

# AER210 VECTOR CALCULUS and FLUID MECHANICS

## Quiz 4

Duration: 70 minutes

26 November 2018

Closed Book, no aid sheets

Non-programmable calculators allowed

Instructor: Prof. Alis Ekmekci

Family Name: Ekmekci

Given Name: Alis

Student #: \_\_\_\_\_

TA Name/Tutorial #: \_\_\_\_\_

FOR MARKER USE ONLY		
Question	Marks	Earned
1	8	
2	10	
3	12	
4	9	
5	12	
TOTAL	51	/50

Hints:

$$\sum \vec{F}_{cv} = \frac{d}{dt} \iiint_{cv} \vec{V}(\rho dV) + \oint_{cs} \vec{V}(\rho \vec{V} \cdot d\vec{A})$$

$$\frac{D}{Dt} = \frac{\partial}{\partial t} + u \frac{\partial}{\partial x} + v \frac{\partial}{\partial y} + w \frac{\partial}{\partial z}$$

$$\frac{p}{\rho} + \frac{V^2}{2} + gz = \text{constant}$$

$$\nabla \cdot \vec{V} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z}$$

(a) [3 marks] Bernoulli equation is given below. Indicate the meaning of each term on the left hand side of this equation:

$$\frac{p}{\rho} + \frac{V^2}{2} + gz = \text{constant}$$

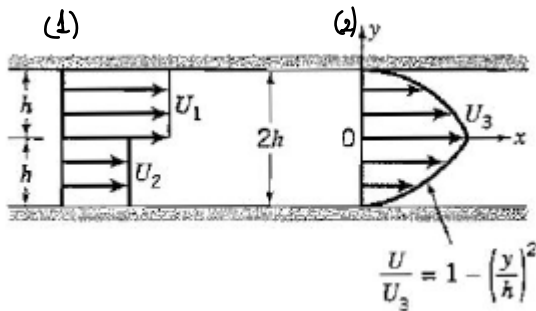
$\frac{p}{\rho}$  = energy due to pressure per unit mass

$\frac{V^2}{2}$  = kinetic energy per unit mass

$gz$  = potential energy per unit mass

(Note:  $\left[ \frac{p}{\rho} \right] = \left[ \frac{V^2}{2} \right] = [gz] = \frac{\text{m}^2}{\text{s}^2} = \frac{\text{kg} \frac{\text{m}^2}{\text{s}^2}}{\text{kg}} = \frac{\text{kg} \frac{\text{m}}{\text{s}^2} \frac{\text{m}}{\text{kg}}}{\text{kg}} = \frac{\text{N} \frac{\text{m}}{\text{kg}}}{\text{kg}} = \frac{\text{J}}{\text{kg}} = \text{energy per unit mass}$ )

(b) [5 marks] In the rectangular duct shown below, two parallel streams of a constant density gas enter on the left with constant velocities  $U_1$  and  $U_2$ . After mixing, the gas exits on the right with a parabolic profile  $U = U_3(1-(y/h)^2)$  where  $U_3$  is the maximum velocity value. Find  $U_3$  in terms of  $U_1$  and  $U_2$ .



$$\begin{aligned} \dot{m}_1 &= U_1 h w + U_2 h w \quad (\text{here } w \text{ is the dimension in } z \text{ direction}) \\ \dot{m}_2 &= \int_{y=-h}^{y=h} U w dy = \int_{-h}^h \left( U_3 - \left( \frac{y}{h} \right)^2 U_3 \right) w dy \\ &= U_3 w y \Big|_{-h}^h - U_3 w \frac{y^3}{3h^2} \Big|_{-h}^h \\ &= U_3 w (h+h) - U_3 w \frac{(h^3+h^3)}{3h^2} \\ &= 2U_3 w h - \frac{2}{3} U_3 w h \\ &= \frac{4}{3} U_3 w h \end{aligned}$$

From continuity:

$$\dot{m}_1 = \dot{m}_2 \Rightarrow U_1 h/w + U_2 h/w = \frac{4}{3} U_3 h/w \Rightarrow$$

$$\boxed{U_3 = \frac{3}{4} (U_1 + U_2)}$$

2) (a) [5 marks] Using the Reynolds Transport theorem, derive the conservation of mass equation for a control volume (in other words, the integral form of the continuity equation). *Hint: Start with the conservation of mass equation for a fluid system. Then use the Reynolds Transport Theorem to convert the conservation of mass equation for a control volume.*

The Reynolds Transport Theorem for a fluid parameter  $B = mb$  can be written as:

$$\frac{dB_{sys}}{dt} = \frac{dB_{CV}}{dt} + \dot{B}_{out} - \dot{B}_{in} \quad \text{or} \quad \frac{dB_{sys}}{dt} = \frac{dB_{CV}}{dt} + \oint_{CS} b \rho \vec{V} \cdot d\vec{A}$$

$$\frac{d(m_{sys})}{dt} = 0 \quad \leftarrow \quad (\text{conservation of mass for a fluid system})$$

$$\begin{aligned} B &= mb \\ \frac{dm_{sys}}{dt} &= \frac{dm_{CV}}{dt} + \oint_{CS} \rho \vec{V} \cdot d\vec{A} \\ 0 &= \frac{d}{dt} \left( \iiint_V \rho dV \right) + \oint_A \rho \vec{V} \cdot d\vec{A} \end{aligned}$$

(or CV)                      (or CS)



$$\boxed{\frac{d}{dt} \iiint_V \rho dV + \oint_A \rho \vec{V} \cdot d\vec{A} = 0}$$

Continuity eqn  
in  
integral form

(b) [5 marks] The x, y and z components of velocity for a certain incompressible steady flow field are respectively:

$$u = 3x + y$$

$$v = xy + z$$

$$w = ?$$

Find the z component (w) required to satisfy the continuity equation.

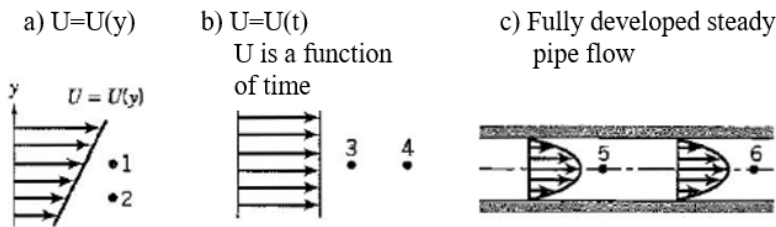
$$\text{Continuity eqn. for incompressible flow} \Rightarrow \nabla \cdot \vec{V} = 0$$

$$\underbrace{\frac{\partial u}{\partial x}}_3 + \underbrace{\frac{\partial v}{\partial y}}_x + \frac{\partial w}{\partial z} = 0 \Rightarrow \frac{\partial w}{\partial z} = -x - 3 \Rightarrow \boxed{w = -xz - 3z + f(x, y)}$$

integrate

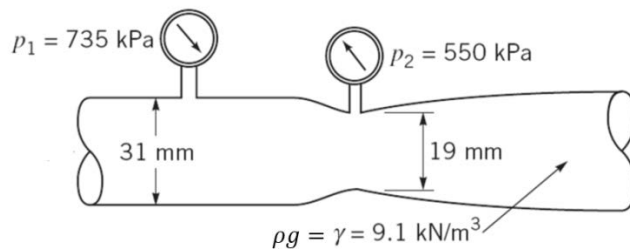
$f(x, y)$  can have any form & conservation of mass will still be satisfied.

3) (a) [6 marks] Indicate TRUE (T) or FALSE (F) to the statements below:



- F Bernoulli can be used between points 1 and 2 in (a) above.  
F Bernoulli can be used between points 3 and 4 in (b) above.  
T Bernoulli can be used between points 5 and 6 in (c) above.  
F The divergence of the velocity vector is the rate of outflow of volume per unit mass.  
T A tiny neutrally buoyant electronic pressure probe is released into the inlet pipe of a water pump and transmits 2000 pressure readings per second as it passes through the pump. This is a Lagrangian measurement.  
T In a steady incompressible flow, substantial derivative of density is zero.

(b) [6 marks] Gauge pressures measured for a pipe are given below for the circular cross-sections 1 and 2. If  $d_1 = 31$  mm and  $d_2 = 19$  mm for sections 1 and 2 respectively, determine the velocity at section 2. Specific weight of the fluid is given as  $\gamma = \rho g = 9.1$  kN/m<sup>3</sup>.



$$\frac{P_1}{\rho} + \frac{V_1^2}{2} + g z_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2} + g z_2 \quad (1)$$

$z_1 = z_2$

Continuity  $\Rightarrow V_1 A_1 = V_2 A_2$

$$V_1 = V_2 \frac{A_2}{A_1} \Rightarrow V_1 = \left( \frac{D_2}{D_1} \right)^2 V_2 \quad (2)$$

Combining ① & ②

$$\frac{P_1}{\rho} + \frac{\left( \frac{D_2}{D_1} \right)^4 V_2^2}{2} = \frac{P_2}{\rho} + \frac{V_2^2}{2}$$

$$\frac{V_2^2}{2} \left( 1 - \left( \frac{D_2}{D_1} \right)^4 \right) = \frac{P_1 - P_2}{\rho}$$

$$V_2 = \sqrt{\frac{2 \left( \frac{P_1 - P_2}{\rho} \right)}{1 - \left( \frac{D_2}{D_1} \right)^4}} = \sqrt{\frac{2 g \left( \frac{P_1 - P_2}{\gamma} \right)}{1 - \left( \frac{D_2}{D_1} \right)^4}} = \sqrt{\frac{2 \left( 9.81 \frac{\text{m}}{\text{s}^2} \right) \left( \frac{735 - 550}{9.1} \right) \text{kPa}}{1 - \left( \frac{19 \text{ mm}}{31 \text{ mm}} \right)^4}} = 21.5 \text{ m/s}$$

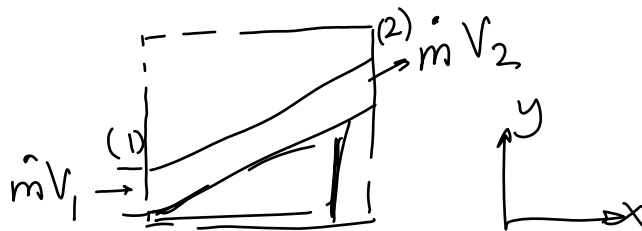
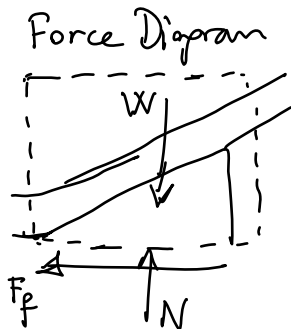
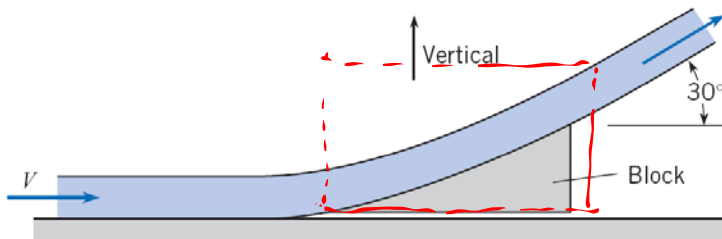
$$V_2 = 21.5 \text{ m/s}$$

4) [9 marks] Water strikes a block as shown and is deflected  $30^\circ$ . The mass flow rate of the water is  $1 \text{ kg/s}$ , and the inlet velocity is  $V = 10 \text{ m/s}$ . The mass of the block is  $1 \text{ kg}$ . The block will move if the friction between the block and the surface exceeds  $1.48 \text{ N}$ .

a) Determine normal and horizontal forces acting on the block (8 marks);

b) Determine whether the block will move (1 mark).

Neglect the weight of the water. Also, as the jet passes over the block neglect elevation changes. (Gravitational acceleration  $g = 10 \text{ m/s}^2$  and the density of water is  $\rho = 1000 \text{ kg/m}^3$ ).



Bernoulli :  $\frac{P_1}{\rho} + \frac{V_1^2}{2} + g z_1 = \frac{P_2}{\rho} + \frac{V_2^2}{2} + g z_2 \Rightarrow V_1 = V_2 = V = 10 \text{ m/s}$

Momentum :  $\sum \vec{F} = \dot{m} \vec{V}_2 - \dot{m} \vec{V}_1$

$$(-W + N)\vec{j} - F_f\vec{i} = \dot{m}(V\cos 30^\circ\vec{i} + V\sin 30^\circ\vec{j}) - \dot{m}V\vec{i}$$

x-direction:

$$\begin{aligned} -F_f &= \dot{m}V\cos 30^\circ - \dot{m}V \\ &= \dot{m}V(1 - \cos 30^\circ) \end{aligned}$$

$$= 1 \times 10 \times (1 - \cos 30^\circ) \Rightarrow \boxed{F_f = 1.34 \text{ N}}$$

## EXTRA PAGE

y-direction:

$$-W + N = V \sin 30^\circ$$

$$N = W + V \sin 30^\circ$$

$$= mg + V \sin 30^\circ$$

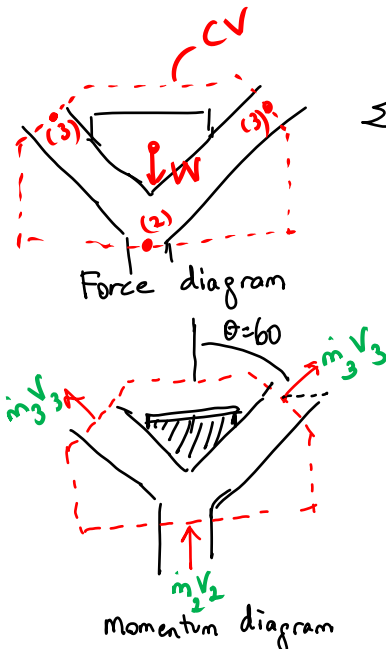
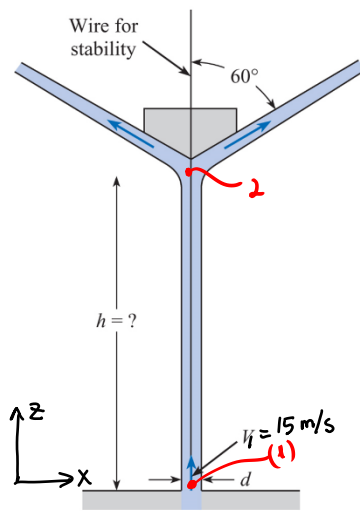
$$= 1 \times 10 + 1 \times 10 \times \sin 30^\circ$$

$$\boxed{N = 15 \text{ N}}$$

$$F_f = 1.34 \text{ N} < 1.48 \text{ N} \Rightarrow \text{block will not slip}$$

5) [12 marks] A cone that is held stable by a wire is free to move in the vertical direction and has a jet of water striking it from below. The cone weighs 30 N. The initial speed of the jet as it comes from the circular orifice is 15 m/s, and the initial jet diameter is  $d = 2$  cm. Find the height to which the cone will rise and remain stationary. (Gravitational acceleration:  $g = 10 \text{ m/s}^2$ , water density  $\rho = 1000 \text{ kg/m}^3$ )

Notes: - The wire is only for stability and should not enter into your calculations.  
 - Assume that the height of the wedge is negligibly small.  
 - Notice that the water jet spreads around the cone three dimensionally (i.e., not only in the paper plane).



Apply Bernoulli between (1) & (2):

$$\frac{V_1^2}{2} + g z_1 + \frac{P_1}{\rho} = \frac{V_2^2}{2} + g z_2 + \frac{P_2}{\rho} \quad \left( P_1 = P_2 = 0 \text{ atmospheric pressure} \right)$$

$$V_2^2 = V_1^2 + 2g(z_1 - z_2)$$

$$\boxed{V_2^2 = V_1^2 - 2gh} \quad (\text{Eqn. 1})$$

Let's apply momentum eqn. in y-direction.

Select a stationary control volume surrounding the cone.

$$\sum \vec{F}_{cv} = \dot{m}_3 \vec{V}_3 - \dot{m}_2 \vec{V}_2$$

in y direction:  $\Delta$

$$-W = \dot{m}(V_3 \cos 60^\circ - V_2)$$

$\cos 60^\circ = 0.5$

$$\dot{m} = \rho_2 V_2 A_2 = \rho_1 V_1 A_1$$

From continuity

$$\boxed{\dot{m}_2 = \dot{m}_3 = \dot{m}}$$

$$\boxed{-30 = (1000)(15) \pi \frac{(0.02)^2}{4} (V_3 (0.5) - V_2)} \quad (\text{eqn. 2})$$

Apply Bernoulli between (2) & (3)

$$\left( \text{with } z_2 \approx z_3 \right) \quad \frac{V_2^2}{2} + g z_2 + \frac{P_2}{\rho} = \frac{V_3^2}{2} + g z_3 + \frac{P_3}{\rho} \Rightarrow \boxed{V_2 = V_3} \quad (\text{eqn. 3})$$

Inserting eqn. 3 into eqn. 2 <sup>we get</sup>

$$-30 = (1000)(15) \pi \frac{(0.02)^2}{4} (V_2 \cdot (0.5) - V_2)$$

Solve for  $V_2$ :

$$V_2 = \frac{(30)(4)}{(1000)(15) \pi (0.02)^2 (1-0.5)} = 12.73 \text{ m/s}$$

$$\boxed{V_2 = 12.73 \text{ m/s}}$$

From eqn. 1

$$V_2^2 = V_1^2 - 2gh \Rightarrow h = \frac{V_1^2 - V_2^2}{2g} = \frac{15^2 - (12.73)^2}{2 \times 10} = 3.15 \text{ m}$$

$$\boxed{h = 3.15 \text{ m}}$$