CHE 260

1)
$$P = CV^{1/3} = (100 \frac{kR}{m}) V^{1/3}$$

$$P_1 = (100 \frac{kPa}{m}) (1 m^3)^{1/3} = 100 kPa$$

$$P_2 = (100 \frac{kR}{m})(3 m^3)^{1/3} = 144.22 kRa.$$

$$W_{12} = - \left(\frac{PdV}{V_1} \right) = - \left(\frac{V_2}{V_1} \right) \left(\frac{V_3}{V_1} \right) \left(\frac{V_4}{V_1} \right) \left(\frac{V_4}{V_1$$

$$C = P_1 V_1^{-1/3} = P_2 V_2$$

$$= -\frac{3}{4} \left[CV_2^{4/3} - CV_1^{4/3} \right]$$

$$= -\frac{3}{4} \left[P_2V_2 - P_1V_1 \right]$$

$$m_2 = \frac{P_2V_2}{RT_2} = \frac{144 \cdot 22 \, \text{bfa} \times 3\text{m}^3}{0.2870 \, \text{k}^3/\text{by} \times 298 \, \text{K}}$$
$$= 5.06 \, \text{kg}$$

on a P-V diagram $V_1 = V_2 = 2V_1$ P, = 200 12Pa T, = 600 K. P2=P1 = 200 kPa. For const P, $T_2 = T_1 \frac{V_2}{V} = 600 \text{ K} \times 2 = 1200 \text{ K}$. T3 = T1 = 600K For const V, P3 = P2 T3 = 200 kPa × 600 K P3 = 100 12 Pa. From tables at 600 14 h=h3=607.02 kJ/hy; U=U3=434.76kJ At 1200K, h2=1277-79 My : U2=933.33 1 For process 1-2. (const P) 9/12 = h2-h, = 1277.79-607.02 = 670.77 k5/p $W_{12} = (u_2 - u_1) - q_{12} = (933.33 - 434.76) - 670.77$ W12 = - 172.22 125/12/. For process 2-3 (const V) W13 = 0 923 = U3-U2 = 434.73 - 933-33

(2)

 $923 = -498.53 \, \text{eJ/hg}$

3) Dyfuser 2

$$P_1 = 100 \text{ kefa}$$
 $T_1 = 300 \text{ K}$
 $V_1 = 200 \text{ m/s}$
 $V_1 = 200 \text{ m/s}$
 $V_1 = 100 \text{ mm}^2$

Enorgy balance
$$h_1 + \frac{V_1^2}{2} + g z_1 = h_2 + \frac{V_2^2}{2} + g z_2$$

 $\Rightarrow h_2 - h_1 = Cp(T_2 - T_1) = \frac{V_1^2 - V_2^2}{2}$
 $\Rightarrow T_2 = T_1 + \frac{V_1^2 - V_2^2}{2Cp}$

$$= 300 \text{ K} + (200 \text{ M/s})^2 - (20 \text{ M/s})^2 = 319.72 \text{ K}$$

$$2 \times 1 - 004 \times 10^3 \text{ J/Hz}$$

$$m = \frac{A_2 V_2}{U_2} = \frac{A_1 V_1}{U_1}$$

$$= \int U_2 = U_1 \left(\frac{A_2 V_2}{A_1 V_1} \right) = \frac{R T_1}{P_1} \left(\frac{A_2 V_2}{A_1 V_1} \right) = \frac{R T_2}{P_2}$$

$$\Rightarrow P_2 = P_1 \left(\frac{T^2}{T_1} \right) \left(\frac{A_1 V_1}{A_2 V_2} \right)$$