

## **INITIAL 1-D SINGLE PHASE LIQUID TRANSIENT VERIFICATION OF COBRA-TF**

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### **ABSTRACT**

Abstract ...

*Key Words:* List no more than five key words

## 1 INTRODUCTION

For the past several decades, the primary focus in nuclear engineering within the United States has been focused on light water reactors (LWR). Commercially, all nuclear reactors are either boiling water reactors (BWR) or pressurized water reactors (PWR). Correct computation of the thermal hydraulics within the reactor core leads to efficient design and accuracy in the safety analysis. A popular subchannel code for modelling the hydrodynamics within the reactor core is COBRA-TF. This FORTRAN based code solves 8 conservation equations for liquid, entrained droplet, and vapor phases in 3-D dimensions [1]. A 1-D residual formulation of the code has been created. This paper outlines an initial verification of the original version of code as well as the residual version of the code. The verification problem is a single phase 1-D channel with transient inlet density and mass flow rate. The problem will undergo a Richardson's extrapolation in the temporal and spatial domains to verify the convergence and order of accuracy of the error. The study of the order of accuracy is considered one of the more rigorous verification criteria [2].

## 2 COBRA-TF

The thermal hydraulics of a LWR core is an important part of nuclear reactor design. COBRA-TF solves 8 conservation equations for liquid, entrained droplet, and vapor phases of water boiling within the rod structure of a LWR reactor core [1]. Currently, the conservation equations analytically reduce into a pressure matrix in a semi-implicit method with rod temperatures solved for explicitly. This work involves representing the 1-D single phase liquid conservation equations and calculated variables in a residual formulation. This residual formulation should allow for easier and more in depth verification analysis. This paper details the initial comparison of the residual formulation to the original code.

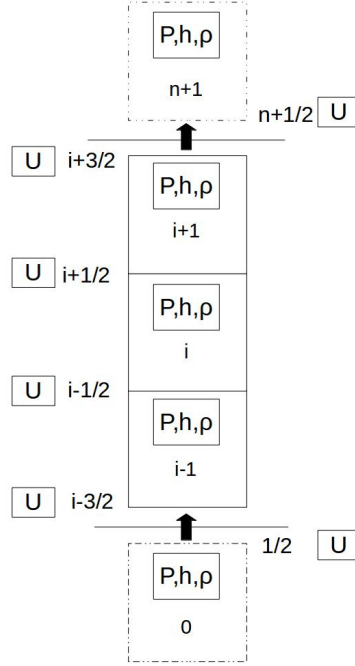
### 2.1 Software Quality Assurance

Software quality assurance is a set of tools and procedures that helps ensure that the software is reliable. COBRA-TF is managed by Github repository setup and maintained by CASL. An extensive test matrix is run before each major push to ensure that the code meets the specified requirements. The test matrix consists of unit tests, code coverage runs, validation problems, and validation problems. The code documentation consists of a theory manual, a users manual, a developers manual, and a validation manual. Further work might involve using aut documentation tools to keep an up to date developers manual. This paper will be the beginning of a verification manual, integrating this verification problem directly into the test matrix.

### 2.2 1-D Single Phase Liquid Conservation Equations

The finite volume structure in COBRA-TF in figure 1 is for a one-dimensional channel in the axial direction with  $n$  number of cells. The first and last cells at 0 and  $n + 1$  are ghost cells and act as the boundary conditions for the problem. Pressure, enthalpy, and density are averaged over the cell volume and are located at the center of the cell. Mass flow rate and velocity are located at the

faces in between cells. The cells are represented with an index  $i$ , and the faces with indexes of  $i + \frac{1}{2}$  or  $i - \frac{1}{2}$ . This project will initially focus on this 1-D configuration. Usually the code is 3-D, with channels connecting to each other in two more dimensions.



**Figure 1. The finite volume structure for COBRA-TF**

The single phase Euler partial differential equations for mass (1), momentum (2), and energy (3) correspond to the unknown variables density  $\rho$ , velocity  $u$ , pressure  $P$ , and enthalpy  $h$ . The first terms in each of the equations are temporal terms. The rest of the terms are steady state spatial terms.

$$\frac{\partial \rho}{\partial t} + \nabla \rho u = 0 \quad (1)$$

$$\frac{\partial \rho u}{\partial t} + \nabla \rho u^2 + \nabla P - \rho g = 0 \quad (2)$$

$$\frac{\partial \rho h}{\partial t} - \frac{\partial P}{\partial t} + \nabla(\rho u h) = 0 \quad (3)$$

### 2.3 Residual Formulation and Jacobian Construction

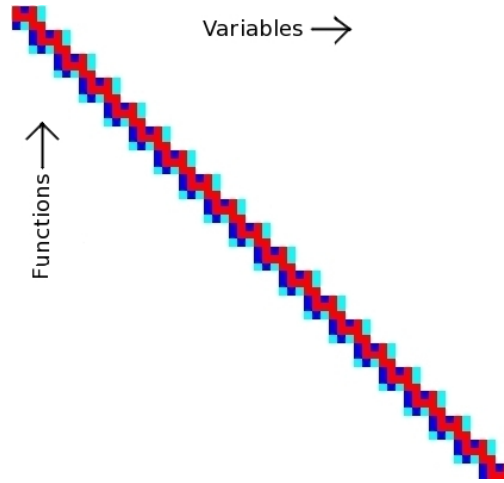
A residual is simply the difference between the value at some future time  $n + 1$  and the value at the current iteration  $k$ . This can be applied to desired variables and equations. For example, the

residual for density,  $\delta\rho_i$ , is difference between iterate levels  $n + 1$  and  $k$ ,  $\rho_i^{n+1} - \rho_i^k$ . The residuals for the equations are determined by substituting the residuals into the discretized equations, which should effectively change all  $n + 1$  into  $k$ . Each cell will have three residual variables and three residual equations. For the entire solution, we will then have a residual variable array  $\delta X$ , and a residual function array  $F(X)$  which defines a linear system  $J\delta X = -F(X)$ .

The Jacobian matrix is defined as the derivative of each response of the function  $F_j$  with respect to each variable  $X_i$ . The derivative can be calculated numerically as shown by equation (4) where  $\epsilon$  is a small numerical value. For COBRA-TF the equations are linear, and this numerical approximation of the Jacobian matrix is exact. This should produce the same jacobian matrix that COBRA-TF currently generates analytically.

$$J_{i,j} = \frac{\partial F_j(X)}{\partial X_i} \approx \frac{F_j(X_i + \epsilon) - F_j(X)}{\epsilon} \quad (4)$$

To build the jacobian matrix, an object oriented class was created that contains three arrays. An array that points to the residual functions, an array that points to the position within a target variable array, and an array that has the index that the function is to be evaluated at. These lists can be appended to in any order, but have to be appended all at the same time so that variables and functions must correspond with each other. Then to construct the jacobian matrix, the residual function and residual variable arrays can each be looped over to numerically build the jacobian matrix as seen in figure 2.



**Figure 2. Structure of the jacobian matrix for single phase liquid**

### 3 ISOKINETIC SINE WAVE ADVECTION

Code verification is the set of procedures set in place to ensure that the code was written properly. The procedures can use the following as code verification criteria from least to most rigorous are expert judgement, error quantification, consistency / convergence, and order of accuracy [3].

For this work the a Richardson Extrapolation will be used to check for convergence and order of accuracy of the error in space and time. As shown by the modified equation analysis in the previous section, the spatial and temporal order of accuracies should be 1.

### 3.1 Problem Setup

The verification problem is defined as a single horizontal channel problem the base parameters listed in table I. The problem will have a fixed channel area and perimeter across the entire height of the channel with no grid spacers. The velocity and pressure are assumed to be constant, but small fluctuations may occur due to coding mistakes or numerical noise. The channel geometry and operating conditions are taken to be approximate a standard PWR. The inlet of the channel has a constant velocity with a fluctuating enthalpy that corresponds to a 37.5 °C temperature change. The length of the transient was defined to be quadruple the time needed for the liquid at the inlet to advect to the outlet. The frequency of the sine wave was defined so generate a full period of a spatial wave across the height of the channel.

**Table I. Problem Parameters**

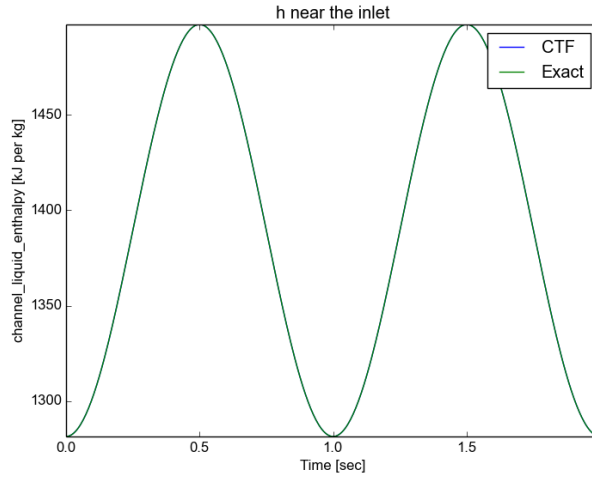
Parameter	Symbol	Value	Unit
Axial Height	$H$	3.6586	$m$
Channel Area	$A_{ch}$	4.94E-005	$m^2$
Wetted Perimeter	$P_w$	1.49E-002	$m$
Velocity	$V_o$	7.35	$\frac{m}{s}$
Pressure	$P_o$	155.00	bar
Temperature 1	$T_1$	289.500	°C
Temperature 2	$T_2$	327.00	°C
Enthalpy 1	$h_1$	1281.55	$\frac{kJ}{kg}$
Enthalpy 2	$h_2$	1497.21	$\frac{kJ}{kg}$
Mass Flow Rate 1	$\dot{m}_1$	0.2713	$\frac{kg}{s}$
Mass Flow Rate 2	$\dot{m}_2$	0.2399	$\frac{kg}{s}$
Final Time	$t_f$	2.00	sec
Wave Frequency	$\omega$	1.00	Hz

The lookup table to vary the inlet enthalpy  $h$  and inlet mass flow rate  $\dot{m}$  use smooth trigonometric functions given in equations 5 and 6. The equations assume constant axial spacing  $\Delta x$  and time step size  $\Delta t$  where  $i$  and  $j$  are the spatial and temporal index respectively. These equations should also behave as the known solutions throughout the entire domain of the problem. The enthalpy and mass flow rate should vary proportionally to the density as to create an isokinetic boundary condition at the inlet. However this is dependent on the steam tables used. A python script was used to generate the data tables according to trigonometric equations using lookup tables that mimic the IAPWS-97 steam tables used by the code [4].

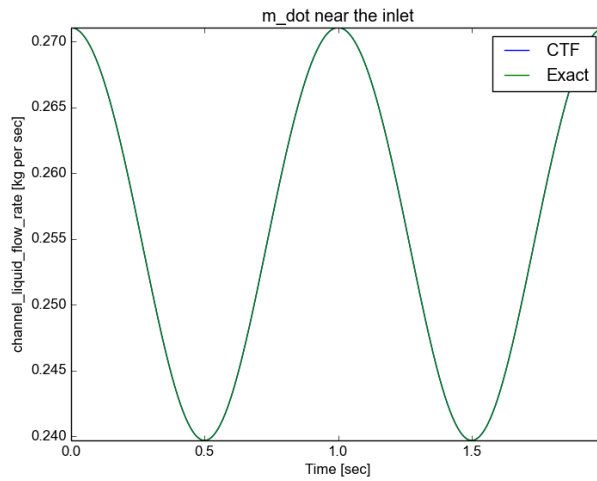
$$h(i, j) = \frac{1}{2} \left( (h_1 + h_2) + (h_1 - h_2) \cos \left( \omega \left( j \Delta t + \frac{i \Delta x}{V_o} \right) \right) \right) \quad (5)$$

$$\dot{m}(i, j) = \frac{1}{2} \left( (\dot{m}_1 + \dot{m}_2) + (\dot{m}_1 - \dot{m}_2) \cos \left( \omega \left( j\Delta t + \frac{i\Delta x}{V_o} \right) \right) \right) \quad (6)$$

The comparison between the data table and the output in CTF are shown for enthalpy and mass flow rate in figures 3 and 4 respectively. The CTF output was read from hdf5 data files at each point in time, which omitted the actual ghost cell where these values were applied. The CTF values are located at the nearest node to the inlet, and therefore will be slightly out of phase to the exact values but this effect is small in the figure.



**Figure 3. Enthalpy Near the Inlet and the Analytical Solution**

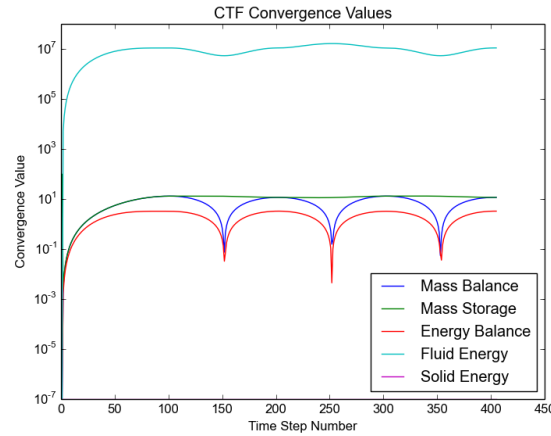


**Figure 4. Density Near the Inlet and the Analytical Solution**

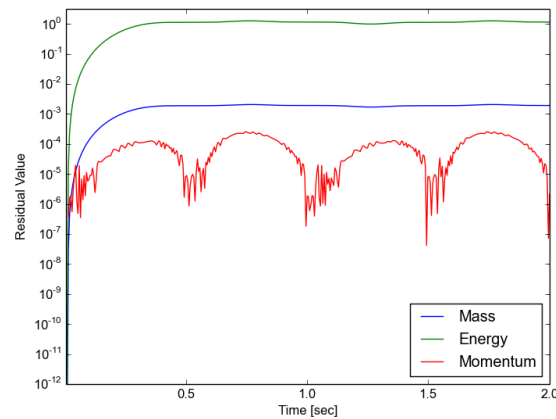
For the original version of COBRA-TF there is a small discrepancy in the way the density is calculated at the inlet that causes the velocity to be non-consistent. This is considered small for this problem and should not greatly affect the order of accuracy. The residual formulation was coded in such a way as to avoid this problem and has considerably less fluctuation in the inlet velocity.

### 3.2 Code Convergence

The current version of COBRA-TF uses global code convergence criteria that are used to estimate the error associated with the solution of the code for transient and steady state problems as shown in figure 5. For this problem, the solid energy storate is zero since there are not any heat structures present. The fluctuating values represent differences between the enrgy and mass entering and leaving the system.



**Figure 5. Code Convergence Criteria for the original version of COBRA-TF**



**Figure 6. Sumnation of the residuals for the residual version of COBRA-TF**

The residual formulation prints out the summation of the residuals functions across the domain to an output file for eac time step and can be seen in figure 6. The mass balance and energy balances present in the code convergence criteria are much smaller for the residual formulation. These residuals provide a much better indication as to the level of error present in the solution of the system. They can even be expanded to provide convergence information at every position, variable, and equation.

### 3.3 Modified Equation Analysis

The original mass balance equation can be re-written to look like equation 7. Using upwinding, the finite difference can be written to look like equation 8. A second order Taylor series approximation can be used for  $\rho_i^{n+1}$  and  $\rho_{i-1}^n$  as shown in equations 9 and 10 respectively. The higher order terms ( $O(\Delta x^2, \Delta t^2)$ ) are not taken into account for this approximation. The Taylor series approximations can then be substituted into 8 to yield 11. This is the beginning of the modified equation analysis. The goal will be to isolate the original PDE and define the truncation error.

$$\frac{\partial \rho}{\partial t} + U_0 \frac{\partial \rho}{\partial x} = 0 \quad (7)$$

$$\frac{\rho_i^{n+1} - \rho_i^n}{\Delta t} + U_0 \frac{\rho_i^n - \rho_{i-1}^n}{\Delta x} = 0 \quad (8)$$

$$\rho_i^{n+1} = \rho_i^n + \frac{\partial \rho}{\partial t} \Delta t + \frac{1}{2} \frac{\partial^2 \rho}{\partial t^2} \Delta t^2 + O(\Delta t^3) \quad (9)$$

$$\rho_{i-1}^n = \rho_i^n - \frac{\partial \rho}{\partial x} \Delta x + \frac{1}{2} \frac{\partial^2 \rho}{\partial x^2} \Delta x^2 + O(\Delta x^3) \quad (10)$$

The lengthy equation 11 can be reduced to equation 12 since the  $\rho_i^n$  terms subtract out and the  $\Delta t$  and  $\Delta x$  terms in the denominator cancel out. This reduced equation can be re-written into equation 13, with the original PDE followed by the truncation terms. Notice how the terms on the right are dependent on both the numerical spacing  $\Delta t$  and  $\Delta x$ , but also on the second derivatives of density with respect to space and time.

$$\frac{\left( \rho_i^n + \frac{\partial \rho}{\partial t} \Delta t + \frac{1}{2} \frac{\partial^2 \rho}{\partial t^2} \Delta t^2 \right) - \rho_i^n}{\Delta t} + U_0 \frac{\rho_i^n - \left( \rho_i^n - \frac{\partial \rho}{\partial x} \Delta x + \frac{1}{2} \frac{\partial^2 \rho}{\partial x^2} \Delta x^2 \right)}{\Delta x} + O(\Delta x^2, \Delta t^2) = 0 \quad (11)$$

$$\frac{\partial \rho}{\partial t} + \frac{1}{2} \frac{\partial^2 \rho}{\partial t^2} \Delta t + U_0 \left( \frac{\partial \rho}{\partial x} - \frac{1}{2} \frac{\partial^2 \rho}{\partial x^2} \Delta x \right) + O(\Delta x^2, \Delta t^2) = 0 \quad (12)$$

$$\frac{\partial \rho}{\partial t} + U_0 \frac{\partial \rho}{\partial x} + \frac{1}{2} \frac{\partial^2 \rho}{\partial t^2} \Delta t - U_0 \frac{1}{2} \frac{\partial^2 \rho}{\partial x^2} \Delta x + O(\Delta x^2, \Delta t^2) = 0 \quad (13)$$



## 4 RICHARDSON EXTRAPOLATION

The richardson extrapolation was performed by refining the spatial and temporal step sizes by a factor of 2 for a set number of times. The spatial and temporal studies are refined seperately in their own study in order to isolate the spatial and temporal affects on the the solution.

### 4.1 Convergence of Error

The relative difference at each point for a particular time step was calculated between each iteration for each quantity of interest. For the spatial refinement, the lower iterate values were numerically integrated to match the shape of the initial domain. The errors were then summed over the entire domain to yield a total error for each variable. The total error for enthalpy is plotted in figures 7 and 8 as a function of temporal and spatial step size respectively. The data points where chosen to be outside of the asymptotic range as shown by the good linear fit of the data. The plots show that as the temporal and spatial step sizes are reduced, the numerical error approaches zero.

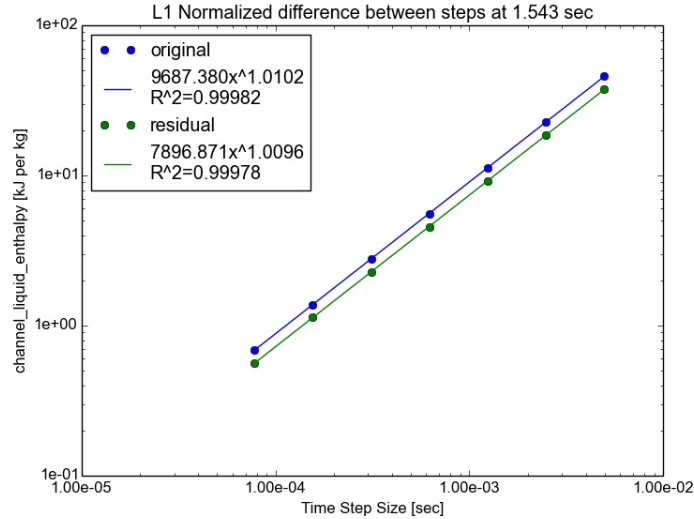
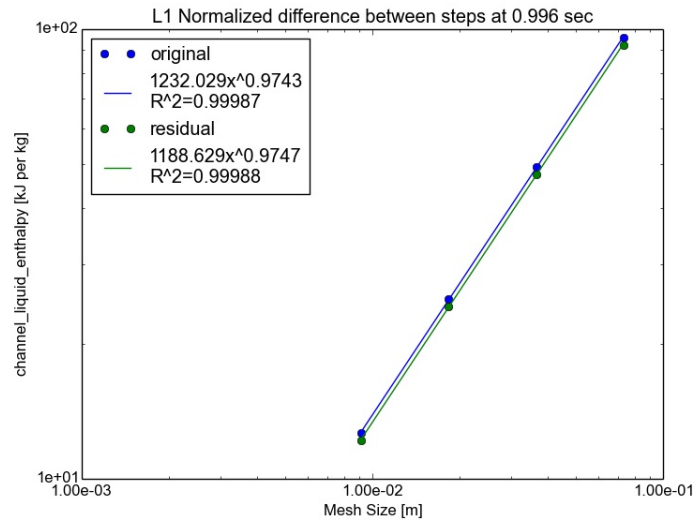


Figure 7. Difference Between Successive Temporal Refinements

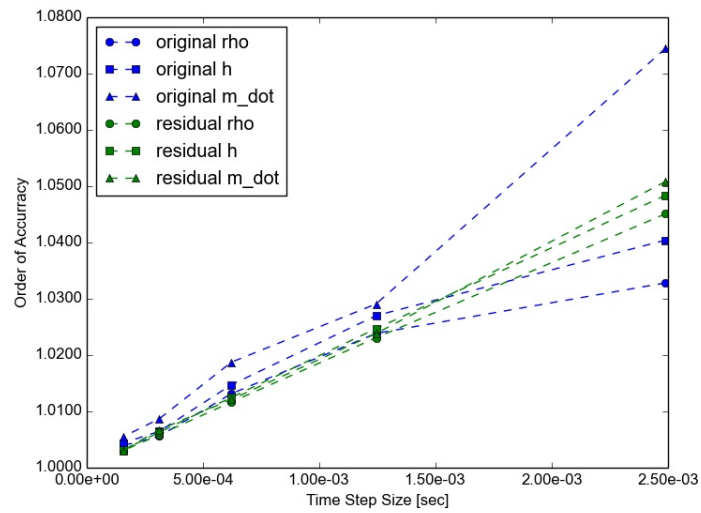
### 4.2 Order of Accuracy

Each study generates at least 3 points  $f_1, f_2, f_3$  with a constant refinement factor  $R$  of 2. The order of accuracy  $p$  between 3 points is given by equation (14).

$$p = \frac{\ln\left(\frac{f_3 - f_2}{f_2 - f_1}\right)}{\ln(R)} \quad (14)$$



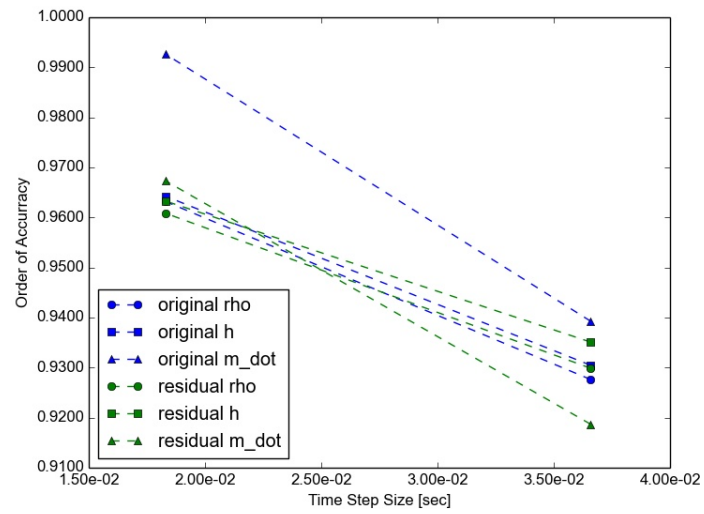
**Figure 8. Difference Between Successive Temporal Refinements**



**Figure 9. Temporal Order of Accuracy**

## 5 CONCLUSIONS

Present your summary and conclusions here.



**Figure 10. Spatial Order of Accuracy**

## 6 ACKNOWLEDGMENTS

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## 7 REFERENCES

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