

# Equations and model

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## Multi substrate enzyme kinetics

### Type 1a - Linear

$$v = \frac{V_{\max} [S_1][S_2]}{K_{is1}K_{m1} + K_{m1}[S_1] + [S_1][S_2]}, \quad (1)$$

### Type 1b - Non-linear

$$v = \frac{V_{\max} [S_1][S_2]}{K_{is1}K_{m1} + K_{m1}[S_1] + K_{m2}[S_2] + [S_1][S_2]}, \quad (2)$$

### Type 2 - Ping-Pong

$$v = \frac{V_{\max} [S_1][S_2]}{K_{m2}[S_1] + K_{m1}[S_2] + [S_1][S_2]}, \quad (3)$$

where:  $V_{\max}$  is the maximum velocity, and:

$$K_{is1} = \frac{[E][S_1]}{[ES_1]}, K_{m1} = \frac{[ES_1][S_2]}{[ES_1S_2]}, K_{m2} = \frac{[ES_2][S_1]}{[ES_1S_2]}. \quad (4)$$

## Statistics

**Assumed measurement uncertainty for  $\chi^2$  scaling.** Because replicate measurements (and thus empirical standard errors) were not available, we assumed a constant measurement uncertainty across all observations. Specifically, for each data point  $i = 1, \dots, n$ ,

$$\sigma_i \equiv \sigma = 0.02 \text{SD}(v),$$

where  $\text{SD}(v)$  denotes the sample standard deviation of the observed rates  $\{v_i\}_{i=1}^n$ .

To avoid division by zero (or nonpositive values), we enforced a lower bound:

$$\sigma \leftarrow \max(\sigma, 1.0).$$

**Chi-square statistic.** Given observations  $v_i$  and model predictions  $\hat{v}_i = f(\hat{\theta}; s_{1,i}, s_{2,i})$  with measurement uncertainty  $\sigma_i$ , the weighted residual is

$$r_i(\theta) = \frac{v_i - f(\theta; s_{1,i}, s_{2,i})}{\sigma_i}. \quad (5)$$

The parameter estimate  $\hat{\theta}$  is obtained by minimizing the weighted sum of squares

$$\hat{\theta} = \arg \min_{\theta} \sum_{i=1}^n r_i(\theta)^2 = \arg \min_{\theta} \sum_{i=1}^n \left( \frac{v_i - \hat{v}_i(\theta)}{\sigma_i} \right)^2. \quad (6)$$

After optimization, the chi-square goodness-of-fit statistic is computed as

$$\chi^2 = \sum_{i=1}^n \left( \frac{v_i - \hat{v}_i}{\sigma_i} \right)^2. \quad (7)$$

**Degrees of freedom and reduced chi-square.** Let  $p$  be the number of fitted parameters and  $n$  the number of observations. The degrees of freedom are

$$\text{dof} = \max(n - p, 1), \quad (8)$$

and the reduced chi-square is

$$\chi_{\text{red}}^2 = \frac{\chi^2}{\text{dof}}. \quad (9)$$

**$R^2$  (coefficient of determination).** Define the residual sum of squares and total sum of squares by

$$SS_{\text{res}} = \sum_{i=1}^n (v_i - \hat{v}_i)^2, \quad SS_{\text{tot}} = \sum_{i=1}^n (v_i - \bar{v})^2, \quad \bar{v} = \frac{1}{n} \sum_{i=1}^n v_i. \quad (10)$$

Then

$$R^2 = 1 - \frac{SS_{\text{res}}}{SS_{\text{tot}}} \quad (\text{if } SS_{\text{tot}} > 0; \text{ otherwise } R^2 \text{ undefined}). \quad (11)$$

## Time Calculation

**Given.** Cofactor  $S_2$  is in excess, so the rate depends effectively only on  $S_1$  via Michaelis–Menten kinetics:

$$v(S_1) = \frac{V_{\text{max}} S_1}{K_m + S_1}, \quad \frac{dS_1}{dt} = -v(S_1). \quad (12)$$

Molecular weight of  $S_1$ :  $MW = 150$  g/mol. Initial and final concentrations:

$$S_{1,0} = 100 \text{ g/L}, \quad S_{1,f} = 1 \text{ g/L}. \quad (13)$$

**Unit conversion (g/L to mM).** Using  $1 \text{ mol/L} = 1000 \text{ mM}$ ,

$$S_0 = \frac{100}{150} \text{ mol/L} \times 1000 = 666.67 \text{ mM}, \quad S_f = \frac{1}{150} \text{ mol/L} \times 1000 = 6.667 \text{ mM}. \quad (14)$$

**Integrated batch MM equation.** Solve

$$\frac{dS}{dt} = -\frac{V_{\max}S}{K_m + S} \implies \left(1 + \frac{K_m}{S}\right) dS = -V_{\max} dt. \quad (15)$$

Integrating from  $S_0$  to  $S_f$  gives

$$\int_{S_0}^{S_f} \left(1 + \frac{K_m}{S}\right) dS = -\int_0^t V_{\max} dt \quad (16)$$

$$(S_f - S_0) + K_m \ln\left(\frac{S_f}{S_0}\right) = -V_{\max} t, \quad (17)$$

hence

$$t = \frac{S_0 - S_f}{V_{\max}} + \frac{K_m}{V_{\max}} \ln\left(\frac{S_0}{S_f}\right). \quad (18)$$

**Numerical evaluation.** Using the fitted parameters (from the best model fit)

$$V_{\max} = 1.0 \text{ mM/s}, \quad K_m = 0.1 \text{ mM},$$

and  $S_0 = 666.67 \text{ mM}$ ,  $S_f = 6.667 \text{ mM}$ ,

$$t = \frac{666.67 - 6.667}{1.0} + \frac{0.1}{1.0} \ln\left(\frac{666.67}{6.667}\right) = 660.0 + 0.1 \ln(100).$$

$$t \approx 660.0 + 0.4605 = 660.46 \text{ s} \approx 11.01 \text{ min.}$$

$t \approx 6.60 \times 10^2 \text{ s} \approx 11.0 \text{ min.}$

## Biomass Production

### Stoichiometric Matrix

	$v_1$	$v_2$	$v_3$	$v_4$	$v_5$	$v_6$	$v_7$	$v_8$	$v_9$
CIT	+1	-1	0	0	0	0	0	0	0
ICT	0	+1	-1	0	0	0	0	0	0
AKG	0	0	+1	-1	0	0	0	0	0
SCA	0	0	0	+1	-1	0	0	0	0
SUC	0	0	0	0	+1	-1	0	0	0
FUM	0	0	0	0	0	+1	-1	0	0
MAL	0	0	0	0	0	0	+1	-1	0
OAA	-1	0	0	0	0	0	0	+1	-1
$X$	0	0	0	0	0	0	0	0	+1

(19)

## Steady-state mass balance equations

$$\text{CIT : } v_1 - v_2 = 0, \quad (20)$$

$$\text{ICT : } v_2 - v_3 = 0, \quad (21)$$

$$\text{AKG : } v_3 - v_4 = 0, \quad (22)$$

$$\text{SCA : } v_4 - v_5 = 0, \quad (23)$$

$$\text{SUC : } v_5 - v_6 = 0, \quad (24)$$

$$\text{FUM : } v_6 - v_7 = 0, \quad (25)$$

$$\text{MAL : } v_7 - v_8 = 0, \quad (26)$$

$$\text{OAA : } v_8 - v_1 - v_9 = 0 \quad (27)$$

$$(28)$$

## Solving the steady-state equations

Given that:

$$v_9 = D, \quad (29)$$

and

$$v_2 = v_1, \quad (30)$$

$$v_3 = v_2 = v_1, \quad (31)$$

$$v_4 = v_3 = v_1. \quad (32)$$

$$v_5 = v_4 = v_1, \quad (33)$$

$$v_7 = v_6, \quad (34)$$

$$v_8 = v_7 = v_6, \quad (35)$$

$$(36)$$

we can obtain this equation:

$$v_6 - v_1 - D = 0 \quad (37)$$

giving us:

$$v_1 = v_6 - D, \quad (38)$$

$$v_6 = v_1 + D, \quad (39)$$

$$D = v_6 - v_1 \quad (40)$$

## Constraints

Irreversibility constraints:

$$v_i \geq 0 \quad \text{for } i \in \{1, 2, 3, 4, 5, 7, 8, 9\}. \quad (41)$$

$$v_1 = v_6 - D \geq 0, \quad (42)$$

$$v_6 \geq D \quad (43)$$

$$v_6 = v_1 + D \geq 0, \quad (44)$$

$$v_1 \geq -D \quad (45)$$

$$D = v_6 - v_1 \geq 0, \quad (46)$$

$$v_6 \geq v_1 \quad (47)$$

$$v_1 \geq 0, \quad (48)$$

$$v_6 \geq 0, \quad (49)$$

$$D \geq 0 \quad (50)$$

Maximal enzyme capacity constraint:

$$v_6 \leq v_{6,max} \quad (51)$$

MM constraints:

$$v_6 = \frac{V_{\max} [\text{SUC}]}{K_m + [\text{SUC}]} - \frac{V_{\max} [\text{FUM}]}{K_m + [\text{FUM}]}, \quad (52)$$

$$|v_6| \leq V_{max} \quad (53)$$

Since  $v_6 \geq D$ ,  $v_6 \geq v_1$  and  $D \geq 0$ ,

$$\max(v_1, D) \leq v_6 \leq U, \quad U := \min(V_{\max}, v_{6,\max}), \quad (54)$$

provided  $D \leq U$ .

### Saturation function

From the provided equation for  $v_6$  we define the saturation function:

$$\phi(x; K_m) := \frac{x}{K_m + x}, \quad x \geq 0, K_m > 0. \quad (55)$$