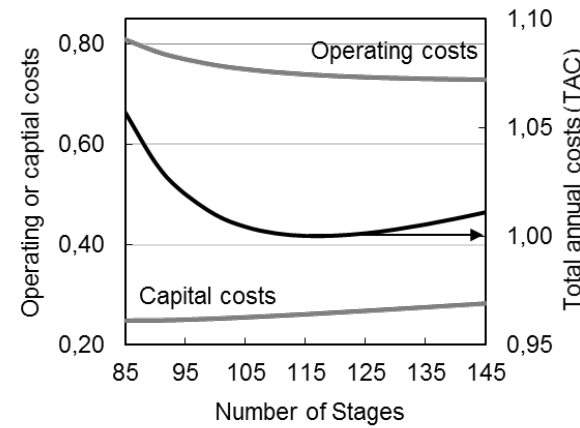
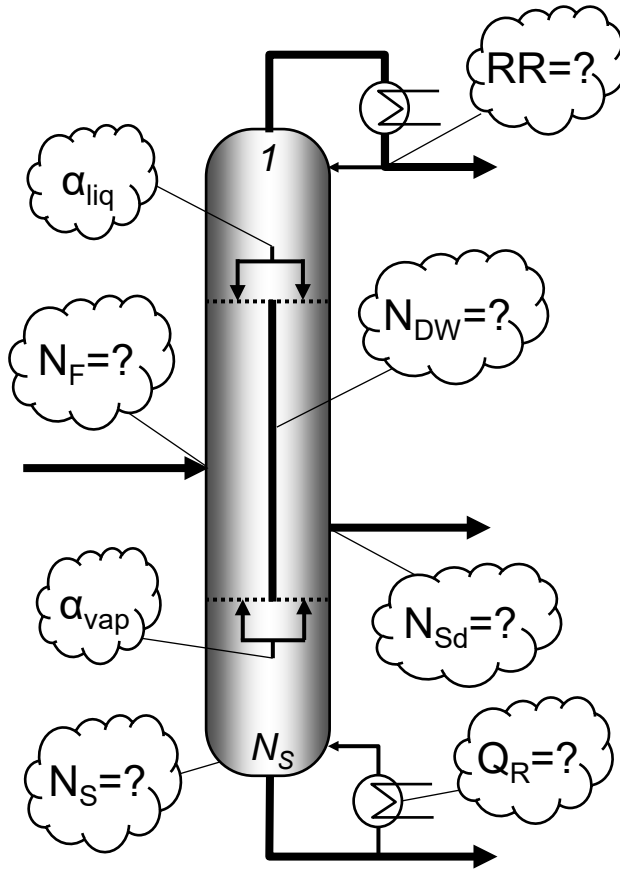


MINLP Optimization of Staged Separation Processes

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University of Twente, SPT Group, Chair of Process Design
and Optimization

For a DWC, many degrees of freedom must be fixed...

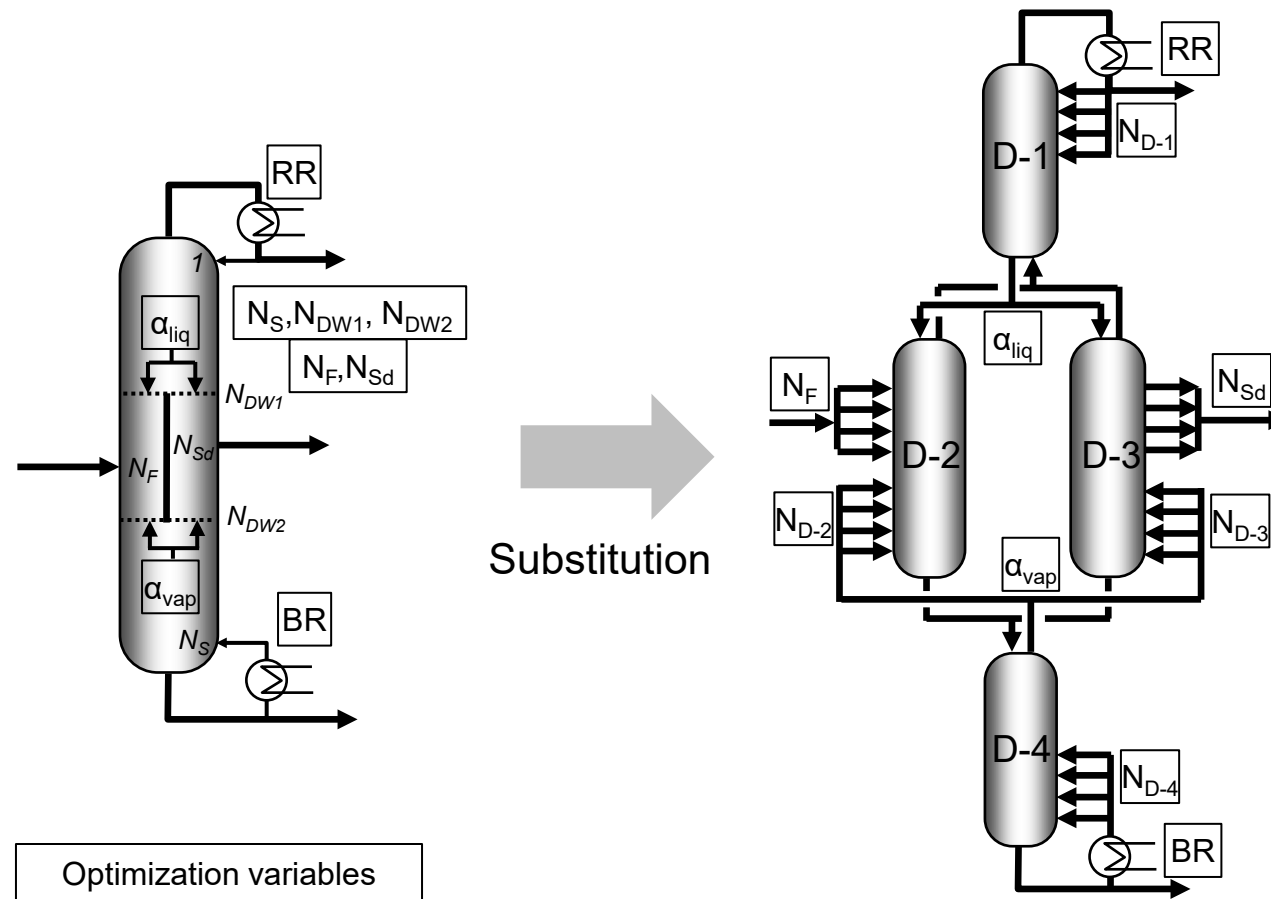


Bayer MaterialScience: Neue TDI-Anlage in Dormagen eröffnet
(plasticer.de)

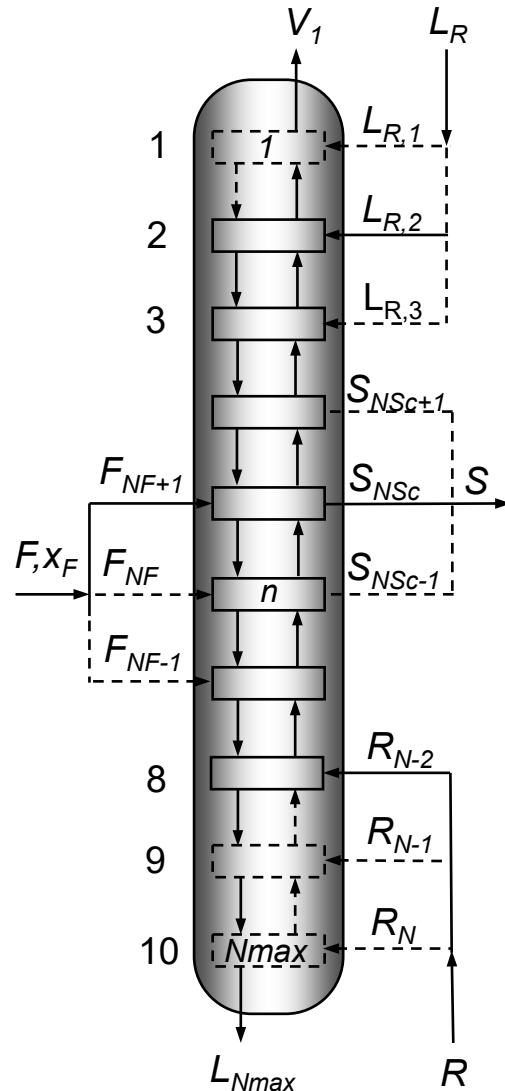
Cost optimal design requires the determination of **continuous** and **integer** optimization variables
Mixed-integer Nonlinear Problem => MINLP

... a suitable model structure must be chosen ...

- Thermodynamic equivalent representation of DWC by 4-section column model



... the model equations must be written ...



- MESH equations for $n = 1 \dots Nmax$ stages:

$$V_{n+1}x_{Vn+1} + L_{n-1}x_{Ln-1} + F_n x_{Fn} + L_{Rn} x_{LRn} + R_n x_{Rn} = V_n x_{Vn} + L_n x_{Ln} + S_n x_{Sn}$$

$$x_{Vn} = K_n x_{Ln}$$

$$\sum x_{Vn} = 1 \quad \text{and} \quad \sum x_{Ln} = 1$$

$$V_{n+1}h_{Vn+1} + L_{n-1}h_{Ln-1} + F_n h_{Fn} + L_{Rn} h_{LRn} + R_n h_{Rn} = V_n h_{Vn} + L_n h_{Ln} + S_n h_{Sn}$$

- Mixed-integer and pure integer constraints:

$$F_n \leq F \cdot y_{F,n} \quad \text{and} \quad \sum y_{F,n} = 1$$

$$L_{R,n} \leq L_R \cdot y_{R,n} \quad \text{and} \quad \sum y_{LR,n} = 1$$

$$R_n \leq R \cdot y_{R,n} \quad \text{and} \quad \sum y_{R,n} = 1$$

$$S_n \leq S \cdot y_{S,n} \quad \text{and} \quad \sum y_{S,n} = 1$$

- Auxiliary model equations:

$$N_S = \sum y_{R,n} \cdot n - \sum y_{LR,n} \cdot n + 1$$

Extended model of Viswanathan and Grossmann (1993), Ind. Eng. Chem. Res., 32, 2942-2949

... and finally, the optimization problem must be set up

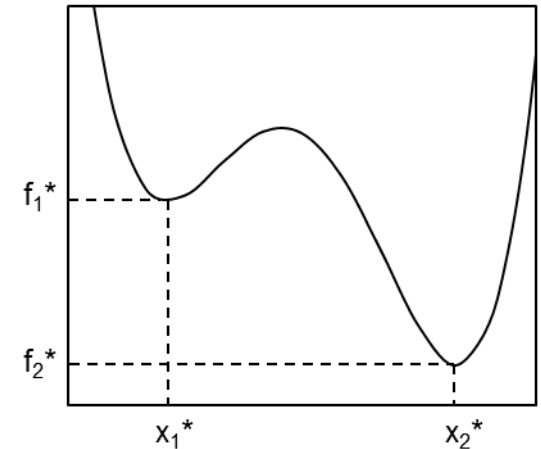
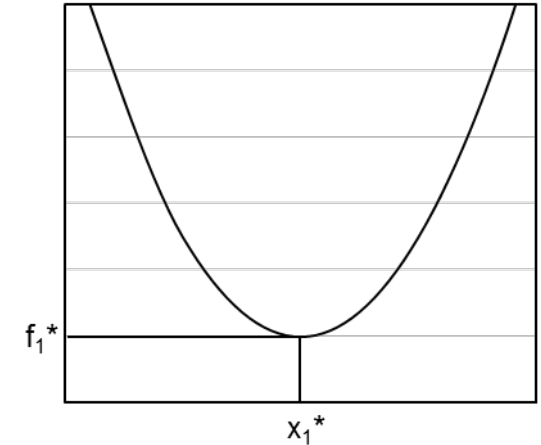
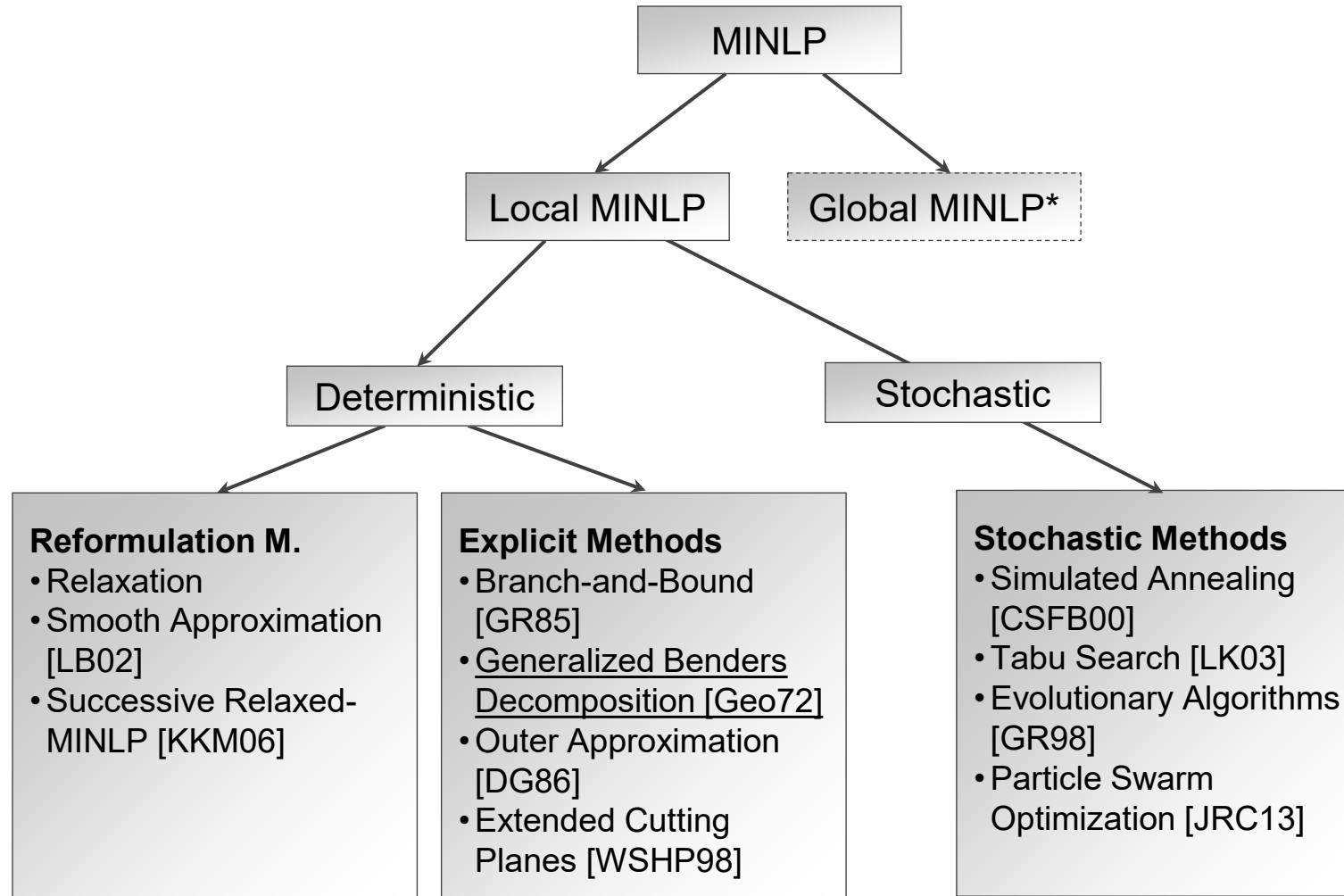
- Objective function $f(\mathbf{x}, \mathbf{y})$:
 - $f(\mathbf{x}, \mathbf{y}) = \text{Total Annual Costs (TAC)}$
 - $\text{TAC} = C_{op} + 5 * C_{eqp} * 0.2$
- Constraints:
 - Equality constraints (model equations) \mathbf{h}
 - Inequality constraints (design specs) \mathbf{g}
 - Mixed-integer constraints $\mathbf{x} - \mathbf{M}\mathbf{y} \leq \mathbf{0}$
 - Pure integer constraints $\mathbf{y}\mathbf{E} = \mathbf{e}$
- Optimization variables:
 - Continuous variables \mathbf{d}
 - Binary (integer) variables \mathbf{y}

$$\begin{aligned} Z &= \min_{\mathbf{d}, \mathbf{y}} f(\mathbf{x}, \mathbf{y}) \\ \text{subject to} \\ \mathbf{h}(\mathbf{x}, \mathbf{y}) &= \mathbf{0} \\ \mathbf{g}(\mathbf{x}, \mathbf{y}) &\leq \mathbf{0} \\ \mathbf{x} - \mathbf{M}\mathbf{y} &\leq \mathbf{0} \\ \mathbf{y}\mathbf{E} &= \mathbf{e} \\ \mathbf{x} &\in R^{n_x}, \mathbf{y} \in \{0,1\}^{n_y} \end{aligned}$$

Remark:

\mathbf{d} is the vector of optimization variables and a subset of all cont. \mathbf{x}

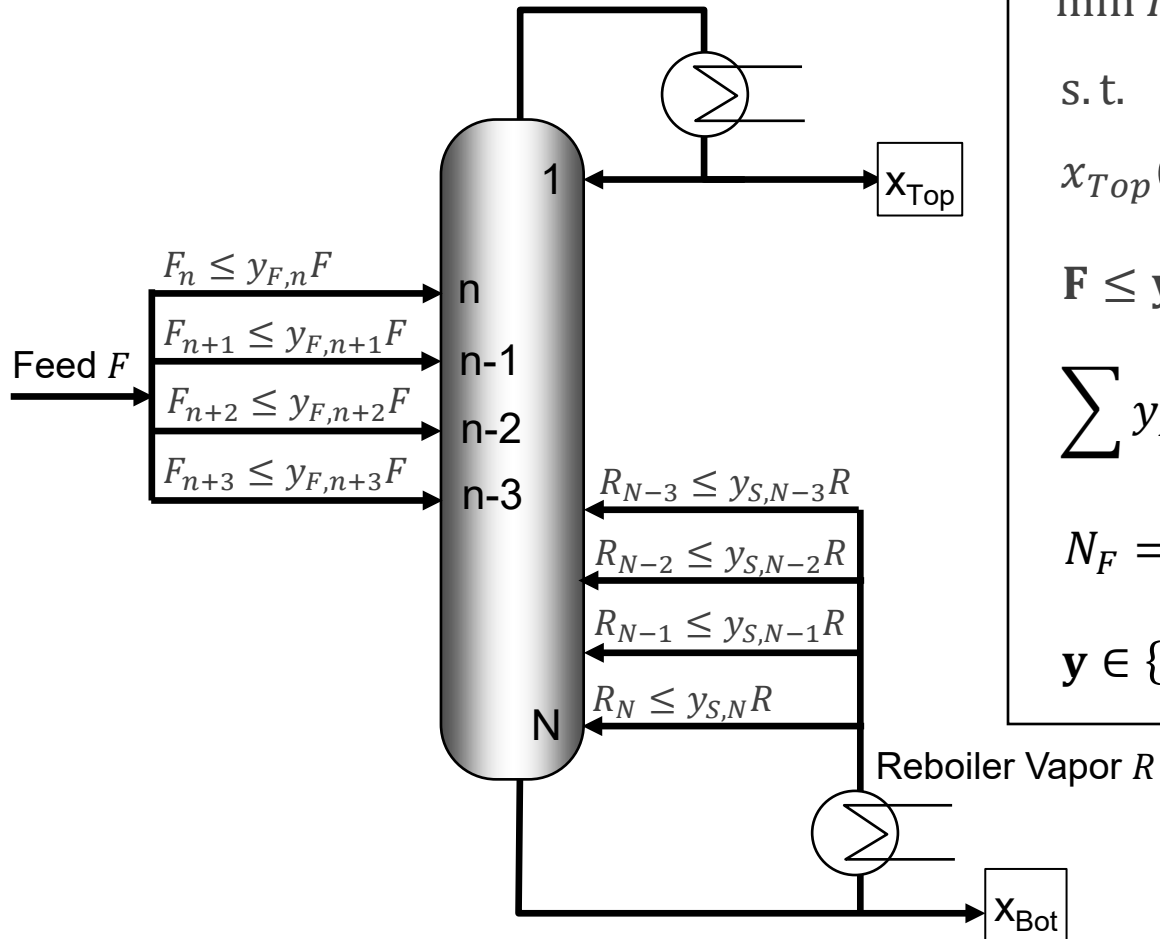
How to Solve It: The Search for the Global Optimum



*guaranteed global optimum in finite number of steps

Optimization with Discrete Variables

Example: Distillation column
for $n = 1 \dots N$ stages:



Optimization problem:

$$\min TAC = f(x_{Top}(RR), x_{Bot}(R), N_F, N_S)$$

s. t.

$$x_{Top}(RR) \geq x_{Top}^* \quad \text{and} \quad x_{Bot}(R) \geq x_{Bot}^*$$

$$\mathbf{F} \leq \mathbf{y}_F F \quad \text{and} \quad \mathbf{R} \leq \mathbf{y}_S R$$

Mixed-integer constraints

$$\sum y_{F,n} = 1 \quad \text{and} \quad \sum y_{S,n} = 1$$

Pure integer constraints

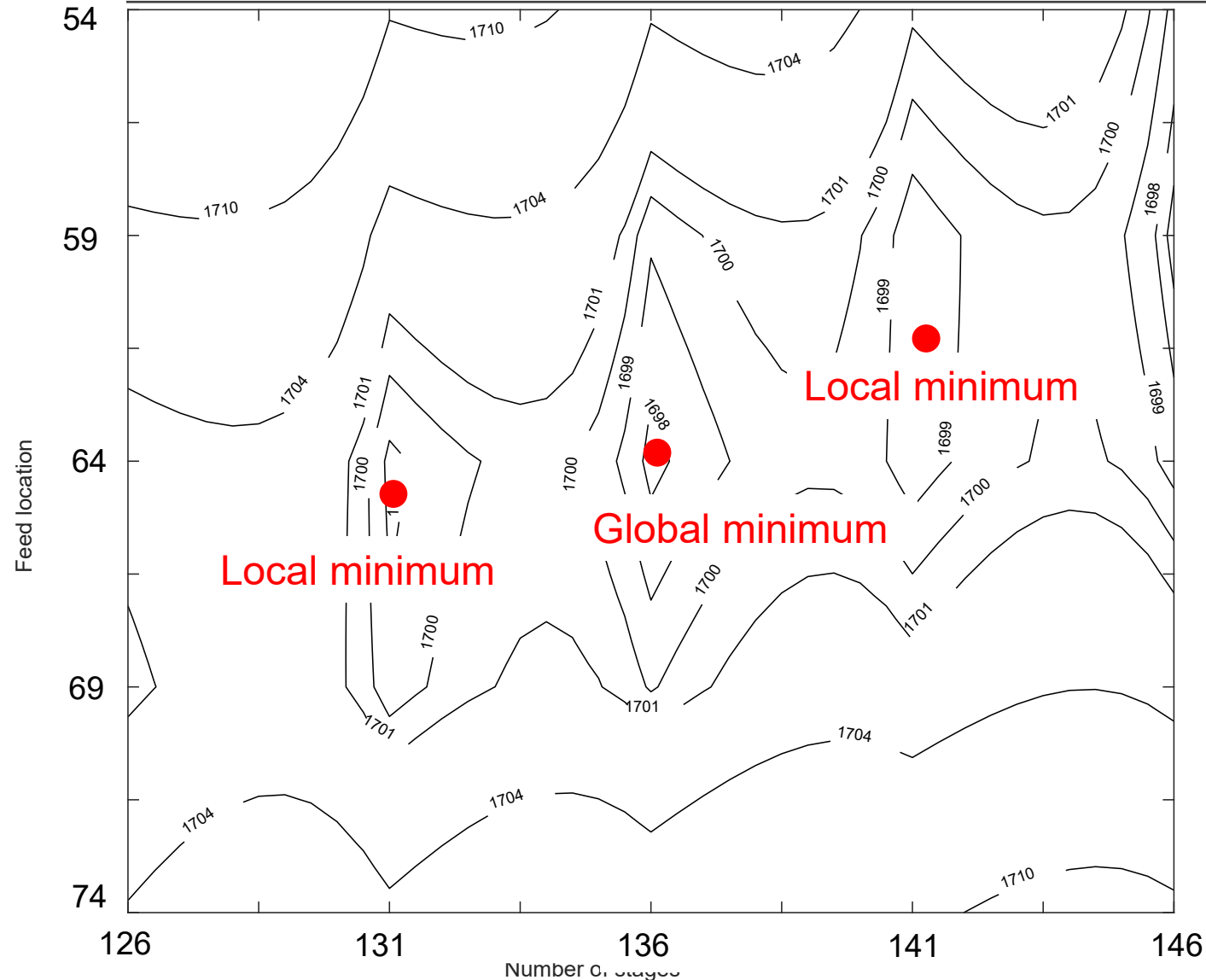
$$N_F = \sum n \cdot y_{F,n} \quad \text{and} \quad N_S = \sum n \cdot y_{S,n}$$

Pure integer constraints

$$\mathbf{y} \in \{0,1\}^{ny} \quad \text{and} \quad N \in \mathbb{N}$$

Definition of stets

Contour Plot with Quasi-continuous Variables



Case study: Hybrid separation process

$$\min TAC = f(x_{Top}^*, x_{Bot}^*, N_F, N_S)$$

Quasi-continuous binary variables:

$$y_F \in [0,1]^{ny} \quad \text{and} \quad y_S \in [0,1]^{ny}$$

Additional integer constraints:

$$y_{F,n} + y_{F,n+5} = 1 \quad \text{and} \quad y_{S,n} + y_{S,n+5} = 1$$

Converting binary in integer variables:

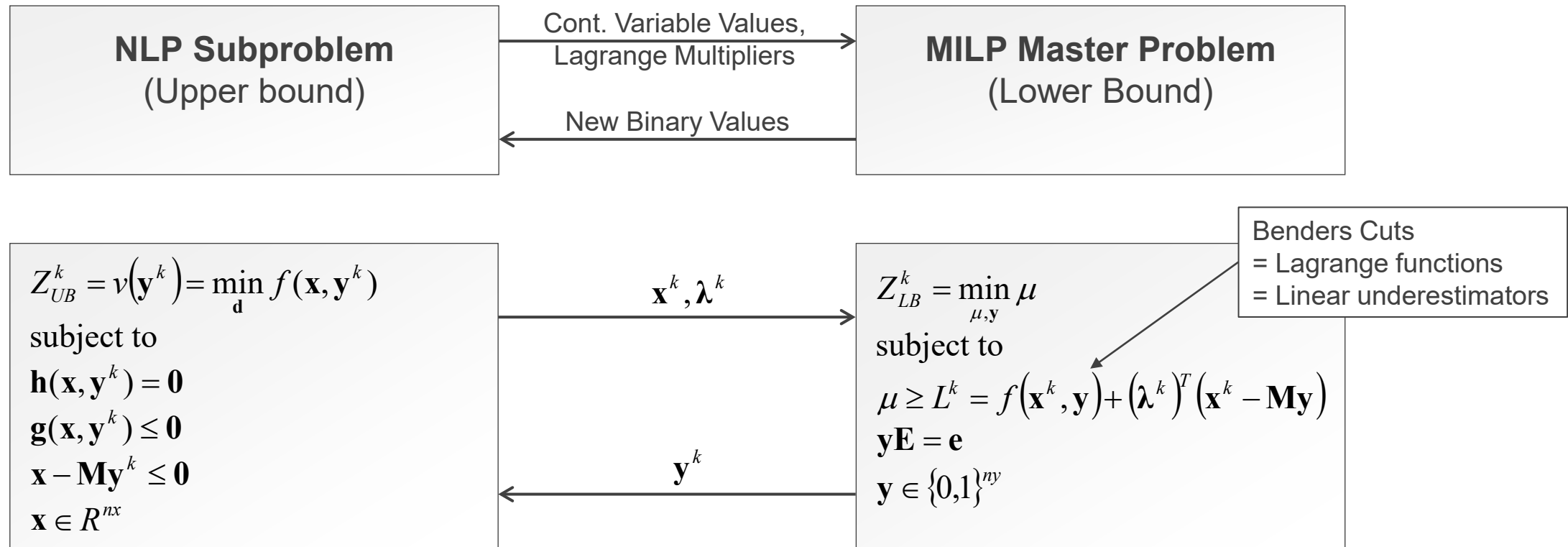
$$N_F = n + 5(1 - y_{F,n}) \quad \text{and} \quad N_S = n + 5(1 - y_{S,n})$$

Discrete-continuous problems

- in quasi-continuous representation -
are often **nonconvex**!

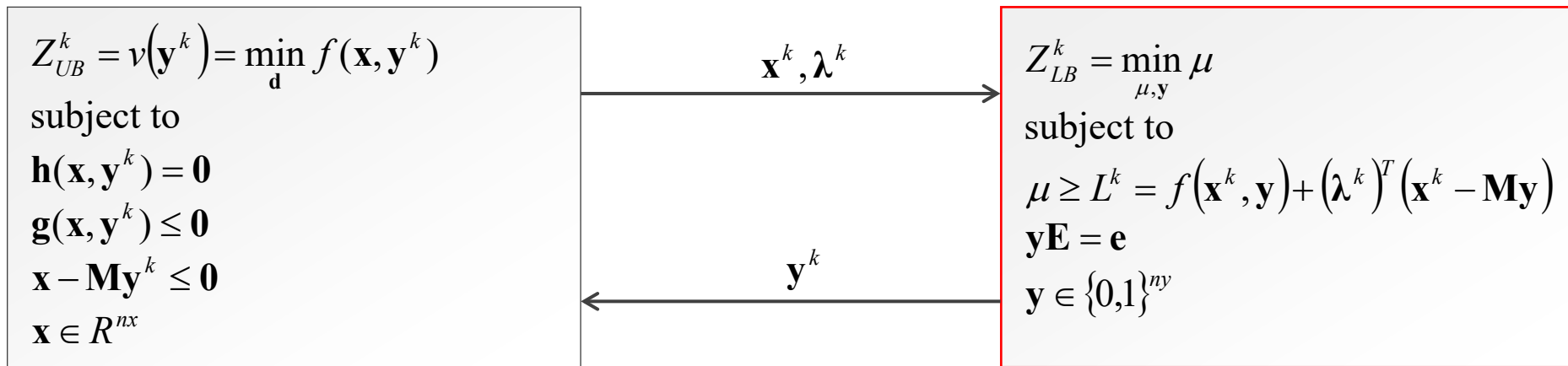
Generalized Benders Decomposition (GBD)¹

- Key principle of GBD: Decomposition

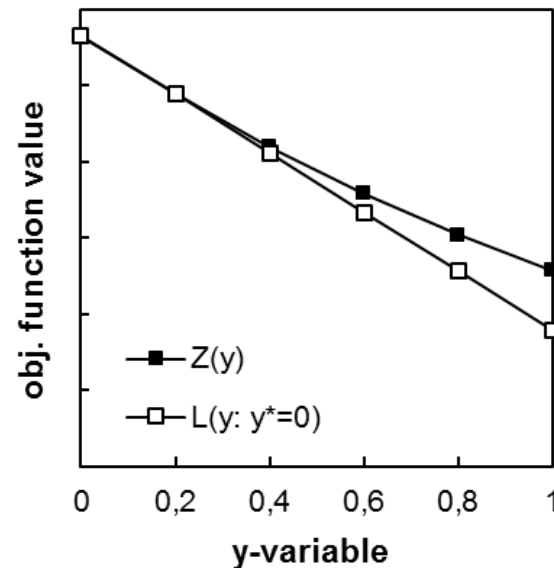


¹Geoffrion (1972), Journal of Optimization Theory and Applications, 10(4), 237-262

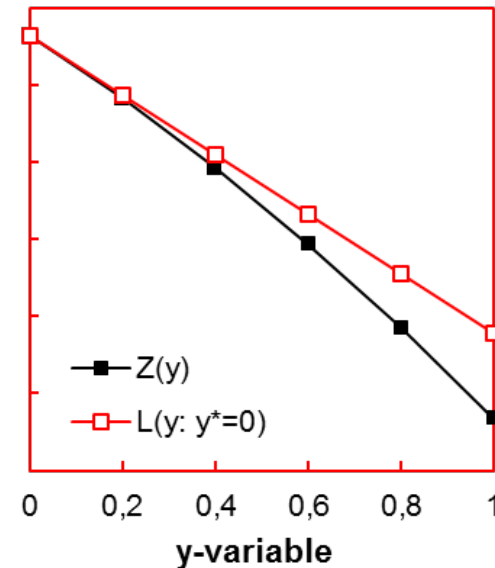
How Non-convexity May Prevent the Global Optimum



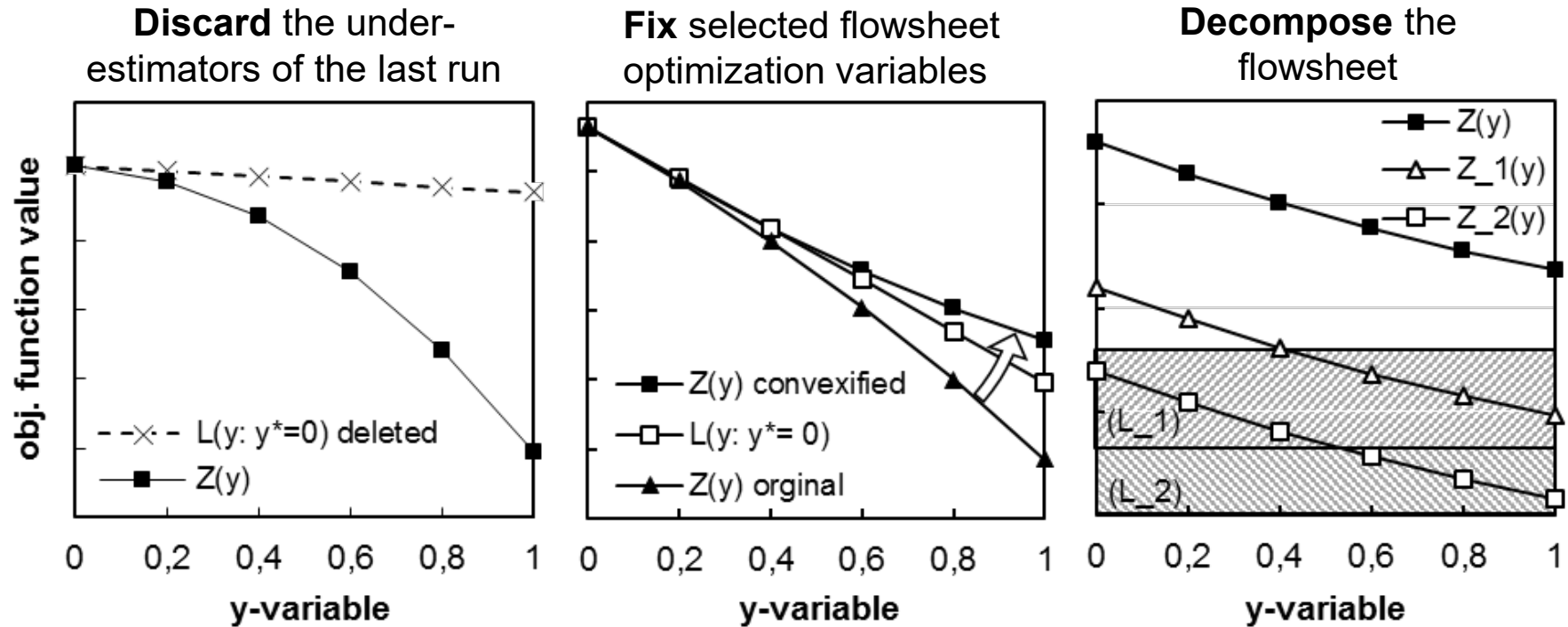
Valid underestimator



Non-valid underestimator



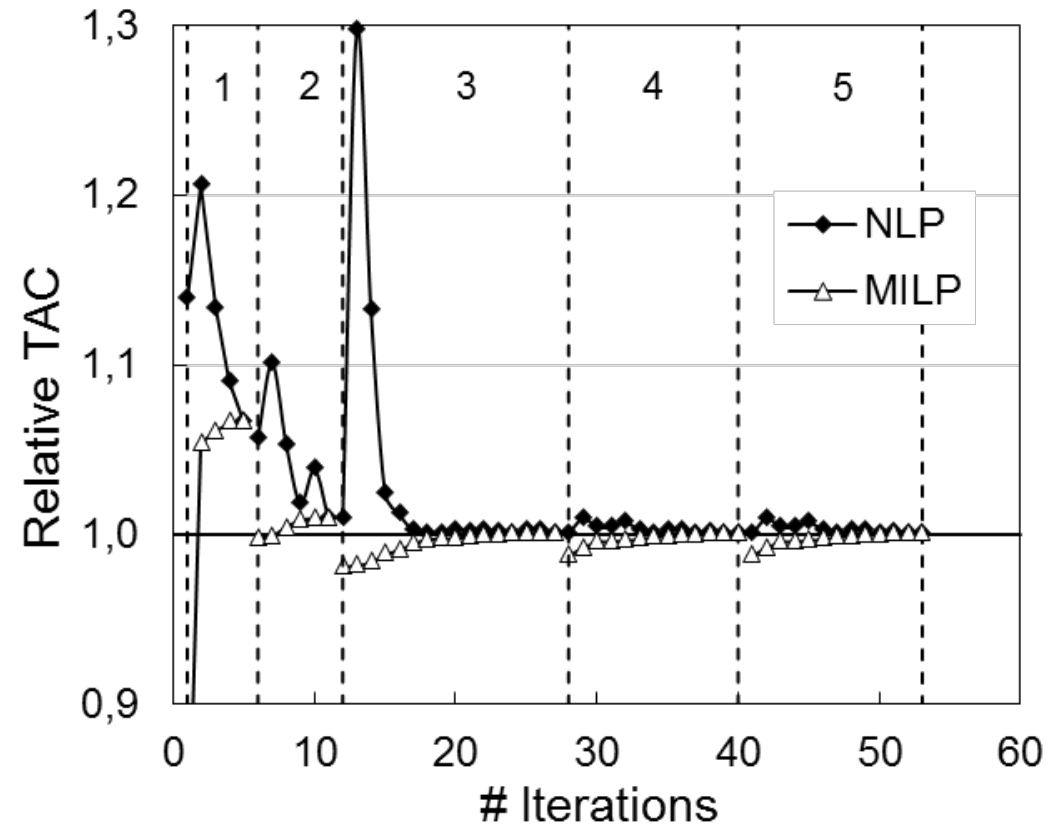
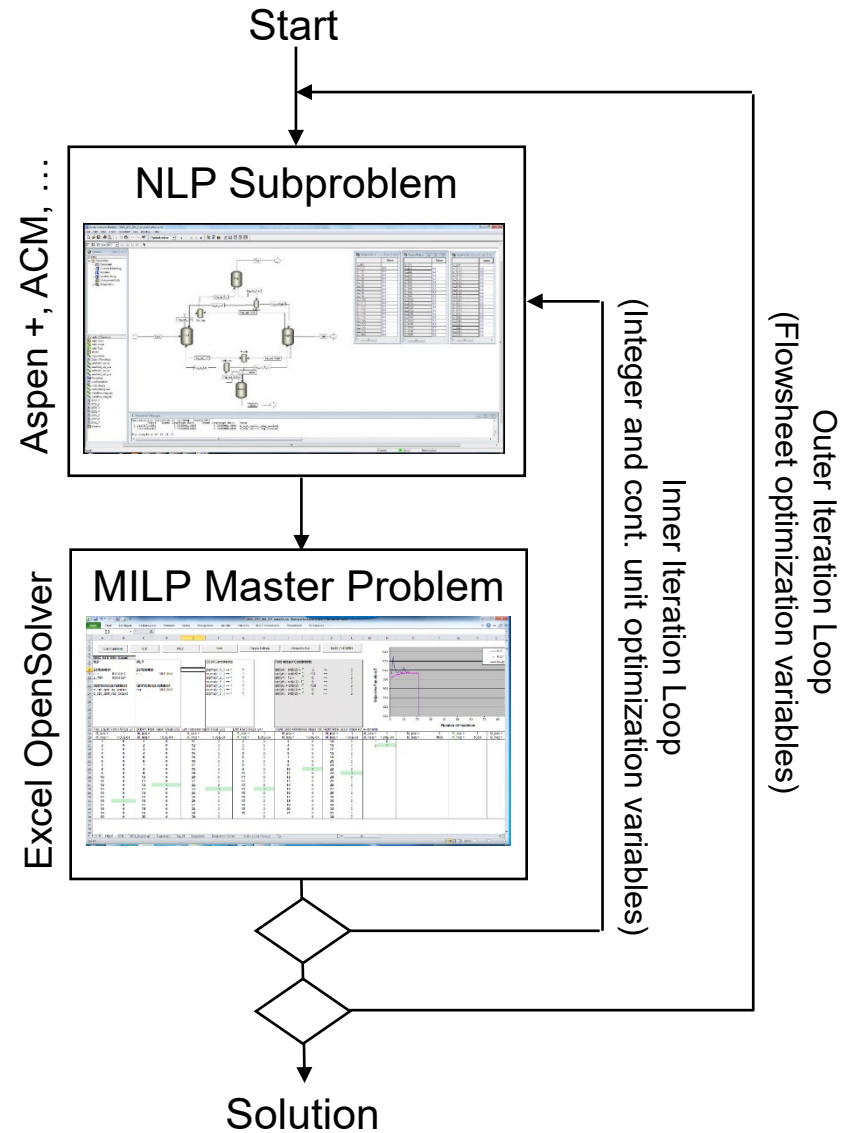
How to Cope With Non-convexity



- With the Discard-Fix-and-Decompose¹ strategy, the likelihood of getting trapped into local optima is reduced

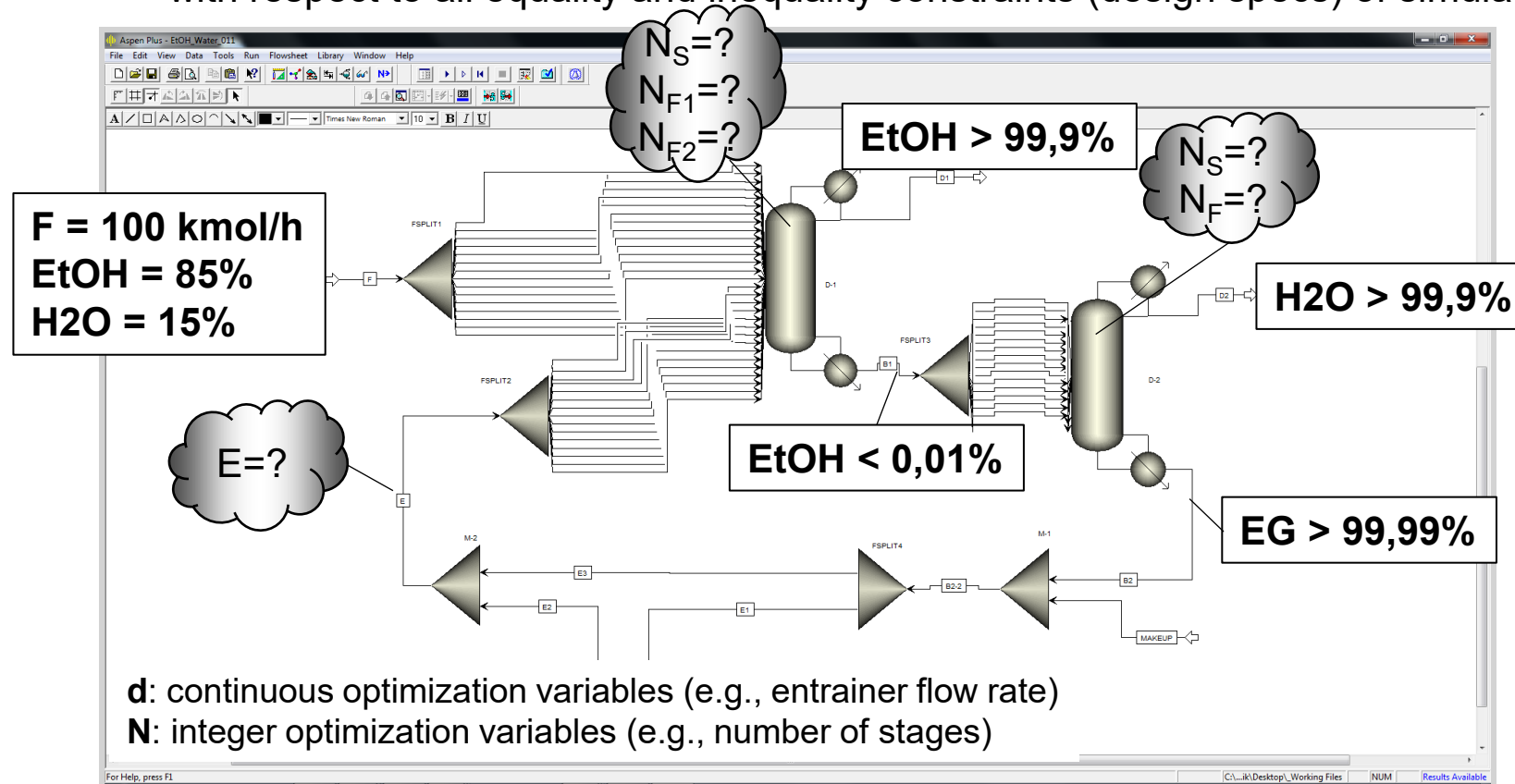
¹Franke (2019), Comp. Chem. Eng., 131, 106583

Implementation of mGBD



Implementation in Sequential-modular Flowsheet Simulator

- Extractive distillation process optimization problem (Ethanol/water with ethylene glycol as entrainer):
 - Minimize objective function $TAC = C_{op}(d) + 5 * C_{eqp}(d, N) * 0.2$
 - with respect to all equality and inequality constraints (design specs) of simulator



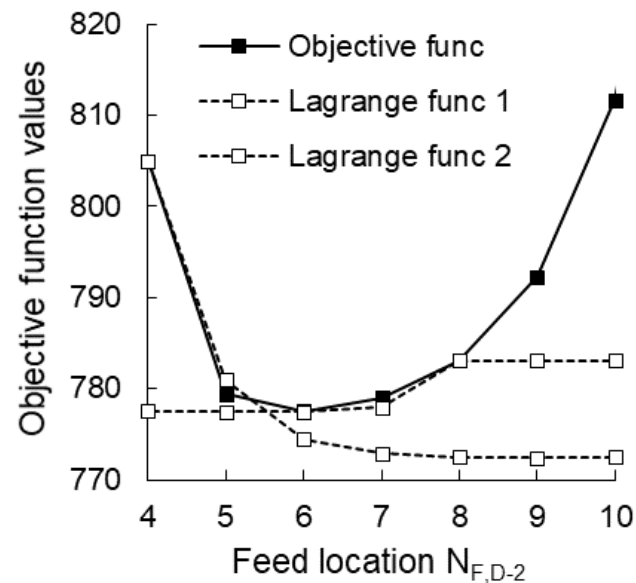
Construction of Linear Underestimators

For calculation of the linear underestimators, the sensitivity information (= Lagrange multipliers) is crucial: $L = f_0(y_0, N_0) + \lambda_{NF}(y_0 - y) + \lambda_{NS}(N_0 - N)$

Feed stage

- Feed is distributed over several stages; lambda is calculated by perturbation of every feed stream

$$\lambda_{NF} = -\frac{\Delta f}{\Delta \varepsilon} = -\frac{(f_0 - f_\varepsilon)}{\Delta \varepsilon}$$

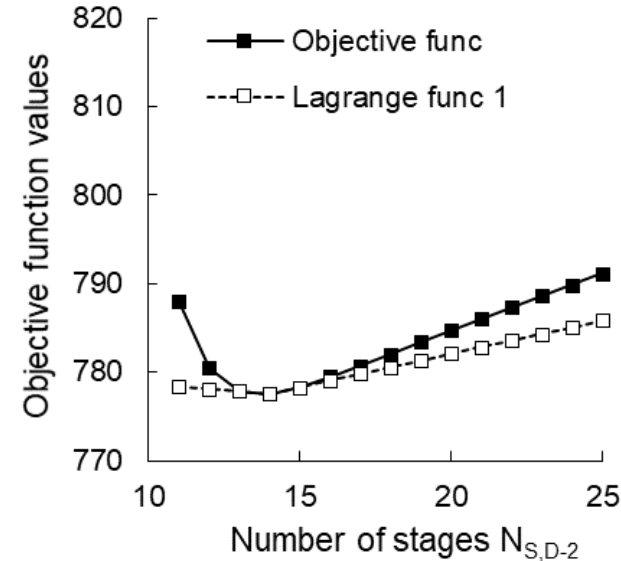


Number of stages

- Expansion and shrinking of column by 1 stage; different for left and right side with respect to actual stage

Left: $\lambda_{NS} = (f_0 - f_{NS-1})$

Right: $\lambda_{NS} = -(f_0 - f_{NS+1})$



Several Case Studies Successfully Accomplished

Separation problems solved by mGBD

	Simulator	Customer	Year
Isomer Mixture 1	ACM	Company	2005
Isomer Mixture 2	ACM	Company	2008
Isocyanate Dividing-Wall Column	ACM	Company	2010
EtOH/H ₂ O Heteroazeotropic Dist.	ACM	Literature	2016
DWC for EtOH/H ₂ O Separation	ACM	Literature	2017
Acetic Acid Recovery	A+	Company	2017
EtOH/H ₂ O Extractive Distillation	A+	Literature	2018

Currently working on

- Reactive distillation (homogeneous)
- Membrane cascades (gas separation)

Other examples

- There are several other examples in literature, most of them rely on GAMS (“self-written models”) and OA (“likely to get trapped in local optima”).
- With more computational power and parallelization, it is likely the stochastic as well global optimization methods will gain more importance.