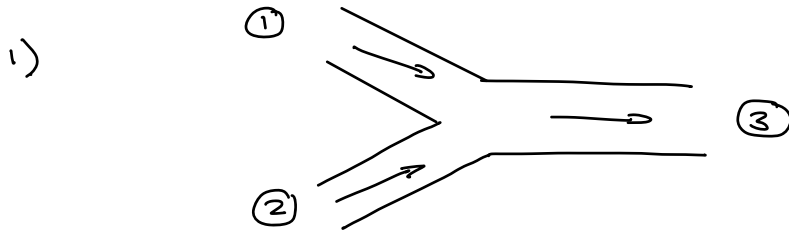


CHE 260
MIDTERM SOLUTION - 2022.



$$\dot{m}_1 + \dot{m}_2 = \dot{m}_3$$

$$\dot{m}_1 h_1 + \dot{m}_2 h_2 = \dot{m}_3 h_3$$

$$\Rightarrow \dot{m}_1 h_1 + \dot{m}_2 h_2 = (\dot{m}_1 + \dot{m}_2) h_3$$

$$\Rightarrow \dot{m}_1 (h_1 - h_3) = \dot{m}_2 (h_3 - h_2)$$

$$\Rightarrow \dot{m}_1 c_p (T_1 - T_3) = \dot{m}_2 c_p (T_3 - T_2)$$

$$\Rightarrow T_3 (\dot{m}_2 + \dot{m}_1) = \dot{m}_1 T_1 + \dot{m}_2 T_2$$

$$\Rightarrow T_3 = \frac{\dot{m}_1 T_1 + \dot{m}_2 T_2}{\dot{m}_2 + \dot{m}_1}$$

$$T_3 = \frac{1 \text{ kg/s} \times 400 \text{ K} + 2 \text{ kg/s} \times 290 \text{ K}}{1 \text{ kg/s} + 2 \text{ kg/s}}$$

$$T_3 = 326.7 \text{ K.}$$

$$\dot{m}_1 s_1 + \dot{m}_2 s_2 + \dot{S}_{\text{gen}} = \dot{m}_3 s_3 = \dot{m}_1 s_3 + \dot{m}_2 s_3$$

$$\Rightarrow \dot{S}_{\text{gen}} = \dot{m}_1 (s_3 - s_1) + \dot{m}_2 (s_3 - s_2)$$

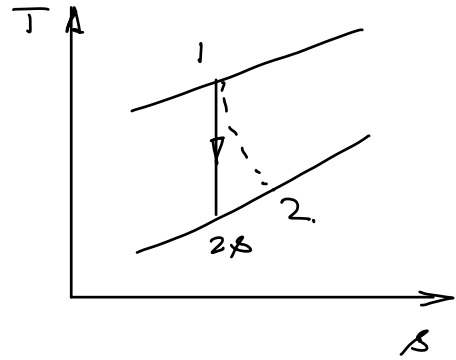
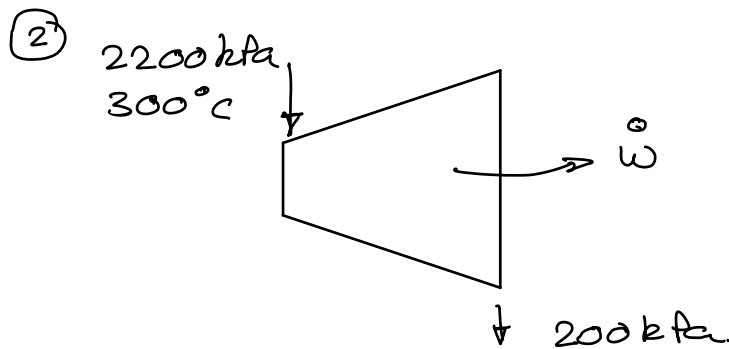
$$P_1 = P_2 = P_3$$

$$\Rightarrow \dot{S}_{\text{gen}} = \dot{m}_1 c_p \ln T_3/T_1 + \dot{m}_2 c_p \ln T_3/T_2$$

$$c_p \approx 1.004 \text{ kJ/kg}\cdot\text{K.}$$

$$\Rightarrow \dot{S}_{\text{gen}} = 1 \text{ kg/s} \times 1.004 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} \ln \frac{326.7 \text{ K}}{400 \text{ K}} + 2 \frac{\text{kg}}{2} \times 1.004 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} \times \frac{326.7 \text{ K}}{290 \text{ K}}$$

$$\dot{S}_{\text{gen}} = 0.036 \text{ kW/K.}$$



$$\frac{T_{2s}}{T_1} = \left(\frac{P_2}{P_1} \right)^{\frac{\gamma-1}{\gamma}}$$

At $T_{avg} \approx 400 \text{ K}$ $C_p = 1.013 \frac{\text{kJ}}{\text{kgK}}$, $\gamma = 1.395$

$$\Rightarrow T_{2s} = 573 \text{ K} \left(\frac{200 \text{ kPa}}{2200 \text{ kPa}} \right)^{\frac{0.395}{1.395}} = 290.6 \text{ K}$$

$$w_{t,s} = C_p (T_{2s} - T_1)$$

$$w_{t,s} = 1.013 \frac{\text{kJ}}{\text{kgK}} (290.6 \text{ K} - 573 \text{ K}) = -286.1 \frac{\text{kJ}}{\text{kg}}$$

$$w_t = \eta_t w_{t,s} = 0.85 (-286.1) \frac{\text{kJ}}{\text{kg}}$$

$$w_t = -243.2 \text{ kJ/kg}$$

$$w_t = C_p (T_2 - T_1)$$

$$\Rightarrow T_2 = T_1 + w_t / C_p$$

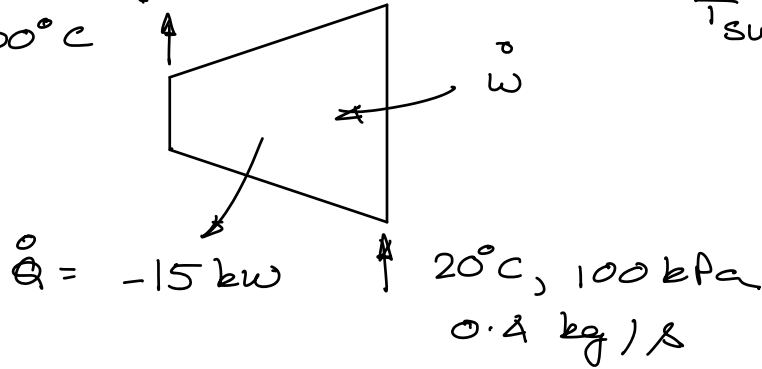
$$= 573 \text{ K} + \frac{(-243.2 \text{ kJ/kg})}{1.013 \text{ kJ/kgK}}$$

$$T_2 = 332.9 \text{ K}$$

③

1200 kPa
300°C

$T_{\text{sur}} = 20^\circ\text{C}$



$$\dot{W} = \dot{m} c_p (T_2 - T_1) - \dot{Q}$$

At $T_{\text{avg}} = 160^\circ\text{C} = 433\text{K}$, $c_p \approx 1.018 \frac{\text{kJ}}{\text{kg}\cdot\text{K}}$

$$\dot{W} = 0.4 \frac{\text{kg}}{\text{s}} \times 1.018 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} (300 - 20)^\circ\text{C} + 15 \text{ kW}$$

$$\dot{W} = 129.0 \text{ kW}$$

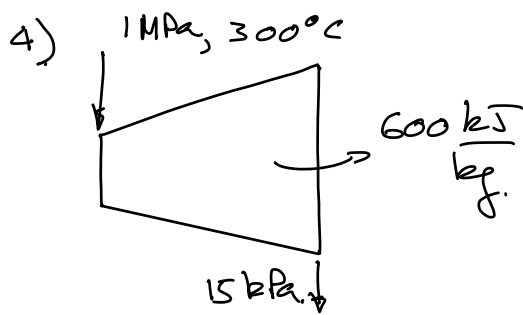
b) Rate of entropy generation

$$\dot{S}_{\text{gen}} = \Delta \dot{S}_{\text{air}} + \Delta \dot{S}_{\text{sur}}.$$

$$\dot{S}_{\text{gen}} = \dot{m} \left(c_p \ln \frac{T_2}{T_1} - R \ln \frac{P_2}{P_1} \right) + \frac{\dot{Q}}{T_{\text{sur}}}.$$

$$\begin{aligned} \dot{S}_{\text{gen}} &= 0.4 \frac{\text{kg}}{\text{s}} \times \left(1.018 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} \ln \frac{573\text{K}}{293\text{K}} - 0.287 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} \ln \frac{1200\text{kPa}}{100\text{kPa}} \right) \\ &\quad + \frac{15 \text{ kW}}{293\text{K}}. \end{aligned}$$

$$\dot{S}_{\text{gen}} = 0.039 \text{ kW/K}.$$



$$\left. \begin{array}{l} 1 \text{ MPa} \\ 300^\circ\text{C} \end{array} \right\} \begin{array}{l} h_1 = 3051.6 \frac{\text{kJ}}{\text{kg}} \\ s_1 = 7.1246 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} \end{array}$$

at 15 kPa

$$\begin{array}{l} h_f = 225.94 \frac{\text{kJ}}{\text{kg}} \quad h_g = 2598.3 \frac{\text{kJ}}{\text{kg}} \\ s_f = 0.7549 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} \quad s_g = 8.0071 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} \end{array}$$

For isentropic expansion $s_2 = s_1$

$$x_{2s} = \frac{s_{2s} - s_f}{s_g - s_f} = \frac{7.1246 - 0.7549}{8.0071 - 0.7549} = 0.8783$$

$$h_{2s} = h_f + x_{2s} (h_g - h_f)$$

$$= 225.94 + 0.8783 (2598.3 - 225.94)$$

$$h_{2s} = 2309.6 \frac{\text{kJ}}{\text{kg}}$$

$$w_s = h_{2s} - h_1 = 2309.6 - 3051.6 = -742.0 \frac{\text{kJ}}{\text{kg}}$$

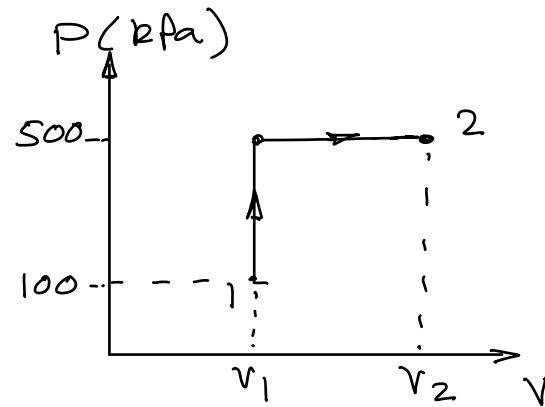
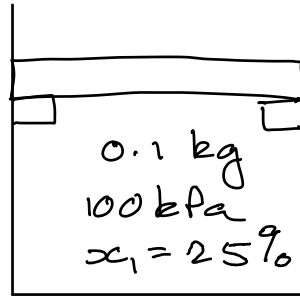
$$\eta_t = \frac{w_a}{w_s} = \frac{-600 \frac{\text{kJ}}{\text{kg}}}{-742.0 \frac{\text{kJ}}{\text{kg}}} = 80.9\%$$

$$h_2 = h_1 + w_a = 3051.6 - 600 = 2451.6 \frac{\text{kJ}}{\text{kg}}$$

$$x_2 = \frac{h_2 - h_f}{h_g - h_f} = \frac{2451.6 - 225.94}{2598.3 - 225.94}$$

$$x_2 = 0.9382$$

5



at 100 kPa $v_f = 0.001043 \text{ m}^3/\text{kg}$, $v_g = 1.6941 \text{ m}^3/\text{kg}$
 $u_f = 417.40 \text{ kJ/kg}$ $u_g = 2505.6 \text{ kJ/kg}$

$$v_1 = v_f + x_1 (v_g - v_f)$$

$$= 0.001043 \text{ m}^3/\text{kg} + 0.25 (1.6941 - 0.001043) \text{ m}^3/\text{kg}$$

$$v_1 = 0.42431 \text{ m}^3/\text{kg}$$

At 500 kPa, $300^\circ\text{C} \Rightarrow v_2 = 0.52261 \text{ m}^3/\text{kg}$

Since $v_2 > v_1 \Rightarrow$ Piston is lifted.

Constant pressure process

$$\Rightarrow w_{12} = -P (v_2 - v_1)$$

$$= -P m (v_2 - v_1)$$

$$\Rightarrow w_{12} = -500 \text{ kPa} \times 0.1 \text{ kg} (0.52261 - 0.42431) \text{ m}^3/\text{kg}$$

$$w_{12} = -4.92 \text{ kJ}$$