

①

For a polytropic process

$$P_1 V_1^n = P_2 V_2^n$$

Assuming ideal gas $PV = mRT$

$$w_{12} = \frac{P_2 V_2 - P_1 V_1}{n-1}$$

$$= mR \frac{(T_2 - T_1)}{n-1}$$

$$T_2 = T_1 \left(\frac{P_1}{P_2} \right)^{\frac{1-n}{n}} = (303 \text{ K}) \left[\frac{120 \text{ kPa}}{1200 \text{ kPa}} \right]^{-0.2}$$

$$= 444.7 \text{ K}$$

$$w_{12} = \frac{W_{12}}{m} = R \frac{(T_2 - T_1)}{n-1}$$

$$= 0.2081 \frac{\text{kJ}}{\text{kg K}} \left[\frac{444.7 \text{ K} - 303 \text{ K}}{0.2} \right]$$

$$= 147.5 \text{ kJ/kg}$$

Energy Balance

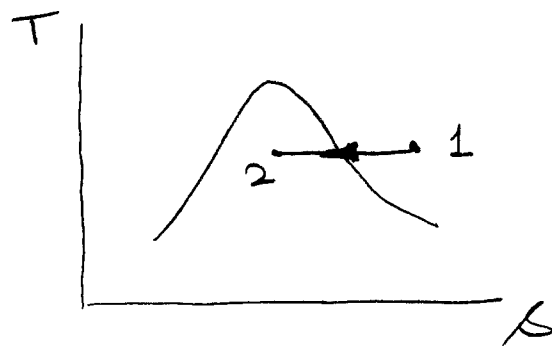
$$q_{12} + w_{12} = \Delta u_{12} = c_v (T_2 - T_1)$$

$$\Rightarrow q_{12} = c_v (T_2 - T_1) - w_{12}$$

$$= 0.312 \frac{\text{kJ}}{\text{kg K}} (444.7 - 303) \text{ K} - 147.5 \frac{\text{kJ}}{\text{kg}}$$

$$= -103.3 \text{ kJ/kg}$$

(2)



$$\left. \begin{array}{l} P_1 = 240 \text{ kPa} \\ T_1 = 20^\circ\text{C} \end{array} \right\} \begin{array}{l} u_1 = 244.30 \text{ kJ/kg} \\ s_1 = 1.0034 \text{ kJ/kg}\cdot\text{K} \end{array}$$

$$\text{At } 20^\circ\text{C} \quad u_f = 76.80 \text{ kJ/kg} \quad u_g = 237.91 \text{ kJ/kg} \\ s_f = 0.2924 \text{ kJ/kg}\cdot\text{K}, \quad s_g = 0.9102 \text{ kJ/kg}\cdot\text{K}$$

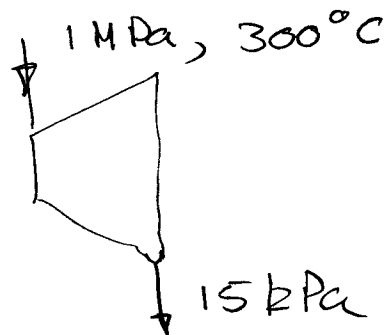
$$\begin{aligned} u_2 &= u_f + x_2(u_g - u_f) \\ &= 76.80 \text{ kJ/kg} + 0.2(237.91 - 76.80) \text{ kJ/kg} \\ &= 109.02 \text{ kJ/kg} \end{aligned}$$

$$\begin{aligned} s_2 &= s_f + x_2(s_g - s_f) \\ &= 0.2924 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} + 0.2(0.9102 - 0.2924) \text{ kJ/kg}\cdot\text{K} \\ &= 0.4160 \text{ kJ/kg}\cdot\text{K} \end{aligned}$$

$$\begin{aligned} \text{Heat Transfer} \quad q_{12} &= \int_1^2 T ds = T_1(s_2 - s_1) \\ &= 293 \text{ K}(0.4160 - 1.0034) \text{ kJ/kg}\cdot\text{K} \\ &= -172.1 \text{ kJ/kg} \end{aligned}$$

$$\begin{aligned} w_{12} &= (u_2 - u_1) - q_{12} \\ &= (109.02 - 244.30) + 172.1 \\ &= 36.82 \text{ kJ/kg} \end{aligned}$$

(3)



$$\left. \begin{array}{l} 1 \text{ MPa} \\ 300^\circ\text{C} \end{array} \right\} \begin{array}{l} h_1 = 3051.2 \text{ kJ/kg} \\ x_1 = 7.1229 \text{ kJ/kgK} \end{array}$$

at 15 kPa

$$\begin{array}{ll} h_f = 225.94 \text{ kJ/kg} & h_g = 2599.1 \text{ kJ/kg} \\ x_f = 0.7549 \text{ kJ/kgK} & x_g = 8.0085 \text{ kJ/kgK} \end{array}$$

For an isentropic process $x_2 = x_1$

$$x_{2,s} = \frac{x_{2s} - x_f}{x_g - x_f} = \frac{7.1229 - 0.7549}{8.0085 - 0.7549} = 0.8779$$

$$h_{2s} = h_f + x_{2,s} (h_g - h_f)$$

$$= 225.94 + 0.8779 (2599.1 - 225.94)$$

$$= 2309.3 \text{ kJ/kg}$$

$$w_s = h_1 - h_{2s} = 3051.2 - 2309.3$$

$$= 741.9 \text{ kJ/kg}$$

$$\eta_t = \frac{w_a}{w_s} = \frac{600 \text{ kJ/kg}}{741.9} = 80.9\%$$

$$h_2 = h_1 - w_a = 3051.2 - 600$$

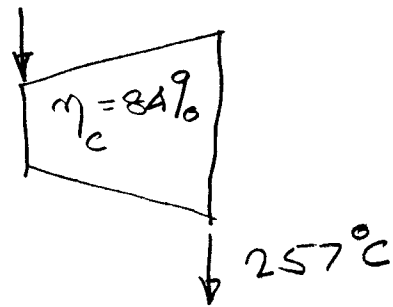
$$= 2451.2 \text{ kJ/kg}$$

$$x_2 = \frac{h_2 - h_f}{h_g - h_f} = \frac{2451.2 - 225.94}{2599.1 - 225.94}$$

$$= 0.9377$$

4)

100 kPa, 17°C



$$\eta_c = \frac{T_{2s} - T_1}{T_2 - T_1}$$

$$\frac{P_{2s}}{P_1} = \left(\frac{T_{2s}}{T_1} \right)^{\frac{\gamma}{\gamma-1}}$$

$$T_2 = 257^\circ\text{C} = 530\text{ K}$$

$$T_{2s} = T_1 + \eta_c (T_2 - T_1)$$

$$= 290\text{ K} + 0.84 (530 - 290) = 491.6\text{ K}$$

$$P_{2s} = P_1 \left(\frac{T_{2s}}{T_1} \right)^{\frac{\gamma}{\gamma-1}}$$

$$= 100\text{ kPa} \left(\frac{491.6\text{ K}}{290\text{ K}} \right)^{1.4}$$

$$= 634\text{ kPa}$$

Density of air

$$\rho = \frac{P}{RT} = \frac{100\text{ kPa}}{0.287 \frac{\text{kJ}}{\text{kg K}} \times 290\text{ K}}$$

$$= 1.20\text{ kg/m}^3$$

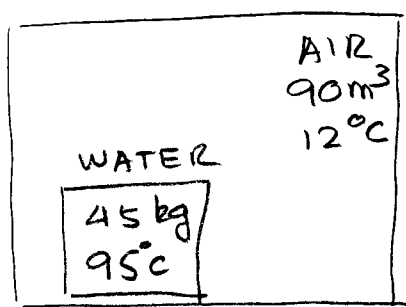
$$\dot{m} = \rho \dot{V} = 1.20 \frac{\text{kg}}{\text{m}^3} \times 2.4 \frac{\text{m}^3}{\text{s}} = 2.88 \frac{\text{kg}}{\text{s}}$$

$$\dot{W} = \dot{m} (h_2 - h_1) = \dot{m} c_p (T_2 - T_1)$$

$$= 2.88 \frac{\text{kg}}{\text{s}} \times 1.004 \frac{\text{kJ}}{\text{kg K}} (530 - 290)\text{ K}$$

$$= 694.0\text{ kW}$$

(5)

Assume $P_{air} = 1 \text{ atm}$

$$m_a = \frac{PV}{RT}$$

$$= \frac{101.3 \text{ kPa} \times 90 \text{ m}^3}{0.287 \text{ kJ/kg} \cdot \text{K} \times 285 \text{ K}}$$

$$= 111.5 \text{ kg}$$

Isolated system $\Rightarrow \Delta U = 0$

$$m_w c_w (T_2 - T_{w,1}) + m_a c_{v,a} (T_2 - T_{a,1}) = 0$$

$$45 \times 4.18 (T_2 - 95) + 111.5 \times 0.717 (T_2 - 12) = 0$$

$$\Rightarrow T_2 = 70.2^\circ \text{C}$$

Heat transfer to air $Q = m_a c_{v,a} (T_2 - T_{a,1})$

$$\Rightarrow Q = 111.5 \text{ kg} \times 0.717 \text{ kJ/kg} \cdot \text{K} (70.2 - 12) = 4660 \text{ kJ}$$

$$\Delta S_w = m_w c_w \ln \frac{T_2}{T_{w,1}} = 45 \times 4.18 \times \ln \frac{343.2}{368}$$

$$= -13.12 \text{ kJ/kg}.$$

$$P_2 = \frac{m_a R T_2}{V} = \frac{111.5 \text{ kg} \times 0.287 \text{ kJ/kg} \cdot \text{K} \times 343.2 \text{ K}}{90 \text{ m}^3}$$

$$= 122.0 \text{ kPa}$$

$$\Delta S_a = m_a \left[c_{p,a} \ln \frac{T_2}{T_1} - R \ln \frac{P_2}{P_1} \right]$$

$$= 111.5 \text{ kg} \left[1.004 \ln \frac{343.2 \text{ K}}{285 \text{ K}} - 0.287 \ln \frac{122.0}{101.3} \right]$$

$$= 14.85 \text{ kJ/K}$$

$$\Delta S_{\text{TOTAL}} = \Delta S_w + \Delta S_a = -13.11 + 14.85$$

$$= 1.74 \text{ kJ/K}.$$