,i} & 1+1999\Delta t \end{vmatrix}}{\det |A|} = \frac{\frac{(1+1999\Delta t)c_{1,i}+1998\Delta tc_{2,i}}{(1-998\Delta t)(1+1999\Delta t)+1998\cdot999\Delta t^2}}{c_{2,i+1}} = \frac{\begin{vmatrix} 1-998\Delta t & c_{1,i} \\ 999\Delta t & c_{2,i} \end{vmatrix}}{\det |A|} = \frac{\frac{-999\Delta tc_{1,i}+(1-998\Delta t)c_{2,i}}{(1-998\Delta t)(1+1999\Delta t)+1998\cdot999\Delta t^2}}{\frac{-999\Delta tc_{1,i}+(1-998\Delta t)c_{2,i}}{(1-998\Delta t)(1+1999\Delta t)+1998\cdot999\Delta t^2}}$$

Forward Euler:  $\Delta t \leq 0.001$  for stability

Backward Euler: always stable, even for  $\Delta t > 100$  (but then not very accurate!)



Cure for stiff problems: use implicit methods! To find out whether your system is stiff: check whether one of the eigenvalues have an imaginary part



### Implicit methods in Python

SciPy offers a solver that detects stiff systems, using method='LSODA'.

$$\frac{dc_1}{dt} = 998c_1 + 1998c_2 \quad \frac{dc_2}{dt} = -999c_1 - 1999c_2, c_1(0) = 1, c_2(0) = 0$$

Create the ode function (see slide\_example\_solve\_ivp\_implicit.py)

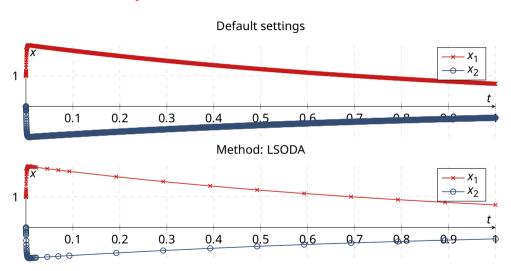
```
function [dcdt] = stiff_ode(t,c)
dcdt = zeros(2,1); % Pre-allocation
dcdt(1) = 998 * c(1) + 1998*c(2):
 dcdt(2) = -999 * c(1) - 1999*c(2);
5 return
```

Compare the resolution of the solutions (see next slide)

```
sol1 = solve_ivp(stiff_ode, [0, 1], [1, 0])
2 # plot sol1
sol2 = solve_ivp(stiff_ode, [0, 1], [1, 0], method = 'LSODA')
 # plot sol2
```



### Implicit methods in Python



The explicit solver requires 1245 data points (default settings), the implicit solver just 48!

```
def euler_implicit(func, c0, t0, tend, n):
    dt = (tend - t0)/n
    t = np.linspace(t0, tend, num=n+1, endpoint=True)
    c0 = np.asarray(c0, dtype=float)
    c = np.zeros((n+1, c0.size))
    c[0] = c0
    print(f"t: {t[0]:f}, c: {np.array2string(c[0])}")
    for i in range(n):
        f = func(c[i])
        ddc = jac(func, c[i])
        dc = np.linalg.solve(np.eye(c0.size) - dt*dfdc, dt*f)
        c[i+1] = c[i] + dc
        print(f"t: {t[i+1]:f}, c: {np.array2string(c[i+1])}")
    return c, t
```

```
def jac(func, c):
    n = c.size
    jac = np.eye(n)
    h = 1e-8
    f = func(c)
    for i in range(n):
        cs = c[i]
        c[i] = c[i] + h
        fh = func(c)
        jac[:,i] = (fh - f)/h
        c[i] = cs
    return jac
```

Vector output needs a bit of processing:

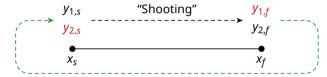
```
c, t = euler_implicit(func, [1, 0, 0], 0, 2, 100)
c = c.T
fig = plt.figure()
plt.plot(t, c[0], 'ro-', label='A')
plt.plot(t, c[1], 'bs-', label='B')
6 plt.plot(t, c[2], 'g^-', label='C')
plt.show()
```

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  - Backward Fule
  - Implicit midpoint method
- Systems of ODEs
  - Solution methods for systems of ODEs
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- Boundary value problems
  - Shooting method
- Conclusion



How to solve a BVP using the shooting method:



- Define the system of ODEs
- Provide an initial guess for the unknown boundary condition
- Solve the system and compare the resulting boundary condition to the expected value
- Adjust the guessed boundary value, and solve again. Repeat until convergence.
  - Of course, you can subtract the expected value from the computed value at the boundary, and use a non-linear root finding method



Boundary value problems 000000000

#### BVP: example in Excel

Consider a chemical reaction in a liquid film layer of thickness  $\delta$ :

$$\mathcal{D}\frac{d^2c}{dx^2} = k_R c \text{ with } c(x=0) = C_{A,i,L} = 1$$
 (interface concentration)  
 
$$c(x=\delta) = 0$$
 (bulk concentration)

Question: compute the concentration profile in the film layer.



Consider a chemical reaction in a liquid film layer of thickness  $\delta$ :

$$\mathcal{D}\frac{d^2c}{dx^2} = k_R c \text{ with}$$
 
$$c(x = 0) = C_{A,i,L} = 1$$
 
$$c(x = \delta) = 0$$

$$c(x=0)=C_{A,i,L}=1$$

(interface concentration)

$$c(x = \delta) = 0$$

(bulk concentration)

Boundary value problems 000000000

Question: compute the concentration profile in the film layer.

#### Step 1: Define the system of ODEs

This second-order ODE can be rewritten as a system of first-order ODEs, if we define the flux q as:

$$q = -\mathcal{D}\frac{dc}{dx}$$

Now, we find:

$$\frac{dc}{dx} = -\frac{1}{\mathcal{D}}q$$

$$\frac{dq}{dx} = -k_R c$$



Consider a chemical reaction in a liquid film layer of thickness  $\delta$ :

$$\mathcal{D}\frac{d^2c}{dx^2} = k_R c \text{ with } c(x=0) = C_{A,i,L} = 1$$

$$c(x=\delta) = 0$$

$$c(x=0)=C_{A,i,L}=1$$

$$f(x=\delta)=0$$

(interface concentration)

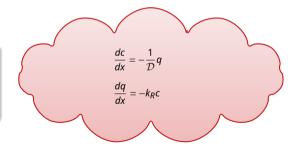
(bulk concentration)

Question: compute the concentration profile in the film layer.

#### Step 2: Set the boundary conditions

The boundary conditions for the concentrations at x = 0and  $x = \delta$  are known.

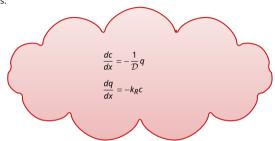
The flux at the interface, however, is not known, and should be solved for.





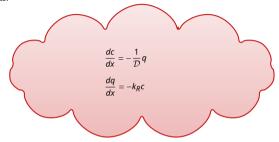
Solving the two first-order ODEs in Excel. First, the cells with constants:

	Α	В	С
1	CAiL	1	mol/m3
2	D	1e-8	m2/s
3	kR	10	1/s
4	delta	1e-4	m
5	N	100	
6	dx	=B4/B5	



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	Α	В	С
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3	kR	10	1/s
4	delta	1e-4	m
5	N	100	
6	dx	=B4/B5	



Now, we program the forward Euler (explicit) schemes for *c* and *q* below:

	Α	В	С
10	х	С	q
11	0	=B1	10
12	=A11+\$B\$6	=B11+\$B\$6*(-1/\$B\$2*C11)	=C11+\$B\$6*(-\$B\$3*B11)
13	=A12+\$B\$6	=B12+\$B\$6*(-1/\$B\$2*C12)	=C12+\$B\$6*(-\$B\$3*B12)
111	=A110+\$B\$6	=B110+\$B\$6*(-1/\$B\$2*C110)	=C110+\$B\$6*(-\$B\$3*B110)

- We now have profiles for c and q as a function of position x.
- The concentration  $c(x = \delta)$  depends (eventually) on the boundary condition at the interface q(x=0)
- We can use the solver to change q(x = 0) such that the concentration at the bulk meets our requirement:  $c(x = \delta) = 0$



We first program the system of ODEs in a separate function:

$$\frac{dc}{dx} = -\frac{1}{D}c_{R}$$

$$\frac{dq}{dx} = -k_{R}c$$

```
# slides_example_bvp_1.py

def diffReactSystem(x, y, param):
    c, q = y
    f = np.zeros_like(y)
    f[0] = -q/param['Diff']
    f[1] = -param['kR']*c
    return f
```



We first program the system of ODEs in a separate function:

$$\frac{dc}{dx} = -\frac{1}{D}q$$

$$\frac{dq}{dx} = -k_R c$$

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# slides_example_bvp_1.py

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    c, q = y
    f = np.zeros_like(y)
    f[0] = -q/param['Diff']
    f[1] = -param['kR']*c
    return f
```

Note that we pass a variable (type: dictionary) that contains required parameters: param.



Let's first try to solve the ODE system using scipy.integrate.solve\_ivp:

```
# slides_example_bvp_1.py
  import numpy as np
  import matplotlib.pyplot as plt
  from scipy.integrate import solve_ivp
  ### Definition of diffReactSystem here (see slide 449 )
  # Set up parameters
  q0 = 1e-3 # Initial guess flux@t=0
  param = {'cAiL': 1.0,'Diff':1e-8,'kR': 10,'delta': 1e-4,'N': 100}
  # Solve ODE system
  sol = solve_ivp(lambda x, y: diffReactSystem(x, y, param), # ODE func with params
                                [0, param['delta']], # Time span
14
                                [param['cAiL'], q0]) # Initial conditions
15
16
  fig.ax1 = plt.subplots()
  ax1.plot(sol.t,sol.y[0,:],'-b',label='Concentration $mol/m^3$')
  ax2 = ax1.twinx() # Create v-v axis
  ax2.plot(sol.t,sol.y[1,:],'-r',label='Flux $mol/m^2/s$')
fig.legend(bbox_to_anchor=(0.5, 0.5))
  plt.show()
```

That seems to work! Now we want to fit the value for q at x=0 (defined below as bcq), such that the concentration at  $x=\delta$  equals zero. We create a function with the output defined as the deviation from the target value:

```
# slides_example_bvp_2.py

def diffReactFitCriterium(bcq, param):
    # Solve the ODE system using changeable parameter bcq
    # (boundary condition for q), other parameters are defined in param
    sol = solve_ivp(lambda x, y: diffReactSystem(x, y, param), [0, param['delta']], [param['cAiL' ], bcq])

# Return the last value of the concentration (column 0 in y) at x=delta (hence [-1])

return sol.y[0,-1] - 0
```



That seems to work! Now we want to fit the value for q at x = 0 (defined below as bcq), such that the concentration at  $x = \delta$  equals zero. We create a function with the output defined as the deviation from the target value:

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# slides_example_bvp_2.py

def diffReactFitCriterium(bcq, param):
    # Solve the ODE system using changeable parameter bcq
    # (boundary condition for q), other parameters are defined in param
    sol = solve_ivp(lambda x, y: diffReactSystem(x, y, param), [0, param['delta']], [param['cAiL' ], bcq])

# Return the last value of the concentration (column 0 in y) at x=delta (hence [-1])

return sol.y[0,-1] - 0
```

#### Note the following:

- We use the interval  $0 < x < \delta$
- Boundary conditions are given as: c(x = 0) = 1 and q(x = 0) = bcq, which is given as a separate argument to the function (i.e. changable from 'outside'!)
- The function returns the concentration at  $x = \delta$



Finally, we should solve the system so that we obtain the right boundary condition q = bcq such that  $c(x = \delta) = 0$ . We can use the scipy.optimize.root\_scalar function to do this. Extend the script from slide 450 by:

Postprocessing of the data can be done similar to the example in slide 450.



# BVP example: analytical solution

#### Compare with the analytical solution:

$$q=k_L E_A C_{A,i,L}$$
 with  $E_A=rac{Ha}{ anh Ha}$  (Enhancement factor)  $Ha=rac{\sqrt{k_R \mathcal{D}}}{k_L}$  (Hatta number)  $k_L=rac{\mathcal{D}}{\delta}$  (mass transfer coefficient)



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#### Other methods

#### Other explicit methods:

Bulirsch-Stoer method (Richardson extrapolation + modified midpoint method)

#### Other implicit methods:

- Rosenbrock methods (higher order implicit Runge-Kutta methods)
- Predictor-corrector methods



#### Summary

- Several solution methods and their derivation were discussed:
  - Explicit solution methods: Euler, Improved Euler, Midpoint method, RK45
  - Implicit methods: Implicit Euler and Implicit midpoint method
  - A few examples of their spreadsheet implementation were shown
- We have paid attention to accuracy and instability, rate of convergence and step size
- Systems of ODEs can be solved by the same algorithms. Stiff problems should be treated with care.
- An example of solving ODEs with Python was demonstrated.

