



## **TRNSYS Type 861**

# Ice Storage Model with ice-on-heat exchangers

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#### **Abstract**

This TRNSYS Type simulates a ice storage with ice-on-coil, ice-on-plates and ice-on-capillary mat heat exchangers. This storage typer does not allow two types in the same deck and direct ports (wihout heat exchangers) are not implemented. This Type is compatible for TRNSYS 17 and 18





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#### 1. Introduction

The mathematical formulation of this model has been presented in Carbonell et al. (2018) for capillary mats and coils and in Carbonell et al. (2017) for flat plate heat exchangers.

### 2. Revison history

Date	Version	Changes
Oct 31, 2018	v1.0	First version released

#### 3. Notes

- The model does not allow to freeze completely one control volume of the storage tank. The
  energy balance is applied to the water of each control volume. Thus, if there is none or too
  little volume of water available, the model suffers from instability
- For stability of the complete system it is recommended to bypass the ice storage once completely iced
- The model has never been tested for other PCM, but probably with minor modifications it should work





## 4. List of parameters

Nr.	Description	Name	Units
1	unused		-
2	Storage Volume	V <sub>tes</sub>	m <sup>3</sup>
3	Storage height	H <sub>tes</sub>	m
4	Storage width	W <sub>tes</sub>	m
5	Storage geometry	S <sub>type</sub>	-
	0: box 1:cylinder (W <sub>tes</sub> not used)		
6	Distance between pipes if hx <sub>type</sub> = 1	x <sub>1</sub>	m
	Distance beween hx if hx <sub>type</sub> = 2		
7	Distance between hx if hx <sub>type</sub> = 1	x <sub>2</sub>	-
8	Effective thermal conductivity of store	k <sub>wat</sub>	W/(mK)
9	Density of storage fluid (water)	$ ho_{wat}$	kg/m <sup>3</sup>
10	Specific heat storage fluid (water)	C <sub>p,wat</sub>	J/(kgK)
11	not used		
12	Thermal conductivity of ice	k <sub>ice</sub>	W/(mk)
13	Water↔ice enthalpy	$\Delta H_{ice}$	kJ/kg
14	Subcooling temp	T <sub>subcool</sub>	°C
15	Freezing temperature	T <sub>freeze</sub>	°C
16	Initial amount of ice in store	kg <sub>ice</sub>	kg
17	not used		
18	Maximum storage ice volume fraction	$V_{\sf ice,max}$	-
19	Parameter check control		
	1 : interrups simulation if parameters out of range		
20	unused		
21	hx height respect to the total ([0-1])	hx <sub>height</sub>	m
22	maximum ice floating ratio in layers were ice is pro- duced (only relevant when deicing is used)		
23	Use of $T_{\text{wall}}$ from previous time step (improves convergence)		m
24	Number fo used hx (only used for $hx_{type}=1$ (capillary mats)		
25	use constabnt physical properties in the water from the storage		
26	use corrugated configuration for flat plates (only used when $hx_{type}$ =2		

<sup>-</sup> continued on next page -





	Heat Exchanger i:		
27 + 19 (i-1)	Hx geometry	hx <sub>type</sub>	
	0=flat plates, 1=capilary mats,2=coils		
28 + 19(i-1)	Number of hx	N <sub>hx</sub>	
29 + 19(i-1)	hx <sub>type</sub> =0 inner tube diameter	d <sub>in,hx</sub>	
	hx <sub>type</sub> =1 height flat plate	H <sub>hx</sub>	
30 + 19(i-1)	hx <sub>type</sub> =0 outer tube diameter	d <sub>out,hx</sub>	
	hx <sub>type</sub> =1 width of flat plate	W <sub>hx</sub>	
31 + 19(i-1)	Lenght of hx	L <sub>hx</sub>	
32 + 19(i-1)	hx <sub>type</sub> =0 additional heat capacity hx		J/m <sup>3</sup>
	hx <sub>type</sub> =1 wall thickness flat plate	dx <sub>wall,hx</sub>	m
33+19(i-1)	Order of hx from 1 to 4. Used only if seriesMode is active		
34+19(i-1)	Hx thermal conductivity	$\lambda_{hx,i}$	W/(mK)
35+19(i-1)	Relative height of inlet on the hx	[0-1]	m
36+19(i-1)	Relative height of outlet on the hx	[0-1]	m
37+19(i-1)	Fluid thermal conductivity	$\lambda_{p,i}$	W/(mK)
38+19(i-1)	Fluid specific heat	C <sub>p,i</sub>	J/(kgK)
39+19(i-1)	Glycol concentration		%
40+19(i-1)	C Factor for Nusselt correlation (heating)	C <sub>hx,i</sub>	
41+19(i-1)	n Factor for Nusselt correlation (heating)	n <sub>hx,i</sub>	
42+19(i-1)	C Factor for Nusselt correlation (cooling)	C <sub>hx,i</sub>	
43+19(i-1)	n Factor for Nusselt correlation (cooling)	n <sub>hx,i</sub>	
44+19(i-1)	Enhanced Nusselt number for laminar flow $(Nu = Nu \cdot Nu_{en})$	Nu <sub>en</sub>	-
	End of Heat Exchanger		
104	U lower lateral side	U <sub>low,lat</sub>	W/(m <sup>2</sup> K)
105	U upper lateral side	U <sub>up,lat</sub>	W/(m <sup>2</sup> K)
106	U bottom side	U <sub>bot</sub>	W/(m <sup>2</sup> K)
107	U upper side	U <sub>top</sub>	W/(m <sup>2</sup> K)
108	$1^{th}$ sensor height position	<b>y</b> s1	m
109	$2^{th}$ sensor height position	y <sub>s2</sub>	m
110	$3^{th}$ sensor height position	<b>y</b> s3	m
111	$4^{th}$ sensor height position	y <sub>s4</sub>	m
112	$5^{th}$ sensor height position	y <sub>s5</sub>	m





## 5. List of inputs

Nr.	Description	Name	Units
1+3(i-1)	Inlet fluid temperature of the hx $\emph{i}$	T <sub>in,hx,i</sub>	°C
2+3(i-1)	Inlet mass flow rate of the hx $\it i$	$\dot{m}_{in,hx,i}$	kg/h
3+3(i-1)	Reverted temperature of the hx $\it i$	T <sub>rev,hx,i</sub>	°C
	Temperature used when $\dot{m}_{in,hx,i}i0$		
:	for i=1 i ≤4 i=i+1	:	:
13	0 : mechanical de-ice off ; 1 : on		
14+(n-1)	Surrounding temperature around the TES (for heat loss calculation)	T <sub>amb,n</sub>	°C
:	for n=1 n ≤nCv n=n+1	:	:
14+(nCv)	Surrounding temperature below TES (for heat loss calculation)		°C
14+(nCv+1)	Surrounding temperature above TES (for heat loss calculation)		°C

### 6. List of derivatives

The definition of derivatives is used to calculate the number of control volumes in the storage nCv

Nr.	Description	Name	Units
n	Initial storage temperature for each Cv n	T <sub>ini,n</sub>	°C
:	for n=1 n $\leq$ nCv n=n+1	:	:

## 7. List of outputs

Nr.	Description	Name	Units
1	Average temperature of the store	$\dot{T}_{s,av}$	°C
2	Total heat provided by the Hx to the storage tank	$\dot{Q}_{hx}$	W
3	Total heat accumulated of the storage tank	$\dot{Q}_{\sf acum}$	W
4	Total heat losses of the storage tank	$\dot{Q}_{loss}$	W
5	Total heat used to melt the ice in the storage tank	$\dot{Q}_{melt}$	W
6	Total heat used to form the ice	$\dot{Q}_{\sf ice}$	W





7	Total imbalance heat	$\dot{Q}_{imb}$	W
8	Mass of floating ice	$\dot{M}_{\sf ice,f}$	kg
9	Total ice thickness in the heat exchangers	ds <sub>ice</sub>	m
10	Total mass of ice (floating + hx,ice)	$\dot{M}_{\sf ice,T}$	kg
11	1: Upper part of the storage is full of ice (no ice can be released); 0: not full		
12 + 7(i-1)	Inlet temperature of heat exchanger $i$	$T_{in,hx,i}$	°C
13 + 7(i-1)	Outlet temperature of heat exchanger $i$	$T_{out,hx,i}$	°C
14 + 7(i-1)	Wall temperature of heat exchanger $i$	$T_{wall,hx,i}$	°C
15 + 7(i-1)	Power provided for all parallel heat exchangers $\emph{i}$	$\dot{Q}_{hx,i}$	W
16 + 7(i-1)	Ice thickness in the heat exchangers $\boldsymbol{i}$	ds <sub>form,i</sub>	m
17 + 7(i-1)	Ice melted in the heat exchangers $\emph{i}$	ds <sub>melt,i</sub>	m
18 + 7(i-1)	Total heat transfer coefficient for all parallel heat exchangers $\boldsymbol{i}$	UA <sub>hx,i</sub>	W/K
:	for i=1 i ≤4 i=i+1	:	:
40	1: Heat exchangers are full of ice (collapse of ice storage); 0: not full		
41 +(n-1)	Temperature of sensor n		°C
46 +(n-1)	Temperature of the storage for the Cv $\boldsymbol{n}$	$T_n$	°C
:	for n=1 n $\leq$ nCv n=n+1	:	:
56	Losses at the bottom	q <sub>loss,bottom</sub>	W
57 +(n-1)	Losses for the Cv $n$	q <sub>loss,n</sub>	W
<b>:</b>	for n=1 n $\leq$ nCv n=n+1	:	:
67	Losses at the top	q <sub>loss,top</sub>	W
68	Temperature of the storage at the bottom	$T_{bottom}$	°C
69	Temperature of the storage at the top	$T_top$	°C
70	Heat transfer coefficient at the bottom	U <sub>bottom</sub>	W/(m <sup>2</sup> K)
71	Average heat transfer coefficient at the side of the storage	U <sub>bottom</sub>	W/(m <sup>2</sup> K)
72	Heat transfer coefficient at the top	$U_{zop}$	W/(m <sup>2</sup> K)

i=1 to 4 which is the maximum number of heat exchangers





#### **References**

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