Compressible Flows Xeno Meienberg

1 General Considerations

$$\frac{D\rho}{Dt} = \frac{\partial\rho}{\partial t} + u_i \frac{\partial\rho}{\partial x_i} \neq 0 \tag{1}$$

- · Wave propagation
- · Convective flows with buoancy
- Flows with variable temperature, friction, sources of heat
- High speed flows with Mach numbers Ma > 1

Compressible flows can still be described through the continuum model and conservation laws. The assumption is also that the thermodynamic state of the fluid is in a local equilibrium.

Assumptions

- Length scale of flows $\underline{\text{large}}$ compared to molecular scales (mean free path λ)
- Length scale of flows $\underline{\text{small}}$ compared to the geometric scales (length L)
- Time scale au_F of the flow $\underline{\mathrm{long}}$ compared to the molecular process (relaxation) time constants au_R

Description of the "Continuum" Flow State

- Three components of flow velocity u(x,t)
- The fluid density $\rho(\underline{x}, t)$
- The fluid pressure p(x,t)
- The energy $e(\underline{x}, t)$

The required equations are the conservation laws for mass, momentum and energy together with suitable thermodynamic equations of state. With corresponding initial and boundary conditions, the evolution can then be computed.

2 Thermodynamic Relations

State Variables

- Density: $\rho = \rho(p, T)$
- Pressure: $p = p(\rho, T)$
- Temperature: $T = T(\rho, p)$
- Internal energy: $e = e(\rho, T) [e] = J/kg$
- Enthalpy: h = h(p, T)
- Entropy: $s = s(\rho, T)$

Van der Waals Gas

$$(p+a\rho^2)\left(\frac{1}{\rho}-b\right) = RT \tag{2}$$

Incompressible Fluid

$$\rho = const. \neq \rho(p, T) \tag{3}$$

3 Conservation Laws for Continuum Flows

$$\frac{Dm}{Dt} = \frac{D}{Dt} \int_{\tilde{V}} \rho d\tilde{V} = 0 \ (material \ volume) \tag{4}$$

$$\int_{V} \frac{\partial \rho}{\partial t} dV + \int_{S} \rho(\mathbf{u} \cdot \mathbf{n}) dS = 0 \ (Eulerian \ Volume) \ \ \textbf{(5)}$$

$$\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x_i}(\rho u_i) = 0 \ (material \ volume \ / \ index)$$
 (6)

$$\frac{D\rho}{Dt} = -\rho \frac{\partial u_i}{\partial x_i} \left(Eulerian \ Volume / \ index \right) \tag{7}$$

Mass Conservation

Material Volume

$$\frac{Dm}{Dt} = \frac{D}{Dt} \int_{\vec{V}} \rho d\vec{V} = 0 \tag{8}$$

$$\frac{\partial \rho}{\partial t} + \frac{\partial \rho}{\partial x_i} (\rho u_i) = 0 \tag{9}$$

Eulerian Volume

$$\int_{V} \frac{\partial \rho}{\partial t} dV + \int_{S} \rho(\vec{u} \cdot \vec{n}) dS = 0$$
 (10)

$$\frac{D\rho}{Dt} = -\rho \frac{\partial u_i}{\partial x_i} \tag{11}$$

Momentum Conservation

$$\frac{\partial}{\partial t}(\rho u_i) + \frac{\partial}{\partial x_i}(\rho u_i u_j) = \frac{\partial}{\partial x_i}\sigma_{ij} + \rho f_i \tag{12}$$

$$\rho \frac{Du_i}{Dt} = \frac{\partial}{\partial x_i} \sigma_{ij} + \rho f_i \tag{13}$$

$$\sigma_{ij} = -p\delta_{ij} + \tau_{ij} \tag{14}$$

$$\tau_{ij} = \mu \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) + \left(\mu_v - \frac{2}{3} \mu \right) \delta_{ij} \frac{\partial u_k}{\partial x_k}$$
 (15)

$$\rho \frac{Du_i}{Dt} = -\frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_j} \left[\mu \left(\frac{\partial u_i}{x_j} + \frac{\partial u_j}{\partial x_i} \right) + \left(\mu_v - \frac{2}{3} \mu \right) \delta_{ij} \frac{\partial u_k}{\partial x_k} \right] + \rho f_i$$
(16)

Energy Conservation

$$\rho \frac{D}{Dt}(e + \frac{1}{2}u_1^2) = \frac{\partial}{\partial x_j}(\sigma_{ij}u_i) + \rho f_i u_i - \frac{\partial q_i}{\partial x_i} + \rho q_v \quad (17)$$

$$\rho \frac{D}{Dt}(e + \frac{1}{2}u_1^2) = -\frac{\partial}{\partial x_i}(pu_i) + \frac{\partial}{\partial x_j}(\tau_{ij}u_i) + \rho f_i u_i - \frac{\partial q_i}{\partial x_i} + \rho q_v$$
(18)

(6)
$$\rho u_{i} \frac{Du_{i}}{Dt} = \rho \frac{D}{Dt} \left(\frac{u_{i}^{2}}{2} \right) = -u_{i} \frac{\partial p}{\partial x_{i}} + u_{i} \frac{\partial}{\partial x_{j}} \tau_{ij} + \rho f_{i} u_{i} \rho \frac{De}{Dt} =$$

$$\rho \frac{D}{Dt} \left(e + \frac{1}{2} u_{i}^{2} \right) - \rho \frac{D}{Dt} \left(\frac{u_{i}^{2}}{2} \right) =$$

$$= -p \frac{\partial u_{i}}{\partial x_{i}} + \tau_{ij} \frac{\partial u_{i}}{\partial x_{j}} + \rho q_{v} - \frac{\partial q_{i}}{\partial x_{i}}$$

$$(7)$$

Dissipation Function Φ

Insert $h=e+rac{p}{
ho}$ to obtain Enthalpy equation, introduce $h_t=h+rac{u_i^2}{2}$ and add kinetic energy (p. 15). For perfect gasses, $h=c_pT$, $q_i=-krac{dT}{dx}$, derive the temperature equation.

Entropy Equation

$$\rho T \frac{Ds}{Dt} = \Phi + \rho q_v - \frac{\partial q_i}{\partial x_i} \tag{19}$$

Vorticity Equation

$$\rho \frac{D}{Dt} \left(\frac{\vec{\omega}}{\rho} \right) = (\vec{\omega} \cdot \nabla) \vec{u} + \frac{1}{\rho^2} \nabla \rho \times \nabla p + \nabla \times \left(\frac{1}{\rho} \nabla \cdot \vec{\tau} \right)$$
 (20)

Crocco Theorem (rewritten momentum equation using Enthalpy and Entropy)

$$\frac{\partial u}{\partial t} + \nabla \left(\frac{1}{2} \vec{u}^2 + h + \psi \right) = \vec{u} \times \vec{\omega} + T \nabla s + \frac{1}{\rho} \nabla \cdot \vec{\tau} \quad (21)$$

Compressible Bernoulli

equation (integrate momentum equation law along particle path). Clasical not feasible

$$\rho\left(\frac{Dh_t}{Dt} - f_i u_i\right) = 0 \tag{22}$$

$$f_i = -\frac{\partial \psi}{\partial x_i} \tag{23}$$

$$\psi \neq \psi(t) \tag{24}$$

$$\frac{D}{Dt}\left(h_t + \psi\right) = 0\tag{25}$$

Between 2 points along stream line

$$h_t + \psi = e + \frac{p}{\rho} + \frac{u_i^2}{2} + \psi = const.$$
 (26)

4 Simplification Strategies

- Unsteady → steady (no wave propagation)
- $3D \rightarrow 2D \rightarrow quasi 1-D$
- Viscous, heat conduction \rightarrow inviscid, adiabatic (isentropic, homentropic)

5 Conservation Laws for Stream Tubes

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