# How cells regulate the type and size of actin structures Ondrej Maxian November 29, 2023

The goal of this write-up is to explore how modeling can help us understand *in vivo* regulation of actin structure and size. We focus on the two predominant types of actin networks: branched structures (which tend to condense into endocytic patches sometimes referred to as "mini-comets"), and linear structures (which form filopodia and the contractile ring). The branched structures are mediated by the arp 2/3 complex, which binds to existing mother filaments to form branches [17], while the latter are mediated by formins, which makes screw-like rotations to allow monomers to enter [21, 12]. Our research question is as follows: how does the cell regulate the type and size of branched vs. linear actin structures, while at the same time preserving the total amount of actin in the cell?

# 1 Introduction

To assemble filaments, actin monomers associate with diffusion-limited rate constant [17]. The barbed end elongation rate has been measured as  $= k_{\rm on}G$ , where G is concentration of G actin and  $k_{\rm on} = 11.6~\mu{\rm M}^{-1}~{\rm s}^{-1}$  [22]. As the dissociation rate is not a function of bulk concentration, an equilibrium exists around bulk concentration of 0.1  $\mu{\rm M}$  where a fixed percentage of actin is in monomeric form, with the rest in polymerized form. While the total amount of incorporated actin is therefore fixed, the kinetics leave undetermined how much is in branched vs. filamentous form. To control this, the conventional viewpoint is that external or internal signals activate signaling cascades which eventually cause the cell to produce more or less of a particular type of network [14, 17, 22]. However, recent experimental evidence has shown that a limiting actin pool must also control the types of structures being produced.

Experiments show that depleting the arp 2/3 complex leads to more filamentous actin networks [20]. Specifically, in fission yeast, inhibition of arp 2/3 by the drug CK-666 leads to new assembly of F-actin, as long as there is sufficient formin present. Subsequent washing out of CK-666 gives

disassembly of the "ectopic" F-actin and reassembly of dense actin patches [3], indicating that the release of F-actin via disassembly is important for the assembly of new structures [22]. On the opposite end, formin depletion also enhances arp 2/3-mediated assembly. In single mutant formin cells, the density of endocytic actin patches is roughly doubles, but the size and lifetime of the patches remains the same [3]. This suggests that the mechanism of size control is independent from the mechanism of choosing filamentous vs. branched structures.

The most curious experimental observations have to do with changes in structure when the actin pool changes. If the structures are a function only of the arp 2/3 and formin concentrations, then we would expect changes in actin concentration to decrease each kind of structure in the same proportion. However, experiments in fission yeast show that underexpression of actin favors formin-mediated contractile rings, while overexpression favors arp 2/3 complex mediated actin patches [3]. These observations imply that the cell assembles formin-mediated structures "first" in some sense, and then assembles arp 2/3 structures with the excess actin. But it isn't clear what is meant by "first" here.

There are additional confounding agents that could tip the scales in one direction or the other. We focus on two: profilin and capping protein. In general, the presence of profilin correlates with more filamentous actin structures [22], as actin binding to profilin prevents filament nucleation but allows for barbed end growth [17]. Depletion of capping protein increases arp 2/3-mediated patches by at least 35% [22]. This is confusing because capping protein competes with formin for barbed ends [11], and so we would expect depleting capping protein to increase formin levels and lead to more filamentous actin.

The modeling that has been done on this problem has so far been limited to the size control of a generic filamentous actin structure, and has been carried out extensively by Kondev and collaborators. Their results can be summarized as follows: when there is competition for a finite pool of subunits, only one quantity is well-defined, the *total* amount of monomer that is found in filamentous form. This means that the length distribution of individual filaments (or structures) is not well defined [16, 9]. In addition, the limiting pool hypothesis by itself predicts that structures with slightly higher on rates will capture all of the monomers at equilibrium. Applying to our problem, their limiting pool model predicts either stochastic swings between branched and filamentous actin (if the on rates are the same), or all of the actin in the structure with faster on rate. Neither of these is what we see *in vivo*, where the balance between branched and filamentous actin is maintained at a relative steady state in time.

Because these models are steady state models, it is certainly possible that the intermediate filament lengths are quasi-stable, and that the drift to steady state occurs on very long timescales [23]. Alternative ideas are covered in recent extensions of Kondev's models [15], which have shown that the correct length distribution of yeast actin cables can be predicted by consider length-dependent attachment rates, as well as sensing of the cell boundaries. Additional work [18] has shown that considering filaments as part of bundles, whose longest fiber sets the length of the bundle, is able to explain the variance of fiber length in actin bundles.

Also papers by Banerjee [2, 1]

## 1.1 The key questions

It's clear from these observations that the partitioning between branched and filamentous actin structures is a function of three variables: (1) the bulk actin concentration, (2) the arp 2/3 concentration, and (3) the formin concentration. What we want to use modeling to understand is how these three agents combine to generate steady state structures, and in particular explain the following experimental observations

- 1. Less arp 2/3 gives more filamentous actin structures.
- 2. Less forming give more branched structures.
- 3. Underexpression of actin gives more filamentous structures.
- 4. Overexpression of actin gives more branched structures.

#### 1.2 A modeling plan

An ideal modeling study would consist of the following procedure:

- 1. Begin with a small system of *discrete* formin, arp 2/3, and actin molecules, which diffuse around randomly.
- 2. Formulate a set of interaction rules by which reactions occur between these.
- 3. See if those rules generate the correct steady states qualitatively.
- 4. Formulate a set of ODEs from the microscopic simulations that describes the interactions.

There is a separate issue of the size control of the individual structures. Because manipulating actin, arp 2/3, and formin concentration keeps the size of the structures the same, this likely occurs by different mechanisms, and is something we can look at later.

# 2 Diffusion

The first thing we do in building up our model is to consider the diffusion of an actin structure with arbitrary configuration. We will assume that the actin structures are

- 1. Made of N spheres of radius a
- 2. Moving as rigid bodies

# 2.1 Kinematics and mobility

Let us denote the structure by the array X. When moving as a rigid body, the structure has velocity

$$U = U_{\text{COM}} + \Omega \times (X - X_{\text{COM}}) := K[X]\alpha$$
 (1)

where  $X_{\text{COM}} = N^{-1} \sum X_p$  denotes the center of mass and  $U_{\text{COM}}$  denotes the velocity of the center of mass. Following the formulation in [4], the mobility matrix which relates the total force and torque on the body to its translational and angular velocity is given by

$$N = (K^T M^{-1} K)^{\dagger}, \qquad (2)$$

where † denotes the pseudo-inverse and  $\mathbf{M} = \mathbf{I}/(6\pi\mu a)$  is the mobility of the particles absent the constraint ( $\mathbf{M}^{-1}$  is the drag coefficient). Here we are not incorporating any hydrodynamics, so the mobility is simply

$$\mathbf{N} = \frac{1}{6\pi\mu a} \left( \mathbf{K}^T \mathbf{K} \right)^{\dagger} = \begin{pmatrix} \mathbf{N}_{\text{tt}} & \mathbf{0} \\ \mathbf{0} & \mathbf{N}_{\text{rr}} \end{pmatrix}. \tag{3}$$

Here there is no coupling between rotation and translation when we measure the mobility about the center of mass. This is a consequence of using the simple hydrodynamic mobility; see [4, Sec. IV(A)] for more discussion.

#### 2.2 Langevin equation

The Ito Langevin equation describing diffusion of the body is given by [13]

$$d\begin{pmatrix} \boldsymbol{X}_{\text{COM}} \\ \boldsymbol{\tau} \end{pmatrix} = \sqrt{2k_BT} \boldsymbol{N}^{1/2} d\boldsymbol{\mathcal{W}}, \tag{4}$$

where  $d\mathcal{W}$  is a 6-vector of Brownian motion increments with the property  $\langle d\mathcal{W}d\mathcal{W}^T \rangle = N\Delta t$ , and  $\tau$  describes any material vector attached to the body. Note that there are no stochastic drift terms because the mobility is measured about the center of mobility [13]. Still not quite written correctly. A numerical method to solve this equation is to [4]

- 1. Compute N[X]
- 2. Set

$$egin{pmatrix} m{U}_{ ext{COM}} \ m{\Omega} \end{pmatrix} = m{lpha} = \sqrt{rac{2k_BT}{\Delta t}} m{N}^{1/2} m{\xi},$$

where  $\xi$  is a vector of six standard i.i.d. Gaussian random numbers.

3. Evolve the center of mass by  $\boldsymbol{X}_{\text{COM}}^{(n+1)} = \boldsymbol{X}_{\text{COM}}^{(n)} + \Delta t \boldsymbol{U}_{\text{COM}}$  and rotate the tangent vectors of each fiber by  $\boldsymbol{\Omega} \Delta t$ .

In practice, because of (de)polymerization, it will be more practical to track the endpoint  $X_0$ . So, we update the center of mass and evolve the tangent vectors, then compute a new  $X_0$  via

$$oldsymbol{X}_0^{(n+1)} = oldsymbol{X}_{ ext{COM}}^{(n+1)} + ext{rotate} \left( oldsymbol{X}_0^{(n)} - oldsymbol{X}_{ ext{COM}}^{(n)}, \Delta t oldsymbol{\Omega} 
ight)$$

# 2.3 Theory

We now examine the translational and rotational diffusion of particles in free space, for which we have theoretical results [13]. Let  $\Delta \mathbf{X}_c(t) = \mathbf{X}_{\text{COM}}(t) - \mathbf{X}_{\text{COM}}(0)$ , then

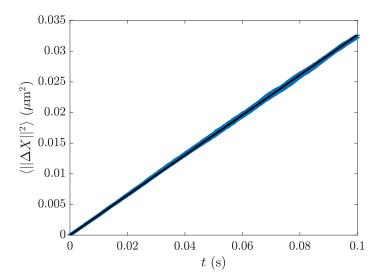
$$\langle \Delta \boldsymbol{X}_c(t) \cdot \Delta \boldsymbol{X}_c(t) \rangle = 2k_B T \operatorname{trace}(\boldsymbol{N}_{\mathrm{tt}}) t.$$
 (5)

Likewise, let  $u_1$  be the eigenvector of  $N_{rr}$  with maximum eigenvalue, and suppose that we express  $u_1$  in terms of the material frame at t = 0. Then

$$\langle \boldsymbol{u}_1(t) \cdot \boldsymbol{u}_1(0) \rangle = e^{-\alpha t} \qquad \alpha = k_B T \left( \lambda_2 + \lambda_3 \right),$$
 (6)

where  $\lambda_2$  and  $\lambda_3$  are the two smallest eigenvalues of  $N_{\rm rr}$ .

In all simulations in this section, we set  $k_BT = 4.1 \times 10^{-3} \text{ pN} \cdot \mu\text{m}$ ,  $a = 0.004 \ \mu\text{m}$  and  $\mu = 1 \text{ Pa·s}$ .



**Figure 1:** Diffusion of monomers. The blue line shows the MSD as a function of time, and the black line shows the theory (7).

# 2.4 Monomers

In the case of monomers, there is no rotational diffusion,  $N_{\rm tt} = 1/(6\pi\mu a)$  and (5) simplifies to

$$\langle \Delta \mathbf{X}_c(t) \cdot \Delta \mathbf{X}_c(t) \rangle = \frac{k_B T}{\pi \mu a} t$$
 (7)

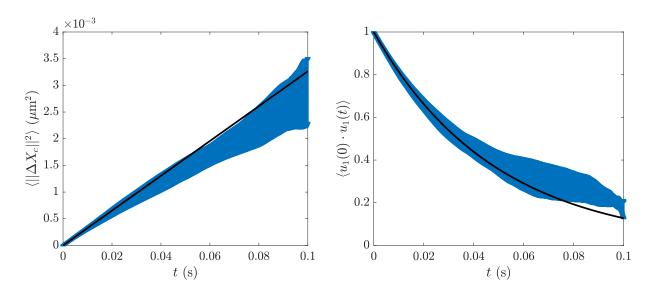
In Fig. 1, we perform simulations with 1000 monomers, repeated 10 times to generate error bars. We observe perfect agreement between our simulation and theory.

# 2.5 Fibers

Continuing on to linear fibers, we perform simulations with 10 fibers, repeated 10 times to generate error bars. Each fiber contains 10 monomers. The results in Fig. 2 show agreement between simulations and theory.

#### 2.6 Branched fibers

We have a lot of freedom for branched fibers. We fix the geometry as shown in Fig. 3. There are 18 monomers here, 10 on the longest fiber, then 5 on the one attached, and then 3 on the small output. As before, we simulate this fiber 10 times to generate a mean, then repeat this 10 times to generate error bars. Results in Fig. 4 show agreement between experiments and theory.



**Figure 2:** Diffusion of linear fibers. The left plot shows translational diffusion, for which we compare the data in blue to the theory (5) in black, while the right plot shows rotational diffusion, for which we compare the data in blue to the theory (6) in black.

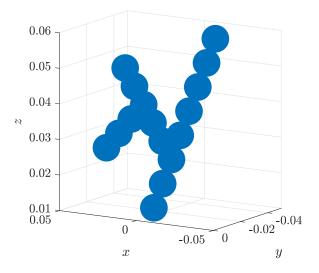
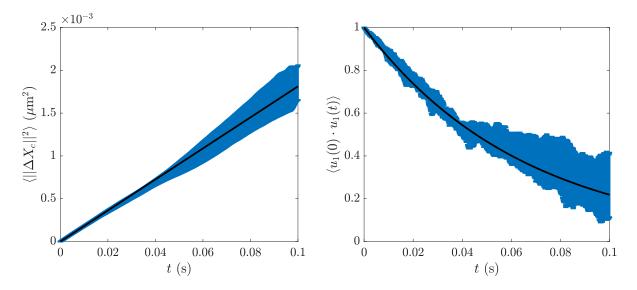


Figure 3: The branched fiber we use for our diffusion test. Axis is in  $\mu$ m.



**Figure 4:** Diffusion of branched fibers. The left plot shows translational diffusion, for which we compare the data in blue to the theory (5) in black, while the right plot shows rotational diffusion, for which we compare the data in blue to the theory (6) in black.

# 3 Reaction network tracking individual monomers

To begin, we will restrict our reaction kinetics to a system of monomers and *linear* fibers. The formation of a "fiber" will occur with two monomers, after which we add monomers to the pointed and barbed ends. There are therefore six reactions in our system:

- 1. Two monomers becoming a fiber of length two:  $A + A \xrightarrow{\lambda_m} A_2$ . This reaction occurs (with rate  $\lambda_m$  (units 1/time)) if two monomers are within a distance  $R_{\rm rxn}$  of each other. In this case, we choose one of the two monomers at random as the fiber "starting point," then choose a random tangent vector  $\boldsymbol{\tau}$  on the unit sphere. The second monomer is inserted a fixed spacing  $\Delta s = 2a$  apart in this direction  $\boldsymbol{\tau}$ .
- 2. A two-monomer fiber becoming two individual monomers:  $A_2 \xrightarrow{\nu_m} A + A$ . This reaction occurs with rate  $\nu_m$  (units 1/time), and is the reverse of the two-monomer binding reaction. We choose one monomer at random to keep in place, then set the location of the other one in a random location inside of the reactive sphere of radius  $R_{\rm rxn}$  centered around the first (fixed) particle.
- 3. A fiber adding to its barbed/pointed end:  $A + A_n \xrightarrow{\lambda_{b/p}} A_{n+1}$ . This reaction occurs with the corresponding rate at each end if the monomer A is within the reactive sphere of radius  $R_{\text{rxn}}$ .

4. A fiber depolymerizing from its barbed/pointed end:  $A_n \xrightarrow{\nu_{b/p}} A_{n-1} + A$ . If this reaction occurs, we place the new monomer A randomly in the reactive sphere of radius  $R_{\text{rxn}}$  centered around the barbed/pointed end of the fiber.

To process these reactions efficiently, at the beginning of each time step we construct a list of all actin monomers that are within  $R_{\text{rxn}}$  of each other (this list includes monomers that are bound to fibers). Then, we process all possible binding reactions. By "process," we simply loop through the list of pairs of monomers. A reaction can occur between two monomers if they are either (a) both monomers or (b) one is a monomer and one is at the pointed/barbed end. If the reaction has rate  $\lambda$ , it occurs if  $r < \lambda \Delta t$ , where r is a random number from the uniform distribution U[0,1] and  $\Delta t$  is the time step over which we evolve the reaction network. After processing the binding reactions, we then repeat for the unbinding reactions. We note that this first order way of treating the reactions avoids the complication of having to update neighbor lists when particles bind and unbind from fibers (see [5] for such a treatment).

#### 3.1 Free monomers and two-monomer "fibers"

As a first step toward validating the code and an exercise in computing macroscopic reaction rates from microscopic ones, we consider a simplified network where  $\lambda_{b/p} = 0$ ; i.e., where two-monomer fibers cannot add to their barbed/pointed ends. The monomers therefore cycle between dimers and free monomers, which can be described by the macroscopic equilibrium

$$k_d^- c_{A_2} = k_d^+ c_A^2$$
 (8a)

$$2c_{A_2} + c_A = c_0, (8b)$$

where  $c_0$  represents the total actin concentration in units of number per volume. This is a system of two equations for the unknowns  $c_A$  and  $c_{A_2}$  and ultimately results in solving the quadratic equation

$$k_d^+ c_A^2 + \frac{k_d^-}{2} c_A - \frac{k_d^- c_0}{2} = 0 (9)$$

for  $c_A$ . The steady state concentration of dimers is then given by  $c_{A_2} = (c_0 - c_A)/2$ . Our goal is to verify that this is what our code outputs.

#### 3.1.1 Macroscopic rate constants from microscopic ones

Prior to doing this, we need to determine how to extract the constants  $k^-$  (units 1/time) and  $k^+$  (units volume/time) from the microscopic parameters. The first of these is simple; since the

macroscopic depolymerization and microscopic depolymerization are the same process, we have  $k^- = \nu_m$ . The same is not true of polymerization, since  $k^-$  describes the speed at which monomers diffuse to find other monomers and react to generate a dimer.

In the case of low densities, the macroscopic reaction rate is related to the microscopic rate  $\lambda$  via [7]

$$k^{+} := k_{0}^{+} = 2\pi D R_{\text{rxn}} \left( 1 - \sqrt{\frac{D}{\lambda R_{\text{rxn}}^{2}}} \tanh \left( \sqrt{\frac{\lambda R_{\text{rxn}}^{2}}{D}} \right) \right). \tag{10}$$

As an approximation, we will set the diffusion coefficient  $D = 2k_BT/(6\pi\mu a)$  to be equal to that of the monomers, although the dimers will diffuse slightly slower.

For finite packing densities, the nature of the process is fundamentally different depending on if it is reaction limited or diffusion limited, as discussed in [5]. The boundary between the two is defined by the dimensionless number

$$r = \frac{\lambda R_{\rm rxn}^2}{D} = \lambda R_{\rm rxn}^2 \frac{2k_B T}{6\pi \mu a},\tag{11}$$

where  $r \ll 1$  denotes a reaction-limited process and  $r \gg 1$  is a diffusion-limited process. In the case when the process is reaction-limited, the system is mixed uniformly, and the rate of the forward reaction is simply the probability of finding a molecule in the reactive sphere of radius  $R_{\rm rxn}$  (which equals  $V_{\rm rxn}c_A$ ), times the rate that the reaction occurs (equal to  $\lambda$ ), times the number of A molecules in the system. This results in a forward rate constant [5, Eq. (2)]

$$k^{+} = k_{\text{mix}}^{+} = \frac{1}{2} \frac{4\pi}{3} R_{\text{rxn}}^{3} \lambda.$$
 (12)

The case of diffusion-limited reactions at finite packing density is more complicated, and there are only empirical results for different algorithms in the literature. Our view is that if we verify our algorithm on reaction-limited processes, and confirm that it works for diffusion-limited processes at low densities, this is sufficient to declare it validated.

# 3.1.2 Simulation results in well-mixed systems

We set up a system of 1000 monomers inside of a 1  $\mu$ m<sup>3</sup> volume, which corresponds to a concentration of about 1.6  $\mu$ M (1  $\mu$ M=602 molecules per  $\mu$ m<sup>3</sup>), but a packing fraction of  $\phi = 2.7 \times 10^{-4}$ , so that the system is quite dilute and the formula (10) should still work well. For reaction rates, we fix  $\lambda_m = 10$ ,  $\nu_b = 5$ , and  $\nu_p = 7$  (so that  $\nu_m = 12$ ) s<sup>-1</sup>, and keep our typical units of  $k_B T = 4.1 \times 10^{-3}$  pN· $\mu$ m,  $a = 0.004 \ \mu$ m, with  $R_{\rm rxn} = 10a$  (this reaction radius is artificially large to generate more

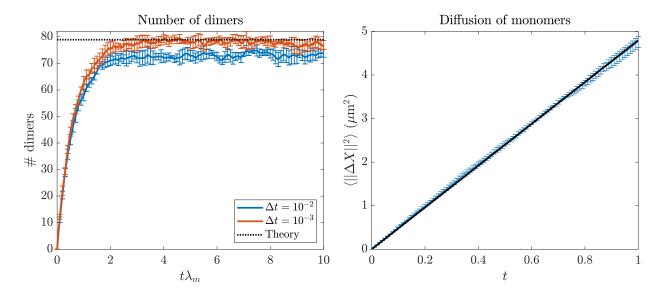


Figure 5: Verifying we obtain the correct mean number of dimers when the system is reaction limited. We consider only monomers and dimers with the parameters detailed at the start of Section 3.1.2, and set  $\mu = 0.068$ , so that r = 0.01 in (11). Left: the number of dimers per  $\mu$ m<sup>3</sup> over time in our algorithm with two different  $\Delta t$  values (the smaller  $\Delta t = 10^{-3}$  has smaller errors). We compare to the theoretical value obtained by solving (9) in black. Right: diffusion of the monomers vs. the theory, confirming that, in this regime, reaction is *not* enhancing diffusion.

dimers). We then use the system viscosity as a control knob to tune the reaction-diffusion limited nature of the system.

We begin with the viscosity  $\mu=0.068$  Pa·s, so that r=0.01 in (11). In this case the result of (10) for the forward rate  $k_d^+$  is indistinguishable from the well-mixed case (12), and the solution of (9) is  $c_{A_2}=78.9/\mu\text{m}^3$  in both cases. In Fig. 5, we verify that our algorithm gives this mean as the time step size shrinks to 0. To do this, we generate 10 trajectories to obtain a mean number of dimers, then repeat five times to generate error bars. A confidence interval is obtained by averaging over the last half of the trajectory (which from Fig. 5 is clearly in steady state), for which we obtain  $c_{A_2}=73.2\pm0.7~\mu\text{m}^{-3}$  for  $\Delta t=10^{-2}$  s and  $c_{A_2}=77.8\pm0.7~\mu\text{m}^{-3}$  for  $\Delta t=10^{-3}$  s. This establishes that our algorithm gives the correct result in the reaction-limited case (at least within statistical errors).

#### 3.1.3 When reaction enhances diffusion

Moving onto cases which are not diffusion limited, we increase the viscosity to  $\mu = 0.68$ , so that r = 0.1 in (11). We repeat the same test as in Fig. 5 and show the results in Fig. 6. This time,

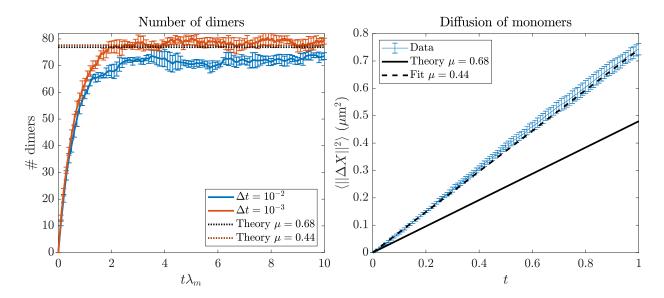


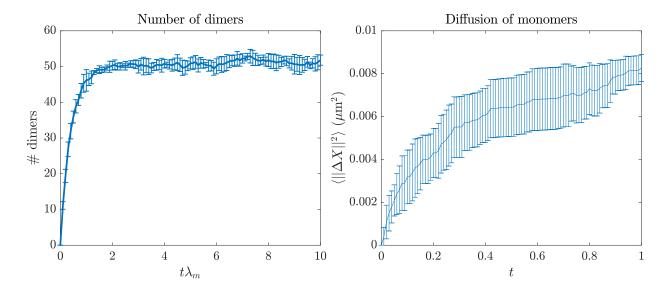
Figure 6: Increasing viscosity to  $\mu = 0.68$  so that r = 0.01 in (11). We show the same quantities as in Fig. 5. Left: the number of dimers over time in our algorithm with two different  $\Delta t$  values (the smaller  $\Delta t = 10^{-3}$  has smaller errors). We compare to the theoretical value obtained by solving (9) in black. Right: diffusion of the monomers vs. the theory. This time, we see enhanced diffusion by about a factor of 1.5; this has the effect of decreasing the viscosity by about 1.5.

we see a deviation from expectations, as we obtain the confidence intervals  $c_{A_2} = 71.9 \pm 0.3 \ \mu \text{m}^{-3}$  for  $\Delta t = 10^{-2}$  and  $c_{A_2} = 78.7 \pm 1.5 \ \mu \text{m}^{-3}$  for  $\Delta t = 10^{-3}$ , while the theoretical value is 76.9  $\mu \text{m}^{-3}$ , which is slightly outside our confidence interval as  $\Delta t \to 0$ .

The errors we make can be understood in terms of the enhanced diffusion we obtain from reactions. In the right panel of Fig. 6, we plot the diffusion of the monomers over time, observing significantly larger displacement over the theoretical expectation when  $\mu = 0.68$ . In particular, the diffusion coefficient is enhanced by a factor of about 1.5 (in terms of absolute, the diffusion coefficient increases by 0.25  $\mu$ m<sup>2</sup>/s). When we obtain a new viscosity from this, we get  $\mu = 0.44$ , which we see is a better fit (predicted # of dimers is 77.7) to our data, although we show in Fig. 7 that the diffusion we get from reaction alone is not of the form  $\Delta X^2 \propto t$ .

We note that there is a huge problem with this algorithm if we actually want to simulate the diffusion-limited regime. The enhancement of the diffusion coefficient scales like  $R_{\text{rxn}}^2 \lambda_m$ , but the ratio in (11) has precisely this in the numerator! So, the ratio r is bounded above by 1 using this numerical method, and we cannot simulate the diffusion-limited regime.

To understand if this is important, an actin monomer has diffusion coefficient 13.7  $\mu$ m<sup>2</sup>/s, while the reaction radius is at most 0.01  $\mu$ m<sup>2</sup>. Then the reaction rate would have to be 1370/s just to



**Figure 7:** Same plot as Fig. 6, but without any diffusion. This illustrates the enhanced diffusion we obtain from reactions.

reach r = 0.01, which is unrealistically large. So it seems that the well-mixed assumption is a good one for this system, and we can move on in the well-mixed regime.

# 3.2 Up to five monomers

Let us now suppose that we can have fibers with up to five monomers in them. Then the system of equations we need to solve is [6]

$$k_f^- c_{A_5} = k_f^+ c_{A_4} c_A \tag{13a}$$

$$k_f^- c_{A_4} = k_f^+ c_{A_3} c_A \tag{13b}$$

$$k_f^- c_{A_3} = k_f^+ c_{A_2} c_A \tag{13c}$$

$$k_d^- c_{A_2} = k_d^+ c_A^2 \tag{13d}$$

$$5c_{A_5} + 4c_{A_4} + 3c_{A_3} + 2c_{A_2} + c_A = c_0. (13e)$$

Here  $k_f^- = k_p^- + k_b^-$  is the rate at which polymers lose a monomer from the pointed or barbed end, and  $k_f^+ = k_p^+ + k_b^+$  is the rate at which monomers are added at the pointed/barbed end. In the well-mixed regime, the rate constants are given from the binding and unbinding rates as

$$k_d^+ = \frac{1}{2} \frac{4\pi}{3} R_{\text{rxn}}^3 \lambda_m \qquad k_d^- = \nu_m \qquad k_f^+ = \frac{4\pi}{3} R_{\text{rxn}}^3 (\lambda_b + \lambda_p) \qquad k_f^- = \nu_b + \nu_p.$$
 (14)

We again consider 1000 monomers with a=0.004,  $k_BT=4.1\times 10^{-3}$ , and  $\mu=0.068$ , and set the rates according to  $\lambda_m=12$ ,  $\nu_m=5$ ,  $\lambda_b=2$ ,  $\lambda_p=4$ ,  $\nu_b=1.5$ , and  $\nu_p=2.5$ . We again use

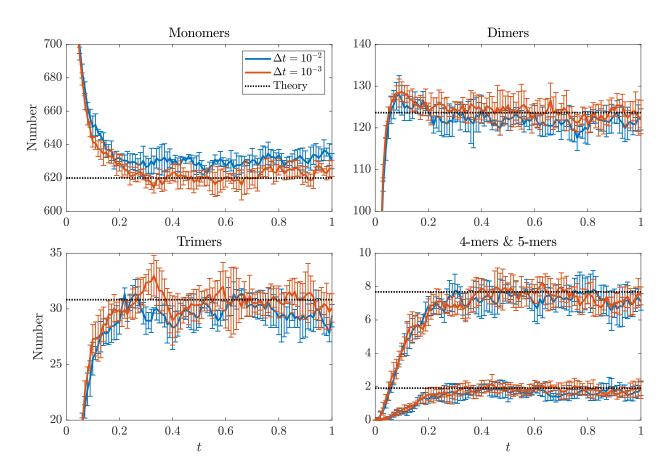


Figure 8: Steady state number per  $\mu$ m<sup>-3</sup> for fibers with up to five monomers. Theory is the solution of (13) with rate constants given by (14). The parameters we use are  $\lambda_m = 12$ ,  $\nu_m = 5$ ,  $\lambda_b = 2$ ,  $\lambda_p = 4$ ,  $\nu_b = 1.5$ , and  $\nu_p = 2.5$ .

the artificially large  $R_{\text{rxn}} = 2.5a$ . Figure 8 confirms that our numerical method gives the correct results in the well-mixed regime.

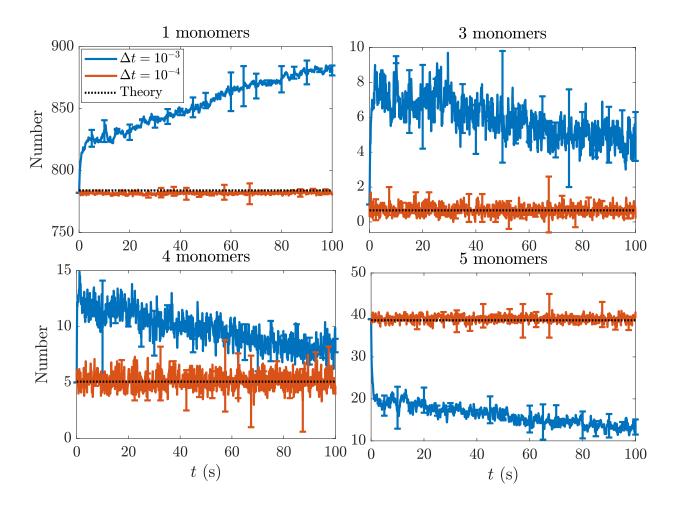
#### 3.3 Using the real actin parameters

Let us now consider the same simulation, but with the parameters equal to those for actin, given in Table 1. This simulation is more demanding because there is a separation of timescales in the pointed and barbed end addition rates, compared to the reaction of two monomers. The only simplification we make in Table 1 is to consider a nucleate as comprising two monomers, as opposed to the three in [19]. This actually speeds up the rate of filament formation, since we skip the equally slow trimer formation step.

If we again allow a maximum of five monomers per fiber, and have 1000 total monomers, the steady state number of fibers (rounded to the nearest whole number) is  $(784, 0, 1, 5, 39)/\mu m^3$ . In

Parameter	Description	Value	Units	Ref	Notes
a	Actin diameter	4	nm		
$R_{ m rxn}$	Reaction radius	8	nm		One diameter
$k_BT$	Thermal energy	$4.1 \times 10^{-3}$	$pN \cdot \mu m$		
$\mu$	Fluid viscosity	0.01	Pa·s		$D = 2k_B T/(6\pi\mu a) \approx 11 \ \mu \text{m}^2/\text{s}$
$k_d^+$	Dimer formation rate	$3.5 \times 10^{-6}$	$\mu \mathrm{M}^{-1} \cdot \mathrm{s}^{-1}$	[19]	
$k_d^+$	Dimer formation rate	$5.8 \times 10^{-9}$	$\mu \mathrm{m}^3 \cdot \mathrm{s}^{-1}$	[19]	$1 \ \mu M = 602.2 \ \mu m^{-3}$
$\lambda_m$	Rate of 2 monomer reaction	$5.4 \times 10^{-3}$	$s^{-1}$	(14)	
$k_d^- = \nu_m$	Dimer dissociation rate	0.041	$s^{-1}$	[19]	
$k_{\mathrm{tr}}^{+}$	Trimer formation rate	$13\times10^{-5}$	$\mu \mathrm{M}^{-1} \cdot \mathrm{s}^{-1}$	[19]	
$k_{ m tr}^+$	Trimer formation rate	$2.2 \times 10^{-7}$	$\mu \mathrm{m}^3 \cdot \mathrm{s}^{-1}$	[19]	$1 \ \mu M = 602.2 \ \mu m^{-3}$
$k_{ m tr}^-$	Trimer dissociation rate	22	$s^{-1}$	[19]	
$k_b^+$	Barbed end addition rate	11.6	$\mu\mathrm{M}^{-1}\cdot\mathrm{s}^{-1}$	[19]	
$k_b^+$	Barbed end addition rate	0.019	$\mu \mathrm{m}^3 \cdot \mathrm{s}^{-1}$	[19]	$1 \ \mu M = 602.2 \ \mu m^{-3}$
$\lambda_b$	Barbed end reaction rate	$9.0 \times 10^{3}$	$s^{-1}$	(14)	
$k_b^- = \nu_b$	Barbed end dissociation rate	1.4	$s^{-1}$	[19]	
$k_p^+$	Pointed end addition rate	1.3	$\mu\mathrm{M}^{-1}\cdot\mathrm{s}^{-1}$	[19]	
$k_p^+$	Pointed end addition rate	$2.2 \times 10^{-3}$	$\mu \mathrm{m}^3 \cdot \mathrm{s}^{-1}$	[19]	$1 \ \mu M = 602.2 \ \mu m^{-3}$
$\lambda_p$	Pointed end reaction rate	$1.0 \times 10^{3}$	$s^{-1}$	(14)	
$k_p^- = \nu_p$	Pointed end dissociation rate	0.8	$s^{-1}$	[19]	

**Table 1:** Parameter values. The trimer rates are only used in simulations with well-mixed monomers and nucleates (Section 4 onward). In Section 3, we skip the trimer step and treat a dimer as a filament with a barbed and pointed end.



**Figure 9:** Steady state for fibers with up to five monomers, with the parameters for actin given in Table 1. Theory is the solution of (13) with rate constants given in Table 1.

Fig. 9, we see that we successfully reproduce this steady state with time step size  $\Delta t = 10^{-4}$  s. For convenience here, we have started at the steady state to skip the initial approach, which takes approximately 10,000 seconds (which is much longer than the timescales we are interested in and is estimated since we reach 10 fibers of length 5 in 2000 s). We see that  $\Delta t = 10^{-4}$  s preserves the steady state, whereas the larger  $\Delta t = 10^{-3}$  s drifts off the steady state.

# 4 Assuming well-mixed monomers and nucleates

The previous section showed that the actin nucleation reaction is severely reaction-limited, and that the steady state can be well-approximated assuming that the system is well mixed. Because of this, we seem to be wasting quite a lot of effort tracking the diffusion of individual monomers, especially since tracking them requires us to search for neighbors at every time step. The need to search for reaction neighbors led us to a first-order accurate reaction scheme for simplicity, which limits the time step size so that  $k\Delta t \ll 1$ , where k is the fastest reaction rate (binding of a monomer to a barbed end). Figure 9 showed that this requires  $\Delta t \approx 10^{-4}$  s, and we are interested in simulating timescales on the order of  $10^3$  to  $10^4$  s. These simulations, while doable, would be quite costly.

We therefore introduce a hybrid simulation technique where we assume that actin filament nucleates are well-mixed. That is, we do not track explicitly filaments of length 3 or smaller, instead only keeping a count of how many are in the system. Once a tetramer forms, we insert it randomly into the spatial domain and start to track its location explicitly. This allows us to retain some spatial dependence (which will be necessary later when we try to mimic *in vitro* experiments) while not wasting computational time on steps we know are well mixed.

#### 4.1 Stochastic simulation algorithm

Let  $N_1$  be the number of free monomers,  $N_2$  be the number of dimers, and  $N_3$  be the number of trimers. Then the full reaction list is as follows:

- 1. Dimer formation occurs with rate  $(k_d^+/V)N_1^2$ . If this reaction is chosen,  $N_1$  decreases by 2 and  $N_2$  increases by 1.
- 2. Dimer breakup occurs with rate  $k_d^- N_2$ . If this reaction is chosen,  $N_1$  increases by 2 and  $N_2$  decreases by 1.
- 3. Trimer formation occurs with rate  $(k_{\text{tr}}^+/V)N_1N_2$ . If this reaction is chosen,  $N_2$  and  $N_1$  decrease by 1 and  $N_3$  increases by 1.
- 4. Trimer breakup occurs with rate  $k_{\rm tr}^- N_3$ . If this reaction is chosen,  $N_2$  and  $N_1$  increase by 1 and  $N_3$  decreases by 1.
- 5. Tetramer formation occurs with rate  $(k_f^+/V)N_3N_1$ , where  $k_f^+=k_p^++k_b^+$  is the rate at which polymers add monomers to the barbed or pointed end. This reaction decreases  $N_1$  and  $N_3$  by 1. Once a tetramer is created, we track it as an individual entity which can diffuse in space. We refer to these entities as fibers.
- 6. For each fiber, addition of monomers occurs at a rate  $(k_f^+/V)N_1$ . If this reaction is selected, we add a monomer to the pointed end with probability  $p_p^+ = k_p^+/k_f^+$ , and add to the barbed end otherwise. We also decrease  $N_1$  by 1.

7. For each fiber, removal of monomers occurs at rate  $k_f^-$ , where  $k_f^- = k_p^- + k_b^-$ . If this reaction is selected, we remove a monomer from the pointed end with probability  $p_p^- = k_p^-/k_f^-$ , and remove from the barbed end otherwise. We also increase  $N_1$  by 1.

We use an exact Gillespie simulation algorithm [8] to simulate these reactions. Letting F be the number of fibers, there are 2F+5 total reactions with rates  $r_i$ . We sample a time for these reactions according to an exponential distribution,  $\Delta t_i = -\log(u)/r_i$ , where  $u \in (0,1]$ . The reaction chosen is then the one that occurs soonest. We increment time by this minimum amount, then recompute all of the rates and times, repeating until the time step is complete.

# 4.2 Validating stochastic simulations with ODEs

The algorithm in Section 4.1 is a stochastic version of the following ODEs [6]

$$\frac{dN_1}{dt} = -2(k_d^+/V)N_1^2 + 2k_d^-N_2 - (k_{\rm tr}^+/V)N_1N_2 + k_{\rm tr}^-N_3 + \sum_{j=4}^M \left(-(k_f^+/V)N_1N_{j-1} + k_f^-N_j\right)$$
(15a)

$$\frac{dN_2}{dt} = (k_d^+/V)N_1^2 - k_d^-N_2 - (k_{\rm tr}^+/V)N_2N_1 + k_{\rm tr}^-N_3$$
(15b)

$$\frac{dN_3}{dt} = (k_{\rm tr}^+/V)N_1N_2 - k_{\rm tr}^-N_3 - (k_f^+/V)N_3N_1 + k_f^-N_4 \tag{15c}$$

$$\frac{dN_j}{dt} = (k_f^+/V)N_1N_{j-1} - k_f^-N_j - (k_f^+/V)N_jN_1 + k_f^-N_{j+1} \qquad 4 \le j < M$$
(15d)

$$\frac{dN_M}{dt} = (k_f^+/V)N_1N_{M-1} - k_f^-N_M \tag{15e}$$

where M represents the maximum number of monomers. Here the cap on the number of monomers is chosen to close the system of equations. Note that these equations could also be written in terms of concentrations instead of number by dividing each side of the equations by the system volume.

We now validate our stochastic simulations using the ODE system (15). We consider the parameters in Table 1, except that we make the formation of dimers and trimers more favorable by setting  $k_d^+ = 3.5 \times 10^{-3} \ \mu\text{M}^{-1} \cdot \text{s}^{-1}$  and  $k_{\text{tr}}^+ = 1.3 \ \mu\text{M}^{-1} \cdot \text{s}^{-1}$  (this represents a factor of 1000 and 10,000 increase over the true values in Table 1, respectively), and use a maximum of M = 5 monomers per fiber.

Using these parameters, we run the stochastic simulation algorithm in Section 4.1 and compare the results to the ODEs (15) in Fig. 10. We observe agreement between the solution of the deterministic ODEs (dashed-dotted lines) and stochastic simulations with arbitrary time step sizes (Fig. 10 shows  $\Delta t = 5$  and 0.5 s). Because our stochastic simulation algorithm is exact, there is no temporal error, and we can make the time step arbitrarily large and still obtain the correct results.

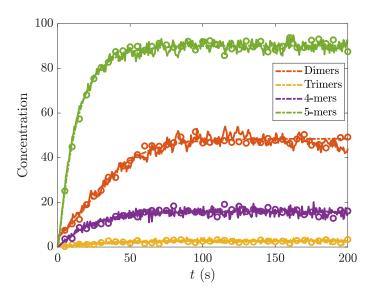


Figure 10: Validating the stochastic simulation algorithm for well-mixed systems. We consider the parameters in Table 1, except that we make the formation of dimers and trimers more favorable by setting  $k_d^+ = 3.5 \times 10^{-3} \ \mu\text{M}^{-1}\cdot\text{s}^{-1}$  and  $k_{\text{tr}}^+ = 1.3 \ \mu\text{M}^{-1}\cdot\text{s}^{-1}$ , and use a maximum of M=5 monomers per fiber. The solution of the ODEs (15) is shown as a dashed-dotted line, while the results of stochastic simulations with  $\Delta t = 5$  s and  $\Delta t = 0.5$  s are shown as circles and solid lines, respectively.

# 4.3 Simulations of actin polymerization without spatial dynamics

We now perform stochastic simulations of actin polymerization using the algorithm in Section 4.1 and the parameters in Table 1. In these simulations, we do not simulate the diffusion of the fibers, as there is no reason to do so if we are not interested in spatial information. We therefore consider the reaction part of the algorithm only, with various concentrations of monomers (2,5, and 10  $\mu$ M) in a box of size 125  $\mu$ m<sup>3</sup> (5  $\mu$ m on each side, although this is not relevant when we do not have diffusion).

Figure 11 shows the results of our simulations. The top set of plots (Fig. 11) shows the concentration of free actin and the number of fibers over time. There we see that the number of fibers per volume reaches a steady state before the concentration of free actin does, which indicates that the second half of the decrease in free actin is driven exclusively by incorporation into existing fibers. After a certain amount of time (which depends on the concentration), the concentration of free actin remains relatively constant at 0.17  $\mu$ M, and the fibers must exchange monomers with other fibers to grow in length [10].

Similar to [1], we do not concern ourselves with the long-time "steady state" distribution of actin

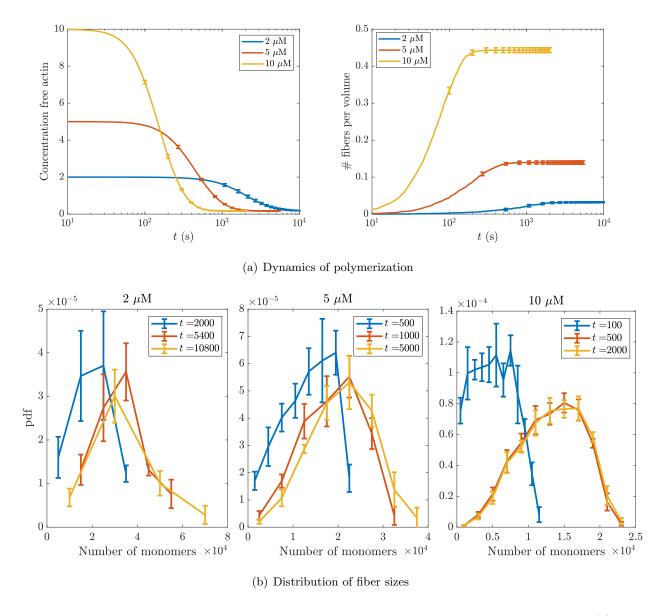


Figure 11: Stochastic simulations of polymerization dynamics at three different concentrations. (a) The dynamics of polymerization, with the concentration of free monomers shown at left and the number of fibers per unit volume  $(1 \mu m^3)$  shown at right. The number of fibers comes to a steady state when about half the actin is depleted. (b) The distribution of fiber sizes (in terms of the number of monomers) at three different time points for each concentration.

filament lengths, which can take days to reach [16], and instead focus on the length distributions on an intermediate timescale of a 30 minutes to 3 hours, which corresponds to a typical timescale for *in vitro* experiments. Our results for the filament length distributions, which are shown in Fig. 11(b), match those of [1] for spontaneous nucleation of filaments: intermediate timescales show a quasi-stable length distribution which is skewed to the left and quite broad (c.f. [1, Fig. 2c]), and higher concentrations have lower mean filament lengths (since more filaments are nucleated faster, the filaments that are nucleated first do not suck up as many monomers prior to nucleation of other filaments).

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